



**UNITED  
TECHNOLOGIES  
HAMILTON  
STANDARD**

SVHSER 10639

NASA Contractor Report 181736

**APPENDICES TO THE USER'S MANUAL**

**FOR**

**A COMPUTER PROGRAM FOR THE  
EMULATION/SIMULATION OF A SPACE STATION  
ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM**

**BY**

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**PREPARED UNDER CONTRACT NO. NAS1-17397**

**FOR**

**NATIONAL AERONAUTICS AND SPACE ADMINISTRATION  
LANGLEY RESEARCH CENTER  
HAMPTON, VIRGINIA**

September 1988

(NASA-CR-181736) APPENDICES TO THE USER'S  
MANUAL FOR A COMPUTER PROGRAM FOR THE  
EMULATION/SIMULATION OF A SPACE STATION  
ENVIRONMENTAL CONTROL AND LIFE SUPPORT  
SYSTEM (Hamilton Standard Div.) 208 p

N89-13896

Unclas  
G3/54 0183245



## ABSTRACT

A User's Manual for the Emulation Simulation Computer Model was published previously. The model consisted of a detailed model (emulation) of a SAWD CO<sub>2</sub> removal subsystem which operated with much less detailed (simulation) models of a cabin, crew, and condensing and sensible heat exchangers. The purpose was to explore the utility of such an emulation/simulation combination in the design, development, and test of a piece of ARS hardware - SAWD.

Extensions to this original effort are presented in this manual. The first extension is an update of the model to reflect change in the SAWD control logic which resulted from test. In addition, slight changes were also made to the SAWD model to permit restarting and to improve the iteration technique. The second extension is the development of simulation models for more pieces of air and water processing equipment. Models are presented for: ECD, Molecular Sieve, Bosch, Sabatier, a new condensing heat exchanger, SPE, SFWES, Catalytic Oxidizer, and multifiltration. The third extension is to create two systems simulations using these models. The first system presented consists of one air and one water processing system. The second system consists of a potential Space Station air revitalization system complete with a habitat, laboratory, four nodes, and two crews.



## FOREWORD

This User's Manual has been prepared by Hamilton Standard Division of United Technologies Corporation for the National Aeronautics and Space Administration's Langely Research Center in accordance with Contract NAS 1-17397, "Development of an Emulation/Simulation Computer Model of a Space Station Environmental Control and Life Support System (ECLSS)". This manual describes the use of the three models developed under this contract.

Appreciation is expressed to the Technical Monitors Messrs. John B. Hall, Jr. and Lawrence F. Rowell of the NASA Langley Research Center for their guidance and advice.

This manual was written by Dr. James L. Yanosy, Program Engineer, with assistance from Mr. Stephen A. Giangrande. The extensions to the program presented in this manual were performed under the direction of Mr. John M. Neel, Program Manager. Thanks is given to Joseph M. Homa for his efforts in the development of the Space Station Model.



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## 1.0

INTRODUCTION

The Original User's manual [4]\* presented the instructions to use the Emulation Simulation Computer Model (ESCM). This model consisted of simple models of a crew, sensible heat exchanger, condensing heat exchanger, and a cabin combined with a very detailed model of the SAWD CO<sub>2</sub> Removal Subsystem. The simple models are called simulations while the very detailed model is called an emulation. The purpose of the program was to explore the utility of a combined emulation/simulation program to assist in the design, development, and testing of a piece of hardware-SAWD.

This original effort was extended to update the ESCM model following SAWD testing, to develop new computer simulations of other air revitalization and wastewater processing equipment, and lastly to develop two system simulations which would incorporate various air revitalization and wastewater processing equipment. The purpose of these additional system simulations is to explore their utility in system design.

This report presents in the form of appendices to the original User's Manual the new instructions for ESCM, the instructions to use ECLSB, and the instructions to use the Space Station Model.

---

\*Numbers in brackets denote references listed in Section 2.0.



ESCM was updated to incorporate the new control logic resulting from tests. In addition several improvements were also made in the output and the iteration procedure. ECLSB is one of the system simulations generated. It models one ARS combines with a water processing system. The User's Manual for this system has already been published [1], but it is included as Appendix B for completeness. Lastly, a Space station model was generated; it consists of a habitat, laboratory, four nodes, and two crews. Only air revitalization processes are simulated; the instructions for this model are presented in Appendix C.

The following are errata in the original User's Manual:

- ( 1) Page 2, Figure 1: above the box titled Launch Operation the words should be "Design changes" instead of Design chanes.
- ( 2) Page 17, Table 5: Delete VLH20 subroutine and its description as ESCM never calls it. Also, change "Subroutine None" to "Subroutine Name".
- ( 3) Page 18, Table 6: Delete DUCT subroutine and its description as ESCM never call it. Also, change "Subroutine None" to "Subroutine Name".
- ( 4) Page 47, Table 8, NSTR15 Card; add the following in the comment field: "Pressure from secondary side".
- ( 5) Page 48, Table 8, NSTRE20 Card; add the following in the comment field; "Pressure from secondary side".





- ( 6 ) Page 49, Table 8, NSTR32 Card; add the following in the comment field: "Tank fluid temperature is specified".
- ( 7 ) Page 50, Table 8; the second TITL 21 3 line should be renumbered to TITL 21 4.
- ( 8 ) Page 50, Table 8: the line after TITL 23 3 should be renumbered from TITL 21 3 to TITL 23 4.
- ( 9 ) Page 51, Table 8: the lines beginning with VALU 71 14 and VALU 71 15 should have the numbers 0.315 and 1.000 deleted.
- (10) Page 53, Figure 8: in Note at top of figure, change the word "nonzero" to "non-blank". The program checks for a blank field; if the field is not blank, then the program takes the specified action.
- (11) Page 65, Section 4.3: add the following for the missing item (7) in the list of eleven values printed to the screen: "7) SAWD bed #1 H<sub>2</sub>O loading, % of dry amine wgt.
- (12) Page 67, first six lines, references to Appendix B should be changed to Appendix C.
- (13) Page 67, item (3) at top of page should read: "3) Schematic printouts at the requested printoff frequency. See Figure 6 and Appendix C.
- (14) Page 67, item (2) in the middle of the page: change "indenpendent" to "independent".
- (15) Page 68, definition of NUMCAS: change sentence in parentheses to read: "(Refer to Appendix B GPLOT.DATA)".
- (16) Page A-10, Section A.4: change ESCMZE to ESCM2E.



## 2.0

REFERENCES

- (1) Yanosy, J., "User's Manual for a Computer Program for the Simulation of a Space Station Environmental Control and Life Support System (ECLSB)", Hamilton Standard Report SVHSER 10630 for the National Aeronautics and Space Administration, Langley Research Center; September 1986.
- (2) "G189A Generalized Environmental/Thermal Control and Life Support System Computer Program Manual", McDonnell Douglas Corporation MDA C-G2444; September 1971.
- (3) "CAETMS User's Manual", Volume 1, Version 2.0, by United Technologies Hamilton Standard Engineering Software Systems; September 1986.
- (4) Yanosy, J., "User's Manual for a Computer Program for the Emulation/Simulation of a Space Station Environmental Control and Life Support System (ESCM)", Hamilton Standard Report SVHSER 9503 for the National Aeronautics and Space Administration, Langley Research Center; NASA CR-181735, September 1988.







SVHSER 10639

## APPENDIX A

### ESCM UPDATE



## A.1 INTRODUCTION

The computer program for the emulation/simulation of a Space Station environmental control and life support system (ESCM) has been updated. Updates to the computer simulation model include: (1) the addition of an energy balance control logic (flow sensor control) for the SAWD CO<sub>2</sub> removal subsystem, the capability of restarting the SAWD subsystem, clamping the SAWD bed segment temperature when iterating on the bed temperature during the energy balance of the bed segment, and the addition of a new output table to the hardcopy and screen output.

A new type of control has been incorporated in the SAWD subsystem. This control method is an energy balance method. Using this method, the amount of water remaining on the bed after absorption can be calculated from an energy balance of the bed. Based on the water remaining on the absorbed bed, the next absorb time is calculated. Thus, the absorption time is regulated to control the amount of water on the bed at the end of absorption. The time to desorb the bed is dependent on the water flow as well as steam generator power.

The capability of restarting the SAWD subsystem has been added to the SAWD subroutine. Previously, the user was required to run the program for steady state before the transient could be run. With the restart capability, the simulation can be executed from a transient start.

## A.2      Description of Program

In order to incorporate the above changes to the ESCM model, two subroutines were modified. These subroutines, GPOLY1 and IR45, required logic changes. All input and output additions to these subroutines will be discussed in this section.

### A.2.1      GPOLY1 Subroutine

GPOLY1 was restructured to the following format:

```
IF (N .EQ. 3) Then  
:  
END IF
```

The following are input additions to be input once at the first execution of GPOLY1.

KK(6,18) = Bed to be desorbed first at start of transient  
          solution  
KK(6,19) = Type of SAWD control 0 = RH control  
          1 = Accum control  
          2 = Flow sensor control

The following are input and output additions to be input and output from GPOLY1 before the solution of component #14 (splitter for gas flow from main cabin to SAWD Bed #1 or SAWD Bed #2).



INPUT:

WV(29,68)	=	steam generator power, watts
WV(27,100)	=	H <sub>2</sub> O supply tank flow, pph
KK(32,16)	=	Type of CO <sub>2</sub> delivery 0 = overboard 1 = CO <sub>2</sub> reduction
WV(32,70)	=	CO <sub>2</sub> accumulator temperature, F

OUTPUT:

CO2REM	=	CO <sub>2</sub> removed from air, lbm
CO2LOD	=	CO <sub>2</sub> removed from air per # of bed, %
TCYCLE	=	Total cycle time, sec
H2OADD	=	H <sub>2</sub> O added to air, lbm
H2OLOD	=	H <sub>2</sub> O added air per # of bed, %
TBLD	=	Time for bleed down, sec
WAIR	=	Total air through bed, lbm
WLOD	=	Total air through bed per # bed, %
TA EX	=	Time for air exchange, sec
BH201	=	Water loading, lbm
WLOAD	=	Water loading per # of bed, lbm
TABDT	=	absorption time, sec
BCO21	=	CO <sub>2</sub> loading on bed, lbm
CLOAD	=	CO <sub>2</sub> loading at end of cycle per # of bed, %
CO2RR	=	CO <sub>2</sub> removal rate, pph

OUTPUT:

TABMAX	=	Next absorb time limit, sec
EFF	=	CO <sub>2</sub> removal efficiency, %
WCO21B	=	CO <sub>2</sub> at end of bleed, lhm
WCO21E	=	CO <sub>2</sub> at end of air exchange, lhm
TDES	=	desorb time, sec
CO2OBD	=	CO <sub>2</sub> to accumulator package, lhm
PCTCO2	=	CO <sub>2</sub> to accumulator package per # of bed, %
TFLAG	=	Lag time after desorption, sec
AVGDLV	=	average rate of CO <sub>2</sub> delivered to accumulator package, pph
WSTEAM	=	amount of steam through the bed, lhm
WSLOD	=	amount of steam through bed per # of bed, %
WSTM	=	steam flow during next desorption cycle, pph
BH202	=	Water loading on bed, lhm
WCO22B	=	CO <sub>2</sub> loading at end of bleed, lhm
BC022	=	CO <sub>2</sub> loading on bed, lhm
WCO22E	=	CO <sub>2</sub> loading at end of air exchange, lhm
ACH20	=	H <sub>2</sub> O vapor flow to accumulator and flow sensor
ACO2	=	O <sub>2</sub> flow to accumulator and flow sensor
ACN2	=	N <sub>2</sub> flow to accumulator and flow sensor
ACCO2	=	CO <sub>2</sub> flow to accumulator and flow sensor
TOTWGT	=	Total vapor flow to accumulator and flow sensor
PURITY	=	CO <sub>2</sub> purity to accumulator and flow sensor

### A.2.2 IR45 Subroutine

Additional logic was incorporated into the IR45 subroutine to allow the SAWD subsystem restart capability. The SAWD can be started from a transient startup without the steady state solution being performed first. The restart capability was incorporated in the IR45 subroutine by initializing the SAWD inlet and exit header values as well as each bed segment (i.e., temperature, pressure, molecular weight ...) in the IR45 subroutine. Previously, these values were initialized in the subroutine STAEDY which is only performed during a steady state solution.

Additional logic was also added to IR45 in subroutine BALNCE. This logic clamps the bed segment temperature which has just been calculated through the iteration technique. If the bed segment inlet temperature is greater than the bed segment temperature at the start of the time step, then the bed segment temperature must increase.

## A.3 Program Use

### A.3.1 Accessing Desired Job Control List

Instructions to access ESCM and use the program have not been changed. However, the command list to be accessed is ESCMECL.CLIST instead of ESCMCL.CLIST. A listing of the ESCMECL.CLIST is given in Table A-1.

TABLE A-1

## LISTING OF ESCMECL FOR ESCM MODEL

```

CONTROL PROMPT NOMSG
ERASE
N1: DELETE PLOT.DATA
    DELETE OUT.DATA
FREE FILE(FT05F001)
FREE FILE(FT06F001)
FREE FILE(FT10F001)
FREE FILE(FT11F001)
FREE FILE(FT16F001)
FREE FILE(FT20F001)
FREE FILE(FT80F001)
FREE FILE(FT81F001)
FREE FILE(FT41F001)
FREE FILE(FT42F001)
FREE FILE(FT48F001)
FREE FILE(FT44F001)
FREE ATTRLIST(A1 B2 C8 D4 E5)
ATTRIB A1 BLKSIZE(844) RECFM(V B) LRECL(844)
ATTRIB B2 BLKSIZE(10000) RECFM(V B-S) LRECL(10000)
ATTRIB C8 BLKSIZE(8404) RECFM(V B-S) LRECL(8404)
ATTRIB D4 BLKSIZE(8990) RECFM(F B-A) LRECL(188)
ATTRIB E5 BLKSIZE(8990) RECFM(F B) LRECL(80)
DELETE DD1
DELETE DD2
DELETE DD8
DELETE DD4
DELETE DD5
DELETE DD6
DELETE IN10
DELETE IN11
WRITE
WRITE
WRITE DATA SETS ARE NOW BEING ALLOCATED.
ALLOC DS(DD1) F(FT41F001) NEW SPACE(844,200) BLOCK(844) +
    USING(A1) DELETE
ALLOC DS(DD2) F(FT42F001) NEW SPACE(200,200) BLOCK(10000) +
    USING(B2) DELETE
ALLOC DS(DD3) F(FT48F001) NEW SPACE(200,200) BLOCK(8404) +
    USING(C8) DELETE
ALLOC DS(DD4) F(FT44F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(DD5) F(FT80F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(DD6) F(FT81F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(IN10) F(FT10F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(IN11) F(FT11F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(ESCM2E.DATA) F(FT05F001)
  
```



TABLE A-1 (Continued)  
LISTING OF ESCMECL FOR ESCM MODEL

```
ALLOC DS(OUT.DATA) F(FT06F001) NEW SPACE(200,200) BLOCK(8120) +  
    USING(D4) CATALOG  
ALLOC DS(PLOT.DATA) F(FT16F001) NEW SPACE(200,200) BLOCK(8408) +  
    UNIT(TSOWRKB) USING(C8) CATALOG  
ALLOC DS(*) F(FT20F001)  
CONTROL MSG  
WRITE  
WRITE DATA SETS HAVE BEEN ALLOCATED. PROGRAM IS NOW EXECUTING.  
TIME  
CALL 'ENG.G15.LM(ESCM2)'  
WRITE  
WRITE THE PROGRAM HAS FINISHED.  
TIME  
END
```

### A.3.2 Input Data

There is an addition to the existing input data set, ESCM2B. An extra KARY card, KARY 19, was added to component #6 (cooling fluid boundary conditions). KARY 19 represents the type of control to be used for the SAWD subsystem. If KARY 19 is 0, relative humidity control is used for the SAWD. Accumulator control will be used if KARY 19 is 1. If KARY 19 is 2, then the newly implemented flow sensor (energy balance) control is used. This new data set is called ESCM2E. The procedure for accessing the data set is the same as in the original User's Manual [4].

### A.3.3 ESCM Output

Additional output is available to two of the three forms of the output (screen and hardcopy output). At the end of each absorption and desorption, a summary of SAWD calculated parameters is output in tabular form. This table will appear on the screen and on hardcopy immediately following the schematic corresponding to the completion of the absorption or desorption. The values printed on the table include:

- (1)  $\text{CO}_2$  removed from air during absorption, lbm
- (2)  $\text{CO}_2$  removed from air during absorption per # of bed, lbm
- (3) Total cycle time, sec
- (4)  $\text{H}_2\text{O}$  added to air during absorption, lbm
- (5)  $\text{H}_2\text{O}$  added to air (absorption) per # of bed, %



- (6) Time for bleed down (absorption), sec
- (7) Total air through bed (absorption), lhm
- (8) Total air through bed (absorption) per # of bed, %
- (9) Time for air exchange (absorption), sec
- (10) Water loading at end of absorption, lhm
- (11) Water loading at end of absorption per # of bed, %
- (12) Absorption time, sec
- (13) CO<sub>2</sub> loading at end of absorption, lhm
- (14) CO<sub>2</sub> loading at end of absorption per # of bed, %
- (15) CO<sub>2</sub> removal rate, pph
- (16) Next absorb time limit, sec
- (17) CO<sub>2</sub> removal efficiency %
- (18) CO<sub>2</sub> on bed at end of bleed (absorbing bed), lhm
- (19) CO<sub>2</sub> on bed at end of air exchange (absorbing bed), lhm
- (20) CO<sub>2</sub> removed from bed (desorption), lhm
- (21) CO<sub>2</sub> removed from bed per # bed (desorbing bed), %
- (22) Desorption time, sec
- (23) CO<sub>2</sub> to accumulator package, lhm
- (24) CO<sub>2</sub> to accumulator package per # of bed, %
- (25) Lag time after desorption sec
- (26) Water added to bed (desorbing bed), lhm
- (27) Water added to bed (desorbing) per # of bed %
- (28) Average rate of CO<sub>2</sub> delivered to accumulator package, pph
- (29) Amount of steam through the bed, lhm
- (30) Steam flow during next desorption cycle, pph
- (31) Water loading at the end of desorption, lhm

- (32) Water loading at end of desorption per # of bed, %
- (33) CO<sub>2</sub> loading at end of bleed (desorption), lbm
- (34) CO<sub>2</sub> loading on bed at end of desorption, lbm
- (35) CO<sub>2</sub> loading on bed at end of desorption per # of bed, %
- (36) CO<sub>2</sub> on desorbing bed at end of air exchange, lbm
- (37) Water vapor flow to accumulator flow sensor
- (38) O<sub>2</sub> vapor flow to accumulator and flow sensor
- (39) N<sub>2</sub> vapor flow to accumulator and flow sensor
- (40) CO<sub>2</sub> vapor flow to accumulator and flow sensor
- (41) Total vapor flow to accumulator and flow sensor
- (42) Carbon dioxide purity of flow to accumulator and flow  
sensors

#### A.4 Sample Problem

A sample problem has been run using the updated ESCM computer simulation/emulation model and the ESCMZE to input data set. The case was run for four hours. The hardcopy output of this sample problem is shown in Table A-3.

TABLE A-2

## SAWD PERFORMANCE SUMMARY OUTPUT

COMPUTER SIMULATION RESULTS FOR SAWD II CYCLE NUMBER 1 TIME = 2310.0 SEC

\*\*\*\*\* ABSORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #1 \*\*\*\*\*

	TOTAL (LBM)	PER % OF BED, %		
CO2 REMOVED FROM AIR	= 0.000	0.00	TOTAL CYCLE TIME	= 2310.0 SEC
H2O ADDED TO AIR	= 0.000	0.00	TIME FOR BLEED DOWN	= 0.0 SEC
TOTAL AIR THROUGH BED	= 0.00	0.0	TIME FOR AIR EXCHANGE	= 0.0 SEC
WATER LOADING AT END	= 2.550	30.000	ABSORPTION TIME	= 2310.0 SEC
CO2 LOADING AT END	= 0.005	0.059	CO2 REMOVAL RATE	= 0.000 PPH
NEXT ABSORB TIME LIMIT	= 3300.0 SEC		CO2 REMOVAL EFFICIENCY	= 0.00 PCT
CO2 AT END OF BLEED	= 0.005 LBM		CO2 AT AIR EXCHG END	= 0.005 LBM

\*\*\*\*\* DESORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #2 \*\*\*\*\*

	TOTAL (LBM)	PER % OF BED, %		
CO2 REMOVED FROM BED	= 0.294	3.46	DESORPTION TIME	= 2310.0 SEC
CO2 TO ACCUM. PKG.	= 0.175	5.00	LAG TIME AFTER DESORB	= 0.0 SEC
H2O ADDED TO BED	= 1.620	19.06	AVG CO2 TO ACCUM. PKG.	= 0.273 PPH
STEAM THROUGH BED	= 1.636	19.25	NEXT DESORB STEAM FLOW	= 2.550 PPH
WATER LOADING AT END	= 3.700	43.530	CO2 AT END OF BLEED	= 0.300 LBM
CO2 LOADING AT END	= 0.006	0.073	CO2 AT AIR EXCHG END	= 0.300 LBM

SUMMARY OF FLOW TO FLOW SENSOR AND ACCUMULATOR

WATER VAPOR	= 0.038 LBM
OXYGEN	= 0.000 LBM
NITROGEN	= 0.000 LBM
CARBON DIOXIDE	= 0.306 LBM
TOTAL	= 0.343 LBM

PURITY = 89.08 PCT



TABLE A-2 (CONTINUED)

SAWD PERFORMANCE SUMMARY OUTPUT

COMPUTER SIMULATION RESULTS FOR SAWD II CYCLE NUMBER 2 TIME = 5790.0 SEC

\*\*\*\*\* ABSORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #2 \*\*\*\*\*

TOTAL PER \$ OF	BED, %	
(LBM)		
CO2 REMOVED FROM AIR	= 0.220	2.59
H2O ADDED TO AIR	= 2.007	23.62
TOTAL AIR THROUGH BED	= 61.28	721.0
WATER LOADING AT END	= 1.693	19.914
CO2 LOADING AT END	= 0.227	2.666
NEXT ABSORB TIME LIMIT	= 1200.0 SEC	
CO2 AT END OF BLEED	= 0.006 LBM	
CO2 AT AIR EXCHG END	= 0.008 LBM	

\*\*\*\*\* DESORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #1 \*\*\*\*\*

TOTAL PER \$ OF	BED, %	
(LBM)		
CO2 REMOVED FROM BED	= -0.012	-0.14
CO2 TO ACCUM. PKG.	= 0.050	5.00
H2O ADDED TO BED	= 1.032	12.15
STEAM THROUGH BED	= 0.329	3.87
WATER LOADING AT END	= 3.582	42.145
CO2 LOADING AT END	= 0.017	0.200
CO2 AT AIR EXCHG END	= 0.034 LBM	

SUMMARY OF FLOW TO FLOW SENSOR AND ACCUMULATOR

WATER VAPOR = 0.034 LBM  
OXYGEN = 0.016 LBM  
NITROGEN = 0.057 LBM  
CARBON DIOXIDE = 0.009 LBM  
TOTAL = 0.116 LBM

PURITY = 7.46 PCT

COMP NO	12	FAN	SUBR NO	23	PRI	SOR	11	SEC	SOR	0	COMP	PASS NO	387	ELAPSED TIME IN MILLISEC	TIME = 5905.0 SEC		
VR( 1)	=	1392.7	VR( 2)	=	49.944	VR( 3)	=	14.689	VR( 4)	=	14.689	VR( 5)	=	1382.7	VR( 6)	=	9.9928
VR( 7)	=	0.00000E+00	VR( 8)	=	0.24310	VR( 9)	=	28.864	VR( 10)	=	305.75	VR( 11)	=	1069.5	VR( 12)	=	7.4079
VR( 13)	=	0.00000E+00	VR( 14)	=	0.00000E+00	VR( 15)	=	0.00000E+00	VR( 16)	=	0.00000E+00	VR( 17)	=	0.00000E+00	VR( 18)	=	0.00000E+00
VR( 19)	=	477.82	VR( 20)	=	0.00000E+00	VR( 21)	=	0.00000E+00	VR( 22)	=	0.00000E+00	VR( 23)	=	0.00000E+00	VR( 24)	=	0.00000E+00
VR( 25)	=	0.00000E+00	VR( 26)	=	0.00000E+00	VR( 27)	=	0.00000E+00	VR( 28)	=	0.00000E+00	VR( 29)	=	0.00000E+00	VR( 30)	=	0.00000E+00
VR( 31)	=	0.00000E+00	VR( 32)	=	0.00000E+00	VR( 33)	=	0.00000E+00	VR( 34)	=	0.00000E+00	VR( 35)	=	0.00000E+00	VR( 36)	=	0.00000E+00
VR( 37)	=	0.00000E+00	VR( 38)	=	0.00000E+00	VR( 39)	=	0.00000E+00	VR( 40)	=	0.00000E+00	VR( 41)	=	0.00000E+00	VR( 42)	=	0.00000E+00
VR( 43)	=	0.00000E+00	VR( 44)	=	1.0000	VR( 45)	=	0.00000E+00	VR( 46)	=	0.00000E+00	VR( 47)	=	0.00000E+00	VR( 48)	=	0.00000E+00
VR( 49)	=	0.00000E+00	VR( 50)	=	0.00000E+00	VR( 51)	=	140.00	VR( 52)	=	0.00000E+00	VR( 53)	=	0.00000E+00	VR( 54)	=	0.00000E+00
VR( 55)	=	0.00000E+00	VR( 56)	=	0.24455	VR( 57)	=	28.740	VR( 58)	=	0.77159E-01	VR( 59)	=	0.44000	VR( 60)	=	0.14600
VR( 61)	=	0.00000E+00	VR( 62)	=	0.00000E+00	VR( 63)	=	0.00000E+00	VR( 64)	=	0.00000E+00	VR( 65)	=	0.00000E+00	VR( 66)	=	0.00000E+00
VR( 67)	=	0.00000E+00	VR( 68)	=	0.00000E+00	VR( 69)	=	0.00000E+00	VR( 70)	=	0.00000E+00	VR( 71)	=	0.00000E+00	VR( 72)	=	0.00000E+00
VR( 73)	=	0.00000E+00	VR( 74)	=	0.00000E+00	VR( 75)	=	0.00000E+00	VR( 76)	=	0.00000E+00	VR( 77)	=	0.00000E+00	VR( 78)	=	0.00000E+00
VR( 79)	=	0.00000E+00	VR( 80)	=	0.00000E+00	VR( 81)	=	0.00000E+00	VR( 82)	=	0.00000E+00	VR( 83)	=	0.00000E+00	VR( 84)	=	0.00000E+00
VR( 85)	=	0.00000E+00	VR( 86)	=	0.00000E+00	VR( 87)	=	0.00000E+00	VR( 88)	=	0.00000E+00	VR( 89)	=	0.00000E+00	VR( 90)	=	0.00000E+00
VR( 91)	=	0.00000E+00	VR( 92)	=	0.00000E+00	VR( 93)	=	0.00000E+00	VR( 94)	=	0.00000E+00	VR( 95)	=	0.00000E+00	VR( 96)	=	0.00000E+00
VR( 97)	=	0.00000E+00	VR( 98)	=	0.00000E+00	VR( 99)	=	0.00000E+00	VR( 100)	=	0.00000E+00	VR( 101)	=	0.00000E+00	VR( 102)	=	0.00000E+00
VR( 103)	=	0.00000E+00	VR( 104)	=	0.00000E+00	VR( 105)	=	0.00000E+00	VR( 106)	=	0.00000E+00	VR( 107)	=	0.00000E+00	VR( 108)	=	0.00000E+00
VR( 109)	=	0.00000E+00	VR( 110)	=	0.00000E+00	VR( 111)	=	0.00000E+00	VR( 112)	=	0.00000E+00	VR( 113)	=	0.00000E+00	VR( 114)	=	0.00000E+00
VR( 115)	=	0.00000E+00	VR( 116)	=	0.00000E+00	VR( 117)	=	0.00000E+00	VR( 118)	=	0.00000E+00	VR( 119)	=	0.00000E+00	VR( 120)	=	0.00000E+00
VR( 121)	=	0.00000E+00	VR( 122)	=	0.00000E+00	VR( 123)	=	0.00000E+00	VR( 124)	=	0.00000E+00	VR( 125)	=	0.00000E+00	VR( 126)	=	0.00000E+00
VR( 127)	=	0.00000E+00	VR( 128)	=	0.00000E+00	VR( 129)	=	0.00000E+00	VR( 130)	=	0.00000E+00	VR( 131)	=	0.00000E+00	VR( 132)	=	0.00000E+00
VR( 133)	=	0.00000E+00	VR( 134)	=	0.00000E+00	VR( 135)	=	0.00000E+00	VR( 136)	=	0.00000E+00	VR( 137)	=	0.00000E+00	VR( 138)	=	0.00000E+00
VR( 139)	=	0.00000E+00	VR( 140)	=	0.00000E+00	VR( 141)	=	0.00000E+00	VR( 142)	=	0.00000E+00	VR( 143)	=	0.00000E+00	VR( 144)	=	0.00000E+00
VR( 145)	=	0.00000E+00	VR( 146)	=	0.00000E+00	VR( 147)	=	0.00000E+00	VR( 148)	=	0.00000E+00	VR( 149)	=	0.00000E+00	VR( 150)	=	0.00000E+00
VR( 151)	=	0.00000E+00	VR( 152)	=	0.00000E+00	VR( 153)	=	0.00000E+00	VR( 154)	=	0.00000E+00	VR( 155)	=	0.00000E+00	VR( 156)	=	0.00000E+00
VR( 157)	=	0.00000E+00	VR( 158)	=	0.00000E+00	VR( 159)	=	0.00000E+00	VR( 160)	=	0.00000E+00	VR( 161)	=	0.00000E+00	VR( 162)	=	0.00000E+00
VR( 163)	=	0.00000E+00	VR( 164)	=	0.00000E+00	VR( 165)	=	0.00000E+00	VR( 166)	=	0.00000E+00	VR( 167)	=	0.00000E+00	VR( 168)	=	0.00000E+00
VR( 169)	=	0.00000E+00	VR( 170)	=	0.00000E+00	VR( 171)	=	0.00000E+00	VR( 172)	=	0.00000E+00	VR( 173)	=	0.00000E+00	VR( 174)	=	0.00000E+00
VR( 175)	=	0.00000E+00	VR( 176)	=	0.00000E+00	VR( 177)	=	0.00000E+00	VR( 178)	=	0.00000E+00	VR( 179)	=	0.00000E+00	VR( 180)	=	0.00000E+00
VR( 181)	=	0.00000E+00	VR( 182)	=	0.00000E+00	VR( 183)	=	0.00000E+00	VR( 184)	=	0.00000E+00	VR( 185)	=	0.00000E+00	VR( 186)	=	0.00000E+00
VR( 187)	=	0.00000E+00	VR( 188)	=	0.00000E+00	VR( 189)	=	0.00000E+00	VR( 190)	=	0.00000E+00	VR( 191)	=	0.00000E+00	VR( 192)	=	0.00000E+00
VR( 193)	=	0.00000E+00	VR( 194)	=	0.00000E+00	VR( 195)	=	0.00000E+00	VR( 196)	=	0.00000E+00	VR( 197)	=	0.00000E+00	VR( 198)	=	0.00000E+00
VR( 199)	=	0.00000E+00	VR( 200)	=	0.00000E+00	VR( 201)	=	0.00000E+00	VR( 202)	=	0.00000E+00	VR( 203)	=	0.00000E+00	VR( 204)	=	0.00000E+00
VR( 205)	=	0.00000E+00	VR( 206)	=	0.00000E+00	VR( 207)	=	0.00000E+00	VR( 208)	=	0.00000E+00	VR( 209)	=	0.00000E+00	VR( 210)	=	0.00000E+00
VR( 211)	=	0.00000E+00	VR( 212)	=	0.00000E+00	VR( 213)	=	0.00000E+00	VR( 214)	=	0.00000E+00	VR( 215)	=	0.00000E+00	VR( 216)	=	0.00000E+00
VR( 217)	=	0.00000E+00	VR( 218)	=	0.00000E+00	VR( 219)	=	0.00000E+00	VR( 220)	=	0.00000E+00	VR( 221)	=	0.00000E+00	VR( 222)	=	0.00000E+00
VR( 223)	=	0.00000E+00	VR( 224)	=	0.00000E+00	VR( 225)	=	0.00000E+00	VR( 226)	=	0.00000E+00	VR( 227)	=	0.00000E+00	VR( 228)	=	0.00000E+00
VR( 229)	=	0.00000E+00	VR( 230)	=	0.00000E+00	VR( 231)	=	0.00000E+00	VR( 232)	=	0.00000E+00	VR( 233)	=	0.00000E+00	VR( 234)	=	0.00000E+00
VR( 235)	=	0.00000E+00	VR( 236)	=	0.00000E+00	VR( 237)	=	0.00000E+00	VR( 238)	=	0.00000E+00	VR( 239)	=	0.00000E+00	VR( 240)	=	0.00000E+00
VR( 241)	=	0.00000E+00	VR( 242)	=	0.00000E+00	VR( 243)	=	0.00000E+00	VR( 244)	=	0.00000E+00	VR( 245)	=	0.00000E+00	VR( 246)	=	0.00000E+00
VR( 247)	=	0.00000E+00	VR( 248)	=	0.00000E+00	VR( 249)	=	0.00000E+00	VR( 250)	=	0.00000E+00	VR( 251)	=	0.00000E+00	VR( 252)	=	0.00000E+00
VR( 253)	=	0.00000E+00	VR( 254)	=	0.00000E+00	VR( 255)	=	0.00000E+00	VR( 256)	=	0.00000E+00	VR( 257)	=	0.00000E+00	VR( 258)	=	0.00000E+00
VR( 259)	=	0.00000E+00	VR( 260)	=	0.00000E+00	VR( 261)	=	0.00000E+00	VR( 262)	=	0.00000E+00	VR( 263)	=	0.00000E+00	VR( 264)	=	0.00000E+00
VR( 265)	=	0.00000E+00	VR( 266)	=	0.00000E+00	VR( 267)	=	0.00000E+00	VR( 268)	=	0.00000E+00	VR( 269)	=	0.00000E+00	VR( 270)	=	0.00000E+00
VR( 271)	=	0.00000E+00	VR( 272)	=	0.00000E+00	VR( 273)	=	0.00000E+00	VR( 274)	=	0.00000E+00	VR( 275)	=	0.00000E+00	VR( 276)	=	0.00000E+00
VR( 277)	=	0.00000E+00	VR( 278)	=	0.00000E+00	VR( 279)	=	0.00000E+00	VR( 280)	=	0.00000E+00	VR( 281)	=	0.00000E+00	VR( 282)	=	0.00000E+00
VR( 283)	=	0.00000E+00	VR( 284)	=	0.00000E+00	VR( 285)	=	0.00000E+00	VR( 286)	=	0.00000E+00	VR( 287)	=	0.00000E+00	VR( 288)	=	0.00000E+00
VR( 289)	=	0.00000E+00	VR( 290)	=	0.00000E+00	VR( 291)	=	0.00000E+00	VR( 292)	=	0.00000E+00	VR( 293)	=	0.00000E+00	VR( 294)	=	0.00000E+00
VR( 295)	=	0.00000E+00	VR( 296)	=	0.00000E+00	VR( 297)	=	0.00000E+00	VR( 298)	=	0.00000E+00	VR( 299)	=	0.00000E+00	VR( 300)	=	0.00000E+00
VR( 301)	=	0.00000E+00	VR( 302)	=	0.00000E+00	VR( 303)	=	0.00000E+00	VR( 304)	=	0.00000E+00	VR( 305)	=	0.00000E+00	VR( 306)	=	0.00000E+00
VR( 307)	=	0.00000E+00	VR( 308)	=	0.00000E+00	VR( 309)	=	0.00000E+00	VR( 310)	=	0.00000E+00	VR( 311)	=	0.00000E+00	VR( 312)	=	0.00000E+00
VR( 313)	=	0.00000E+00	VR( 314)	=	0.00000E+00	VR( 315)	=	0.00000E+00	VR( 316)	=	0.00000E+00	VR( 317)	=	0.00000E+00	VR( 318)	=	0.00000E+00
VR( 319)	=	0.00000E+00	VR( 320)	=	0.00000E+00	VR( 321)	=	0.00000E+00	VR( 322)	=	0.00000E+00	VR( 323)	=	0.00000E+00	VR( 324)	=	0.00000E+00
VR( 325)	=	0.00000E+00	VR( 326)	=	0.00000E+00	VR( 327)	=	0.00000E+00	VR( 328)	=	0.00000E+00	VR( 329)	=	0.00000E+00	VR( 330)	=	0.00000E+00
VR( 331)	=	0.00000E+00	VR( 332)	=	0.00000E+00	VR( 333)	=	0.00000E+00	VR( 334)	=	0.00000E+00	VR( 335)	=	0.00000E+00	VR( 336)	=	0.00000E+00
VR( 337)	=	0.00000E+00	VR( 338)	=	0.00000E+00	VR( 339)	=	0.00000E+00	VR( 340)	=	0.00000E+00	VR( 341)	=	0.00000E+00	VR( 342)	=	0.00000E+00
VR( 343)	=</																

TABLE A-2 (CONTINUED)

## SAWD PERFORMANCE SUMMARY OUTPUT

ORIGINAL TAGS IN  
OF POOR QUALITY

COMPUTER SIMULATION RESULTS FOR SAWD II CYCLE NUMBER 3 TIME = 7050.0 SEC

\*\*\*\*\* ABSORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #1 \*\*\*\*\*

TOTAL PER % OF			
(LBM)	BED, %		
CO2 REMOVED FROM AIR = 0.082	0.96	TOTAL CYCLE TIME = 1260.0 SEC	
H2O ADDED TO AIR = 1.246	14.66	TIME FOR BLEED DOWN = 60.0 SEC	
TOTAL AIR THROUGH BED = 22.30	262.4	TIME FOR AIR EXCHANGE = 0.0 SEC	
WATER LOADING AT END = 2.336	27.482	ABSORPTION TIME = 1200.0 SEC	
CO2 LOADING AT END = 0.099	1.162	CO2 REMOVAL RATE = 0.245 PPH	
NEXT ABSORB TIME LIMIT = 1200.0 SEC		CO2 REMOVAL EFFICIENCY = 0.00 PCT	
CO2 AT END OF BLEED = 0.011 LBM		CO2 AT AIR EXCHG END = 0.011 LBM	

\*\*\*\*\* DESORPTION SUMMARY \*\*\*\*\*  
\*\*\*\*\* FOR BED #2 \*\*\*\*\*

TOTAL PER % OF			
(LBM)	BED, %		
CO2 REMOVED FROM BED = 0.216	2.54	DESORPTION TIME = 1200.0 SEC	
CO2 TO ACCUM. PKG. = 0.093	5.00	LAG TIME AFTER DESORB = 585.0 SEC	
H2O ADDED TO BED = 1.201	14.13	AVG CO2 TO ACCUM. PKG. = 0.265 PPH	
STEAM THROUGH BED = 0.425	5.00	NEXT DESORB STEAM FLOW = 0.156 PPH	
WATER LOADING AT END = 2.894	34.048	CO2 AT END OF BLEED = 0.087 LBM	
CO2 LOADING AT END = 0.011	0.124	CO2 AT AIR EXCHG END = 0.087 LBM	

## SUMMARY OF FLOW TO FLOW SENSOR AND ACCUMULATOR

WATER VAPOR = 0.098 LBM  
OXYGEN = 0.059 LBM  
NITROGEN = 0.208 LBM  
CARBON DIOXIDE = 0.143 LBM  
TOTAL = 0.509 LBM  
PURITY = 28.16 PCT

COMP NO	12	FAN	SUBR NO	23	FAILURE	23	PRI	SOR	11	SEC	SOR	0	ELAPSED TIME IN MILLISEC	471	COMP PASS NO	471	TIME = 7065.0 SEC
VR( 1)	=	1392.4	VR( 2)	=	50.062	VR( 3)	=	14.687	VR( 4)	=	14.687	VR( 5)	=	1382.3	VR( 6)	=	10.035
VR( 7)	=	0.00000E+00	VR( 8)	=	0.24308	VR( 9)	=	28.868	VR( 10)	=	305.62	VR( 11)	=	1068.8	VR( 12)	=	7.8741
VR( 13)	=	0.00000E+00	VR( 14)	=	0.00000E+00	VR( 15)	=	0.00000E+00	VR( 16)	=	0.00000E+00	VR( 17)	=	0.00000E+00	VR( 18)	=	0.00000E+00
VR( 65)	=	477.82	VR( 66)	=	0.00000E+00	VR( 67)	=	0.00000E+00	VR( 68)	=	0.00000E+00	VR( 69)	=	0.00000E+00	VR( 70)	=	0.00000E+00
VR( 71)	=	0.00000E+00	VR( 72)	=	0.00000E+00	VR( 73)	=	0.00000E+00	VR( 74)	=	0.00000E+00	VR( 75)	=	0.00000E+00	VR( 76)	=	300.00
VR( 77)	=	0.00000E+00	VR( 78)	=	0.00000E+00	VR( 79)	=	0.00000E+00	VR( 80)	=	0.00000E+00	VR( 81)	=	0.00000E+00	VR( 82)	=	0.00000E+00
VR( 83)	=	0.00000E+00	VR( 84)	=	1.0000	VR( 85)	=	0.00000E+00	VR( 86)	=	0.00000E+00	VR( 87)	=	0.00000E+00	VR( 88)	=	0.00000E+00
VR( 89)	=	0.00000E+00	VR( 90)	=	0.00000E+00	VR( 91)	=	140.00	VR( 92)	=	0.00000E+00	VR( 93)	=	0.00000E+00	VR( 94)	=	0.00000E+00
			CPS	=	0.24454												
			MTHS	=	0.00000E+00												
			MTHS	=	28.743												
			RHOS	=	0.00000E+00												
			VISSCP	=	0.77141E-01												
			XXP	=	0.14600												
			XXS	=	0.00000E+00												



SVHSER 10639

SAWD PERFORMANCE SUMMARY OUTPUT

A-14





SVHSER 10639

### ESCM SAMPLE PROBLEM OUTPUT

A-15



TABLE A-3 (CONTINUED)

## ESCM SAMPLE PROBLEM OUTPUT

```

2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60
CABIN (2)          CREW (1)          FROM CABIN          *****
= 8000. CU-FT      = 3              M= 9354.          *
= 593.84 LBM      TOTAL Q = 1350.0 B/HR      T= 69.2          *
= 69.2 F          METABOLIC Q = 450.0 B/HR/HAN  A          *
= 50.7 F          SENSIBLE = 327.0 B/HR/HAN  A          *
= 14.67 PSIA      LATENT = 123.0 B/HR/HAN  A          *
TOTAL PRESS       O2 USAGE = 0.2200 PPH      A          *
112 X             CO2 PROO = 0.2592 PPH      A          *
113 X             FROM
114 X             CABIN
115 X             M= 1391.
116 X             T= 69.2
117 X             A
118 X             SENSIBLE = 17065. B/HR
119 X             LATENT = 255. B/HR
120 X             ECLSS Q:
121 X             SENSIBLE = 6273. B/HR
122 X             LATENT = 779. B/HR
123 X             REL HUMIDITY = 51.40 PCT
124 X
125 X
126 X
127 X
128 X
129 X
130 X             FROM CABIN
131 X             M= 0.00
132 X             T= 69.2
133 X             A
134 X             Q = 0.
135 X             [CFH= 0.
136 X             A
137 X             M= 0.00
138 X             T= 69.5
139 X             S
140 X             S
141 X             S
142 X             S
143 X             S
144 X             S
145 X             S
146 X             S
147 X             S
148 X             S
149 X             S
150 X             S
151 X             S
152 X             S
153 X             S
154 X             S
155 X             S
156 X             S
157 X             S
158 X             S
159 X             S
160 X             S
161 X             S
162 X             S
163 X             S
164 X             S
165 X             S
166 X             S
167 X             S
168 X             S
169 X             S
170 X             S
171 X             S
172 X             S
173 X             S
174 X             S
175 X             S
176 X             S
177 X             S
178 X             S
179 X             S
180 X             S
181 X             S
182 X             S
183 X             S
184 X             S
185 X             S
186 X             S
187 X             S
188 X             S
189 X             S
190 X             S
191 X             S
192 X             S
193 X             S
194 X             S
195 X             S
196 X             S
197 X             S
198 X             S
199 X             S
200 X             S
201 X             S
202 X             S
203 X             S
204 X             S
205 X             S
206 X             S
207 X             S
208 X             S
209 X             S
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617 X             S
618 X             S
619 X             S
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622 X             S
623 X             S
624 X             S
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TABLE A-3 (CONTINUED)

1	SPACE STATION AIR REVITALIZATION SUBSYSTEM SAND II DEMONSTRATION MODEL.	MISSION TIME: 3400. SEC ( 1.00 HR)	DATE: 02/10/87
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TABLE A-3 (CONTINUED)

## ESCM SAMPLE PROBLEM OUTPUT

SPACE STATION AIR REVITALIZATION SUBSYSTEM SANO II DEMONSTRATION MODEL. MISSION TIME: 5400. SEC ( 1.50 HR ) DATE: 02/10/87

CABIN (2)										CREW (1)										FROM CABIN										*****										TO CABIN									
VOLUME = 8000. CU-FT										NO OF MEN = 3										M= 9361.										*****										M= 9360.									
= 594.26 LBM										TOTAL Q = 1755.0 B/HR										T= 69.3										* T= 68.8										T= 63.5									
AIR MASS = 69.3 F										METABOLIC Q = 585.0 B/HR/MAN										A										[SENSIBLE]										[SENSIBLE]									
TEMP = 51.2 F										SENSIBLE = 331.7 B/HR/MAN										A										[HX FAN (4)]										[HX (5)]									
TOTAL PT = 14.69 PSIA										LATENT = 253.3 B/HR/MAN										A										T= 70.5										A									
DEM PRESS = 2.89 PSIA										O2 USAGE = 0.2861 PPH										A										Q = 2843. [A]A										[A]A									
C02 PRESS = 2.62 MM-HG										C02 PROD = 0.3370 PPH										A										[CFM= 2100.]										[A]A									
GAS LEAKAGE = 0.083 PPH										FROM CABIN										A										M=1827.										A									
O2 MAKEUP = 0.000 PPH										CABIN										A										T= 60.0 *										TO CABIN									
15 X N2 MAKEUP										M= 1323.										*****										T= 50.5										M= 1391.									
16 X N2 MAKEUP										T= 69.3										* T= 54.1										A										T= 50.5									
17 X NON ECLSS Q:										A										A										A										A									
18 X SENSIBLE										A										A										A										A									
20 X SENSIBLE										A										A										A										A									
21 X SENSIBLE										A										A										A										A									
22 X LATENT										A										A										A										A									
23 X REL HUMIDITY = 52.20 PCT										A										A										A										A									
24 X										A										A										A										A									
25 X										A										A										A										A									
26 X										A										A										A										A									
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59 X										A										A										A										A									
60 X										A										A										A										A									



TABLE A-3 (CONTINUED)

[illegible]



SVHSER 10639

### ESCM SAMPLE PROBLEM OUTPUT

[illegible]



SVHSER 10639

### ESCM SAMPLE PROBLEM OUTPUT

A-21

TABLE A-3 (CONTINUED)

## ESCM SAMPLE PROBLEM OUTPUT

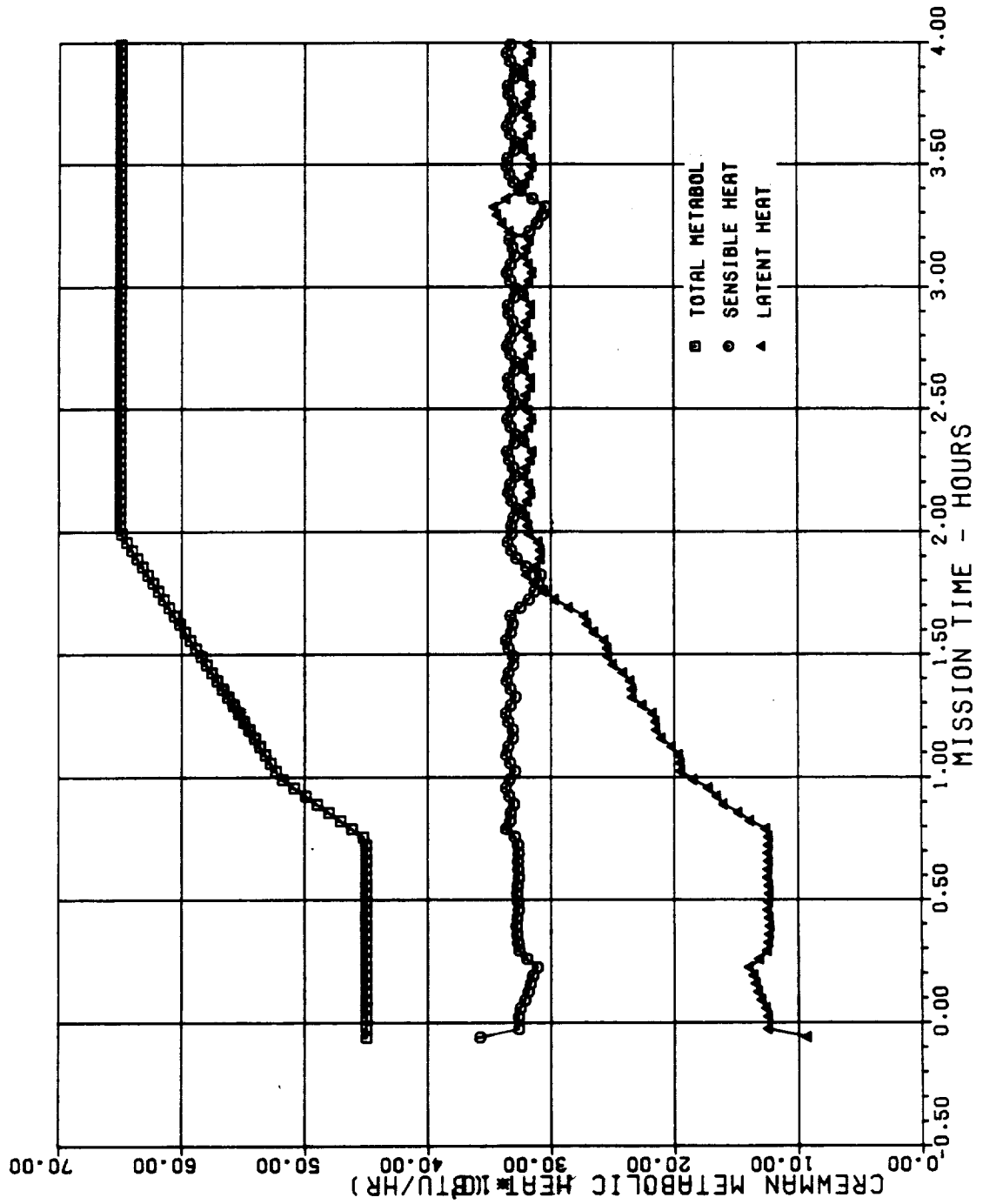
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1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAND II DEMONSTRATION MODEL. MISSION TIME: 14400. SEC ( 4.00 HR) DATE: 02/10/87
2
3 *****
4 X
5 X
6 X
7 X VOLUME = 8000. CU-FT NO OF MEN = 3 FROM CABIN ***** TO CABIN X
8 X AIR MASS = 595.01 LBH TOTAL Q = 1950.0 B/HR M= 9370. T= 69.3 M= 9372. X
9 X TEMP = 69.3 F METABOLIC Q = 650.0 B/HR/MAN A [SENSIBLE] [T= 70.2] X
10 X DEM PT = 52.4 F SENSIBLE = 331.4 B/HR/MAN A [SENSIBLE] [T= 70.5] [HX FAN (4)] [HX FAN (5)] X
11 X TOTAL PRESS = 14.70 PSIA LATENT = 318.6 B/HR/MAN A [SENSIBLE] [T= 70.5] [HX FAN (4)] [HX FAN (5)] X
12 X O2 PRESS = 2.90 PSIA O2 USAGE = 0.3178 PPH A [SENSIBLE] [T= 70.5] [HX FAN (4)] [HX FAN (5)] X
13 X CO2 PRESS = 3.08 MM-HG CO2 PROD = 0.3744 PPH A [SENSIBLE] [T= 70.5] [HX FAN (4)] [HX FAN (5)] X
14 X GAS LEAKAGE = 0.083 PPH FROM ***** X
15 X O2 MAKEUP = 0.000 PPH CABIN M= 1347. T= 69.3 M= 1392. X
16 X N2 MAKEUP = 0.000 PPH M= 1347. T= 69.3 M= 1392. X
17 X NON ECLSS Q: ***** X
18 X SENSIBLE = 1706.5 B/HR * T= 54.5 X
19 X LATENT = 255. B/HR * T= 54.5 X
20 X ECLSS Q: ***** X
21 X SENSIBLE = 4461. B/HR [REL. HUMID.] M= 1390. X
22 X LATENT = 498. B/HR V A T= 70.2 [HX (7)] T= 49.3 M= 1348. X
23 X REL HUMIDITY = 54.61 PCT (31) [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
24 X
25 X
26 X
27 X
28 X
29 X
30 X FROM CABIN ***** X
31 X M= 44.63 [SAND FAN (19)] M= 44.63 X
32 X T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
33 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
34 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
35 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
36 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
37 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
38 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
39 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
40 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
41 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
42 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
43 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
44 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
45 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
46 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
47 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
48 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
49 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
50 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
51 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
52 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
53 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
54 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
55 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
56 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
57 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
58 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
59 X A [M= 44.63] T= 69.3 [Q = 171. [CFM= 10. [M= 44.63] T= 69.3] ANINE [BED 1 (16)] [SENSIBLE] [T= 70.2] [HX (7)] T= 49.3 M= 1348. X
60 X

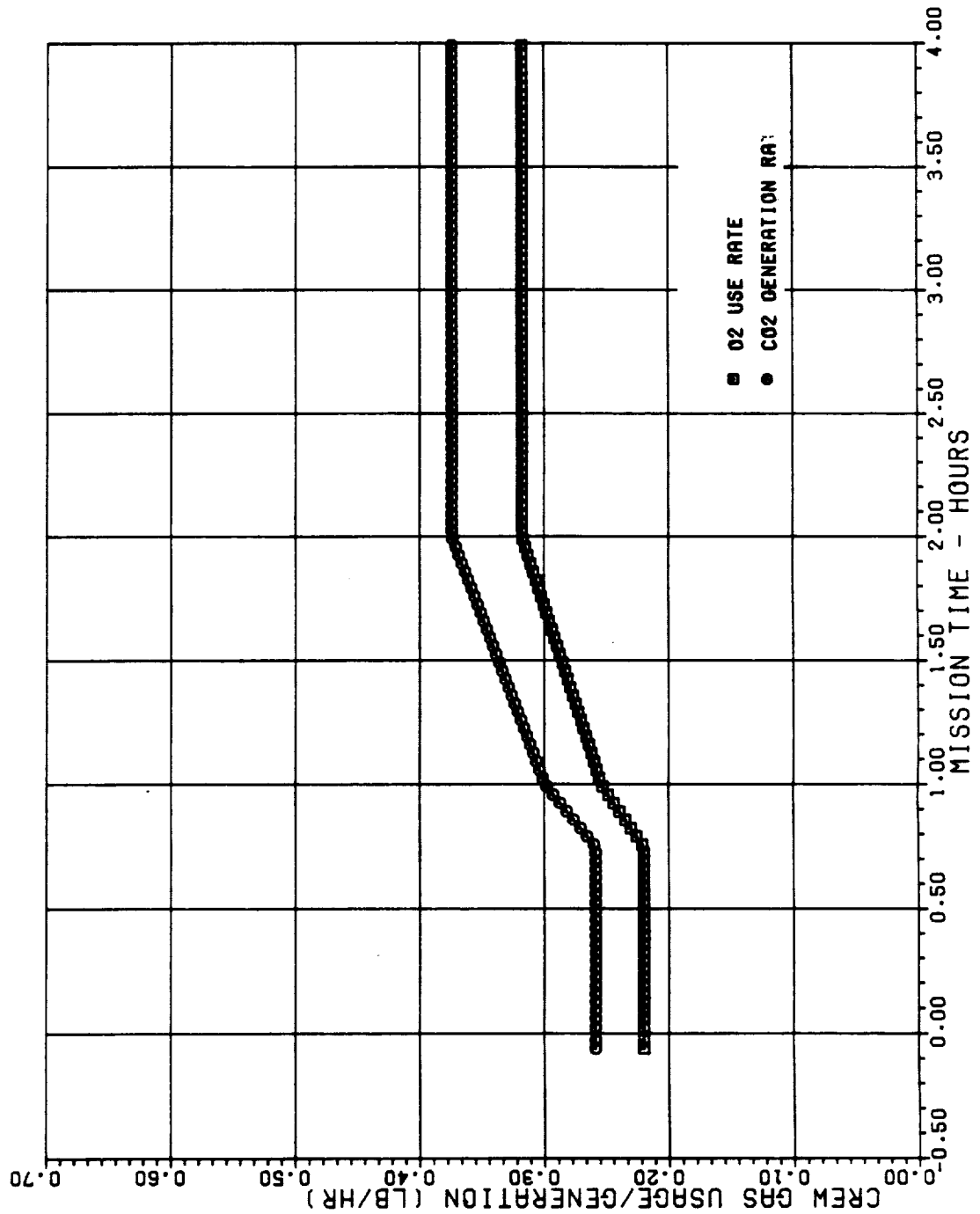
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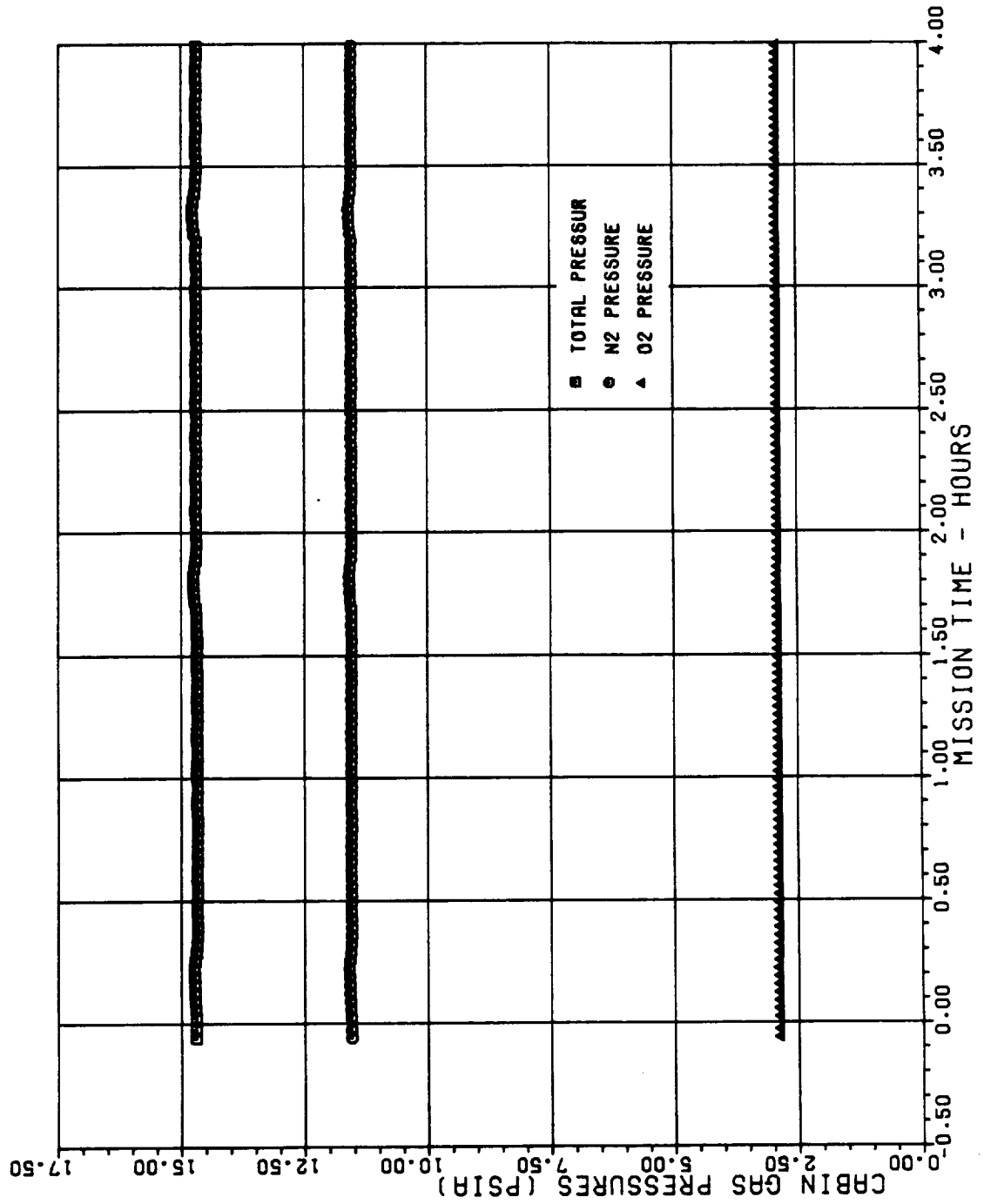
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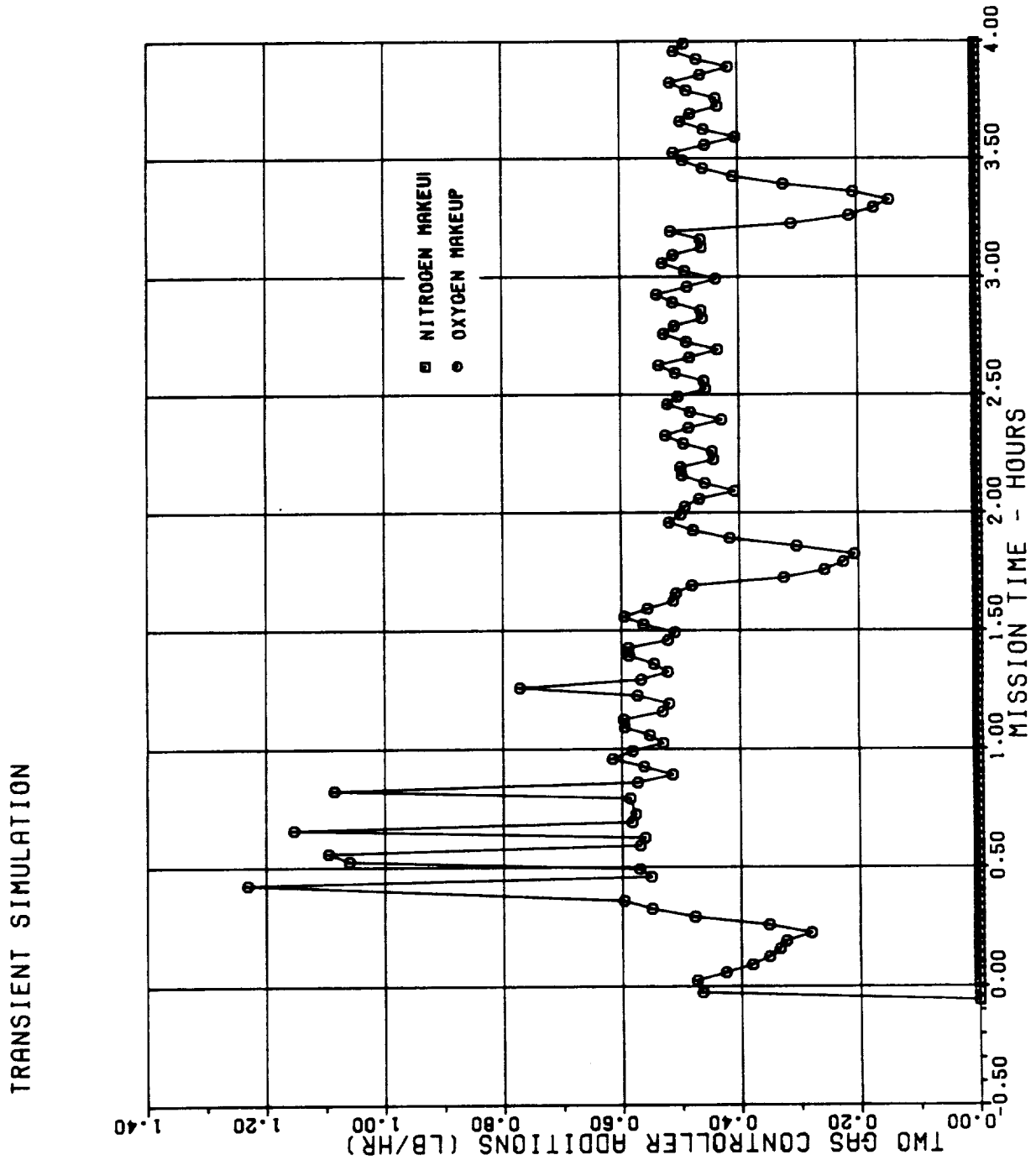


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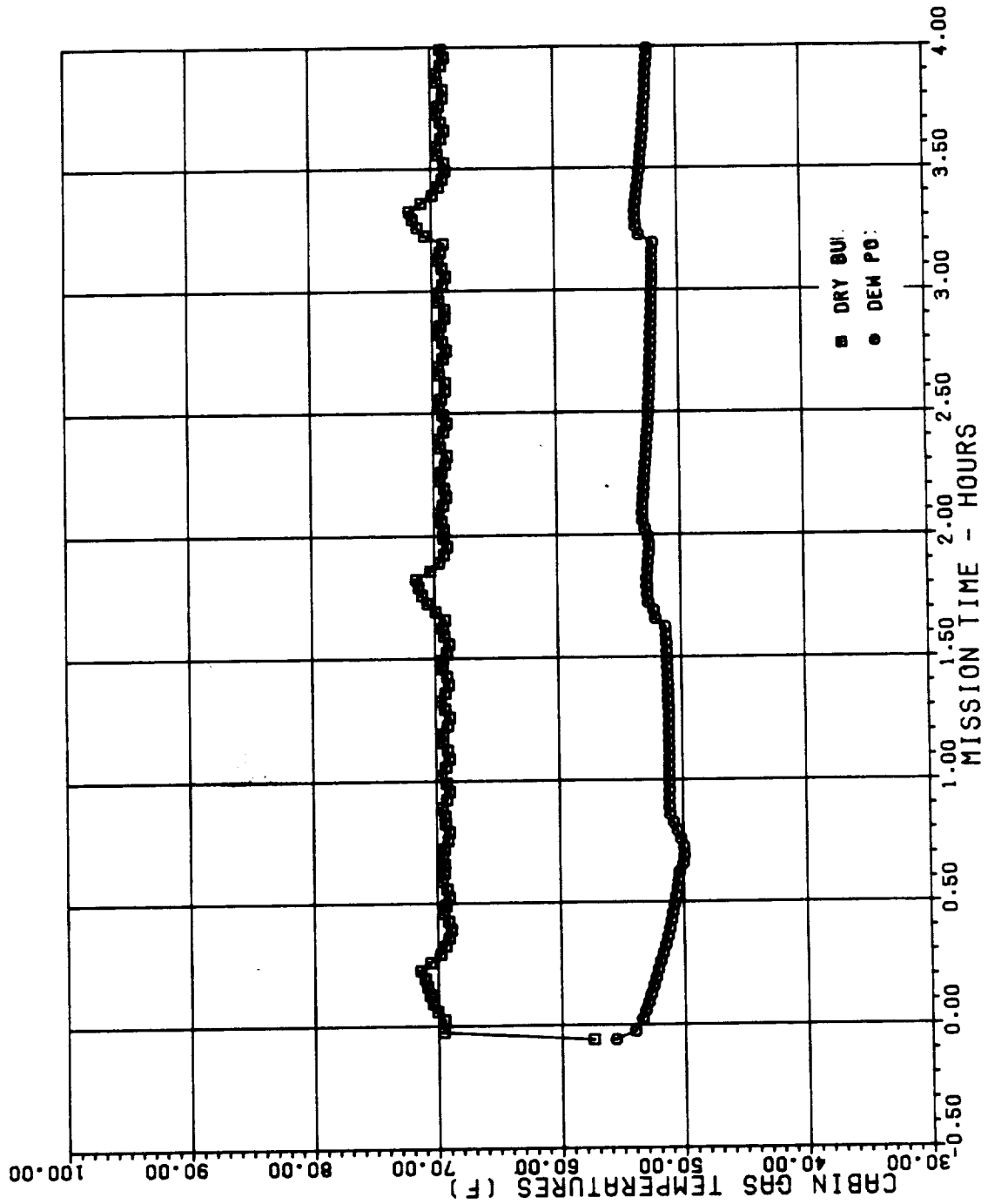


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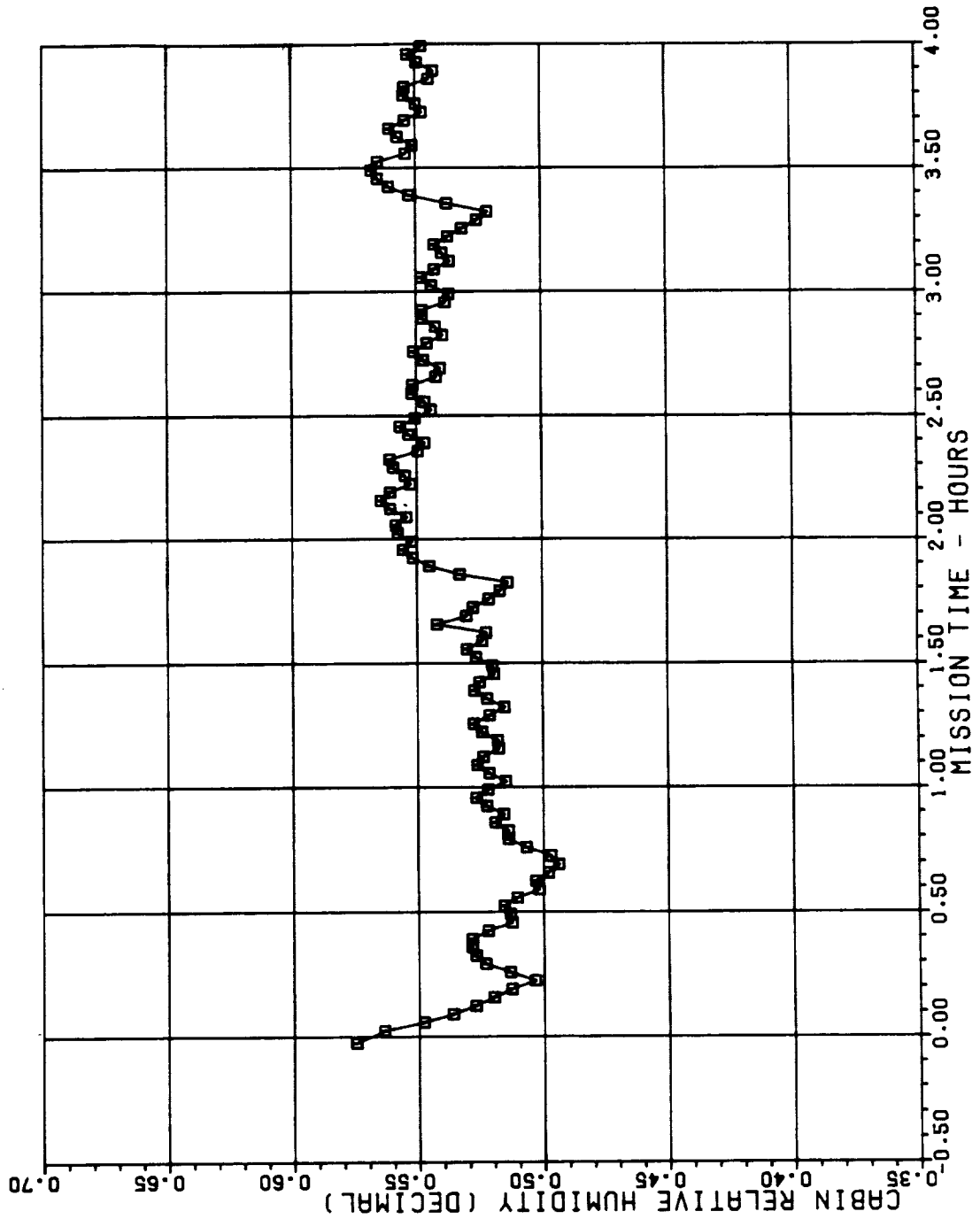


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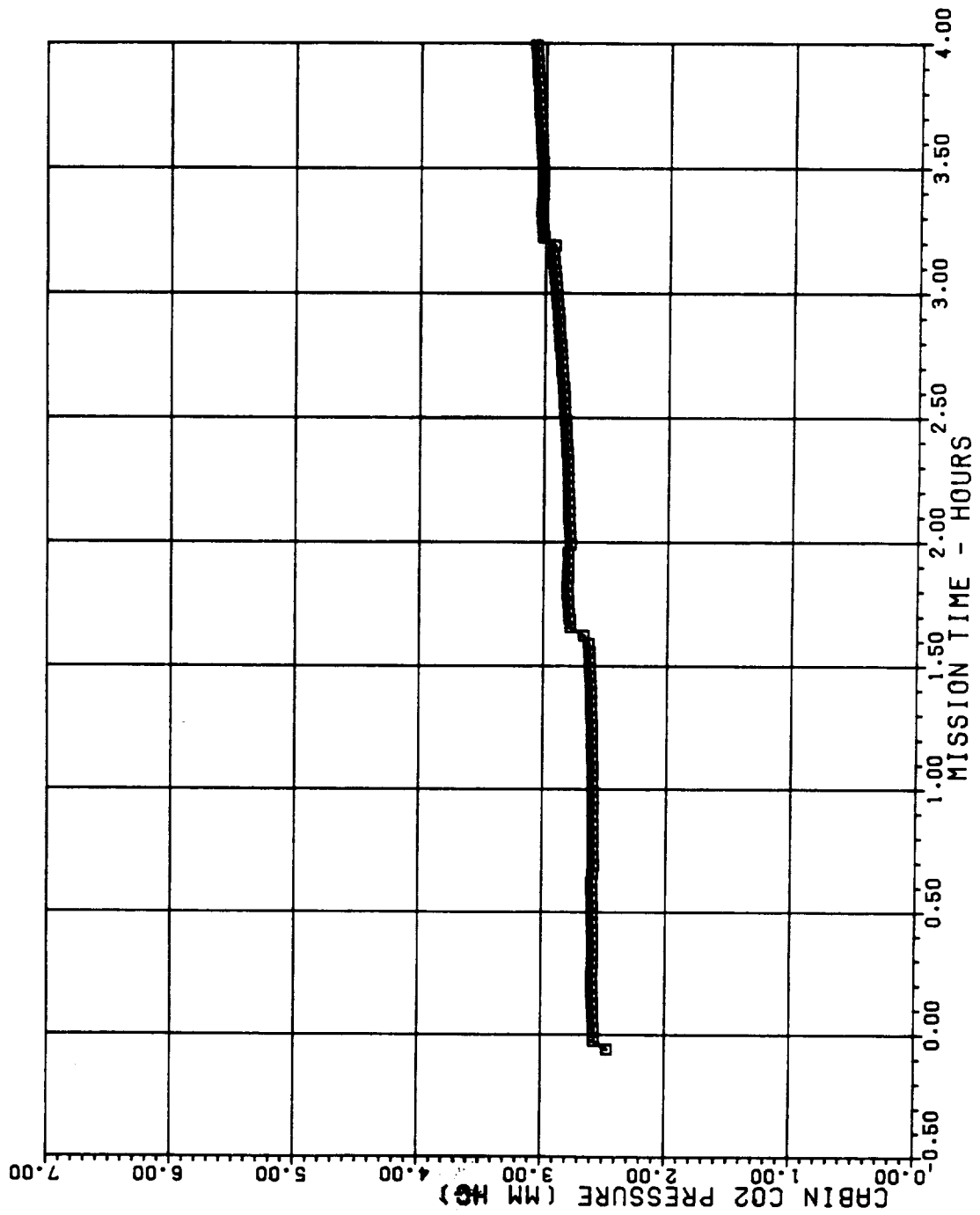




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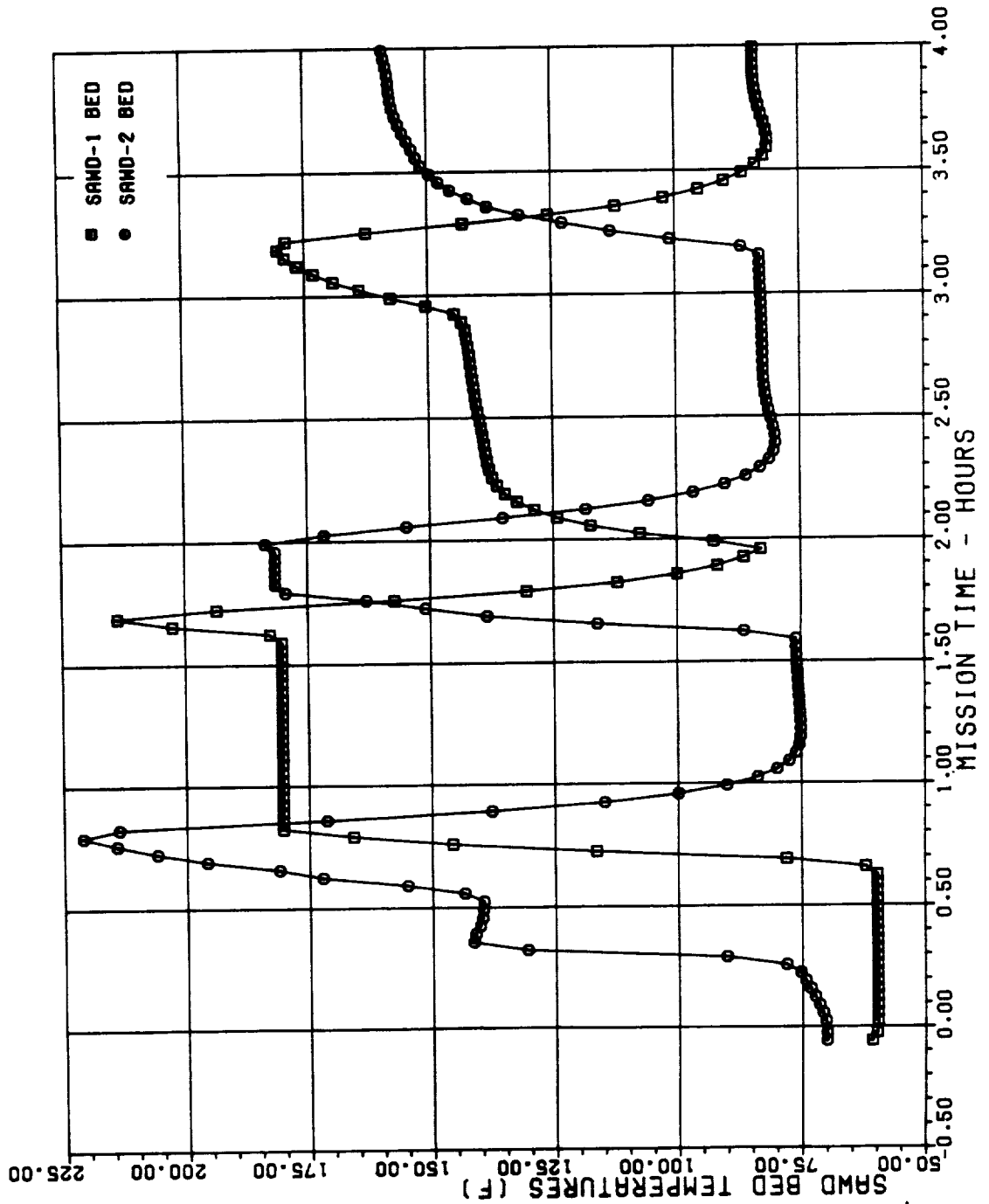


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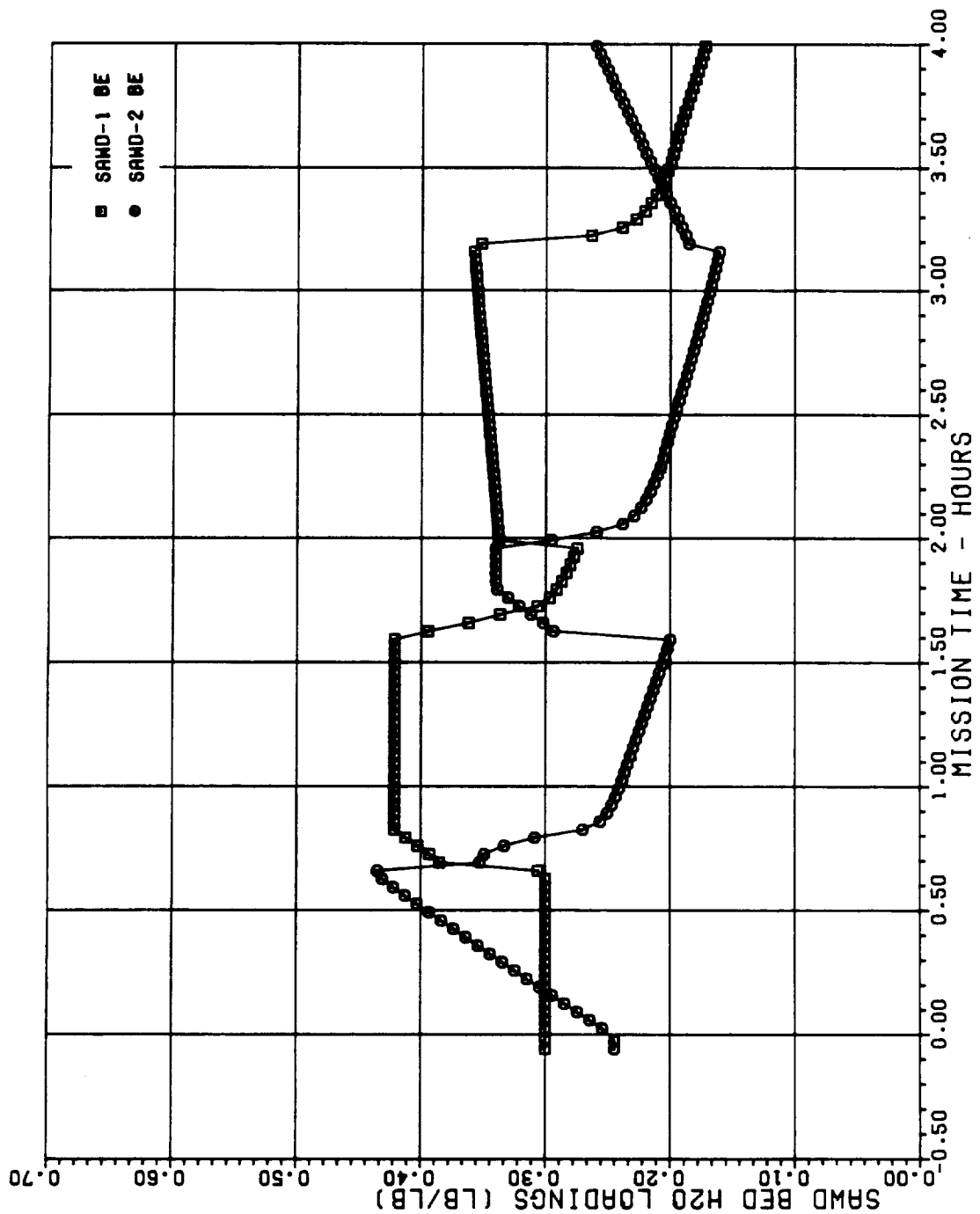


TRANSIENT SIMULATION

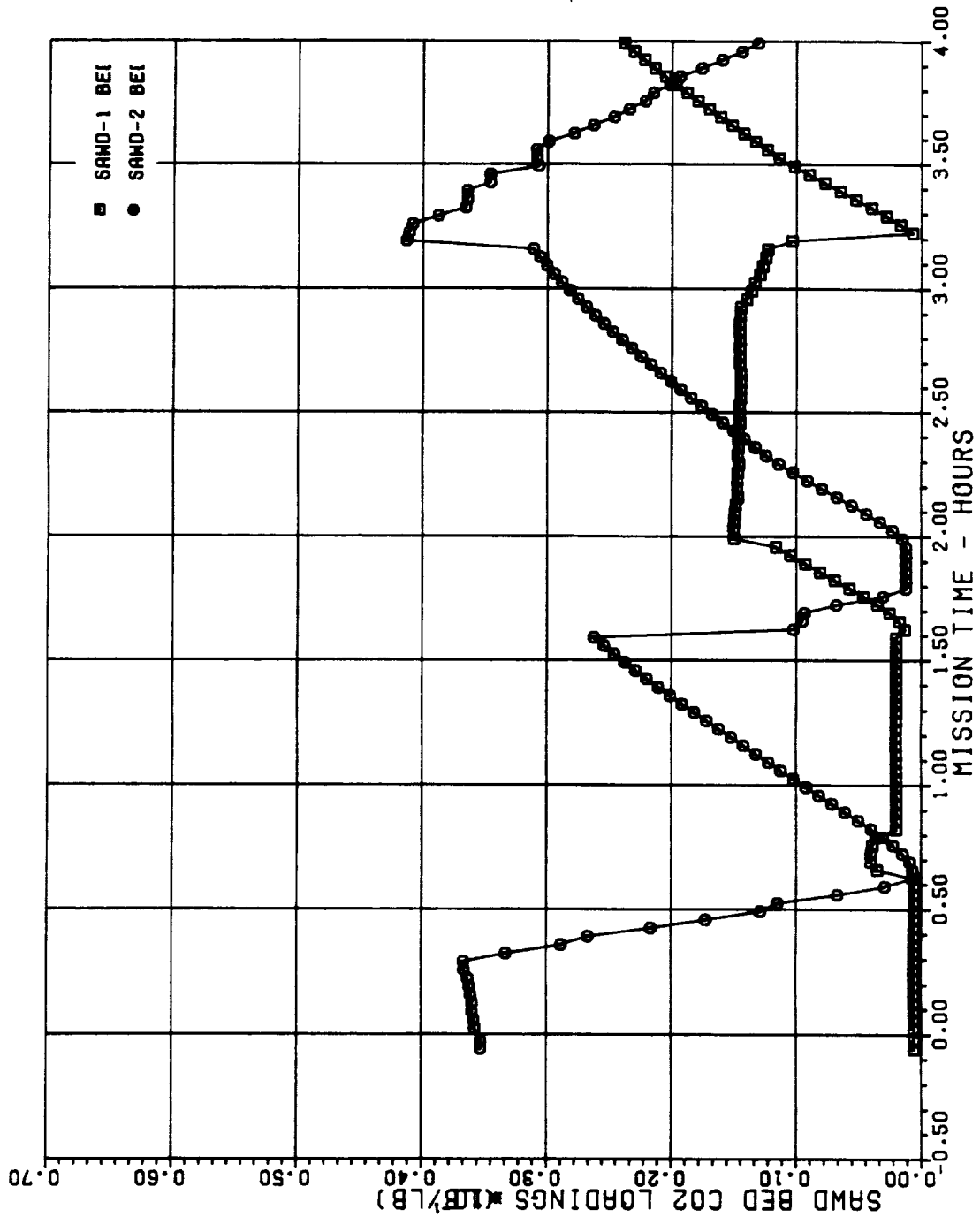




TRANSIENT SIMULATION



TRANSIENT SIMULATION



APPENDIX B

USER'S MANUAL FOR ECLSB MODEL



An extension of the original ESCM program is to develop lightweight simulation models of various life support equipment and to combine them into a system. Unlike the SAWD emulation model, these simulation models are not detailed and principally simulate the output for a given input. The system modelled consists of one air revitalization group and one waste water management group. The major components in the group are:

<u>Function</u>	<u>Subsystem</u>
CO <sub>2</sub> Removal	Electrochemical Depolarized Concentrator
CO <sub>2</sub> Reduction	Sabatier
O <sub>2</sub> Generation	Static Feed Solid Polymer Electrolysis
Trace Gas Removal	Catalytic Oxidizer
Condensate Processing	Multifiltration
Urine Reclamation	Vapor Compression Distillation

The model is called ECLSB and a complete User's Manual [1] for it has been published.



## APPENDIX C

### SPACE STATION MODEL





## C.1 INTRODUCTION

As part of the extension to the ESCM contract, a model of a potential Space Station Air Revitalization System was put together using the G189A [2] computer program. Unlike the ECLSB model described in Appendix B, this model treats only the ARS and does not treat any of the waste water and condensate storage tanks or processing equipment.

The Space Station model includes a habitat, a laboratory, four connecting nodes, and four air revitalization systems. The G189A input data set and the schematic were architected to provide the user with a great deal of flexibility to easily swap subsystems of the same function.

The model was also planned to permit growth whereby hyperbaric chamber loads or loads from additional models could easily be added or various bussing schemes can be explored.

Lastly, an additional plotting capability was added where plots of Space Station simulation transients can be reviewed on the IBM 3179G graphic terminals and/or plotted on the Versatec plotter. The software package used to create these plots is CAETMS [3].

## C.2 DESCRIPTION OF SYSTEM

The system modelled is presented in Figures C-1 through C-14, and they are arranged in a hierarchical manner. Figure C-1 gives the overview of the entire model where rectangular blocks are used to represent groupings of equipment or a specific physical volume. The numbers in the blocks are the component number or groups of numbers which are used by G189A. The letters "P" and "S" denote primary and secondary flow paths in keeping with the G189A scheme for component flow connections [2].

Figure C-2 presents the fan, mixers, and splitters needed to represent the action of the four nodes on the air stream circulating between the habitat and laboratory modules. The nodes may also receive air from other sources like a hyperbaric chamber.

The ARS equipment for the habitat module and the laboratory module is presented in Figures C-3 and C-4. Again, rectangular blocks are used to represent groups of equipment or components. Accordingly, Figures C-5 and C-6 present the components for the cooling packages in the habitat and laboratory modules respectively. The following identifies the remaining figures.:

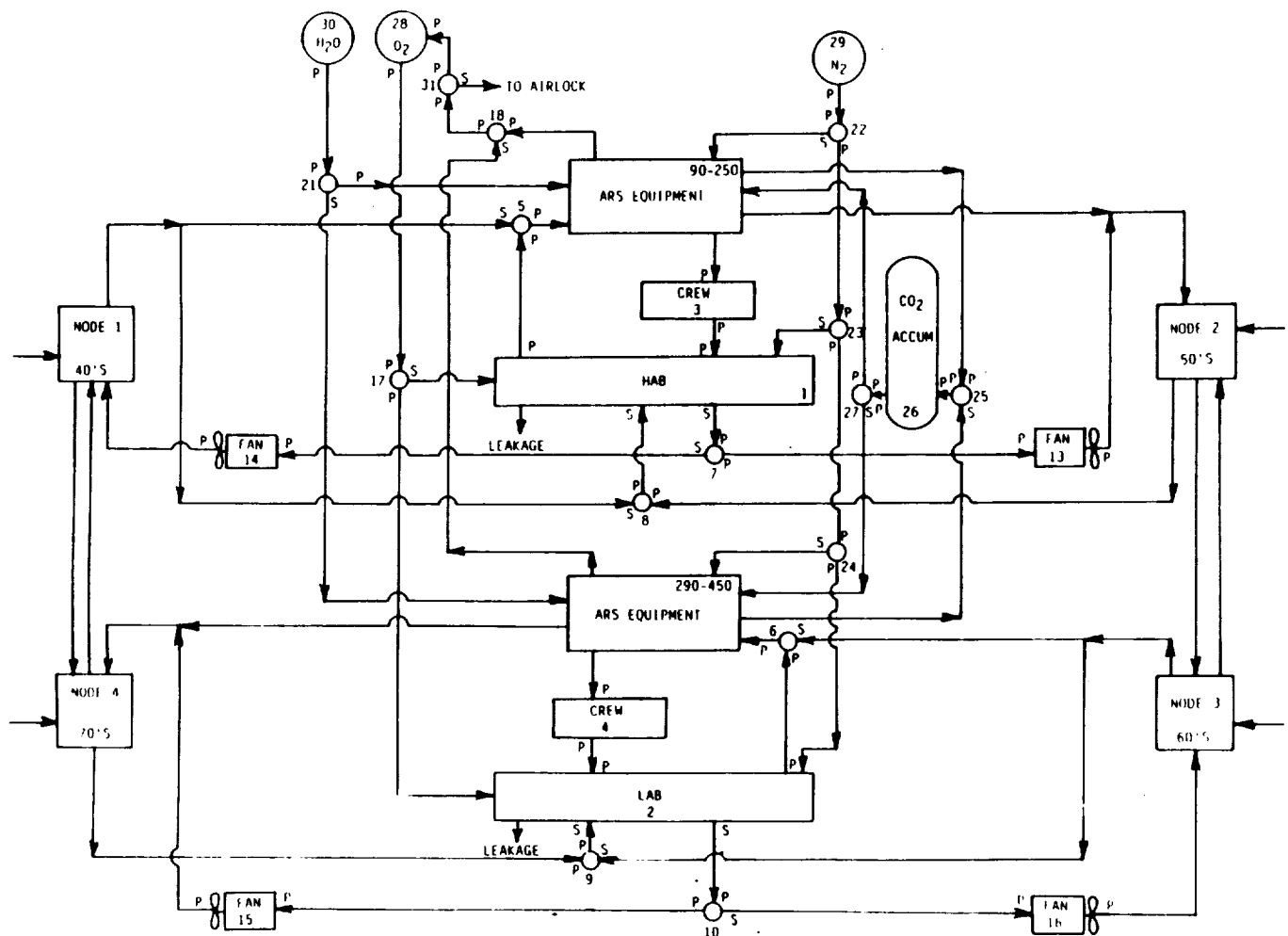


FIGURE C-1  
SPACE STATION MODEL OVERVIEW

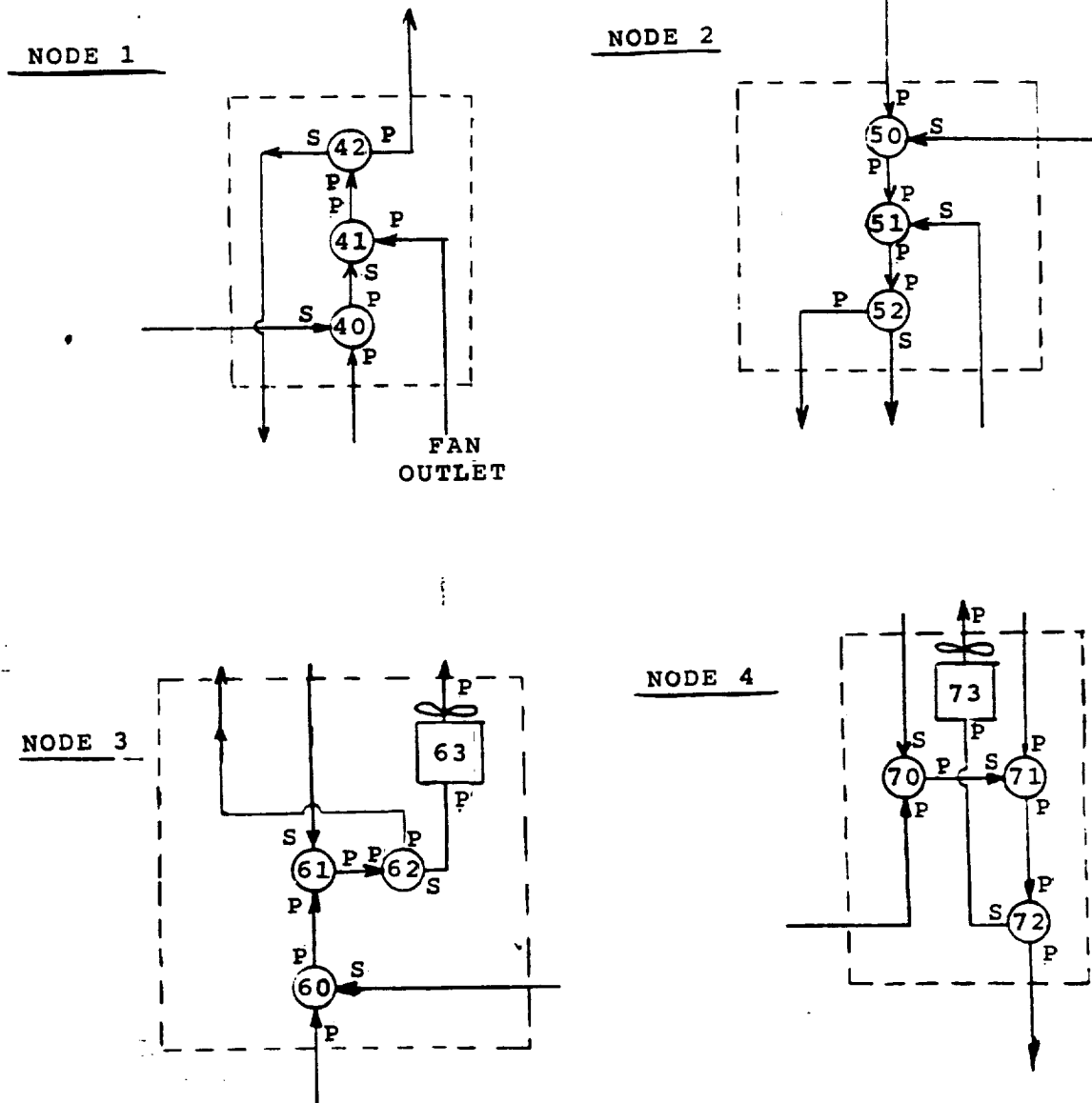


FIGURE C-2  
SPACE STATION NODES

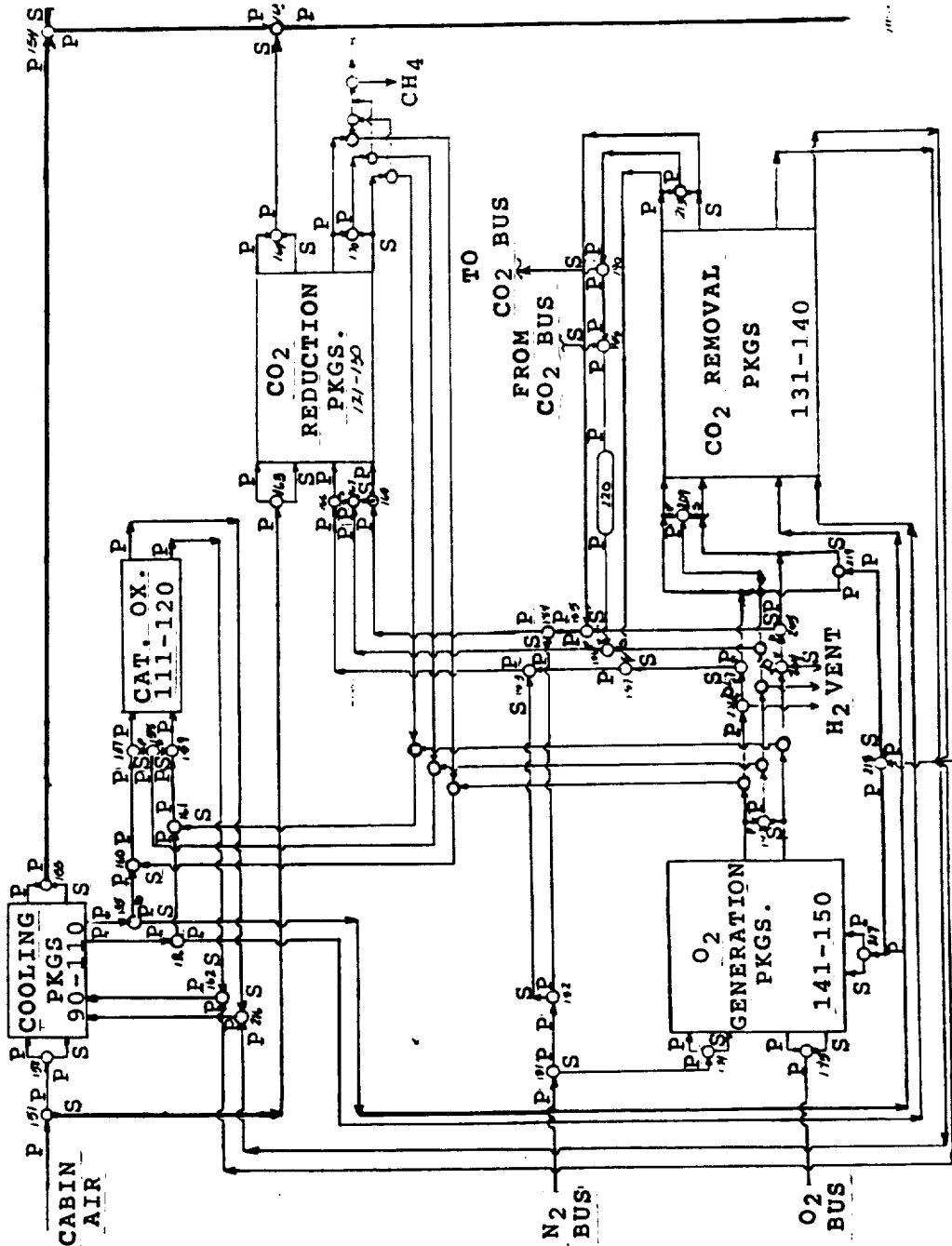


FIGURE C-3  
OVERVIEW OF HABITAT ARS

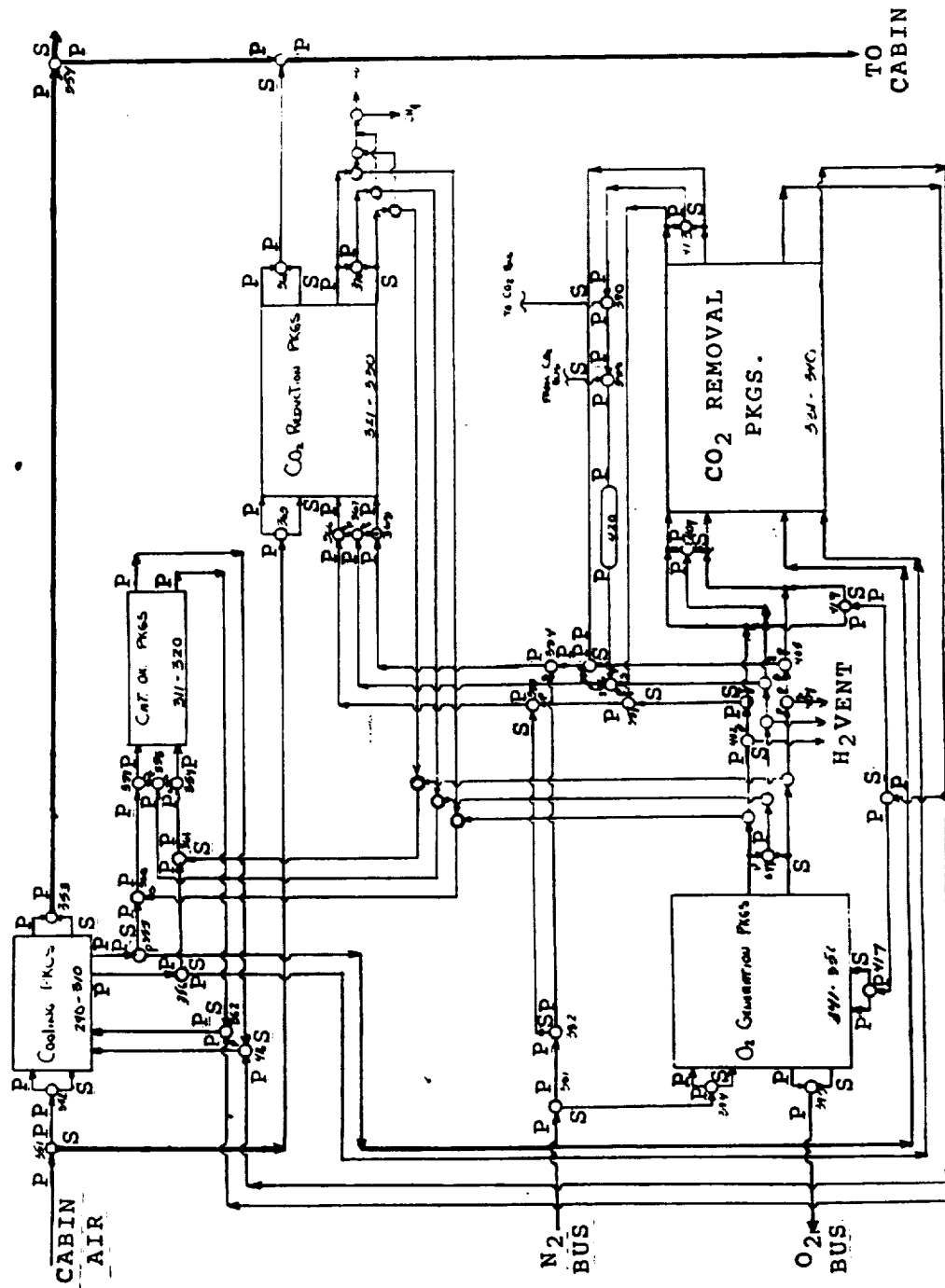


FIGURE C-4  
OVERVIEW OF LABORATORY ARS

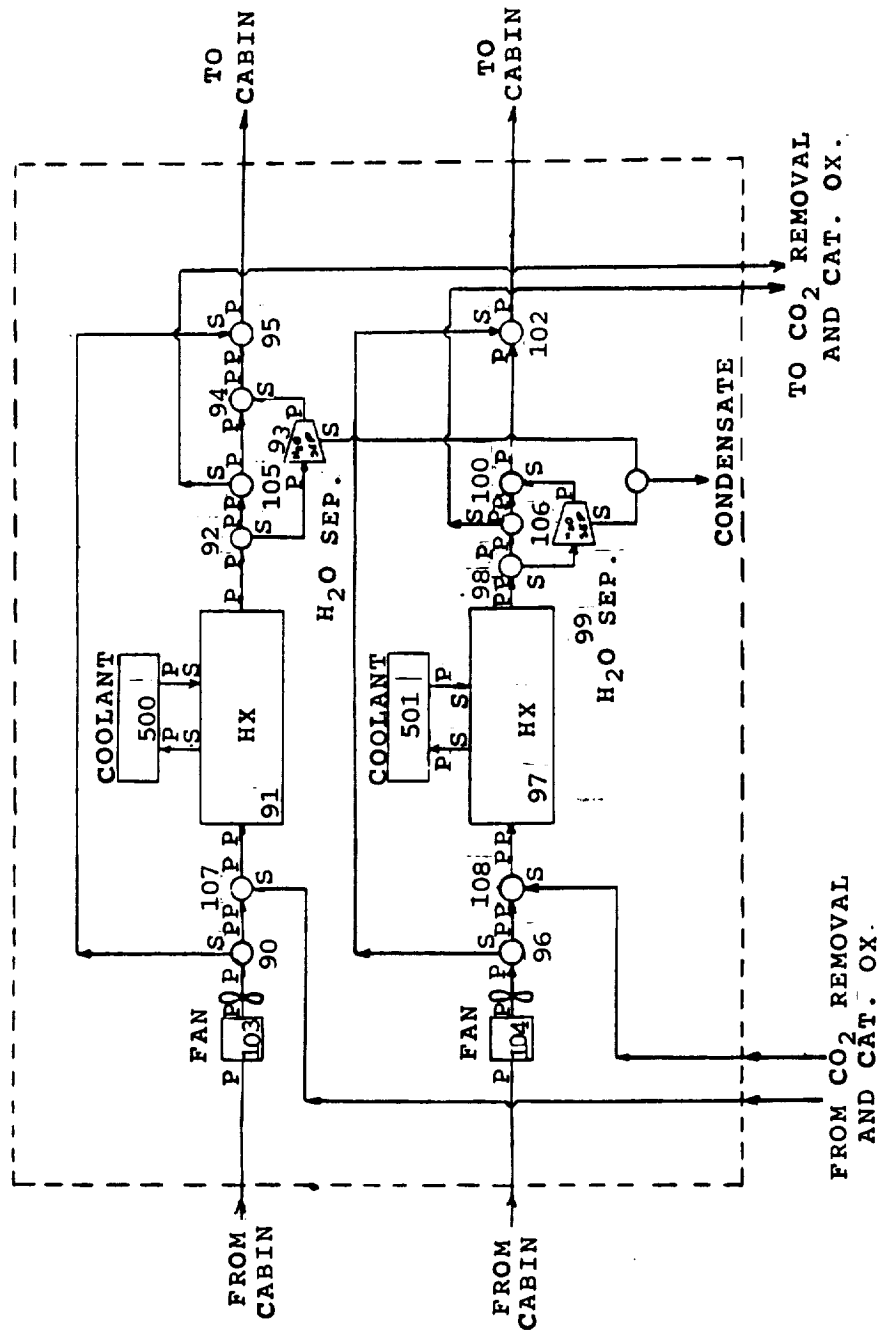


FIGURE C-5  
HABITAT COOLING PACKAGES

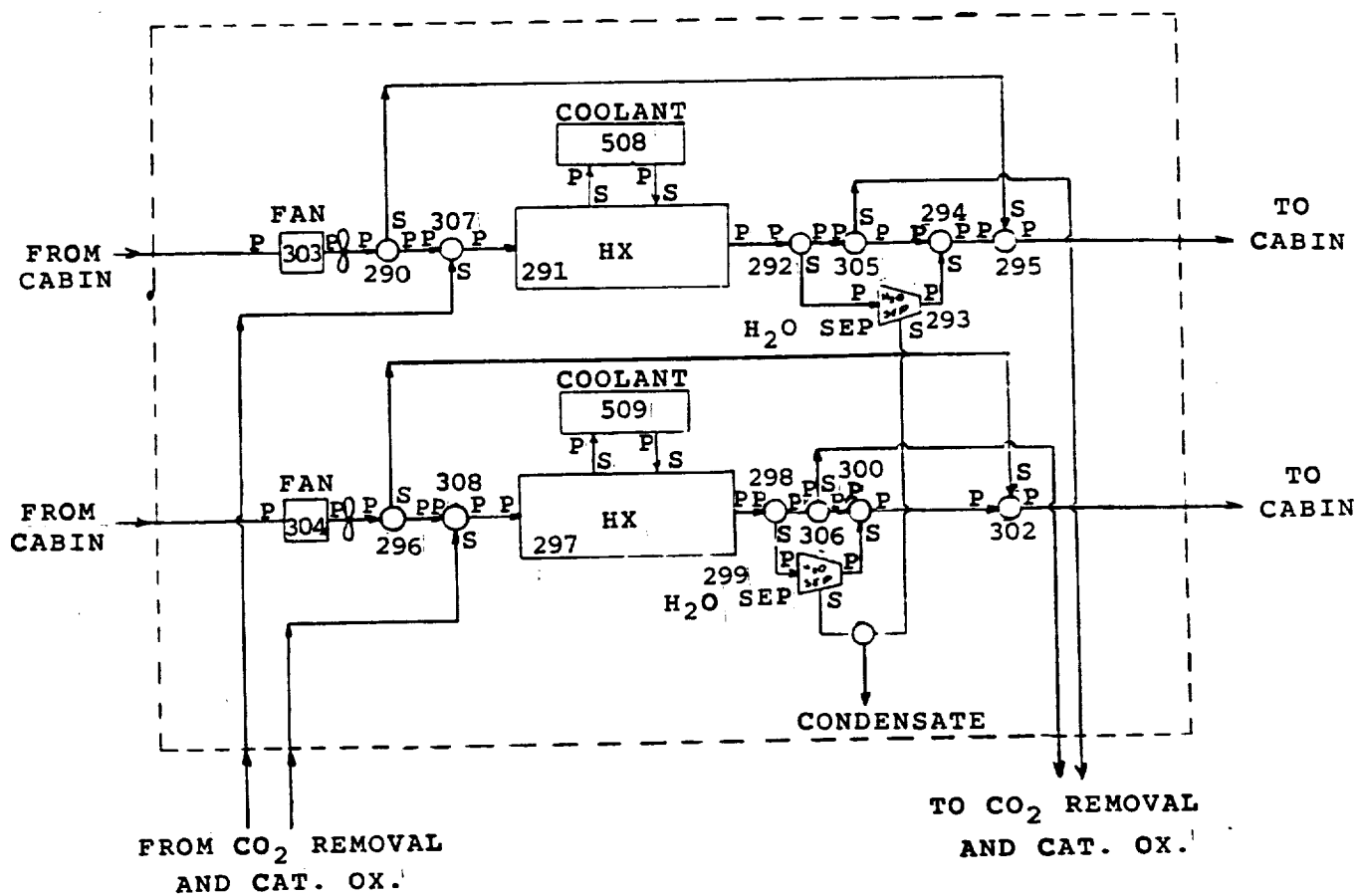


FIGURE C-6  
LABORATORY COOLING PACKAGES



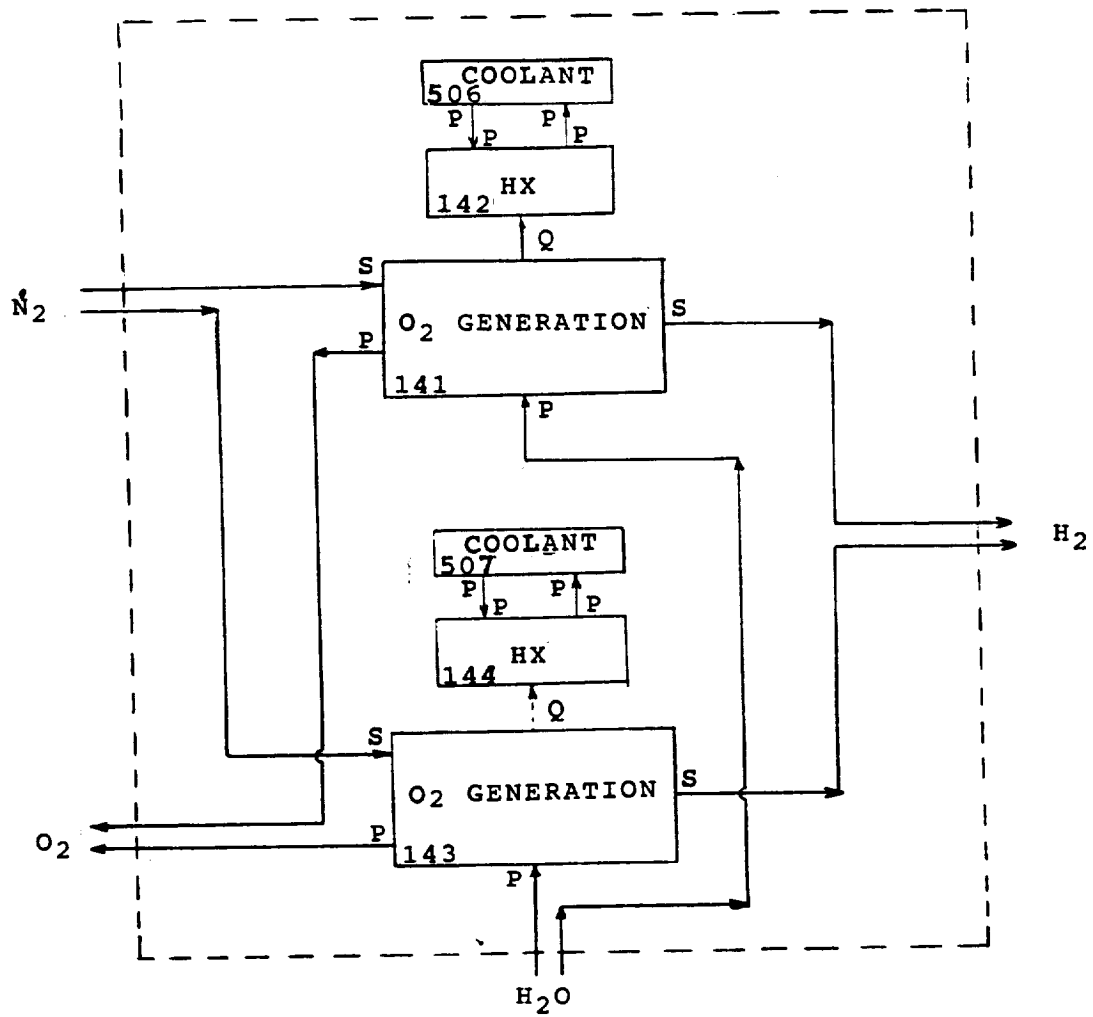


FIGURE C-7  
HABITAT OXYGEN GENERATORS

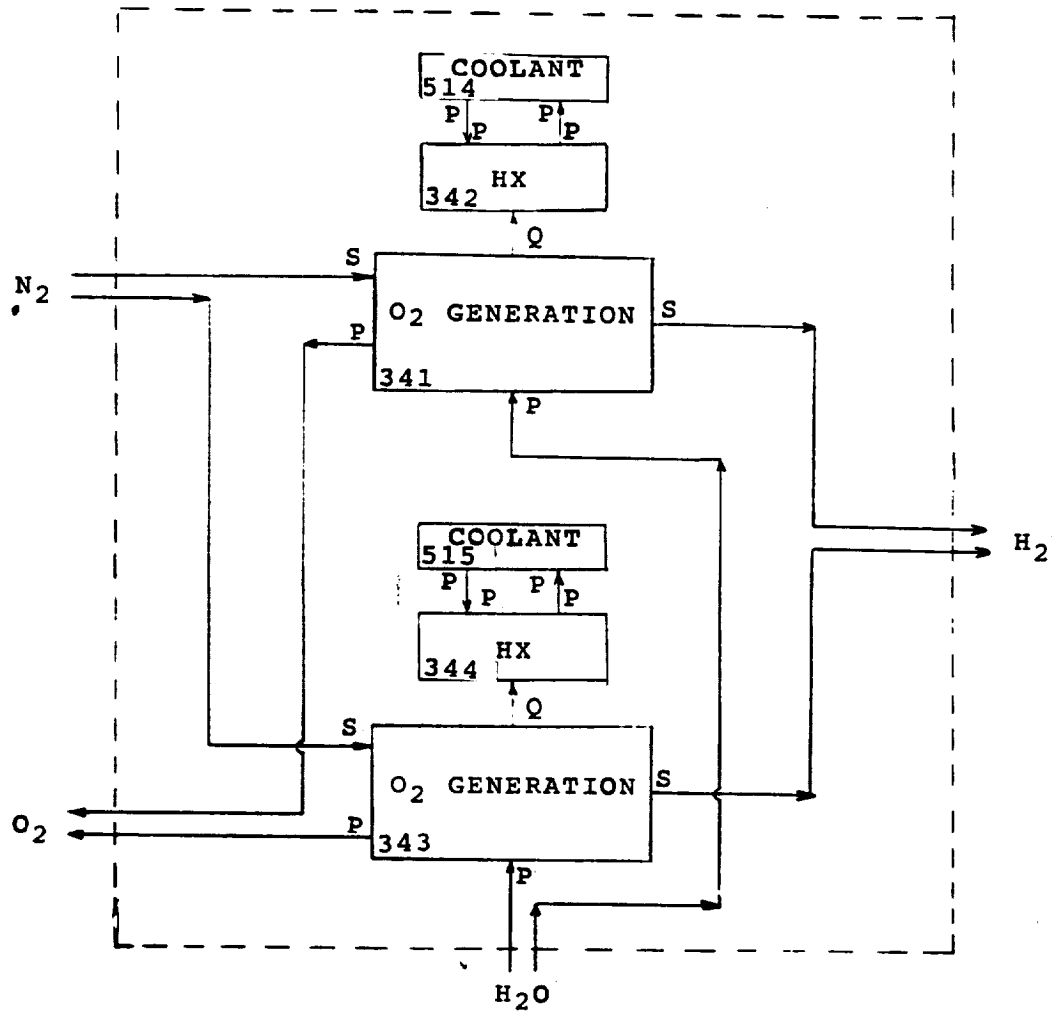


FIGURE C-8  
LABORATORY OXYGEN GENERATORS

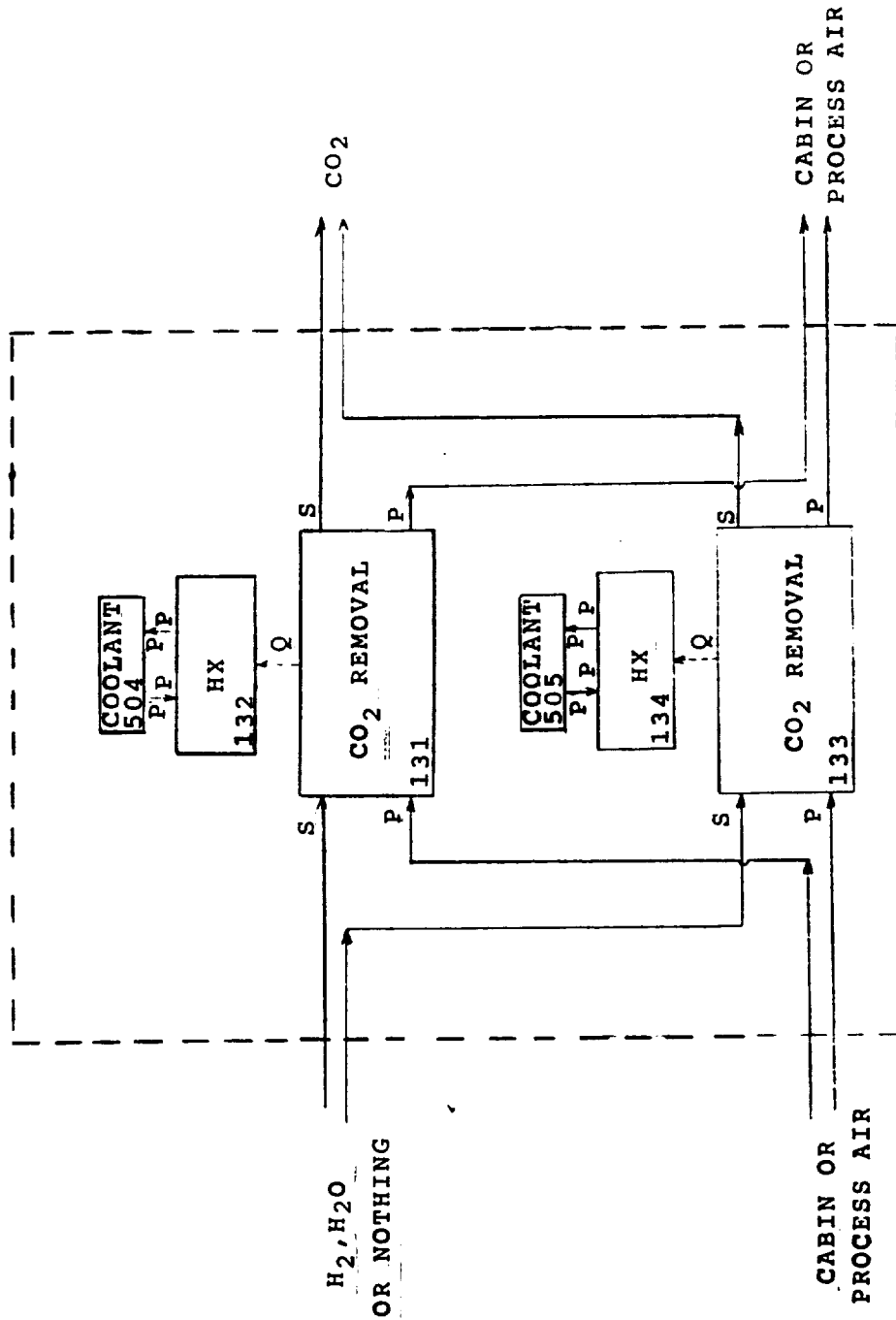


FIGURE C-9  
HABITAT CO<sub>2</sub> REMOVAL UNITS

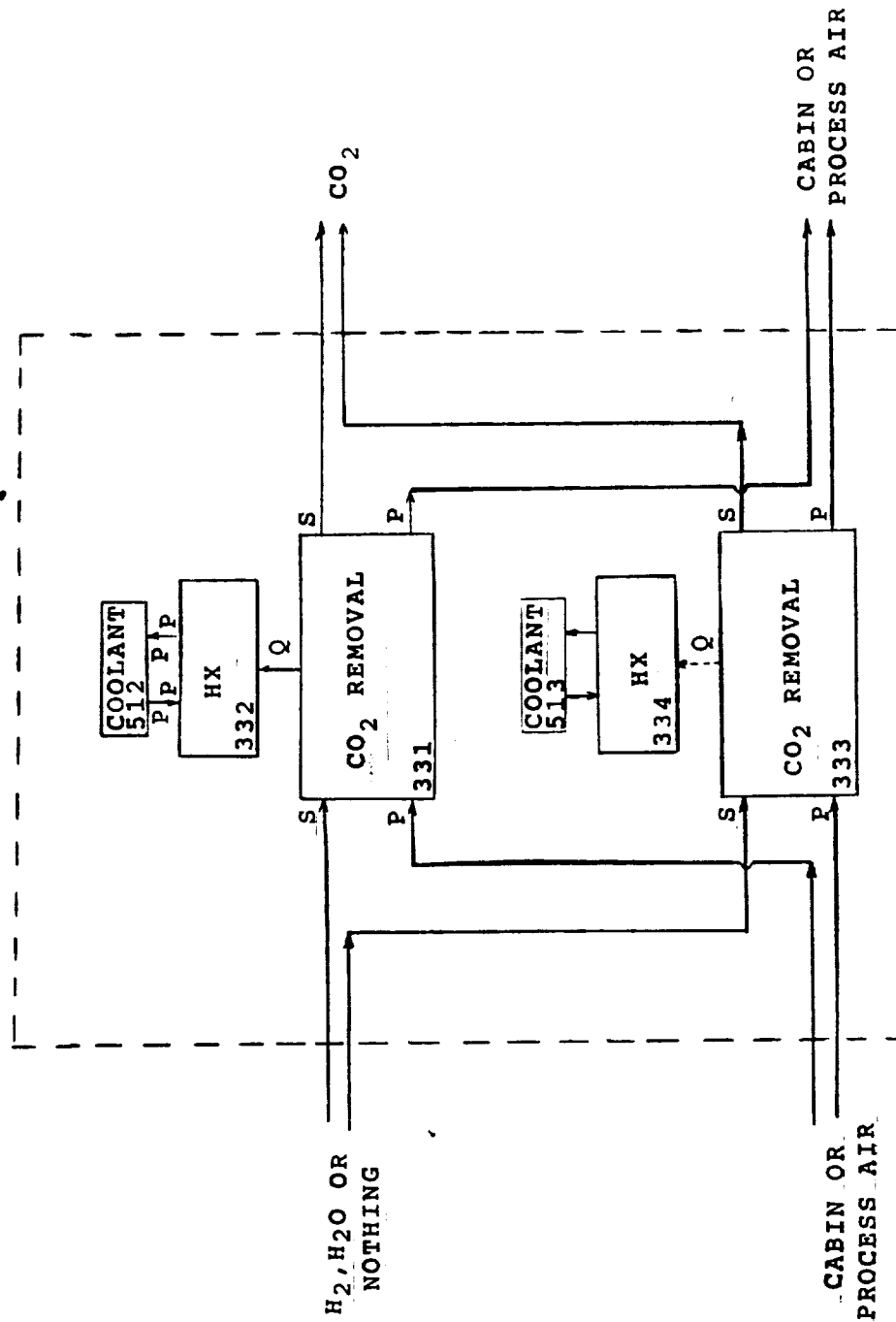


FIGURE C-10  
LABORATORY CO<sub>2</sub> REMOVAL UNITS

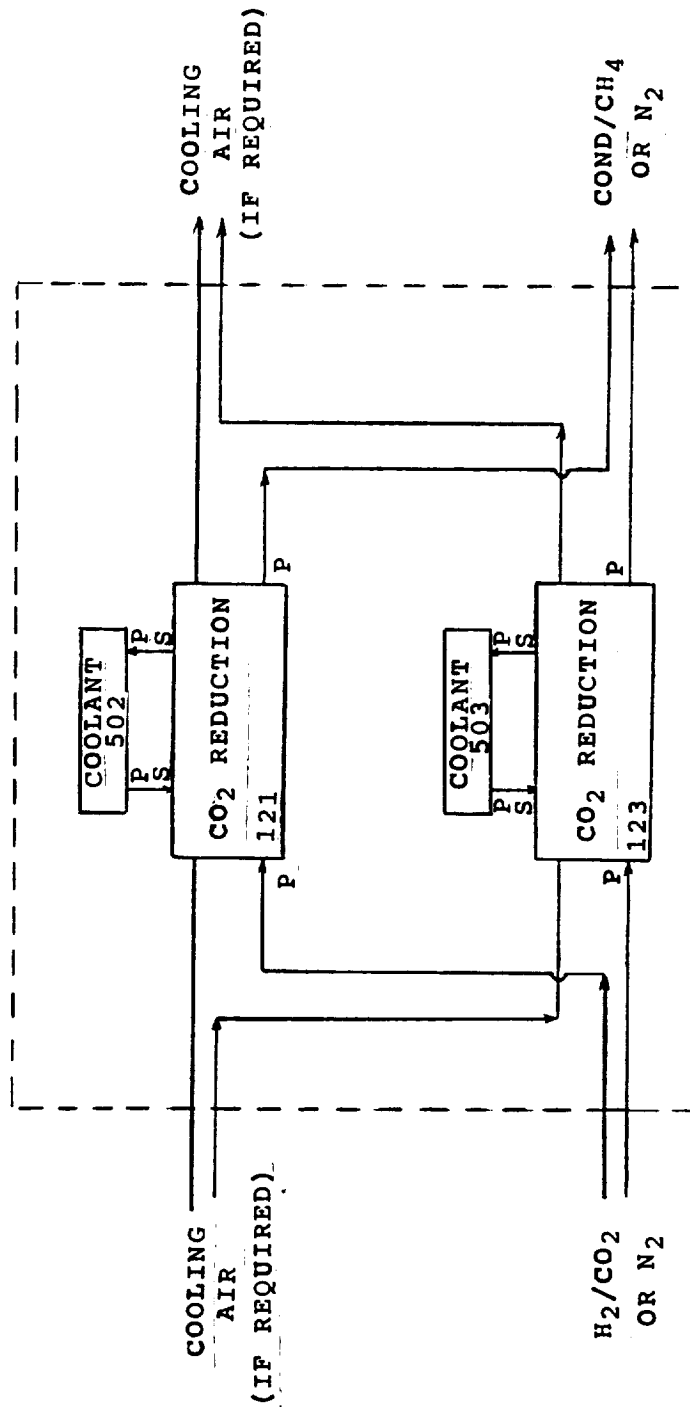


FIGURE C-11  
HABITAT CO<sub>2</sub> REDUCTION UNITS

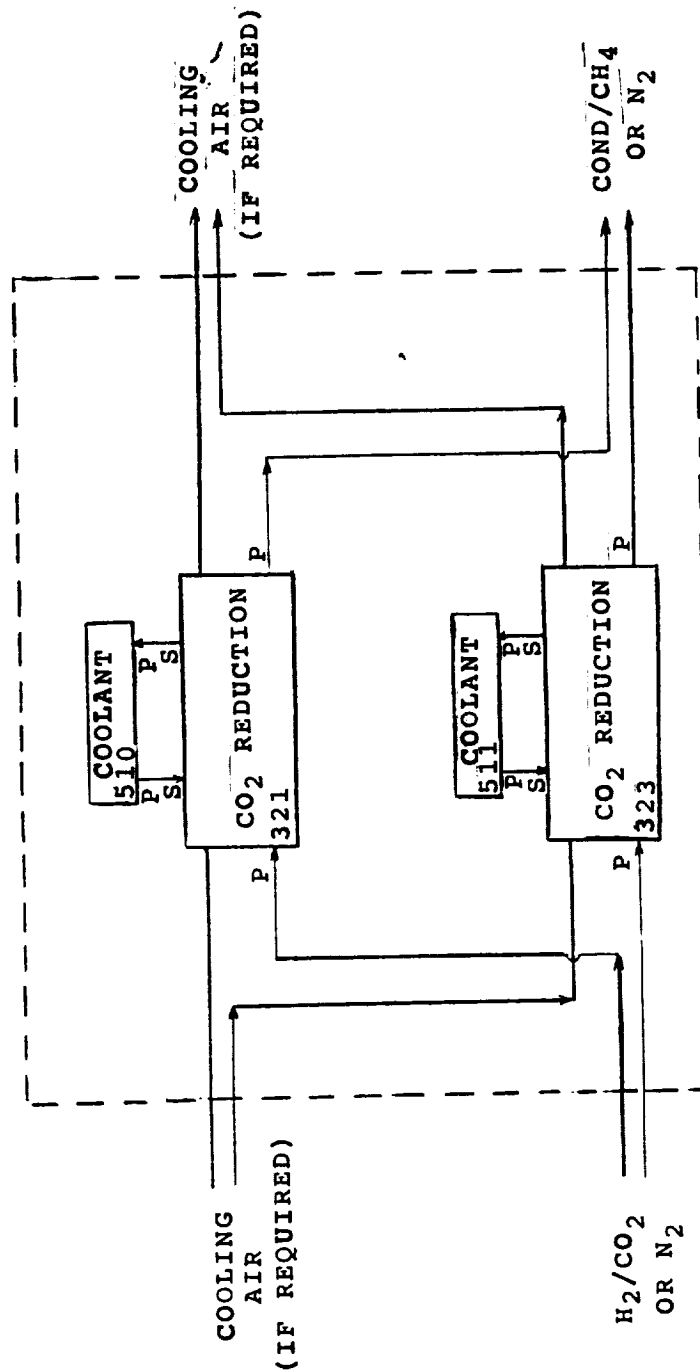


FIGURE C-12  
LABORATORY CO<sub>2</sub> REDUCTION UNITS

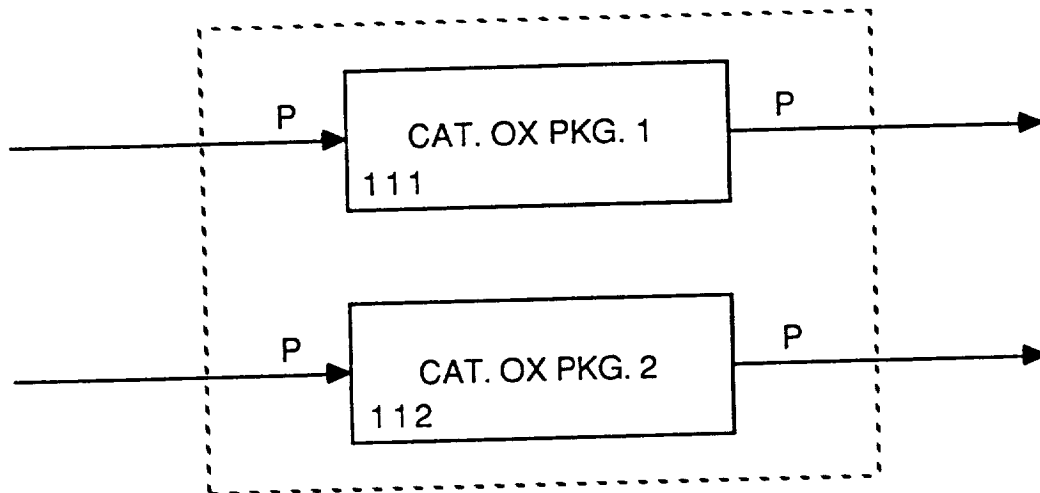


FIGURE C-13  
HABITAT CATALYTIC OXYDIZERS

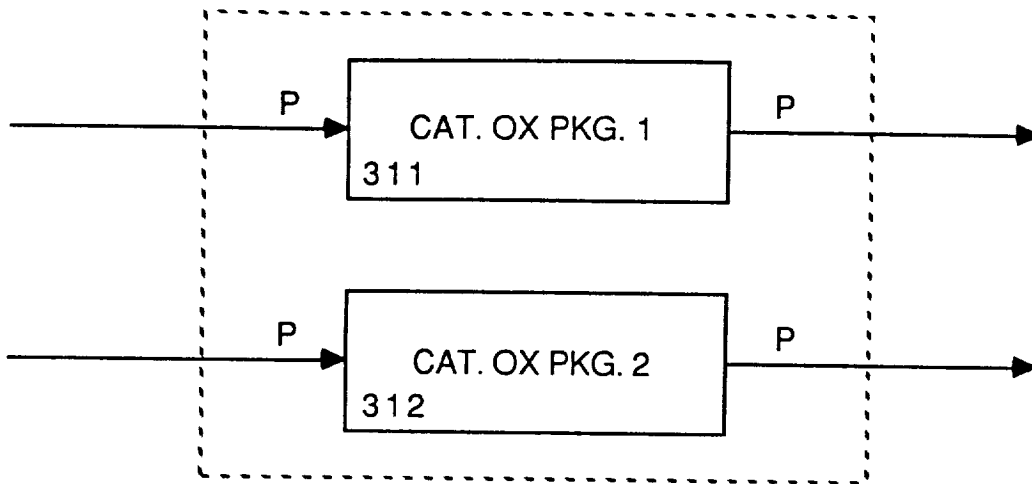


FIGURE C-14  
LABORATORY CATALYTIC OXYDIZERS



C.2 DESCRIPTION OF SYSTEM (Continued)

<u>Package</u>	<u>Habitat</u>	<u>Laboratory</u>
Oxygen Generator	C-7	C-8
CO <sub>2</sub> Removal	C-9	C-10
CO <sub>2</sub> Reduction	C-11	C-12
Catalytic Oxidizer	C-13	C-14

The following sections discuss the operation of the system.

C.2.1 Overall Operation

The air stream circulates through both habitats and the four nodes. First, the air leaves the habitat and splits to each of nodes 1 and 2. Inside these nodes, air from the habitat mixes with air from the corresponding laboratory nodes. This mixed air then splits and flows back to the habitat and back to the corresponding laboratory node.

Air is also drawn from the habitat and laboratory modules by ARS equipment. The ARS equipment provides air cooling, humidity removal, CO<sub>2</sub> removal, oxygen generation, and trace gas removal. Any oxygen generated goes into an oxygen bus which contains an oxygen storage tank. Oxygen generation equipment is supplied water from a water supply tank. At present, carbon dioxide removed by

### C.2.1 Overall Operation (Continued)

each CO<sub>2</sub> removal unit is stored in each unit's own CO<sub>2</sub> accumulator. The architecture exists for possible CO<sub>2</sub> bussing concepts; however, these concepts have not been explored and validated on the model. In addition, the architecture exists for a nitrogen bus for equipment purging. This architecture can be used at a future date when equipment models are developed further to simulate the effects of nitrogen purging and the need arises to explore these effects.

Air from the equipment is then altered by crew additions of CO<sub>2</sub> and water vapor and by subtraction of oxygen before returning to the habitat and laboratory modules.

### C.2.2 ARS Equipment Operation

Figures C-3 and C-4 show the arrangement of ARS equipment packages for the model. As shown in Figures C-5 through C-14, two units are available in each of the packages represented by a rectangle in Figures C-3 and C-4. Therefore, in the habitat, two oxygen generator units exist; and in the laboratory, two oxygen generator units exist. This gives a total of four in the modeled Space Station. The same is true for the condensing heat exchangers, CO<sub>2</sub> removal units, CO<sub>2</sub> reduction units, and the catalytic oxidizer units.

### C.2.2      ARS Equipment Operation (Continued)

The model is configured presently to have each group of ARS equipment operate independently of the other; a group of equipment is defined as a condensing heat exchanger, an oxygen generator, a CO<sub>2</sub> removal unit, a CO<sub>2</sub> reduction unit, and a catalytic oxidizer. The architecture of the model is constructed to permit exploration of different plumbing configurations and bussing arrangements at a later date.

Water is drawn into the oxygen generator where oxygen and hydrogen are produced. The oxygen flows to an oxygen bus while the hydrogen flows to a CO<sub>2</sub> reduction unit, and if needed to a CO<sub>2</sub> removal unit. An EDC CO<sub>2</sub> removal unit requires hydrogen for operation, while a SAWD or molecular sieve do not. Air from the cooling package flows through the CO<sub>2</sub> removal package where CO<sub>2</sub> is removed from the air and then sent to mix with hydrogen before entering a CO<sub>2</sub> reduction package. The air now with little CO<sub>2</sub> returns to the cooling package.

The CO<sub>2</sub> and the hydrogen flow to the CO<sub>2</sub> reduction package where the CO<sub>2</sub> is reduced to a solid or gas depending upon the reduction process.

### C.2.2      ARS Equipment Operation (Continued)

Air from the cooling package also flows to the catalytic oxidizers where trace gases are burned. The air then returns back to the inlet of the cooling package.

### C.3        Description Of Computer Program

A description of G189A is contained in the original User's Manual [1]. The subroutines newly written for this Space Station Model are described here. These new subroutines are:

GPOLY1	=	Control Logic
GPOLY2	=	Control Logic
ARSS	=	Tabular and Graphical Output
CNDHEX	=	Condensing Heat Exchanger
BOSCHS	=	Bosch CO <sub>2</sub> Reduction
MOLSIV	=	Molecular Sieve CO <sub>2</sub> Removal
KOHHS	=	Static Feed Water Vapor Electrolysis O <sub>2</sub> Generation

FORTTRAN 77 is used extensively in these newly written routines.

**C.3.1**      GPOLY1 Subroutine

GPOLY1 simulates the control of functions required for operating the Space Station model. Since FORTRAN 77 is used, the standard construct changes from that described in the original manual. Essentially, the construct divides the subroutine into the various control functions for the equipment. The construct is:

```
IF    ( N .EQ. 3 ) THEN  
      .  
      . .  
      .  
      .  
END IF
```

The following are input once at the first execution of GPOLY1; these are various options to be selected by the user:

```
KK(80,16) = Process Air Bus?  1 = Yes, 0 = No  
KK(80,17) = CO2 Gas Bus?  0 = None, 1 = Intramod, 2 = Intermod  
KK(80,19) = N2 Gas Bus?  1 = Yes, 0 = No  
KK(80,19) = H2 Gas Bus?  0 = None, 1 = Intramod  
KK(80,20) = Habitat O2 Gen #1 On?  1 = Yes, 0 = No  
KK(80,21) = Habitat CO2 Removal #1 On?  1 = Yes, 0 = No
```

C.3.1 GPOLY1 Subroutine (Continued)

KK(80,22) = Habitat CO<sub>2</sub> Reduction #1 On? 1 = Yes, 0 = No  
KK(80,23) = Habitat Cat. Ox. #1 On? 1 = Yes, 0 = No  
KK(80,24) = Habitat O<sub>2</sub> Gen. #2 On? 1 = Yes, 0 = No  
KK(80,25) = Habitat CO<sub>2</sub> Removal #2 On? 1 = Yes, 0 = No  
KK(80,26) = Habitat CO<sub>2</sub> Reduction #2 On? 1 = Yes, 0 = No  
KK(80,27) = Habitat Cat. Ox. #2 On? 1 = Yes, 0 = No  
KK(80,28) = Laboratory O<sub>2</sub> Gen. #1 On? 1 = Yes, 0 = No  
KK(80,29) = Laboratory CO<sub>2</sub> Removal #1 On? 1 = Yes, 0 = No  
KK(80,30) = Laboratory CO<sub>2</sub> Reduction #1 On? 1 = Yes, 0 = No  
KK(80,31) = Laboratory Cat. Ox. #1 On? 1 = Yes, 0 = No  
KK(80,32) = Laboratory O<sub>2</sub> Gen. #2 On? 1 = Yes, 0 = No  
KK(80,33) = Laboratory CO<sub>2</sub> Removal #2 On? 1 = Yes, 0 = No  
KK(80,34) = Laboratory CO<sub>2</sub> Reduction #2 On? 1 = Yes, 0 = No  
KK(80,35) = Laboratory Cat. Ox. #2 On? 1 = Yes, 0 = No

These are then used to set up the proper solution path, the fluid flow fractions for splitters, and to make any adjustments in component to component flow connections.

C.3.1 GPOLY1 Subroutine (Continued)

Printoff frequency, habitat and laboratory air conditions, and fan flows are input once at the first execution:

WV(80,55) = Printoff frequency, time steps per printoff  
WV(80,66) = Habitat gas mixture initial temperature, °F  
WV(80,67) = Habitat total pressure, pin  
WV(80,68) = Habitat CO<sub>2</sub> partial pressure, mm Hg  
WV(80,69) = Habitat dew point temperature, °F  
WV(80,70) = Habitat O<sub>2</sub> partial pressure, psia  
WV(80,71) = Laboratory gas mixture initial temperature, °F  
WV(80,72) = Laboratory total pressure, psia  
WV(80,73) = Laboratory CO<sub>2</sub> partial pressure, mm Hg  
WV(80,74) = Laboratory dew point temperature, °F  
WV(80,75) = Laboratory O<sub>2</sub> partial pressure, psia  
  
WV(13,76) = Nodal mixer fan flow, cfm  
WV(103,76) = Cooling package fan flow, cfm

After all these values are input and various initializations done, total pressure and oxygen partial pressure control laws are executed for the habitat and the laboratory. The following are input and output from the habitat (component number 1):

C.3.1 GPOLY1 Subroutine (Continued)Input

R(4) = Habitat total pressure, psia

R(94) = Present oxygen partial pressure, psia

Output

R(165) = Oxygen flow required into habitat, lbm/hr

R(166) = Nitrogen flow required into habitat, lbm/hr

The analogous variables are used for the component number 2 laboratory.

Following oxygen partial pressure and total pressure control is the calculation of crew metabolic loads. The following are input and output from the crew represented as component number 3:

Input

TIME = Elapsed time of simulation, sec.

VV(1,104) = Habitat temperature, °F



C.3.1 GPOLY1 Subroutine (Continued)Output

R(66) = Sensible load per man, Btu/Hr

R(67) = Latent heat load generated per man, Btu/Hr

R(82) = Total metabolic heat generated per man, Btu/Hr

The analogous variables are used for the other crew which is represented by component number 4.

Control of oxygen generation units is performed next. The four units are represented as components 141, 143, 341, and 343. The first two components are in the habitat while the three hundred series components are in the laboratory. The following are input and output from the oxygen generation control logic represented by component number 141.

Input

GENH1 = Habitat O<sub>2</sub> Gen. #1 On? 1 = Yes, 0 = No

R(72) = Nominal design SPE electrolysis current, amps

W(28,72) = Pressure in the oxygen bus accumulator, psia

Output

R(69) = Actual current applied to SPE unit, amps

C.3.1      GPOLY1 Subroutine (Continued)

The condensing heat exchangers in the cooling package are followed by water separators. To model the action of the separator in its removal of entrained liquid water, GPOLY logic is employed. The following are input and output for the water separator components represented by components 93, 99, 293 and 299:

Input

A(7)      =   Entrained liquid entering water separator, lbm/hr  
DTIME    =   Simulation time step, seconds  
R(68)    =   Cumulative water removed by separator, lbm  
A(1)      =   Total mass flow into separator, lbm/hr  
A(5)      =   Total dry mass flow into separator, lbm/hr  
A(6)      =   Specific heat at dry mass, flow into separator,  
                 Btu/lbm-F  
CPCONV   =   Specific heat of water vapor, Btu/lbm-F

Output

A(7)      =   New entrained liquid entering water separator, lbm-hr  
A(1)      =   New total flow entering separator, lbm/hr  
CPA      =   New specific heat of flow entering separator, Btu/lbm-F  
R(67)    =   Flow of liquid water leaving separator, lbm/hr  
R(68)    =   New cumulative water removed by separator, lbm

C.3.1 GPOLY1 Subroutine (Continued)

Temperature of the habitat and laboratory is effected by regulating the bypass flow of air around the condensing heat exchangers. The following are input and output for the component number 90 splitter upstream of the component number 91 condensing heat exchanger:

Input

WV(1,104) = Habitat temperature, °F  
WV(1,87) = Habitat setpoint temperature, °F  
DTIME = Simulation time step, seconds

Output

R(65) = fraction of flow bypassing the heat exchanger

Following some mass balance updates for G189A is a calculation of the water flow consumed by electrolysis and the flow split of water to be divided between the habitat and laboratory oxygen generator units. The following are input and output:

C.3.1 GPOLY1 Subroutine (Continued)Input

WV(141,67) = Habitat SPE unit #1 water demand, pph  
WV(143,67) = Habitat SPE unit #2 water demand, pph  
WV(341,67) = Laboratory SPE unit #1 water demand, pph  
WV(343,67) = Laboratory SPE unit #2 water demand, pph  
DTIME = Simulation time step, seconds  
WV(30,67) = Water consumed by SPEs to date, lbm

Output

WV(30,67) = New water consumed by SPEs, lbm

Next, the control of CO<sub>2</sub> out of the accumulator to feed the CO<sub>2</sub> reduction unit is done. The amount of flow is updated every molecular sieve cycle.

Input

WV(135,72) = Pressure in accumulator tank, psia  
WV(1,104) = Habitat temperature, °F  
WV(131,65) = Molecular sieve half cycle time, minute  
TIME = Elapsed time of simulation, seconds  
WV(131,87) = CO<sub>2</sub> removal rate by molecular sieve, pph  
DTIME = Simulation time step, seconds

C.3.1 GPOLY1 Subroutine (Continued)Output

R(1) = Flow out of accumulator, pph

Analogous variables are used for the other CO<sub>2</sub> accumulators and removal units.

Hydrogen vent control is accomplished by the use of flow splitter components 202 and 204 for the habitat and 402 and 404 for the laboratory. The following are the input and output:

Input

WV(135,72) = Habitat CO<sub>2</sub> removal unit #1 accumulator pressure, psia

RATE1 = Flow out of accumulator to reduction unit, lbm/hr

A(1) = Flow into splitter, lbm/hr

Output

R(65) = Fraction of input H<sub>2</sub> flow to be vented

Lastly, the flow out of the oxygen accumulator component 28 and the flow of oxygen to the habitat and laboratory are computed. For the component 28 oxygen accumulator.

C.3.1 GPOLY1 Subroutine (Continued)Input

WV(1,104) = Habitat temperature, F

WV(1,165) = Oxygen addition rate required by habitat, lbm/hr

WV(2,165) = Oxygen addition rate required by laboratory, lbm/hr

Output

R(70) = Temperature of oxygen in tank, F

R(1) = Flow out of oxygen tank, lbm/hr

The flow split to the habitat and laboratory is represented by  
component 17:

Input

WV(1,165) = Oxygen addition rate required by habitat, lbm/hr

WV(2,165) = Oxygen addition rate required by laboratory, lbm/hr

Output

R(65) = Function of inlet flow to laboratory.

**C.3.2**      GPOLY2 Subroutine

GPOLY2 computes the mass additions to the habitat that arise from components in the primary and secondary flow streams. These additions are then input into the habitat through the R array. This is done because of the manner in which the out flow is computed for the habitat in G189A [2]. Essentially, the exit flow is set equal to the inlet flow. The mass changes only due to mass additions. The following are input and output for the component number 3 crew who are in the habitat.

Input

R(70)            = Water added by crew, lbm/hr

WV(131,88)    = Water removal rate of Co2 removal unit #1 in habitat,  
                  lbm/hr

WV(133,88)    = Water removal rate of Co2 removal unit #2 in habitat,  
                  lbm/hr

WV(93,67)     = Water removed by unit #1 condensing Hx, lbm/hr

WV(99,67)     = Water removed by unit #2 condensing Hx, lbm/hr

WV(1,25)       = Water leaving habitat to nodes, lbm/hr

WV(8,6)        = Water returning to habitat from nodes, lbm/hr

R(68)           = Oxygen removed by crew, lbm/hr



C.3.2      GPOLY2 Subroutine    (Continued)

VV(1,29)    =   Oxygen leaving habitat to nodes, lbm/hr  
VV(8,10)    =   Oxygen returning to habitat from nodes, lbm/hr  
R(69)       =   CO<sub>2</sub> generated by crew lbm/hr  
VV(133,87) =   CO<sub>2</sub> removed by molecular sieve unit #2, lbm/hr  
VV(1,31)    =   CO<sub>2</sub> leaving habitat to nodes, lbm/hr  
VV(8,12)    =   CO<sub>2</sub> returning to habitat from nodes, lbm/hr

Output

VV(1,137)   =   Water addition rate to habitat, lbm/hr  
VV(1,175)   =   Oxygen addition rate to habitat, lbm/hr  
VV(1,177)   =   CO<sub>2</sub> addition rate to habitat, lbm/hr

Analogous variables are used for the laboratory module.

C.3.3      ARSS Subroutine

ARSS is the subroutine which prints the output of the Space Station model and which generates a plot file for use by CAETMS [3] for generation of plots. As no significant calculations are performed in ARSS, the input and output variables are virtually identical. A complete description of the output is presented in Section C.4.





C.3.4      Component Subroutines

Models were generated for the following components:

KOHHS    =   Static feed water vapor electrolysis (KOH)

MOLSIV   =   Molecular sieve CO<sub>2</sub> removal

BOSCHS   =   Bosch CO<sub>2</sub> reduction

CNDHEX   =   Condensing heat exchanger

Tables C-1 through C-4 contain a listing of these programs and provide their documentation as well as a listing of their input and output.

TABLE C-1

## LISTING OF KOHHS

## SUBROUTINE KOHHS

```

C
C THIS SUBROUTINE MODELS A KOH ELECTROLYSIS MODULE MADE UP
C OF A NUMBER OF CELLS. FEEDWATER IS CONVERTED INTO HYDROGEN
C AND OXYGEN. PRODUCTION DEPENDS ON ELECTRICAL CURRENT APPLIED,
C EFFECTIVE AREA PER CELL, NUMBER OF CELLS, AND EFFICIENCIES.
C THE UNIT MAY BE COOLED BY GAS OR LIQUID FLOW.
C
C INPUTS:
C
C K(16) - TABLE NUMBER FOR CELL OVERALL EFFICIENCY
C K(17) - ALICOM NUMBER FOR LIQUID COOLING
C K(18) - TABLE NUMBER FOR UA TO ALICOM
C R(52) - EFFECTIVE SUMMED CONDUCTANCE (BTU/HR-F)
C R(54) - AMBIENT GAS TEMPERATURE (F)
C R(55) - AMBIENT GAS TO INSULATION UA (BTU/HR-F)
C R(57) - AMBIENT WALL TEMPERATURE (F)
C R(58) - AMBIENT WALL TO INSULATION SURFACE FA (1/SQ.FT.)
C R(60) - STRUCTURE TEMPERATURE (F)
C R(61) - CELL TO STRUCTURE UA (BTU/HR-F)
C R(64) - INSULATION SURFACE TO CELL UA (BTU/HR-F)
C R(66) - CELL POWER EFFICIENCY (%), IF CONSTANT
C R(67) - VALUE OF 1ST INDEP. VARIABLE FOR EFFICIENCY INTERPOL.
C R(68) - VALUE OF 2ND INDEP. VARIABLE FOR EFFICIENCY INTERPOL.
C R(69) - CURRENT (AMPS)
C R(70) - DELIVERY PRESSURE (PSIA)
C R(71) - CELL TEMPERATURE (F), FIRST GUESS
C R(78) - KOH CONCENTRATION (WEIGHT %)
C R(74) - UA BETWEEN CELL AND LIQUID COOLANT (BTU/HR-F)
C R(75) - VALUE OF 1ST INDEP. VARIABLE FOR UA INTERPOL.
C R(76) - VALUE OF 2ND INDEP. VARIABLE FOR UA INTERPOL.
C R(81) - TRIAL AND ERROR CONVERGENCE TOLERANCE (%)
C R(82) - PRODUCT OXYGEN RELATIVE HUMIDITY (%)
C R(88) - PRODUCT HYDROGEN RELATIVE HUMIDITY (%)
C R(84) - UNIT LUMPED THERMAL CAPACITANCE (BTU/F)
C R(85) - COMPONENT INITIAL TEMPERATURE (F)
C R(87) - EFFECTIVE AREA PER CELL (SQ. FT.)
C R(89) - NUMBER OF CELLS
C
C OUTPUTS:
C
C R(10) - PRODUCT OXYGEN (LB/HR)
C R(38) - PRODUCT HYDROGEN (LB/HR)
C R(51) - CELL TEMPERATURE (F)
C R(53) - COMPONENT TOTAL HEAT LOSS (EXCL. LOSS TO ALICOM) (BTU/HR)
C R(56) - HEAT LOSS TO AMBIENT GAS BY CONVECTION (BTU/HR)
C R(59) - HEAT LOSS TO AMBIENT WALL BY RADIATION (BTU/HR)
C R(62) - HEAT LOSS TO STRUCTURE BY CONDUCTION (BTU/HR)
C R(63) - INSULATION SURFACE TEMPERATURE (F)
C R(65) - TOTAL HEAT LOSS (SURROUNDINGS + HX) (BTU/HR)

```



TABLE C-1 (CONTINUED)

## LISTING OF KOHHS

```

C
C      ELECTROLYSIS RATE
TC - 0.0
R(88) - R(69) / R(87)
R(72) - NCELLS * ( R(69)/ 1850.0 )
MH2 - R(72)/ 18.0
MO2 - MH2 / 2.0
PHI - 0.0

C
C      START TRIAL AND ERROR HEAT BALANCE
C      INITIAL GUESS FOR TEMP
TCELL - R(71)
IF ( TCELL .EQ.0.0 ) TCELL - 120.0

C
DO 8500 KO - 1,100
IF( TRANS ) QT - R(84)*(TCELL - R(85)) * 8600.0 / DTIME

C
C      FRACTION DISSOLVED SOLIDS
IF( A(1) .LE. 0.0) THEN
FRAC - 0.0
ELSE
FRAC - (A(16)+A(17)+A(18) + A(19))/ A(1)
END IF
WATRIN - A(1) * (1.0 - FRAC)

C
C      MOLAR WATER RATES
IF ( R(73) .LT.0.0101 ) THEN
PS - PSAT(TCELL)
ELSE
IF ( (TCELL-140.)/(TCELL+459.69) .GT. 10.) THEN
PS - -10000.
ELSE
PS - 0.01984 * (57.48 + 26.18 *
1      (( TCELL - 140.0)/ (TCELL + 459.69) ) - R(73) )
2      / (0.8074 * 2.777 ** (-17.66 *
8      (( TCELL - 140.0)/ (TCELL + 459.69) ) ) )
END IF
END IF

C
MH200 - MO2 /(((100.0 * R(70)/ PS)/ R(82)) - 1.0 )
1      + MH2 /(((100.0 * R(70)/ PS)/ R(83)) - 1.0 )
MH20I - MH200 + MH2
QSIGR - MH20I *(18.0 * (A(2) - 77.0) - 68.8 * 1800.0 )
TC - (TCELL +459.69 ) / 1.8
QSIGP - MH2* QFUNC(6.947,-0.2,0.481,TC) + MO2*QFUNC(6.148,
1      8.10,-0.928,TC) + MH200*(QFUNC(7.256,2.80,0.288,TC)
2      - 57.8 *1800.0 )
CALL QSURR

```



TABLE C-1 (CONTINUED)

LISTING OF KOHHS

```
C
C      HEAT LOSS TO LIQUID COOLANT
C
QLOSS = 0.0
IF ( NALT .NE. 0 ) THEN
  CALL FLOARY (AX, NALT ,0,NPFSX,NPFSTX ,NAX1)
  CALL PROP( AX,NPFSX,NPFSTX,CPC,WTMX,RHOX,VISCX,XXK )
C
C      FIND UA
C
IF( NSTR(2) .NE. 0 .AND. NSTR(2) .NE. 2 ) THEN
  R(75) = AX(1)
  R(76) = AX(2)
END IF
IF( NSTR(2) .NE. 0 ) THEN
  R(74) = VALUE( NTHC, R(75), R(78) )
END IF
IF( AX(1).GT. 0.0 ) THEN
  BETA = R(74) / (AX(1)*CPC)
ELSE
  BETA = 0.0
END IF
IF (BETA.GT.10.) THEN
  TOUT = TCELL
ELSE
  TOUT = TCELL + ( AX(2) - TCELL ) * EXP(-BETA)
END IF
QLOSS = AX(1)* CPC * ( TOUT - AX(2) )
NAX = LV ( NALT,65)
V(NAX) = QLOSS
V(NAX +1) = TOUT
END IF
QLOSS = QLOSS + R(58)
C
C      FIND CELL EFFICIENCY
C
IF( NSTR(1) .NE. 0 .AND. NSTR(1) .NE. 2 ) THEN
  R(67) = TCELL
END IF
IF ( NSTR(1) .NE. 0 ) THEN
  EFF = VALUE ( NTEFF, R(67), R(68) )
END IF
VOLTS1 = VALUE ( 1, TCELL, 0.0 )
IF(TCELL.LT.110.) VOLTS1 = 1.70
DVDA = VALUE ( 2, R(88), 0.0 )
VOLTS = VOLTS1 + DVDA * ( R(88) - 150. )
EFF = 1.48 / VOLTS * 100.
IF( EFF .GT. 99.) EFF = 99.
C
C      ELECTRICAL POWER
```

## TABLE C-1 (CONTINUED)

## LISTING OF KOHHS

```

C      P -      NCELLS * ( 1.48 * R(69) *841.8 / EFF )
C
C      SUM OF HEAT EFFECTS
C
C      PHI      - - QT + QSIGR - QSIGP - QLOSS + P
C
C      FIND ZERO VALUE OF PHI AS FCN OF TCELL
C
C      IF(ABS ( PHI/( P )) .LE. R(81) /100.0 ) GO TO 4000
C      IF ( KO. GT. 99 ) THEN
C          WRITE(6,2600) NSUBR,N ,KO
C          CNVRGE = .FALSE.
C          GO TO 4000
C      END IF
C      ZERO = 0.0
C      CALL ESTIM(TCELL,PHI,ZERO,TL,PH,ZERO,0.5,J,NSTR(1) )
C      8500 CONTINUE
C
C      4000 CONTINUE
C
C      R(78) - MH2OI * 18.0
C      R(10) - MO2 * 32.0
C      R(6)  - MH2OO * 6.0
C      R(25) - 2.0 * R(6)
C      R(2)  - TCELL
C      R(21) - TCELL
C      R(38) - MH2 * 2.0
C      R(3)  - R(70)
C      R(4)  - R(70)
C      R(22) - R(70)
C      R(28) - R(70)
C      R(65) - QLOSS
C      R(77) - R(78) * FRAC
C      R(90) - VOLTS
C      R(91) - EFF
C      R(92) - P
C
C      IF( TRANS ) THEN
C          R(86) - R(86) + R(77) * DTIME /8600.0
C          R(85) - TCELL
C      END IF
C
C      IF( KTRANS.EQ.1 ) R(85) - TCELL
C
C      IF ( ABS((A(1)*(1.0 -FRAC) - R(78))/ R(78)).GT..01 ) THEN
C          NCFL -1
C          WRITE(6,9013) NCFL
C      END IF
C

```

## TABLE C-1 (CONTINUED)

## LISTING OF KOHHS

```
IF ( NSIR(17) .EQ.0 .AND. .NOT. CNVRGE ) THEN
  CALL VDATPT (N)
  WRITE(6,9015)
  END IF
2600 FORMAT ('0',//,10X, '***** NOTICE ***** ',/, 10X,
1'THE ELECTROLYSIS CELL, SUBROUTINE NO.' ,I3,
2', COMPONENT NO.' ,I4,' DOES NOT HAVE ' , /, 10X,
8'A CONVERGENT SOLUTION AFTER ', I4,' TRIALS',
4'CURRENT VALUES WILL BE RETURNED'
9013 FORMAT(1X,'*** INLET FLOWS DO NOT MATCH ... NCFL = ',I2)
9015 FORMAT(1X,'*** NSIR(17) = 0 AND NO CNVRGE')
  RETURN
  END
```

TABLE C-2

## LISTING OF MOLSIV

## SUBROUTINE MOLSIV

## MOLECULAR SIEVE SUBROUTINE

## VARIABLES USED:

ABSHUM - ABSOLUTE HUMIDITY OF ENTERING AIR  
 CMPCFM - COMPRESSOR FLOWRATE, CFM  
 CO2AD - AMOUNT OF CO2 ADSORBED IN THE PRESENT HALF CYCLE, LB  
 CO2AD1 - AMOUNT OF CO2 ADSORBED IN MOLECULAR SIEVE BED #1  
 IN THE PREVIOUS CYCLE, LB  
 CO2AD2 - AMOUNT OF CO2 ADSORBED IN MOLECULAR SIEVE BED #2  
 IN THE PREVIOUS CYCLE, LB  
 CO2DES - AMOUNT OF CO2 DESORBED IN THE PRESENT HALF CYCLE, LB  
 CO2LFT - 1 - (REMOVAL EFFICIENCY, CO2RE)  
 CO2NET - NET CO2 FLOW IN AIR THROUGH MOLSIV SUBSYSTEM, LB/HR  
 CO2RE - CO2 REMOVAL EFFICIENCY  
 CTIME - TIME TO COMPLETE ONE FULL CYCLE, SEC  
 DHMS - ENTHALPY CHANGE FOR ADSORBING MOLECULAR SIEVE BED,  
 BTU/LB CO2  
 DHSG - ENTHALPY CHANGE FOR ADSORBING SILICA GEL BED,  
 BTU/LB-H2O  
 DTIMES - COMPUTATIONAL TIME STEP, HOURS  
 FANCFM - FAN FLOWRATE, CFM  
 FANDP - PRESSURE RISE ACROSS FAN, INCHES H2O  
 FANEFF - FAN EFFICIENCY  
 H2OAD - AMOUNT OF H2O ADSORBED IN THE PRESENT HALF CYCLE, LB  
 H2OAD1 - AMOUNT OF H2O ADSORBED IN SILICA GEL BED #1  
 IN THE PREVIOUS CYCLE, LB  
 H2OAD2 - AMOUNT OF H2O ADSORBED IN SILICA GEL BED #2  
 IN THE PREVIOUS CYCLE, LB  
 H2ODES - AMOUNT OF H2O DESORBED IN THE PRESENT HALF CYCLE, LB  
 H2ONET - NET H2O FLOW IN AIR THROUGH MOLSIV SUBSYSTEM, LB/HR  
 HCTIME - TIME TO COMPLETE ONE HALF CYCLE, SEC  
 HCTIMM - TIME TO COMPLETE ONE HALF CYCLE, MIN  
 MCAIR - MASS FLOWRATE \* SPECIFIC HEAT OF BONE DRY GAS,  
 BTU/HR-F  
 MC02IN - MASS FLOWRATE OF CO2 CURRENTLY ADSORBED, LB/HR  
 MC02D - MASS FLOWRATE OF CO2 CURRENTLY EXITING THE  
 DESORBING MOL. SIEVE BED, LB/HR  
 MC02X - MASS FLOWRATE OF CO2 CURRENTLY EXITING THE  
 ADSORBING MOLECULAR SIEVE BED  
 MH2OX - MASS FLOWRATE OF H2O CURRENTLY EXITING THE  
 DESORBING SILICA GEL BED  
 OC02AD - AMOUNT OF CO2 ADSORBED IN THE PREVIOUS CYCLE, LB  
 OH2OAD - AMOUNT OF H2O ADSORBED IN THE PREVIOUS CYCLE, LB  
 P7 - PRESSURE INSIDE THE DESORBING MOL. SIEVE BED, PSIA  
 P8 - PRESSURE OF CO2 ACCUMULATOR, PSIA  
 PC02MM - CO2 PARTIAL PRESSURE OF ENTERING AIR, MM HG





LISTING OF MOLSIV

C-41



TABLE C-2 (CONTINUED)

LISTING OF MOLSIV

DIMENSION V(1),K(1)  
EQUIVALENCE (V(1),K(1))

C

```
REAL      MCAIR, MCO2AD, MCO2D, MH2OX, MCO2X
REAL      MWN2,MWO2,MWH2O,MWCO2,NDOT,MWTOT
PARAMETER (FANCFM = 28.625, FANDP = 11., FANEFF = 0.85)
PARAMETER (PFAN = (FANCFM * FANDP) / (8.5 * FANEFF))
PARAMETER (QFAN = 8.414 * PFAN)
PARAMETER (CMPCFM = 1.05, PCOMPR = 90.)
PARAMETER (QCOMPR = 8.414 * PCOMPR)
PARAMETER (DHSG = 1400., DHMS = 1800.)
PARAMETER (CO2RE = 0.65)
PARAMETER (CO2LFT = 1.- CO2RE)
```

C

C

INITIALIZATIONS

C

IF ( R(71) .EQ. 1. ) THEN

C

INITIALIZATIONS:

```
H2OAD1 = 0.
H2OAD2 = 0.
CO2AD1 = 0.
CO2AD2 = 0.
H2OAD = 0.
CO2AD = 0.
H2ODES = 0.
CO2DES = 0.
OH2OAD = H2OAD2
OC2AD = CO2AD2
CYCLE = 0.
R(90) = H2OAD1
R(91) = H2OAD2
R(92) = CO2AD1
R(93) = CO2AD2
R(94) = H2OAD
R(95) = CO2AD
R(96) = H2ODES
R(97) = CO2DES
R(98) = OH2OAD
R(99) = OC2AD
```

END IF

C

```
HCTIMM = R(65)
P7 = R(66)
P8 = R(67)
TMSDES = R(68)
TSGDES = R(69)
TCABIN = R(70)
HCTIME = HCTIMM * 60.
CTIME = 2. * HCTIME
DTIMEH = DTIME / 8600.
```

## TABLE C-2 (CONTINUED)

## LISTING OF MOLSIV

```

R(72) - HCTIME
R(78) - CTIME
R(74) - DTIMEH
HALF1 - R(75)
H2OAD1 - R(90)
H2OAD2 - R(91)
CO2AD1 - R(92)
CO2AD2 - R(93)
H2OAD - R(94)
CO2AD - R(95)
H2ODES - R(96)
CO2DES - R(97)
OH2OAD - R(98)
OCO2AD - R(99)
CYCLE - R(100)
T2 - R(101)
T8 - R(102)
T5 - R(103)
T6 - R(104)
PCO2MM - VV(2,69)
PCO2 - PCO2MM / 51.715

C
IF( A(1) .LE. 0.) GOTO 100

C
C ----- CALCULATE CYCLE AND HALF-CYCLE TIME -----
C
TCYCLE - AMOD (TIME,CTIME)
THCYCL - AMOD (TIME,HCTIME)
IF (TCYCLE .EQ. 0.) CYCLE = CYCLE + 1.

C
C ----- FAN -----
C
C
C FAN EXIT TEMPERATURE:
T2 = A(2) + QFAN / ( A(1)*CPA )
C ABSOLUTE HUMIDITY AT FAN EXIT:
ABSHUM = ( A(6) + A(7) ) / A(5)

C
C ----- ADSORBING SILICA GEL BED -----
C
C
C MAXIMUM EXIT TEMPERATURE FROM ADSORBING SILICA GEL BED:
T8MAX = T2 + ABSHUM * DHSG / CPA

C
C TEMPERATURE OF DRY AIR LEAVING ADSORBING SILICA GEL BED:
IF ( R(71) .EQ. 1. ) THEN
  T8 = 60.
ELSE
  IF ( THCYCL .EQ. 0. ) THEN
    T8 = T6
  ELSE

```

TABLE C-2 (CONTINUED)

## LISTING OF MOLSIV

```

      IF ( THCYCL .LT. 600. ) THEN
        SLOPSG = ( T8MAX-T8 ) / ( 600.-THCYCL )
        T8 = T8 + SLOPSG * DTIME
        IF ( T8 .GE. T8MAX ) T8 = T8MAX
      ELSE
        T8 = T8MAX
      END IF
    END IF
  END IF

C
C  WATER REMOVED BY THE ADSORBING SILICA GEL BED:
    H2OAD = H2OAD + ( A(6) + A(7) ) * DTIMEH
C
C  ----- HEAT EXCHANGER -----
C
C  TEMPERATURE AND MASS FLOW OF COOL, DRY AIR LEAVING HX:
    TCOOL = R(76)
    T4 = TCOOL + 5.
    MCAIR = A(5) * A(8)
    QHX = MCAIR * (T8 - T4)
C
C  ----- ADSORBING MOLECULAR SIEVE BED -----
C
C  CO2 ADSORBED BY ADSORBING MOLECULAR SIEVE BED:
    MCO2AD = A(12) * CO2RE
    CO2AD = CO2AD + MCO2AD * DTIMEH
C
C  PARTIAL PRESSURE OF CO2 REMAINING IN THE DRY, CO2 DEFICIENT AIR
C  EXITING THE ADSORBING MOLECULAR SIEVE BED:
    PCO2S = PCO2 * CO2LFT
    MCO2X = A(12) * CO2LFT
C
C  MINIMUM EXIT TEMPERATURE OF ADSORBING MOLECULAR SIEVE BED:
    T5MIN = T4 + (MCO2AD * DHMS) / MCAIR
C
C  ACTUAL EXIT TEMPERATURE OF ADSORBING MOLECULAR SIEVE BED:
    IF( THCYCL .EQ. 0. ) T5 = TMSDES
    IF ( R(71) .EQ. 1. ) T5 = T4
    IF (THCYCL .NE. 0. .AND. THCYCL .LT. 1800.) THEN
      SLOPMS = (T5MIN - T5) / (1800. - THCYCL)
      T5 = T5 + SLOPMS * DTIME
      IF ( T5 .LE. T5MIN ) T5 = T5MIN
    ELSE
      T5 = T5MIN
    END IF
C
C  ----- DESORBING SILICA GEL BED -----
C
C  ACTUAL EXIT TEMPERATURE OF WETTED, CO2 DEFICIENT AIR
C  LEAVING THE DESORBING SILICA GEL BED:

```



TABLE C-2 (CONTINUED)

LISTING OF MOLSIV

```
C      IF(THCYCL .EQ. 0.) T6 = R(102)

C      IF (TIME .LT. 8600.) THEN
          T6 = T5
      ELSE
          IF ( THCYCL .LT. 1020.) THEN
              SLSGD = ( TSGDES - T6 ) / (1020.-THCYCL)
              T6 = T6 + SLSGD * DTIME
              IF( T6 .GT. TSGDES) T6 = TSGDES
          END IF
          IF ( THCYCL .EQ. 1020.) T6 = TSGDES
          IF ( THCYCL .GT. 1020. .AND. THCYCL .LT. 2040.) THEN
              SLSGD = (T5MIN - T6)/ (2040. - THCYCL)
              T6 = T6 + SLSGD * DTIME
              IF(T6 .LT. T5MIN) T6 = T5MIN
          END IF
          IF(THCYCL .GE. 2040. .AND. THCYCL .LT. 8600.) T6 = T5MIN
      END IF

C      WATER EXITING THE DESORBING SILICA GEL BED:
C      PH2OX = PSAT(T6)
      MH2OX = (18./A(9)) * (PH2OX / ( A(8)-PH2OX)) * A(5)
      H2OD  = H2ODES
      H2ODES = H2ODES + MH2OX*DTIMEH
      IF ( H2ODES .GE. OH2OAD ) THEN
          MH2OX = (OH2OAD-H2OD)/DTIMEH
          H2ODES = OH2OAD
      END IF

C      HEATER POWER TO DESORBING SILICA GEL BED:
C      IF(THCYCL .LT. 240.) THEN
          PHTR = 0.
      ELSE
          PHTR = 657.
      END IF
      QHTR = PHTR * 8.418

C      AVERAGE HEAT GIVEN UP BY DESORBING SILICA GEL BED TO CABIN:
C      QSG = 22. * (TSGDES - TCABIN) / 110.

C      DESORBING MOLECULAR SIEVE BED
C      CO2 DESORPTION OF MOLECULAR SIEVE BED
      IF (THCYCL .GE. 480.) THEN
          V7 = 85.8*(T4+460.) / (P7*144.)
          FACT = 1.01 - 0.01*(P8/P7)**0.769
          MC02D = FACT*CMPCFM/V7*60.
      ELSE
          MC02D = 0.
      END IF
```

TABLE C-2 (CONTINUED)

## LISTING OF MOLSIV

```

CO2D - CO2DES
CO2DES - CO2DES + MC02D * DTIMEH
IF ( CO2DES .GE. OC02AD ) THEN
  MC02D - (OC02AD-CO2D)/DTIMEH
  CO2DES - OC02AD
END IF

C
C  AVERAGE HEAT GIVEN UP BY DESORBING MOLEC. SIEVE BED TO CABIN:
C  QMS - 46. * (TMSDES - TCABIN) / 290.
C
C
C  ----- UPDATES AT THE END OF ONE HALF-CYCLE -----
C
IF (THCYCL .EQ. 0. ) THEN
  IF (HALF1 .EQ. 1. ) THEN
    H2OAD1 - H2OAD
    OH2OAD - H2OAD1
    CO2AD1 - CO2AD
    OC02AD - CO2AD1
    H2OAD - H2OAD2 - H2ODES
    CO2AD - CO2AD2 - CO2DES
    H2ODES - 0.
    CO2DES - 0.
    HALF1 - 0.
  ELSE
    H2OAD2 - H2OAD
    OH2OAD - H2OAD2
    CO2AD2 - CO2AD
    OC02AD - CO2AD2
    H2OAD - H2OAD1 - H2ODES
    CO2AD - CO2AD1 - CO2DES
    H2ODES - 0.
    CO2DES - 0.
    HALF1 - 1.
  END IF
END IF
100 IF( A(1) .LE. 0. ) THEN
  MH2OX - A(6)
  MC02X - A(12)
  MC02D - 0.
  QHTR - 0.
  QHX - 0.
  QSG - 0.
  QMS - 0.
  H2OAD - 0.
  CO2AD - 0.
  H2ODES - 0.
  CO2DES - 0.
  CYCLE - 0.
  T2 - A(2)

```

TABLE C-2 (CONTINUED)

## LISTING OF MOLSTV

```

      T8 - A(2)
      T5 - A(2)
      T6 - A(2)
END IF
CO2NET = A(12)-MC02X
H2ONET = A(6)+A(7)-MH20X
IF(R(71) .EQ. 1.) R(71) = 0.
T8OLD = T8
R(2) = T6
R(3) = A(8)
R(4) = A(4)
R(6) = MH20X
R(7) = 0.
R(10) = A(10)
R(11) = A(11)
R(12) = MC02X
R(21) = R(70)
R(22) = P8
R(28) = P8
R(81) = MC02D
R(71) = 0.
R(75) = HALF1
IF( A(1) .LE. 0.) THEN
      R(81) = 0.
      R(82) = 0.
ELSE
      R(81) = QCOMPR
      R(82) = QFAN
END IF
R(83) = QHTR
R(84) = QHX
R(85) = QSG
R(86) = QMS
R(87) = CO2NET
R(88) = H2ONET
R(90) = H2OAD1
R(91) = H2OAD2
R(92) = CO2AD1
R(93) = CO2AD2
R(94) = H2OAD
R(95) = CO2AD
R(96) = H2ODES
R(97) = CO2DES
R(98) = OH2OAD
R(99) = OC02AD
R(100) = CYCLE
R(101) = T2
R(102) = T8
R(103) = T5
R(104) = T6

```

TABLE C-3

## LISTING OF BOSCHS

## SUBROUTINE BOSCHS

```

C
C THIS SUBROUTINE MODELS A BOSCH REACTOR SYSTEM, CONSISTING OF THE
C REACTOR, A REGENERATIVE HEAT EXCHANGER, A COMPRESSOR, AND A CON-
C DENSER.

REAL MRECYC,MH2CE,MCO2CE,MCH4CE,MCOCE,MH2OCE,MPCRC,MASSC
REAL IDNUM,MWCMPO
COMMON /CASE/ NCASE,NRSCS,NRECS
COMMON /COMP/ DS(15),N,NA1,NB1,NC,NCAB,NCFL,NEXT,NEXV,NK,
1 NKEX,NKS,NKT,NLFL,NP,NPASS,NPF,NPFT(6),NQ,NS,NSF,NSFT(6),
2 NSTR(18),NSUBR,NV,NVT,Y(12)
COMMON /ECLST1/ KCHOUT,KPRNT,KPTINV(4),KWIT,KWIT1,KWIT2,
1 KWIT3,KWIT4,NUFF,KSTEDY
COMMON /GPOLYF/ IGPOLY
COMMON /KANDV/ K
COMMON /KASE/ NEWRUN,LASTGO,NUCASE,KASAVE
COMMON /KLOC/ IK,IKC,IKS,IKT,IKEX,IP1
COMMON /MAXR1/ MAXR
COMMON /MISC/ DTIME,GRAV,KFLSYS,KOUTPT,KPDROP,KSYPAS,KTRANS,
1 LPSUM(6),MAXCI,MAXLP,MAXSLP,MAXSSI,NCOMPS,NEWDT,NLAST,NPASPD,
2 MINSSI,PGMIN,PLMIN,START,STEADY,TIME,TIMEMX,TMAX,TMIN,WIMAX
COMMON /PROPTY/ CPO,CP(99),CPCONL,CPCONV,CPCO2,CPDIL,CPOXY,CPTC,
1 GAMGAS,RHOO,RHO(99),VISCO,VISC(99),VISGAS,WIMO,WIM(99),WIMCON,
2 WIMDIL,WIMTC,XKO,XK(99),XKGAS,XKLIQ,VISLIQ
COMMON /RARRAY/ IMAXR,R(105)
COMMON /SOURCE/ A(19),B(19),CPA,CPB,IA1,IB1,NA,NB,NPFS,NPFST(6),
1 NSFS,NSFST(6),RHOA,RHOB,VISCA,VISCB,WIMA,WIMB,XKA,XKB
COMMON /VLENTH/ ISSO,ISS(100),IQLO,IQL(100),ITRO,ITR(100)
COMMON /VLOC/ IP,IS,IC,IQ,IV,IVT,IEX,INEXK
COMMON /VPRI/ SLPATH(400),ALPHA(100),ISLP1
DIMENSION V(1),K(1)
DOUBLE PRECISION ALPHA
EQUIVALENCE (V(1),K(1))
LOGICAL STEADY

C
C INPUTS:
C
C A(12) - CO2 INLET FLOW (LB/HR)
C A(14) - H2 INLET FLOW (LB/HR)
C B(2) - INLET COOLANT TEMPERATURE (F)
C R(65) - MAX. CARBON LOADING FOR CARTRIDGE (LB): CMAX
C R(66) - DRY BASIS VOLUME FRACTION OF CO2 IN EXIT GASES: FRCO2
C R(67) - DRY BASIS VOLUME FRACTION OF H2 IN EXIT GASES: FRH2
C R(68) - DRY BASIS VOLUME FRACTION OF CH4 IN EXIT GASES: FRCH4
C R(69) - DRY BASIS VOLUME FRACTION OF CO IN EXIT GASES: FRCO
C R(70) - EFFECTIVENESS FACTOR FOR CONDENSER: EC
C R(71) - EFFECTIVENESS FACTOR FOR REGEN HX: EHX
C R(78) - REACTOR PRESSURE (PSIA): PRCTR
C R(74) - CONDENSER PRESSURE (PSIA): PCOND

```



TABLE C-3 (CONTINUED)

## LISTING OF BOSCHS

```

C   R(76) - AERODYNAMIC EFFICIENCY OF COMPRESSOR:  AECOMP
C   R(77) - MOTOR EFFICIENCY OF COMPRESSOR:  ECOMP
C   R(78) - DESIRED REACTOR TEMP (F):  TRCTRD
C   R(79) - RECYCLE FLOW RATE (LB/HR):  MRECYC
C
C   OUTPUTS:
C
C   R(1) - PRODUCT WATER (LB/HR):  PRH2O
C   R(2) - PRODUCT WATER TEMP (F):  TPRH2O
C   R(7) - R(1) - PRODUCT WATER (LB/HR)
C   R(51) - BOSCH REACTOR TEMP (F):  TRCTR
C   R(53) - TOTAL HEAT LOSS TO AMB. (REACTOR + COMPRESSOR), BTU/HR:
C           QLR + QLCOMP
C   R(72) - HEAT LOSS TO AMBIENT FROM REACTOR, BTU/HR:  QLR
C   R(80) - MASS RATE OF H2 OUT OF COMPRESSOR (LB/HR):  MH2CE
C   R(81) - MASS RATE OF CO2 OUT OF COMPRESSOR (LB/HR):  MCO2CE
C   R(82) - MASS RATE OF CH4 OUT OF COMPRESSOR (LB/HR):  MCH4CE
C   R(83) - MASS RATE OF CO OUT OF COMPRESSOR (LB/HR):  MCOCE
C   R(84) - MASS RATE OF H2O OUT OF COMPRESSOR (LB/HR):  MH2OCE
C   R(85) - RATE OF CARBON PRODUCTION (LB/HR):  MPRC
C   R(86) - MASS OF CARBON IN CARTRIDGE (LB):  MASSC
C   R(87) - IDENTIFICATION NUMBER OF CARTRIDGE IN USE:  IDNUM
C   R(88) - MOLECULAR WEIGHT OF GASES OUT OF COMPRESSOR (LB/LB MOLE):
C           MWCMPO
C   R(89) - SPECIFIC HEAT OF GASES OUT OF COMPRESSOR (BTU/LB-F):
C           CPCMPO
C   R(90) - SPECIFIC HEAT RATIO OF GASES OUT OF COMPRESSOR (CP/CV):
C           GAMCMO
C   R(91) - CONDENSER HEAT LOAD (BTU/HR):  QLCOND
C   R(92) - HEAT LOSS TO AMBIENT FROM COMPRESSOR (BTU/HR):  QLCOMP
C   R(93) - HEAT OF REACTION (BTU/HR):  QRXN
C   R(94) - ACTUAL HEATER POWER BEING DRAWN (BTU/HR):  QHTRNO
C   R(95) - TEMP OF GASES LEAVING REACTOR (F):  T1
C   R(96) - TEMP OF GASES ENTERING REACTOR (F):  T5
C   R(97) - TEMP OF GASES ENTERING CONDENSER (F):  T2
C   R(98) - TEMP OF GASES LEAVING COMPRESSOR (F):  T4
C   R(99) - TEMP OF GASES LEAVING CONDENSER (F):  T3
C   R(100) - TEMP OF GASES ENTERING COMPRESSOR (F):  T6
C   R(101) - THERMAL CAPACITANCE OF BOSCH REACTOR (BTU/F):
C           (INITIAL VALUE IS MODIFIED AS CARBON DEPOSITS)
C   R(102) - REACTOR TEMP BELOW WHICH HEATER TURNS ON, F
C   R(103) - REACTOR TEMP ABOVE WHICH HEATER TURNS OFF, F
C   R(104) - REACTOR TEMP AT PREVIOUS STEP, F
C   R(105) - TOTAL POWER TO COMPRESSOR (WATTS):  QCOMPT
C
C   ITRATE -0
C
C   IF(NPASS.EQ.0) THCAPO = R(101)
C

```



TABLE C-3 (CONTINUED)

LISTING OF BOSCHS

TRCTR - R(51)  
CMAX - R(65)  
FRCO2 - R(66)  
FRH2 - R(67)  
FRCH4 - R(68)  
FRCO - R(69)  
EC - R(70)  
EHX - R(71)  
QLR - R(72)  
PRCTR - R(73)  
PCOND - R(74)  
QHTR - R(75)  
ARECOMP - R(76)  
ECOMP - R(77)  
TRCTRD - R(78)  
MRECYC - R(79)

C  
C  
C  
C

---

CALCULATE MOLECULAR WEIGHT OF BONE DRY RECYCLE GASES  
IF ( A(14) .EQ. 0.) THEN  
    WMH2 - 0.  
ELSE  
    WMH2 - A(14)/2.016  
END IF  
WMC02- A(12)/44.011  
XWBDG - 16.048\*FRCH4 + 44.011\*FRCO2 + 2.016\*FRH2 + 28.011\*FRCO

C  
C  
C  
C  
C

---

BEGIN ITERATION ON MASS AND HEAT BALANCES  
ASSUME THAT TEMPERATURE OF GASES OUT OF CONDENSER IS 20 DEG ABOVE  
INLET COOLANT TEMPERATURE, AS A FIRST GUESS.  
T3OLD - B(02) + 20.  
T8 - T3OLD

C  
C  
C  
C  
C  
C  
C  
C  
C

---

CALCULATE PARTIAL PRESSURE OF WATER IN CONDENSER EXIT GASES

---

---

---

C  
C

---

CALCULATE RATE OF CARBON FORMATION AND WATER PRODUCTION  
SEE IF REACTANTS ARE WITHIN 1 PERCENT OF STOICHIOMETRIC RATIO  
NX - NKS+1  
IF (WMH2 .EQ. 0.) THEN  
    TEST - 999.  
ELSE

TABLE C-3 (CONTINUED)

## LISTING OF BOSCHS

```

      TEST - WMC02/WMH2 * 2.0 - 1.
END IF
K(NX) - 1
IF( ABS(TEST) .LE. .01 ) K(NX) - 0
TEST1 - A(10)+ A(11)+ A(13) + A(15)+A(16)+A(17)+A(18)+A(19)
C  TEST FOR EXTRANEUS FLOWS IN FEED SUCH AS O2 AND DILUENT
NX1- NX+1
K(NX1) - 0
IF( TEST1 .NE. 0. ) K(NX1)-1
C
C
C  SEE WHICH IS LIMITING REACTANT
IF( TEST .LE. 0.0 ) THEN
C    CO2 LIMITING, HYDROGEN RICH FEED.
MPRC - WMC02 *12.011
PRH20 - WMC02 *2. * 18.016 + A(6) + A(7)
ELSE
C    H2 LIMITING, CO2 RICH FEED
MPRC - WMH2 * .5 * 12.011
PRH20 - WMH2 * 18.016 + A(6) + A(7)
END IF
C
C
C  CALCULATE TOTAL FLOW OUT OF CONDENSER
WCONDO - MRECYC - PRH20 - MPRC
WATERO - PRH20
DUM1 - 18.016/XWBDG
C
C
C  CALCULATE COMPRESSOR FACTORS THAT STAY CONSTANT DURING ITERATIONS
PRATIO - PRCTR/PCOND
C
C
C
C
C  DO 200 IB - 1,20,1
C
PW - PSAT( T8 )
ITRATE - ITRATE + 1
C
C
C
C  CALCULATE FLOW RATE OF BONE DRY GAS
WBDG-WCONDO / (1.+DUM1* PW/(PCOND-PW) )
C
C
C  CALCULATE FLOWS OUT OF COMPRESSOR
BDGMOL- WBDG/XWBDG
WATER - BDGMOL * PW/PCOND * 18.016
C  H2
MH2CE - A(14) + BDGMOL * FRH2 * 2.016

```



TABLE C-3 (CONTINUED)

LISTING OF BOSCHS

```

C   CO2
C   MCO2CE - A(12) + BDGMOL * FRCO2 * 44.011
C   CH4
C   MCH4CE - BDGMOL * FRCH4 * 16.048
C   CO
C   MCOCE - BDGMOL * FRCO * 28.011
C   H2O
C   MH2OCE - WATER + A(6) + A(7)
C   CPBDG - ((MH2CE-A(14))*8.42 + (MCO2CE-A(12))*0.21 + MCH4CE* .55
1 + MCOCE*.25 + R(10)*0.22 + R(11)*0.249) /WBDG
C   CALCULATE MOLECULAR WEIGHT OF GASES OUT OF COMPRESSOR
C   MWCMP - MRECYC/(MH2CE/2.016 + MCO2CE/44.011 + MCH4CE/16.048
1 + MH2OCE/18.016 + MCOCE/28.011 + R(10)/82. + R(11)/28.008)
C   CALCULATE SPECIFIC HEAT OF COMPRESSOR GASES
C   CPCMP - (8.42*MH2CE + .21 * MCO2CE + .55 * MCH4CE + .25 * MCOCE
1 + .49 * MH2OCE + 0.22*R(10) + 0.249*R(11) )/ MRECYC
C
C   WCOMP - MH2CE+MCO2CE+MCH4CE+MCOCE+MH2OCE
C   WPCMP - WCOMP * CPCMP
C   CALCULATE GAMMA OF COMPRESSOR GASES
C   GAMCMO - CPCMP/( CPCMP - 1.987/MWCMP )
C
C
C   CALCULATE ISENTROPIC POWER REQUIREMENT(BTU/HR)
C   FIRST CALCULATE TEMP AT MIX POINT
C   T6 - ((WBDG *CPBDG + .49*WATER)* T8 + ( A(12)*.21+A(14)*8.42
1 + A(6)* .49 + A(7)* 1.0 ) * A(2))/MRECYC/CPCMP
C   TO - 459.6 + T6
C   XN - (GAMCMO-1.)/GAMCMO
C   QCOMP - MRECYC*1545.*TO*GAMCMO*(PRATIO**XN-1.)/778./MWCMP/
1 (GAMCMO - 1.)/ AECOMP
C   TOTAL POWER TO COMPRESSOR(WATTS)
C   QCOMPT - QCOMP/ECOMP/8.41
C   HEAT FLOW FROM COMPRESSOR TO AMBIENT(BTU/HR)
C   QLCOMP - QCOMPT*8.41 - QCOMP
C
C
C   HEAT OF REACTION(BTU/HR)
C   QRXN - 978. * A(12)
C
C
C   TEMPERATURE OUT OF COMPRESSOR
C   T4 - T6 + QCOMP/MRECYC/CPCMP
C
C
C   TEMPERATURE OUT OF REACTOR
C   T1 - TRCTR - QLR / WPCMP
C
C

```



TABLE C-3 (CONTINUED)

LISTING OF BOSCHS

```
C    TEMPERATURE INTO CONDENSER
    T2 - T1 - EHX*( T1 - T4 )
C
C
C    TEMPERATURE OF GASES LEAVING CONDENSER
    T8 - T2 - EC *(T2- B(2) )
C
C
C    THIS COMPLETES ONE ITERATION ON THERMAL BALANCE
C
C
C    TESTI - T8OLD - T8
    T8OLD - T8
    IF ( ABS(TESTI).LT. .8 .OR. ITRATE .GT. 10 ) GO TO 250
200 CONTINUE
C
C
C
C
C
C
C    250 CONTINUE
C
C    HEAT INTO RECYCLE GASES BY THE REACTOR
    Q42 - WCPCMP * ( T2 - T4 )
    Q51 - Q42
C    TEMPERATURE INTO REACTOR
    T5 - T1 - Q51/WCPCMP
C    TOTAL HEAT LOST TO ENVIRONMENT
    QLTOT - QLR + QLCOMP
    R(58) - QLTOT
C    HEATER SIZING
    QHTR - Q51 + QLR - QRXN
    R(75) - QHTR
    QHTRNO - QHTR
C
C
C    CALCULATE CARBON LOADING
    DHOUR - DTIME/8600.
    IF( STEADY ) THEN
        IDNUM - 0.
        MASSC - CMAX/2.
        TRCTR - TRCTRD
    END IF
C
C
C    HEATER CONTROL LOGIC
    IF ( TRCTR .LT. R(102) ) QHTRNO - QHTR
    IF ( TRCTR .GT. R(103) ) QHTRNO - 0.
    R(104) - TRCTR
```

TABLE C-3 (CONTINUED)

## LISTING OF BOSCHS

```

C
C
      IF( .NOT. STEADY) THEN
C      CALCULATE LBS OF CARBON IN CARTRIDGE
      IF( NPASS .EQ. 0 ) THEN
        MASSC=0.
      END IF
      IF ( MASSC .GE. CMAX ) THEN
        MASSC = 0.
        R(101) = THCAPO
        IDNUM = IDNUM + 1.
      END IF
      MASSC = MASSC + MPRC * DHOURL
      R(101) = R(101) + MASSC*.5
      TRCTR = (MRECYC*(T1-T5)*CPCMP0-R(58)+
1      QRXN + QHTRNO)*DHOURL/R(101) + TRCTR
      END IF
C
C
      QLCOND = (WBDG * CPBDG +PRH20*.49)*(T2- T5) +1050.*PRH20
      R(1) = PRH20
      R(2) = T5
      R(3) = A(4)
      R(4) = PCOND
      R(7) = WATERO
      R(8) = CPCONL
      R(9) = WTMCON
      R(20) = B(1)
      R(21)= B(2) + QLCOND/B(1)/CPB
      R(22)= B(4)
      R(23)= B(4)
      R(80) = MH2CE
      R(81) = MCO2CE
      R(82) = MCH4CE
      R(83) = MCOCE
      R(84) = MH2OCE
      R(85) = MPRC
      R(86) = MASSC
      R(87) = IDNUM
      R(88) = MWCMP0
      R(89) = CPCMP0
      R(90) = GAMCMO
      R(91) = QLCOND
      R(92) = QLCOMP
      R(93) = QRXN
      R(94) = QHTRNO
      R(95) = T1
      R(96) = T5
      R(97) = T2
      R(98) = T4

```

## TABLE C-3 (CONTINUED)

## LISTING OF BOSCHS

```
      R(99) - T8  
      R(100) - T6  
      R(105) - QCOMPT  
C  
      RETURN  
C  
      END
```



TABLE C-4

LISTING OF CNDHEX

SUBROUTINE CNDHEX

```
C
C THIS SUBROUTINE COMPUTES THE PERFORMANCE OF A PLATE FIN
C CONDENSING HEAT EXCHANGER.
C
COMMON /PROPTY/ CP0,CP(99),CPCONL,CPCONV,CPCO2,CPDIL,CPOXY,CPTC,
1 GAMGAS,RH00,RHO(99),VISCO,VISC(99),VISGAS,WIMO,WIM(99),WIMCON,
2 WIMDIL,WIMTC,XK0,XK(99),XKGAS,XKLIQ,VISLIQ
COMMON /CANYHX/ FINAL,CC,CH,XCP(2),KBUZ(3)
1,IFCPP,IFCPS,IFPIEM,IFSTEM,IFSIZE,IFFLOW
COMMON /COMP/ DS(15),N,NA1,NB1,NC,NCAB,NCFL,NEXT,NEXV,NK,
1 NKEX,NKS,NKT,NLFL,NP,NPASS,NPF,NPFT(6),NQ,NS,NSF,NSFT(6),
2 NSTR(18),NSUBR,NV,NVT,Y(12)
COMMON /RARRAY/ IMAXR,R(128)
COMMON /MISC/ DTIME,GRAY,KFLSYS,KOUTPT,KPDROP,KSTPAS,KTRANS,
1 LPSUM(5),MAXCI,MAXLP,MAXSLP,MAXSSI,NCOMPS,NEWDT,NLAST,NPASPD,
2 MINSSI,PGMIN,PLMIN,START,STEADY,TIME,TIMEMX,TMAX,TMIN,WIMAX
COMMON /SOURCE/ A(19),B(19),CPA,CPB,IA1,IB1,NA,NB,NPFS,NPFST(6),
1 NSFS,NSFST(6),RHOA,RHOB,VISCA,VISCB,WIMA,WIMB,XKA,XKB
EQUIVALENCE ( RT(1), R(79))
DIMENSION RT(1)
EQUIVALENCE(INSTR(1),NSTR(1))
DIMENSION INSTR(18)
LOGICAL STEADY,FINAL
REAL PTOT,PPTHK,INWPP,INABSH,MDOTL
INTEGER COOLPO

C
C DEFINITION OF PARAMETERS
C
C INPUTS:
C
C HOTFW - HOT FLOW WIDTH (INCHES)
C HOTFLL - HOT FLOW LENGTH (INCHES)
C NCOOLP - NUMBER OF COOLANT PASSES
C NCFILL - NUMBER OF COLD FIN LAYERS
C NHFINL - NUMBER OF HOT FIN LAYERS
C CFINHT - COLD FIN HEIGHT (INCHES)
C HFINHT - HOT FIN HEIGHT (INCHES)
C CFINTK - COLD FIN THICKNESS (INCHES)
C HFINTK - HOT FIN THICKNESS (INCHES)
C NCFIN - NUMBER OF COLD FINS
C NHFIN - NUMBER OF HOT FINS
C CFINK - COLD FIN THERMAL CONDUCTIVITY
C HFINK - HOT FIN THERMAL CONDUCTIVITY
C
C INTERMEDIATE:
C
C CFL - COLD FLOW LENGTH (INCHES)
C CSSAR - COLD SECONDARY SURFACE AREA (FT-2)
C HSSAR - HOT SECONDARY SURFACE AREA (FT-2)
C
```





TABLE C-4 (CONTINUED)

LISTING OF CNDHEX

C	CPRSA	- COLD PRIMARY SURFACE AREA (FT-2)
C	HPRSA	- HOT PRIMARY SURFACE AREA (FT-2)
C	TCSA	- COLD SIDE TOTAL SURFACE AREA (FT-2)
C	THSA	- HOT SIDE TOTAL SURFACE AREA (FT-2)
C	CFLWA	- COLD FLOW AREA (FT-2)
C	HFLWA	- HOT FLOW AREA (FT-2)
C	CHYDRD	- COLD HYDRAULIC DIAMETER (FT)
C	HHYDRD	- HOT HYDRAULIC DIAMETER (FT)
C	INABSH	- INLET ABSOLUTE HUMIDITY
C	INWPP	- INLET WATER VAPOR PARTIAL PRESSURE (PSIA)
C	DPIN	- INLET DEW POINT (F)
C	OUTWPP	- OUTLET WATER VAPOR PARTIAL PRESSURE (PSIA)
C	OUTABH	- OUTLET ABSOLUTE HUMIDITY
C	QLAT	- LATENT HEAT LOAD (BTU/HR)
C	QSENS	- SENSIBLE HEAT LOAD (BTU/HR)
C	QTOT	- TOTAL HEAT LOAD (BTU/HR)
C	FS	- FACTOR OF SAFETY
C	COUT	- COOLANT OUTLET TEMPERATURE (F)
C	CVISC	- COOLANT VISCOSITY (LB/FT-HR)
C	HVISC	- HOT VISCOSITY (LB/FT-HR)
C	CCOND	- COLD THERMAL CONDUCTIVITY (BTU/HR-FT-F)
C	HCOND	- HOT THERMAL CONDUCTIVITY (BTU/HR-FT-F)
C	CPRAND	- COLD PRANDLT NUMBER
C	HPRAND	- HOT PRANDLT NUMBER
C	CFLWUA	- COLD FLOW PER UNIT AREA (LB/HR-FT-2)
C	HFLWUA	- HOT FLOW PER UNIT AREA (LB/HR-FT-2)
C	CRENNO	- COLD REYNOLDS NUMBER
C	HRENNO	- HOT REYNOLDS NUMBER
C	CCOBRN	- COLD COBURN FACTOR
C	HCOBRN	- HOT COBURN FACTOR
C	CCFMOD	- COLD MODIFIED COBURN FACTOR
C	HCFMOD	- HOT MODIFIED COBURN FACTOR
C	CFCOF	- COLD FILM COEFFICIENT (BTU/HR-FT <sup>2</sup> -F)
C	HFCOF	- HOT FILM COEFFICIENT (BTU/HR-FT <sup>2</sup> -F)
C	COFINE	- COLD OVERALL FIN EFFICIENCY
C	HOFINE	- HOT OVERALL FIN EFFICIENCY
C	CEFC	- COLD EFFECTIVE FILM COEFFICIENT (BTU/HR-FT <sup>2</sup> -F)
C	HEFC	- HOT EFFECTIVE FILM COEFFICIENT (BTU/HR-FT <sup>2</sup> -F)
C	HACEFF	- COLD EFFECTIVE UA (BTU/HR-F)
C	HAHEFF	- HOT EFFECTIVE UA (BTU/HR-F)
C	TEDUA1	- TOTAL DRY UA (BTU/HR-F)
C	HWCP	- HOT SIDE (W CP) (BTU/HR-F)
C	AIRPP	- PINCH POINT AIR SIDE TEMPERATURE (F)
C	COOLPP	- PINCH POINT COOLANT TEMPERATURE (F)
C	WTLMTD	- WET SECTION LMTD (F)
C	DYLMTD	- DRY SECTION LMTD (F)
C	WSDUA	- WET SECTION DRY UA (BTU/HR-F)
C	DSDUA	- DRY SECTION DRY UA (BTU/HR-F)
C	TEDUA2	- TOTAL EFFECTIVE DRY UA (BTU/HR-F)
C		

TABLE C-4 (CONTINUED)

## LISTING OF CNDHEX

```

C      OUTPUT:
C
C      R(2)  - HOT SIDE OUTLET TEMPERATURE (F)
C      R(6)  - HOT SIDE CONDENSABLE VAPOR FLOW (LBM/HR)
C      R(7)  - HOT SIDE ENTRAINED LIQUID FLOW (LBM/HR)
C      R(21) - COLD SIDE OUTLET TEMPERATURE (F)
C
C      PARAMETER(HOTFW - 8.60)
C      PARAMETER(HOTFLL - 11.18)
C      PARAMETER(NCOOLP - 4)
C      PARAMETER(NCFINL - 28)
C      PARAMETER(NHFINL - 28)
C      PARAMETER(CFINHT - 0.1)
C      PARAMETER(HFINHT - 0.20)
C      PARAMETER(CFINTK - .002)
C      PARAMETER(HFINTK - .002)
C      PARAMETER(NCFIN - 28)
C      PARAMETER(NHFIN - 16)
C      PARAMETER(CFINK - 9.4)
C      PARAMETER(HFINK - 9.4)
C      PARAMETER(CFL- (HOTFW+HFINHT*2.)-2.*CFINHT)
C      PARAMETER(CSSAR - CFL*HOTFLL*NCFINL*NCFIN*(CFINHT-CFINTK)/72.0)
C      PARAMETER(HSSAR - HOTFW*HOTFLL*NHFINL*NHFIN*(HFINHT-HFINTK)/72.0)
C      PARAMETER(CPRSA - CFL*HOTFLL*NCFINL*(1.-NCFIN*CFINTK)/72.)
C      PARAMETER(HPRSA - HOTFW*HOTFLL*NHFINL*(1.-NHFIN*HFINTK)/72.)
C      PARAMETER(TCSA - CSSAR+CPRSA)
C      PARAMETER(THSA - HSSAR+HPRSA)
C      PARAMETER(CFLWA - HOTFLL/NCOOLP*NCFINL*(1.-NCFIN*CFINTK)*
1      (CFINHT-CFINTK)/144.)
C      PARAMETER(HFLWA - HOTFW*NHFINL*(1.-NHFIN*HFINTK)*(HFINHT
1      -HFINTK)/144.)
C      PARAMETER(CHYDRD - (1./NCFIN-CFINTK)*(CFINHT-CFINTK)/(6.*((1./
1      NCFIN-CFINTK)+(CFINHT-CFINTK)))
C      PARAMETER(HHYDRD - (1./NHFIN-HFINTK)*(HFINHT-HFINTK)/(6.*((1./
1      NHFIN-HFINTK)+(HFINHT-HFINTK)))
C
C      INITIALIZE THE R ARRAY
C
C      DO 10 I=1,19
C      R(I) = A(I)
10     R(I+19) = B(I)
C
C      INITIALIZE PROGRAM VARIABLES
C
C      IF(A(1) .GT. B(1)/10.) THEN
C      CCP - CPB
C      HCP - CPA
C      STEMCP - CPCONV
C      HOTFLW - R(1)
C      COLFLW - R(20)

```



TABLE C-4 (CONTINUED)

LISTING OF CNDHEX

```
HOTIN  - R(2)
CIN    - R(21)
PTOT   - R(8)
COOLPO - KK(N,16)
HOTOUT - ((HOTIN-CIN)/4.)*CIN

C
C
C    CALCULATE INLET DEW POINT

INABSH - R(6)/R(5)
INWPP  - (PTOT*INABSH)/(INABSH+0.622)
DPIN   - TSAT(INWPP)
RJ     - 0.
BAND   - CIN+2.0

C
    DO 50 I=1,50
    OUTWPP - PSAT(HOTOUT)
    OUTABH - 0.622*OUTWPP/(PTOT-OUTWPP)
    OUTABH - AMIN1(OUTABH,INABSH)

C
C
C    LATENT, SENSIBLE AND TOTAL HEAT LOAD (BTU/HR)

AVEHFG - 1094.1-0.575*(DPIN+HOTOUT)/2.
QLAT   - R(5)*(INABSH-OUTABH)*AVEHFG
QLAT   - AMAX1(0.,QLAT)
QSENS  - HOTFLW*HCP*(HOTIN-HOTOUT)
QTOT   - QLAT+QSENS

C
C
C    CALCULATE FACTOR OF SAFETY

IF(COOLPO .EQ. 1) THEN
    CONST - 0.44
ELSE
    CONST - -0.04
END IF
FS - 1.094 *QTOT/QSENS+CONST

C
C
C    OUTLET COLD FLUID TEMPERATURE (F)

COOT - CIN+QTOT/COLFLW*CCP

C
C
C    VISCOSITY, THERMAL CONDUCTIVITY, PRANDLT NO., FLOW/AREA, REYNOLDS
    NO., COBURN FACTOR, MODIFIED CF

CVISC - -0.808+219.56/((CIN+COOT)/2.)*2286.14/(
1      (CIN+COOT)/2.)*2.
HVISC - 0.0000685*((HOTIN+HOTOUT)/2.0)+0.08991

C
    CCOND - 0.2905+0.00095*((CIN+COOT)/2.)*-0.000002186*(
1      (CIN+COOT)/2.)*2.
HCOND - 0.0000206*((HOTIN+HOTOUT)/2.0)+0.01884
```

TABLE C-4 (CONTINUED)

## LISTING OF CNDHEX

```

C      CPRAND = CVISC*CCP/CCOND
      HPRAND = HVISC*HCP/HCOND
C
C      CFLWUA = COLFLW/CFLWA
      HFLWUA = (1.+(INABSH*OUTABH)/2.)*HOTFLW/HFLWA
C
C      CRENNO = CHYDRD*CFLWUA/CVISC
      HRENNO = HHYDRD*HFLWUA/HVISC
C
      IF (CRENNO .LE. 500.) THEN
        CCOBRN = (1./CRENNO**0.2288)*0.07081
      ELSE
        CCOBRN = (1./CRENNO**0.4249)*0.2454
      END IF
      IF (HRENNO .LE. 500.) THEN
        HCOBRN = (1./HRENNO**0.2288)*0.07081
      ELSE
        HCOBRN = (1./HRENNO**0.4249)*0.2454
      END IF
C
      CCFMOD = (18./NCFIN)**0.284*CCOBRN
      HCFMOD = (18./NHFIN)**0.284*HCOBRN
C
C      FILM COEFFICIENT (BTU/HR-FT2-F)
C
      TEMP1 = 8.65*CCOND/CHYDRD
      TEMP2 = CCFMOD*CCP*CFLWUA/CPRAND**0.6667
      CFCOF = AMAX1(TEMP1,TEMP2)
      TEMP3 = 8.65*HCOND/HHYDRD
      TEMP4 = HCFMOD*HCP*HFLWUA/HPRAND**0.6667
      HFCOF = AMAX1(TEMP3,TEMP4)
C
C      FIN EFFICIENCY AND OVERALL FIN EFFICIENCY CALCULATION
C
      TEMPC = SQRT(2.*CFCOF/(12.*CFINK*CFINTK))*CFINHT/2.
      TEMPH = SQRT(2.*HFCOF/(12.*HFINK*HFINTK))*HFINHT/2.
      CFINEF = (EXP(TEMPC)-EXP(-TEMPC))/(EXP(TEMPC)+EXP(-
1    TEMPC))/TEMPC
      HFINEF = (EXP(TEMPH)-EXP(-TEMPH))/(EXP(TEMPH)+EXP(-TEMPH))/
1    TEMPH
      COFINE = 1.-CSSAR/TCSA*(1.-CFINEF)
      HOFINE = 1.-HSSAR/THSA*(1.-HFINEF)
C
      CEFC = COFINE*CFCOF
      HEFC = HOFINE*HFCOF
C
C      EFFECTIVE HA (BTU/HR-F)
C
      HACEFF = CEFC*TCSA
  
```



## TABLE C-4 (CONTINUED)

## LISTING OF CNDEX

```

1      QTOT/QSENS)/(QTOT/QSENS*(HACEFF/HAHEFF+1.))
      ELSE
        WSDUA = 0.0
      END IF
      TEMP1 = COUT-COOLPP
      IF(DYLMTD .GT. 0.0 .AND. TEMP1 .GT. 0.0) THEN
        DSDUA = COLFLW*(COUT-COOLPP)/DYLMTD
      ELSE
        DSDUA = 0.0
      END IF

      TOTAL EFFECTIVE DRY UA (BTU-HR-F)

      TEDUA2 = WSDUA+DSDUA

      NEWTON-RHAPSON ITERATION ON THE HOT SIDE OUTLET
      TEMP. UNTIL THE EFFECTIVE DRY UA'S ARE WITHIN 1 BTU-HR-F

      ERROR = TEDUA2-TEDUA1
      IF (ABS(ERROR) .LE. 8.0) GO TO 100
      IF (I .EQ. 1) THEN
        HOTNEW = 1.01*HOTOUT
      ELSE
        CHCK1 = HOTOUT-HOTOLD
        IF (CHCK1 .GT. -0.00001 .AND. CHCK1 .LT. 0.00001) THEN
          CHCK1 = 0.0001
        END IF
        IF (ABS(ERROR-ERROLD) .GT. 0.00001) THEN
          SLOPE = (ERROR-ERROLD)/CHCK1
          CRINC = ERROR/SLOPE
          HOTNEW = HOTOUT-CRINC/4.
        ELSE
          HOTNEW = HOTNEW*1.01
        END IF
        IF (HOTNEW .GT. HOTIN) THEN
          HOTNEW = (HOTIN-CIN)/4.+CIN-RJ
          RJ = RJ+1.
        END IF
        IF (HOTNEW .LT. CIN) THEN
          HOTNEW = (HOTOUT+BAND)/2.0
          IF (ABS(HOTNEW-HOTOUT) .LT. 0.0001) GO TO 100
        END IF
      END IF
      HOTOLD = HOTOUT
      ERROLD = ERROR
      HOTOUT = HOTNEW
      IF (I .EQ. 50) THEN
        WRITE(6,45) I
        NSTR(17) = 1
      END IF

```



TABLE C-4 (CONTINUED)

LISTING OF CNDHEX

```
ELSE
  IF(COOLPO .EQ. 1) THEN
    C1 = (12.*CFINHT)/(CFINK*NCFIN*CFINTK*HOTFLL*HOTFW*
1      NCFINL)
    ELSE
      C1 = 0.0
    END IF
    DRYUA = (1./(2.*(1./HACEFF+1./HAHEFF))+1./(2.*(1./HACEFF
1      +1./HAHEFF)+C1))*(1./FS)
C
C      NTU'S PER PASS
C
C      PSSNTU = DRYUA/(HOTFLW*HCP*NCOOLP)
C
C      MASS FLOW RATIO
C
C      FLWRTO = HOTFLW*HCP/(COLFLW*CCP)
C
C      EFFECTIVENESS PER PASS
C
C      C2 = EXP(-PSSNTU**0.78*FLWRTO)
C      C8 = EXP((C2-1.)/(FLWRTO/PSSNTU**0.22))
C      EFFPP = 1.-C8
C
C      OVERALL EFFECTIVENESS
C
C      C4 = ((1.-EFFPP*FLWRTO)/(1.-EFFPP))*NCOOLP
C      OVEFF = (C4-1.)/(C4-FLWRTO)
C
C      AIR OUTLET TEMPERATURE
C
C      HOTNEW = HOTIN-OVEFF*(HOTIN-CIN)
C      IF (ABS(HOTNEW-HOTOUT) .LE. 0.1) GO TO 100
C      HOTOUT = HOTNEW
    END IF
50    CONTINUE
C
C      CALCULATED THE CONDENSED LIQUID (LBM/HR)
C
C      100 MDOTL = R(5)*(INABSH-OUTABH)
C      H2OV = R(6)-MDOTL
C
C      STORE RESULTS IN R ARRAY FOR G189 SOLUTION
C
C      R(2) = AMAX1(HOTOUT,B(2))
C      R(6) = H2OV
C      R(7) = MDOTL
C      R(21) = COUT
    ELSE
```

## TABLE C-4 (CONTINUED)

## LISTING OF CNDHEX

```
      R(2) - B(2)
      R(21) - B(2)
END IF
C
C PROGRAM DEBUG OUTPUT
C
C IF (TIME .GE. 8000. .AND. TIME .LE. 3600.) THEN
C   NSTR(17) - 1
C ELSE
C   NSTR(17) - 0
C END IF
C
C FORMAT STATEMENTS
C
45 FORMAT (' *****ERROR*****THE CONDENSING HEAT EXCHANGERS UA DOES
NOT CONVERGE AFTER ',I2,' INTERACTIONS. ')
RETURN
END
```



#### C.4 Program Use

The following section presents the procedures to use the program on the Hamilton Standard IBM or the NASA Langley Prime Computers. Also, instructions are given to allow the user to swap one CO<sub>2</sub> removal subsystem for another, to modify the input data, and to change control logic.

##### C.4.1 Operation Using the Hamilton Standard IBM Computer

To run the Space Station simulation model, use the following sequence of steps:

- (1) Access the command list from the G15UARL library:

LGCL G189CL G15UARL

- (2) Access the input data set:

LG SSDATA DATA SO(G15UARL)

#### C.4      Program Use    (Continued)

(3)    Make desired changes to SSDATA.DATA.

(4)    Enter the following command:

EX G189CL

More detailed information on each of these steps is provided in the following sections.

##### C.4.1.1    The Command List G189CL

G198CL is a general command list to run any FORTRAN 77 G198A load module. A listing of this command list is provided in Table C-5 and a description of the file assignments is given in Table C-6.

TABLE C-5

## LISTING OF G189CL FOR SPACE STATION MODEL

```

CONTROL PROMPT NOMSG
ERASE
N1: DELETE PLOT.DATA
    DELETE PLTCAT.DATA
    DELETE OUT.DATA
    DELETE OUT1.DATA
    DELETE OUT2.DATA
    DELETE OUT8.DATA
FREE FILE(FT05F001)
FREE FILE(FT06F001)
FREE FILE(FT07F001)
FREE FILE(FT08F001)
FREE FILE(FT09F001)
FREE FILE(FT10F001)
FREE FILE(FT11F001)
FREE FILE(FT16F001)
FREE FILE(FT20F001)
FREE FILE(FT80F001)
FREE FILE(FT81F001)
FREE FILE(FT41F001)
FREE FILE(FT42F001)
FREE FILE(FT48F001)
FREE FILE(FT44F001)
FREE FILE(FT45F001)
FREE ATTRLIST(A1 B2 C8 D4 E5)
ATTRIB A1 BLKSIZE(844) RECFM(V B) LRECL(844)
ATTRIB B2 BLKSIZE(10000) RECFM(V B S) LRECL(10000)
ATTRIB C8 BLKSIZE(8404) RECFM(V B S) LRECL(8404)
ATTRIB D4 BLKSIZE(8990) RECFM(F B A) LRECL(188)
ATTRIB E5 BLKSIZE(8990) RECFM(F B) LRECL(80)
DELETE DD1
DELETE DD2
DELETE DD8
DELETE DD4
DELETE DD5
DELETE DD6
DELETE IN10
DELETE IN11
WRITE
WRITE
WRITE DATA SETS ARE NOW BEING ALLOCATED.
ALLOC DS(DD1) F(FT41F001) NEW SPACE(844,200) BLOCK(844) +
    USING(A1) DELETE
ALLOC DS(DD2) F(FT42F001) NEW SPACE(200,200) BLOCK(10000) +
    USING(B2) DELETE
ALLOC DS(DD8) F(FT48F001) NEW SPACE(200,200) BLOCK(8404) +
    USING(C8) DELETE
ALLOC DS(DD4) F(FT44F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C8) DELETE
ALLOC DS(DD5) F(FT80F001) NEW SPACE(200,200) BLOCK(8408) +

```

TABLE C-5 (CONTINUED)

## LISTING OF G189CL FOR SPACE STATION MODEL

```
        USING(C8)  DELETE
ALLOC DS(DD6) F(FT81F001) NEW SPACE(200,200) BLOCK(8408) +
        USING(C8)  DELETE
ALLOC DS(IN10) F(FT10F001) NEW SPACE(200,200) BLOCK(8408) +
        USING(C8)  DELETE
ALLOC DS(IN11) F(FT11F001) NEW SPACE(200,200) BLOCK(8408) +
        USING(C8)  DELETE
ALLOC DS(SSDATA.DATA) F(FT05F001)
ALLOC DS(OUT.DATA) F(FT06F001) NEW SPACE(200,200) BLOCK(8120) +
        USING(D4)  CATALOG
ALLOC DS(OUT1.DATA) F(FT07F001) NEW SPACE(200,200) BLOCK(8120) +
        USING(D4)  CATALOG
ALLOC DS(OUT2.DATA) F(FT08F001) NEW SPACE(200,200) BLOCK(8120) +
        USING(D4)  CATALOG
ALLOC DS(OUT8.DATA) F(FT09F001) NEW SPACE(200,200) BLOCK(8120) +
        USING(D4)  CATALOG
ALLOC DS(PLTCAT.DATA) F(FT45F001) NEW SPACE(200,200) BLOCK(8120) +
        USING(E5)  CATALOG
ALLOC DS(PLOT.DATA) F(FT16F001) NEW SPACE(200,200) BLOCK(8408) +
        UNIT(TSOWRKB) USING(C8)  CATALOG
ALLOC DS(*)  F(FT20F001)
CONTROL MSG
WRITE
WRITE  DATA SETS HAVE BEEN ALLOCATED.  PROGRAM IS NOW EXECUTING.
TIME
CALL 'ENG.G15.LM(SS) '
WRITE
WRITE  THE PROGRAM HAS FINISHED.
TIME
END
```

TABLE C-6  
I/O FILE ASSIGNMENTS

<u>File Name</u>	<u>No.</u>	<u>File Type</u>	<u>Status</u>	<u>Comments</u>
SSDATA	5	Formatted	INPUT	Problem Input Data
OUT	6	Formatted	OUTPUT	Output For Printer Listing of Habitat Conditions
OUT1	7	Formatted	OUTPUT	Printer Output of Nodal Conditions
OUT2	8	Formatted	OUTPUT	Printer Output of Station Performance
OUT3	9	Formatted	OUTPUT	Printer Output of Station Performance
IN10	10	Unformatted	INPUT	Input File for Data Tape
IN11	11	Unformatted	OUTPUT	Output File for Data Tape
PLOT	16	Formatted	OUTPUT	Plot File for Use with MERIAM
---	20	Formatted	OUTPUT	Special Output to Interactive Terminal
DD5	30	Formatted	Unknown	Used by IEDIT Subroutine
DD6	31	Formatted	OUTPUT	Card Punch File (Used Only When Punch Card Selected)
DD1	41	Formatted	SCRATCH	File Built in IEDIT, Containing Problem Input Data for Current Run
DD2	42	Unformatted	SCRATCH	File Used for Merging Operations During Creations of Basic Cases Used for Holding K/V Array Data of Basic Case or Restart Case
DD3	43	Unformatted	SCRATCH	File Which Contains the Sorted Component Data Card Images Plus Sort Number for the Basic Case
DD4	44	Unformatted	SCRATCH	File Which Contains the Sorted Table Data Card Images Plus Sort Number for the Basic Case
PLTCAT	45	Unformatted	OUTPUT	File for Storing Data to be Plotted With CAET/MS Plot Program

#### C.4.1.2 Input Data SSDATA Description

The input data for the Space Station simulation model is shown in Table C-7. The data set is divided into five sections. The first section contains user options and initial conditions for the habitat and laboratory air. These are located up front for ease of the user to make selections.

The second section contains the KBAS cards for all components in the system except for ECLS equipment like an O<sub>2</sub> generator. The KBAS card defines the subroutine for analyzing the component, the components which provide film to the component, and the next component to be solved in the solution path.

The third section contains all the other cards for all components in the system except for ECLS equipment. These are the ID, NSTR, KARY, and VARY cards.

The forth section is the library of all ECLS components. These components to date in the library are:

CO<sub>2</sub> Reduction

. Sabatier

. Bosch

O<sub>2</sub> Generation

. SPE

. SFWES (KOH)

TABLE C-7

## INPUT DATA FOR SPACE STATION MODEL

## INPUT CARD IMAGES LISTED BELOW

```

IOUT =    0  IPRT =    0
      **** NAMELIST, BASIC CASE
TAPE      0
BASIC     1    593    21    2    YEA    MAY
CASE      SPACE STATION ARS SIMULATION MODEL

$CASE1
KPTINV(1)= 1, KPTINV(2)= 5, KPTINV(3)= 10, KPTINV(4)=30,
KCHOUT= 0, KPUNCH= 0, KPRNT= 0, KRUN= 2, KSTEDY= 0,
MAXSLP= 4, MAXSSI= 15, MINSSI= 10, NOLIM=0,
DTIME=60., START= 0.0, TIMEMX=86400.,
TMAX= 500.0, TMIN= 0.0, WTMAX= 1.6E6 $END

$PROP1
CP(1)=1.0, RHO(1)=62.4000, VISC(1)=2.420, WTM(1)=18.016, XK(1)=0.34,
CP(2)=0.2, RHO(2)=0.00045, VISC(2)=0.378, WTM(2)=44.01, XK(2)=0.0098,
CP(3)=3.42, RHO(3)=0.00520, VISC(3)=0.021, WTM(3)=2.016, XK(3)=0.1032,
CP(4)=0.52, RHO(4)=0.04150, VISC(4)=0.026, WTM(4)=16.04, XK(4)=0.0191,
CPCONL=1., CPCONV=0.445, CPCO2=0.2, CPDIL=0.25, CPOXY=0.22, CPTC=0.2,
GAMGAS=1.4, VISGAS=.44, WTMCON=18.016, WTMOIL=28.013, WTMTC=20.,
XKGAS=0.146 $END

ID** 80  1  THE FOLLOWING ARE OPTIONS TO BE SELECTED BY THE USER:
ID** 80  2
KBAS 80  49 11 22      2
NSTR 80  0
      SUBROUTINE OPTIONS
KARY 80 16      0      PROCESS AIR BUS? 1=YES, 0=NO
KARY 80 17      0      CO2 GAS BUS? 0=NONE, 1=INTRAMOD, 2=INTERMOD
KARY 80 18      0      N2 GAS BUS? 1=YES, 0=NO
KARY 80 19      0      H2 GAS BUS? 0=NONE, 1=INTRAMOD
KARY 80 20      1      HABITAT O2 GEN #1 ON? 1=YES, 0=NO
KARY 80 21      1      HABITAT CO2 REMOVAL #1 ON? 1=YES, 0=NO
KARY 80 22      1      HABITAT CO2 REDUCTION #1 ON? 1=YES, 0=NO
KARY 80 23      1      HABITAT CAT OX #1 ON? 1=YES, 0=NO
KARY 80 24      0      HABITAT O2 GEN #2 ON? 1=YES, 0=NO
KARY 80 25      0      HABITAT CO2 REMOVAL #2 ON? 1=YES, 0=NO
KARY 80 26      0      HABITAT CO2 REDUCTION #2 ON? 1=YES, 0=NO
KARY 80 27      0      HABITAT CAT OX #2 ON? 1=YES, 0=NO
KARY 80 28      1      LABORATORY O2 GEN #1 ON? 1=YES, 0=NO
KARY 80 29      1      LABORATORY CO2 REMOVAL #1 ON? 1=YES, 0=NO
KARY 80 30      1      LABORATORY CO2 REDUCTION #1 ON? 1=YES, 0=NO
KARY 80 31      1      LABORATORY CAT OX #1 ON? 1=YES, 0=NO
KARY 80 32      0      LABORATORY O2 GEN #2 ON? 1=YES, 0=NO
KARY 80 33      0      LABORATORY CO2 REMOVAL #2 ON? 1=YES, 0=NO
KARY 80 34      0      LABORATORY CO2 REDUCTION #2 ON? 1=YES, 0=NO
KARY 80 35      0      LABORATORY CAT OX #2 ON? 1=YES, 0=NO
VARY 80 65      5.0    PRINTOFF FREQUENCY, TIMESTEPS PER PRINTOFF
VARY 80 66      70.0    HABITAT GAS MIXTURE: INITIAL TEMPERATURE (F)
VARY 80 67      14.7    HABITAT TOTAL PRESSURE (PSIA)
VARY 80 68      2.8      HABITAT GAS CO2 PRESSURE (MMHG)
VARY 80 69      50.0    HABITAT DEW POINT TEMPERATURE (F)
VARY 80 70      3.09    HABITAT O2 PARTIAL PRESSURE (PSIA)
VARY 80 71      70.0    LABORATORY GAS MIXTURE: INITIAL TEMP (F)
VARY 80 72      14.7    LABORATORY TOTAL PRESSURE (PSIA)
VARY 80 73      2.5      LABORATORY GAS CO2 PRESSURE (MMHG)
VARY 80 74      50.0    LABORATORY DEW POINT TEMPERATURE (F)
VARY 80 75      3.09    LABORATORY O2 PARTIAL PRESSURE (PSIA)
KBAS  1      1 26      3 2 3      -8 2 3      7 1

```

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

KBAS	2	1	26	4	2	3	-9	2	3	10	2
KBAS	3	2	1	165	2	3				2	1
KBAS	4	2	1	365	2	3				18	2
KBAS	5	6		1	2	3	-42	2	3	216	1
KBAS	6	6		2	2	3	-62	2	3	351	2
KBAS	7	10		-1	2	3				13	1
KBAS	8	6		52	2	3	-42	2	3	151	1
KBAS	9	6		72	2	3	-62	2	3	351	2
KBAS	10	10		-2	2	3				15	2
KBAS	13	23		7	2	3				14	1
KBAS	14	23		-7	2	3				40	1
KBAS	15	23		10	2	3				16	2
KBAS	16	23		-10	2	3				60	2
KBAS	17	10		28	2	3				21	1
KBAS	18	6		195	2	3	-395	2	3	31	1
KBAS	19	10		18	2	3				31	1
KBAS	20	6		19	2	3	-28	2	3	17	1
KBAS	21	10		30	0	1				1	1
KBAS	22	10		29	2	3				23	2
KBAS	23	10		22	2	3				24	2
KBAS	24	10		23	2	3				1	2
KBAS	25	6		190	2	3	-390	2	3	26	1
KBAS	26	30	4	25	2	3				27	1
KBAS	27	10		26	2	3				1	1
KBAS	28	30		31	2	3				17	1
KBAS	29	49									
KBAS	30	49	1								
KBAS	31	10		18	2	3				28	1
KBAS	40	6		73	2	3	-516	2	3	41	1
KBAS	41	6		14	2	3	-40	2	3	42	1
KBAS	42	10		41	2	3				50	1
KBAS	50	6		13	2	3	-517	2	3	51	1
KBAS	51	6		50	2	3	-63	2	3	52	1
KBAS	52	10		51	2	3				8	1
KBAS	60	6		16	2	3	-518	2	3	61	2
KBAS	61	6		60	2	3	52	2	3	62	2
KBAS	62	10		61	2	3				63	2
KBAS	63	23		-62	2	3				70	2
KBAS	70	6		519	2	3	42	2	3	71	2
KBAS	71	6		15	2	3	-70	2	3	72	2
KBAS	72	10		71	2	3				73	2
KBAS	73	23		-72	2	3				9	2
KBAS	90	10		103	2	3				107	1
KBAS	91	80	1	107	2	3	-500	0	1	92	1
KBAS	92	10	7	91	2	3				93	1
KBAS	93	49	2	-92	2	3				105	1
KBAS	94	6		105	2	3	-93	2	3	95	1
KBAS	95	6		94	2	3	90	2	3	104	1
KBAS	96	10		104	2	3				108	1
KBAS	97	80	1	108	2	3	-501	0	1	98	1
KBAS	98	10	7	97	2	3				99	1
KBAS	99	49	2	-98	2	3				106	1
KBAS	100	6		106	2	3	-99	2	3	102	1
KBAS	102	6		100	2	3	96	2	3	153	1
KBAS	103	23		152	2	3				90	1
KBAS	104	23		-152	2	3				96	1
KBAS	105	10		92	2	3				94	1
KBAS	106	10		98	2	3				100	1
KBAS	107	6		90	2	3	-216	2	3	91	1
KBAS	108	6		96	2	3	-162	2	3	97	1



TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

KBAS 111	75	2	-155	2	3				112	1
KBAS 112	75	2	-156	2	3				216	1
KBAS 151	10		1	2	3				152	1
KBAS 152	10		151	2	3				103	1
KBAS 153	6		95	2	3	-102	2	3	154	1
KBAS 154	10		153	2	3				155	1
KBAS 155	10		-105	2	3				156	1
KBAS 156	10		-106	2	3				163	1
KBAS 157	6		180	2	3	-158	2	3	159	1
KBAS 158	10		-179	2	3				111	1
KBAS 159	6		178	2	3	158	2	3	111	1
KBAS 160	6		111	2	3	-112	2	3	161	1
KBAS 161	6		154	2	3	-160	2	3	165	1
KBAS 162	6		133	2	3	-112	2	3	165	1
KBAS 163	10		-151	2	3				218	1
KBAS 164	6		121	2	3	-123	2	3	170	1
KBAS 165	6		154	2	3	-164	2	3	3	1
KBAS 166	6		183	2	3	-167	2	3	168	1
KBAS 167	10		186	2	3				121	1
KBAS 168	6		184	2	3	167	2	3	121	1
KBAS 170	7		121	0	1	-123	0	1	111	1
KBAS 172	10	7	-123	3	3 4				174	1
KBAS 173	10	7	170	3	3 4				177	1
KBAS 174	10	7	-121	3	3 4				176	1
KBAS 176	6		-174	3	3 4	172	3	3 4	177	1
KBAS 177	10	12	170	3	3 4	0	1		111	1
KBAS 178	6		172	3	3 4	201	2	3	180	1
KBAS 179	6		173	3	3 4	200	2	3	156	1
KBAS 180	6		174	3	3 4	199	2	3	158	1
KBAS 181	10		-22	2	3				182	1
KBAS 182	10		181	2	3				194	1
KBAS 183	6		187	2	3	182	2	3	184	1
KBAS 184	6		185	2	3	-182	2	3	121	1
KBAS 185	6		136	2	3	205	2	3	187	1
KBAS 186	6		213	2	3	206	2	3	163	1
KBAS 187	6		135	2	3	207	2	3	121	1
KBAS 188	6		213	2	3				167	1
KBAS 190	10		213	2	3				188	1
KBAS 194	10		-181	2	3				141	1
KBAS 195	6		141	2	3	-143	2	3	202	1
KBAS 197	6		-141	2	3	143	2	3	203	1
KBAS 199	10		-141	2	3				201	1
KBAS 200	10		197	2	3				203	1
KBAS 201	10		-143	2	3				202	1
KBAS 202	10		-141	2	3				204	1
KBAS 203	10		197	2	3				206	1
KBAS 204	10		-143	2	3				205	1
KBAS 205	10		204	2	3				207	1
KBAS 206	10		203	2	3				131	1
KBAS 207	10		202	2	3				131	1
KBAS 209	10		206	2	3				131	1
KBAS 213	6		131	2	3	-133	2	3	220	1
KBAS 216	6		131	2	3	-111	2	3	162	1
KBAS 217	10		218	0	1				219	1
KBAS 218	10		21	0	1				217	1
KBAS 219	10		-218	0	1				141	1
KBAS 220	30	4	213	2	3				186	1
KBAS 290	10		303	2	3				307	2
KBAS 291	80	1	307	2	3	-508	0	1	292	2
KBAS 292	10	7	291	2	3				293	2

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

KBAS 293	49	2	-292	2	3				305	2
KBAS 294	6		305	2	3				295	2
KBAS 295	6		294	2	3	-293	2	3	304	2
KBAS 296	10	7	304	2	3	290	2	3	308	2
KBAS 297	80	1	308	2	3				298	2
KBAS 298	10	7	297	2	3	-509	0	1	299	2
KBAS 299	49	2	-298	2	3				306	2
KBAS 300	6		306	2	3	-299	2	3	302	2
KBAS 302	6		300	2	3	296	2	3	353	2
KBAS 303	23		352	2	3				290	2
KBAS 304	23		-352	2	3				296	2
KBAS 305	10		292	2	3				294	2
KBAS 306	10		298	2	3				300	2
KBAS 307	6		290	2	3	-416	2	3	291	2
KBAS 308	6		296	2	3	-362	2	3	297	2
KBAS 311	75	2	-355	2	3				312	2
KBAS 312	75	2	-356	2	3				416	2
KBAS 351	10		2	2	3				352	2
KBAS 352	10		351	2	3				303	2
KBAS 353	6		295	2	3	-302	2	3	354	2
KBAS 354	10		353	2	3				355	2
KBAS 355	10		-305	2	3				356	2
KBAS 356	10		-306	2	3				363	2
KBAS 357	6		380	2	3	-358	2	3	359	2
KBAS 358	10		-379	2	3				311	2
KBAS 359	6		378	2	3	358	2	3	311	2
KBAS 360	6		311	2	3	-312	2	3	361	2
KBAS 361	6		354	2	3	-360	2	3	365	2
KBAS 362	6		333	2	3	-312	2	3	365	2
KBAS 363	10		-351	2	3				418	2
KBAS 364	6		321	2	3	-323	2	3	370	2
KBAS 365	6		354	2	3	-364	2	3	4	2
KBAS 366	6		383	2	3	-367	2	3	368	2
KBAS 367	10		386	2	3				321	2
KBAS 368	6		384	2	3	367	2	3	321	2
KBAS 370	7		321	0	1	-323	0	1	311	2
KBAS 372	10	7	-323	3	3 4				374	2
KBAS 373	10	7	370	3	3 4				377	2
KBAS 374	10	7	-321	3	3 4				376	2
KBAS 376	6		-374	3	3 4	372	3	3 4	377	2
KBAS 377	10	12	370	3	3 4	0	1		311	2
KBAS 378	6		372	3	3 4	401	2	3	380	2
KBAS 379	6		373	3	3 4	400	2	3	356	2
KBAS 380	6		374	3	3 4	399	2	3	358	2
KBAS 381	10	7	-24	2	3				382	2
KBAS 382	10	7	381	2	3				394	2
KBAS 383	6		387	2	3	382	2	3	384	2
KBAS 384	6		385	2	3	-382	2	3	321	2
KBAS 385	6		336	2	3	405	2	3	387	2
KBAS 386	6		413	2	3	406	2	3	383	2
KBAS 387	6		335	2	3	407	2	3	321	2
KBAS 388	6		413	2	3				367	2
KBAS 390	10		413	2	3				388	2
KBAS 394	10		-381	2	3				341	2
KBAS 395	6		341	2	3	-343	2	3	402	2
KBAS 397	6		-341	2	3	343	2	3	403	2
KBAS 399	10		-341	2	3				401	2
KBAS 400	10		397	2	3				403	2
KBAS 401	10		-343	2	3				402	2
KBAS 402	10		-341	2	3				404	2

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

KBAS 403	10		397 2 3		406	2
KBAS 404	10		-343 2 3		405	2
KBAS 405	10		404 2 3		407	2
KBAS 406	10		403 2 3		331	2
KBAS 407	10		402 2 3		331	2
KBAS 409	10		406 2 3		331	2
KBAS 413	6		331 2 3	-333 2 3	386	2
KBAS 416	6		331 2 3	-311 2 3	362	2
KBAS 417	10		418 0 1		419	2
KBAS 418	10		-21 0 1		417	2
KBAS 419	10		-418 0 1		341	2
KBAS 420	30	4	413 2 3		386	2
KBAS 500	49		-91 0 1			
KBAS 501	49		-97 0 1			
KBAS 502	49		-121 0 1			
KBAS 503	49		-123 0 1			
KBAS 504	49		132 0 1			
KBAS 505	49		134 0 1			
KBAS 506	49		142 0 1			
KBAS 507	49		144 0 1			
KBAS 508	49		-291 0 1			
KBAS 509	49		-297 0 1			
KBAS 510	49		-321 0 1			
KBAS 511	49		-323 0 1			
KBAS 512	49		332 0 1			
KBAS 513	49		334 0 1			
KBAS 514	49		342 0 1			
KBAS 515	49		344 0 1			
KBAS 516	49					
KBAS 517	49					
KBAS 518	49					
KBAS 519	49					
ID**	1	CABIN - SPACE STATION HABITAT				
NSTR	1	151011000	0	PRI P, 5 RESETS, SPECIFY NET FLOWS		
VARY	1	2	CABIN GAS MIXTURE: INITIAL TEMPERATURE			
VARY	1	3	4	TOTAL PRESSURE (PSIA)		
VARY	1	6	H2O VAPOR FLOW (LB/HR)			
VARY	1	10	OXYGEN FLOW (LBM/HR)			
VARY	1	11	NITROGEN FLOW (LBM/HR)			
VARY	1	12	CO2 FLOW (LBM/HR)			
VARY	1	21	CABIN GAS MIXTURE: INITIAL TEMPERATURE			
VARY	1	22	4	TOTAL PRESSURE (PSIA)		
VARY	1	25	H2O VAPOR FLOW (LB/HR)			
VARY	1	29	OXYGEN FLOW (LBM/HR)			
VARY	1	30	NITROGEN FLOW (LBM/HR)			
VARY	1	31	CO2 FLOW (LBM/HR)			
VARY	1	65	TOTAL HEAT ADDED TO CABIN GAS MIX (BTU/HR)			
VARY	1	66	6826.	NON ECLS HEAT LOAD (BTU/HR)		
VARY	1	71	HEAT LOSS DUE TO OUTBOARD LEAKAGE (BTU/HR)			
VARY	1	72	HEAT GAIN DUE TO MASS ADDITIONS (BTU/HR)			
VARY	1	73	HEAT REQD TO FLASH ENTRAINED H2O(BTU/HR)			
VARY	1	74	FLASH EVAP RATE OF ENTRAINED H2O (LBM/HR)			
VARY	1	87	70.0	CABIN GAS DESIGN TEMP (DEGF)		
VARY	1	88	15.0	CABIN GAS DESIGN TEMP TOL. (F)		
VARY	1	89	CABIN GAS RELATIVE HUMIDITY (DECIMAL)			
VARY	1	90	14.7	DESIGN TOTAL PRESSURE (PSIA)		
VARY	1	91	2.0	DESIGN TOTAL PRESSURE TOLERANCE (PSIA)		
VARY	1	92	2.9	DESIGN OXYGEN PRESSURE (PSIA)		
VARY	1	93	1.0	DESIGN OXYGEN PRESSURE TOL (PSIA)		
VARY	1	94	CABIN GAS OXYGEN PRESSURE (PSIA)			

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY	1	95	CABIN GAS NITROGEN PRESSURE (PSIA)
VARY	1	96	50.0 DESIGN DEM PT (F)
VARY	1	97	25.0 DESIGN DEM POINT TOL (F)
VARY	1	98	CABIN GAS DEM POINT
VARY	1	99	10.0 MAX ALLOWABLE CO2 PRESSURE (MM-HG)
VARY	1	100	CABIN GAS CO2 PRESSURE (MM-HG)
VARY	1	101	250.0 MAX ALLOWABLE TRACE CONTAMINENT LEVEL (PPM)
VARY	1	102	CABIN GAS TRACE CONTAMINENT LEVEL (PPM)
VARY	1	103	CABIN GAS MIXTURE, TOTAL MASS (LBM)
VARY	1	104	CABIN GAS MIXTURE, TEMPERATURE (F)
VARY	1	105	CABIN GAS MIXTURE, TOTAL PRESSURE (PSIA)
VARY	1	107	CABIN GAS MIXTURE, NON-CONDENSABLES MASS
VARY	1	108	CABIN GAS MIXTURE, H2O VAPOR MASS (LBM)
VARY	1	109	CABIN GAS MIXTURE, ENTRAINED H2O MASS (LBM)
VARY	1	110	CABIN GAS MIXTURE, NON-COND SPECIFIC HEAT
VARY	1	111	CABIN GAS MIXTURE, NON-COND MOLECULAR WT.
VARY	1	112	CABIN GAS MIXTURE, OXYGEN MASS (LBM)
VARY	1	113	CABIN GAS MIXTURE, NITROGEN MASS (LBM)
VARY	1	114	CABIN GAS MIXTURE, CO2 MASS (LBM)
VARY	1	115	CABIN GAS MIXTURE, TRACE CONTAMINENTS MASS
VARY	1	122	.104167 OUTBOARD LEAKAGE RATE (LBM/HR)
VARY	1	123	NON-CONDENSABLES LEAKAGE RATE (LBM/HR)
VARY	1	124	H2O VAPOR LEAKAGE RATE (LBM/HR)
VARY	1	125	ENTRAINED H2O LEAKAGE RATE (LBM/HR)
VARY	1	126	TOTAL MASS ADDITION RATE (LBM/HR)
VARY	1	127	NON-CONDENSABLES ADDITION RATE (LBM/HR)
VARY	1	128	0.0 H2O VAPOR ADDITION RATE (LBM/HR)
VARY	1	129	0.0 ENTRAINED H2O ADDITION RATE (LBM/HR)
VARY	1	130	AVERAGE TEMPERATURE OF MASS ADDITIONS (F)
VARY	1	132	70.0 ADD COND VAPOR TEMP (F)
VARY	1	135	NET TOTAL FLOW INTO CABIN (LBM/HR)
VARY	1	136	NET NON-COND FLOW INTO CABIN (LBM/HR)
VARY	1	137	NET H2O FLOW INTO CABIN - GPOLY CALC
VARY	1	139	10000. CABIN FREE VOLUME (FT-3)
VARY	1	170	70.0 OXYGEN ADDITION TEMP (F)
VARY	1	171	70.0 NITROGEN ADDITION TEMP (F)
VARY	1	172	70.0 CO2 ADDITION TEMP (F)
VARY	1	173	70.0 TRACE CONTAMINENT ADDITION TEMP (F)
VARY	1	174	70.0 SPECIAL FLOW NO.1 ADDITION TEMP (F)
VARY	1	175	NET O2 ADDITION (LBM/HR)-GPOLY2 CALC
VARY	1	176	NET N2 ADDITION (LBM/HR)-GPOLY2 CALC
VARY	1	177	0.0 NET CO2 ADDITION (LBM/HR)-GPOLY2 CALC
VARY	1	178	0.0 NET TRACE CONTAMINENT ADDITION (LBM/HR)
VARY	1	179	0.0 NET SPECIAL FLOW 1 ADDITION (LBM/HR)
VARY	1	180	0.0 O2/N2 REG FLAG = 0.0 IF O2 USED LAST, = 1.0
VARY	1	181	MISSION TIME (SEC)
VARY	1	182	MISSION TIME (MIN)
ID**	2		CABIN - SPACE STATION LABORATORY
NSTR	2	151011000	PRI P, 5 RESETS, SPECIFY NET FLOWS
VARY	2	2	CABIN GAS MIXTURE: INITIAL TEMPERATURE
VARY	2	3	4 TOTAL PRESSURE (PSIA)
VARY	2	6	H2O VAPOR FLOW (LB/HR)
VARY	2	10	OXYGEN FLOW (LBM/HR)
VARY	2	11	NITROGEN FLOW (LBM/HR)
VARY	2	12	CO2 FLOW (LBM/HR)
VARY	2	21	CABIN GAS MIXTURE: INITIAL TEMPERATURE
VARY	2	22	4 TOTAL PRESSURE (PSIA)
VARY	2	25	H2O VAPOR FLOW (LB/HR)
VARY	2	29	OXYGEN FLOW (LBM/HR)
VARY	2	30	NITROGEN FLOW (LBM/HR)

TABLE C-7 (CONTINUED)

VARY	2	31		CO2 FLOW (LBM/HR)
VARY	2	65		TOTAL HEAT ADDED TO CABIN GAS MIX (BTU/HR)
VARY	2	66	6826.	NON ECLS HEAT LOAD (BTU/HR)
VARY	2	71		HEAT LOSS DUE TO OUTBOARD LEAKAGE (BTU/HR)
VARY	2	72		HEAT GAIN DUE TO MASS ADDITIONS (BTU/HR)
VARY	2	73		HEAT REQD TO FLASH ENTRAINED H2O(BTU/HR)
VARY	2	74		FLASH EVAP RATE OF ENTRAINED H2O (LBM/HR)
VARY	2	87	70.0	CABIN GAS DESIGN TEMP (DEGF)
VARY	2	88	15.0	CABIN GAS DESIGN TEMP TOL. (F)
VARY	2	89		CABIN GAS RELATIVE HUMIDITY (DECIMAL)
VARY	2	90	14.7	DESIGN TOTAL PRESSURE (PSIA)
VARY	2	91	2.0	DESIGN TOTAL PRESSURE TOLERANCE (PSIA)
VARY	2	92	2.9	DESIGN OXYGEN PRESSURE (PSIA)
VARY	2	93	1.0	DESIGN OXYGEN PRESSURE TOL (PSIA)
VARY	2	94		CABIN GAS OXYGEN PRESSURE (PSIA)
VARY	2	95		CABIN GAS NITROGEN PRESSURE (PSIA)
VARY	2	96	50.0	DESIGN DEM PT (F)
VARY	2	97	25.0	DESIGN DEM POINT TOL (F)
VARY	2	98		CABIN GAS DEM POINT
VARY	2	99	10.0	MAX ALLOWABLE CO2 PRESSURE (MM-HG)
VARY	2	100		CABIN GAS CO2 PRESSURE (MM-HG)
VARY	2	101	250.0	MAX ALLOWABLE TRACE CONTAMINENT LEVEL (PPM)
VARY	2	102		CABIN GAS TRACE CONTAMINENT LEVEL (PPM)
VARY	2	103		CABIN GAS MIXTURE, TOTAL MASS (LBM)
VARY	2	104		CABIN GAS MIXTURE, TEMPERATURE (F)
VARY	2	105		CABIN GAS MIXTURE, TOTAL PRESSURE(PSIA)
VARY	2	107		CABIN GAS MIXTURE, NON-CONDENSABLES MASS
VARY	2	108		CABIN GAS MIXTURE, H2O VAPOR MASS (LBM)
VARY	2	109		CABIN GAS MIXTURE, ENTRAINED H2O MASS (LBM)
VARY	2	110		CABIN GAS MIXTURE, NON-COND SPECIFIC HEAT
VARY	2	111		CABIN GAS MIXTURE, NON-COND MOLECULAR WT.
VARY	2	112		CABIN GAS MIXTURE, OXYGEN MASS(LBM)
VARY	2	113		CABIN GAS MIXTURE, NITROGEN MASS (LBM)
VARY	2	114		CABIN GAS MIXTURE, CO2 MASS (LBM)
VARY	2	115		CABIN GAS MIXTURE, TRACE CONTAMINENTS MASS
VARY	2	122	.104167	OUTBOARD LEAKAGE RATE (LBM/HR)
VARY	2	123		NON-CONDENSABLES LEAKAGE RATE (LBM/HR)
VARY	2	124		H2O VAPOR LEAKAGE RATE (LBM/HR)
VARY	2	125		ENTRAINED H2O LEAKAGE RATE (LBM/HR)
VARY	2	126		TOTAL MASS ADDITION RATE (LBM/HR)
VARY	2	127		NON-CONDENSABLES ADDITION RATE (LBM/HR)
VARY	2	128	0.0	H2O VAPOR ADDITION RATE (LBM/HR)
VARY	2	129	0.0	ENTRAINED H2O ADDITION RATE (LBM/HR)
VARY	2	130		AVERAGE TEMPERATURE OF MASS ADDITIONS (F)
VARY	2	132	70.0	ADD COND VAPOR TEMP (F)
VARY	2	135		NET TOTAL FLOW INTO CABIN (LBM/HR)
VARY	2	136		NET NON-COND FLOW INTO CABIN (LBM/HR)
VARY	2	137		NET H2O FLOW INTO CABIN - GPOLY CALC
VARY	2	139	10000.	CABIN FREE VOLUME (FT-3)
VARY	2	170	70.0	OXYGEN ADDITION TEMP (F)
VARY	2	171	70.0	NITROGEN ADDITION TEMP (F)
VARY	2	172	70.0	CO2 ADDITION TEMP (F)
VARY	2	173	70.0	TRACE CONTAMINENT ADDITION TEMP (F)
VARY	2	174	70.0	SPECIAL FLOW NO.1 ADDITION TEMP (F)
VARY	2	175		NET O2 ADDITION (LBM/HR)-GPOLY2 CALC
VARY	2	176		NET N2 ADDITION (LBM/HR)-GPOLY2 CALC
VARY	2	177	0.0	NET CO2 ADDITION(LBM/HR)-GPOLY2 CALC
VARY	2	178	0.0	NET TRACE CONTAMINENT ADDITION (LBM/HR)
VARY	2	179	0.0	NET SPECIAL FLOW 1 ADDITION (LBM/HR)
VARY	2	180	0.0	O2/N2 REG FLAG = 0.0 IF O2 USED LAST, = 1.0

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY	2	181		MISSION TIME (SEC)
VARY	2	182		MISSION TIME (MIN)
ID**	3		SPACE STATION	HABITAT CREW
NSTR	3	0		1 NO TESTS, SS CALC
KARY	3	16	4	NUMBER OF CREWMEN
VARY	3	65		TOTAL METABOLIC HEAT - ALL CREWMEN (BTU/HR)
VARY	3	66		SENSIBLE HEAT LOAD PER CREWMAN(BTU/HR)
VARY	3	67		LATENT HEAT PER CREWMAN (BTU/HR)
VARY	3	68		TOTAL OXYGEN USE RATE (LBM/HR)
VARY	3	69		TOTAL CO2 GENERATION RATE (LBM/HR)
VARY	3	70		TOTAL H2O VAPOR GENERATION RATE (LBM/HR)
VARY	3	75		INLET GAS RELATIVE HUMIDITY (DECIMAL)
VARY	3	76		INLET GAS DEW POINT (F)
VARY	3	77		OUTLET GAS RELATIVE HUMIDITY (DECIMAL)
VARY	3	78		OUTLET GAS DEW POINT (F)
VARY	3	82		TOTAL METABOLIC RATE PER CREWMAN (BTU/HR)
ID**	4		SPACE STATION	LABORATORY CREW
NSTR	4	0		1 NO TESTS, SS CALC
KARY	4	16	4	NUMBER OF CREWMEN
VARY	4	65		TOTAL METABOLIC HEAT - ALL CREWMEN (BTU/HR)
VARY	4	66		SENSIBLE HEAT LOAD PER CREWMAN(BTU/HR)
VARY	4	67		LATENT HEAT PER CREWMAN (BTU/HR)
VARY	4	68		TOTAL OXYGEN USE RATE (LBM/HR)
VARY	4	69		TOTAL CO2 GENERATION RATE (LBM/HR)
VARY	4	70		TOTAL H2O VAPOR GENERATION RATE (LBM/HR)
VARY	4	75		INLET GAS RELATIVE HUMIDITY (DECIMAL)
VARY	4	76		INLET GAS DEW POINT (F)
VARY	4	77		OUTLET GAS RELATIVE HUMIDITY (DECIMAL)
VARY	4	78		OUTLET GAS DEW POINT (F)
VARY	4	82		TOTAL METABOLIC RATE PER CREWMAN (BTU/HR)
ID**	5			GAS MIXER - HABITAT AIR AND SPLIT 12
NSTR	5			
ID**	6			GAS MIXER - LABORATORY AIR AND SPLIT 11
NSTR	6			
ID**	7			SPLITTER - TO FAN 14 AND FAN 13
NSTR	7			
VARY	7	65	0.5	FLOW FRACTION TO FAN 13 AND FAN 14
ID**	8			GAS MIXER - FROM COMP 12 AND NODE 2
NSTR	8			
ID**	9			GAS MIXER - FROM COMP 11 AND NODE 4
NSTR	9			
ID**	10			SPLITTER - TO FAN 14 AND FAN 15
NSTR	10			
VARY	10	65	0.5	FLOW FRACTION TO FAN 14 AND FAN 15
ID**	13			FAN FOR NODAL MIXERS
NSTR	13	1		INPUT CFM AND Q
VARY	13	76	130.0	FAN FLOW (CFM)
VARY	13	84	1.0	FAN ON/OFF SWITCH,(1.0=ON,0.0=OFF)
VARY	13	91	152.0	FAN HEAT ADDITION (WATTS)
ID**	14			FAN FOR NODAL MIXERS
NSTR	14	1		INPUT CFM AND Q
VARY	14	76	130.0	FAN FLOW (CFM)
VARY	14	84	1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)
VARY	14	91	152.0	FAN HEAT ADDITION (WATTS)
ID**	15			FAN FOR NODAL MIXERS
NSTR	15	1		INPUT CFM AND Q
VARY	15	76	130.0	FAN FLOW (CFM)
VARY	15	84	1.0	FAN ON/OFF SWITCH,(1.0=ON,0.0=OFF)
VARY	15	91	152.0	FAN HEAT ADDITION (WATTS)
ID**	16			FAN FOR NODAL MIXERS

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

NSTR	16	1		
VARY	16	76	130.0	FAN FLOW (CFM)
VARY	16	84	1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)
VARY	16	91	152.00	FAN HEAT ADDITION (WATTS)
ID**	17			SPLITTER - O2 BUS FLOW TO HAB AND LAB
NSTR	17			
VARY	17	65	0.5	FLOW FRACTION TO HAB AND LAB
ID**	18			GAS MIXER - O2 BUS MIXER FROM ARS #1 AND #2
NSTR	18			
ID**	19			SPLITTER - TO O2 STORAGE OR TO O2 BUS
NSTR	19			
VARY	19	65	0.0	FLOW FRACTION TO O2 STORAGE AND BUS
ID**	20			GAS MIXER - O2 STORAGE AND RETURN O2 BUS
NSTR	20			
ID**	21			SPLITTER - WATER TO ARS #1 AND ARS #2
NSTR	21			
VARY	21	65	0.5	FLOW FRACTION TO ARS #1 AND ARS #2
ID**	22			SPLITTER - N2 TO ARS #1 AND SPLIT 23
NSTR	22			
VARY	22	65		FLOW FRACTION TO ARS #1 AND SPLIT 23
ID**	23			SPLITTER - N2 TO HABITAT AND SPLIT 24
NSTR	23			
VARY	23	65		FLOW FRACTION TO HABITAT AND SPLIT 24
ID**	24			SPLITTER - N2 TO ARS #2 AND LABORATORY
NSTR	24			
VARY	24	65		SPLIT RATIO TO ARS #2 AND LABORATORY
ID**	25			GAS MIXER - FROM ARS #1 AND ARS #2 CO2 BUS
NSTR	25			
ID**	26			TANK - CO2 STORAGE ACCUMULATOR
NSTR	26	01010		COMPUTE OUTLET FLOW IN GPOLY1
VARY	26	68		TANK MAX CAPACITY (LBM)
VARY	26	69		TANK INITIAL FILL (LBM)
VARY	26	70		TANK FLUID TEMPERATURE (F)
VARY	26	71		TANK VOLUME (FT-3)
VARY	26	72		TANK PRESSURE (PSIA)
VARY	26	92		THERMAL CAPACITANCE OF SHELL (BTU/HR)
VARY	26	94		MAX TEMP CHANGE IN ONE TIME STEP
VARY	26	98		FLUID USED FROM TANK - GPOLY2 CALC.
VARY	26	99		FLUID ADDED TO TANK - GPOLY2 CALC.
VARY	26	100		FLUID FLOW - GPOLY1 CALC.
ID**	27			SPLITTER - CO2 BUS TO ARS #1 AND ARS #2
NSTR	27			
VARY	27	65		FLOW FRACTION TO ARS #1 AND ARS #2
ID**	28			OXYGEN ACCUMULATOR
NSTR	28	01000		FLUID TEMP EQUALS HABITAT TEMP.
VARY	28	69	79.844	TOTAL MASS OF FLUID IN TANK, LBM
VARY	28	70	70.0	FLUID TEMPERATURE IN TANK, F
VARY	28	71	13.5	TANK VOLUME, CUBIC FEET
VARY	28	72	1051.0	FLUID PRESSURE IN TANK, PSIA
VARY	28	78	79.844	MASS OF O2 IN TANK, LBM
ID**	29			ALTCOM - NITROGEN SOURCE
NSTR	29			PASS VALUES UNCHANGED
ID**	30			ALTCOM - H2O SOURCE
NSTR	30			PASS VALUES UNCHANGED
VARY	30	2	45.0	WATER TEMPERATURE, F
VARY	30	3	14.7	4 WATER PRESSURE, PSIA
VARY	30	67	0.0	CUMULATIVE WATER CONSUMED, LBM
ID**	31			SPLITTER - O2 FROM BUS TO STORAGE OR AIR LOCK
NSTR	31			
VARY	31	65	0.0	FLOW FRACTION TO AIR LOCK AND STORAGE

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

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ID** 40      GAS MIXER - NODE 1
NSTR 40
ID** 41      GAS MIXER - NODE 1
NSTR 41
ID** 42      SPLITTER - NODE 1 TO MIXER 12 AND NODE 4
NSTR 42
VARY 42 65    0.5          FLOW FRACTION TO MIXER 12 AND NODE 4(GPOLY
ID** 50      GAS MIXER - NODE 2
NSTR 50
ID** 51      GAS MIXER - NODE 2
NSTR 51
ID** 52      SPLITTER - NODE 2 TO MIXER 8 AND NODE 3
NSTR 52
VARY 52 65    0.5          FLOW FRACTION TO MIXER 8 AND NODE 3(GPOLY C
ID** 60      GAS MIXER - NODE 3
NSTR 60
ID** 61      GAS MIXER - NODE 3
NSTR 61
ID** 62      SPLITTER - NODE 3 TO MIXER 11 AND NODE 2
NSTR 62
VARY 62 65    0.5          FLOW FRACTION TO MIXER 11 AND NODE 2(GPOLY
ID** 63      FAN FOR NODAL MIXERS
NSTR 63      1
VARY 63 76    130.0        FAN FLOW (CFM)
VARY 63 84    1.0          FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)
VARY 63 91    152.0        FAN HEAT ADDITION (WATTS)
ID** 70      GAS MIXER - NODE 4
NSTR 70
ID** 71      GAS MIXER - NODE 4
NSTR 71
ID** 72      SPLITTER - NODE 4 TO MIXER 9 AND NODE 1
NSTR 72
VARY 72 65    0.5          FLOW FRACTION TO MIXER 9 AND NODE 1(GPOLY C
ID** 73      FAN FOR NODAL MIXERS
NSTR 73      1
VARY 73 76    130.0        FAN FLOW (CFM)
VARY 73 84    1.0          FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)
VARY 73 91    152.0        FAN HEAT ADDITION (WATTS)
ID** 90
ID** 90      ARS #1 EQUIPMENT
ID** 90
ID** 90      SPLITTER - CABIN AIR BYPASS TO HX 91 AND MIXER 95
NSTR 90
VARY 90 65    0.5          FLOW FRACTION TO BYPASS AND HX 91(GPOLY CAL
ID** 91      ARS #1 HEAT EXCHANGER #1
NSTR 91      0
KARY 91 16    0          REDUNDANT COOLANT LOOPS? 1=YES, 0=NO
ID** 92      SPLITTER - TO WATER SEP 93
NSTR 92      10          SPLIT RATIOS ARE INPUT
VARY 92 66    0.03         SPLIT RATIO CONDENSABLE VAPOR
VARY 92 67    1.0          SPLIT RATIO CONDENSED LIQUID
VARY 92 68    0.03         SPLIT RATIO OXYGEN
VARY 92 69    0.03         SPLIT RATIO NITROGEN
VARY 92 70    0.03         SPLIT RATIO CARBON DIOXIDE
VARY 92 71    0.03         SPLIT RATIO TRACE CONTAMINANTS
VARY 92 72    0.03         SPLIT RATIO SPECIAL FLOW #1 (HYDROGEN)
ID** 93      WATER SEPARATOR
NSTR 93      2
VARY 93 65    13.1         HEAT ADDED (BTU/HR)
VARY 93 67          CONDENSATE REMOVED, LBM/HR GPOLY1 CALC

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TABLE C-7 (CONTINUED)

INPUT DATA FOR SPACE STATION MODEL

VARY	93	68	0.0	CUMULATIVE H2O REMOVED, LBM GPOLY1 CALC
ID**	94			GAS MIXER - FROM WATER SEP AND HEAT EXCHANGER #1
NSTR	94			
ID**	95			GAS MIXER - BYPASS FLOW AND MIXER 94
NSTR	95			
ID**	96			SPLITTER - CABIN AIR BYPASS TO HX 97 AND MIXER 102
NSTR	96			
VARY	96	65	0.5	FLOW FRACTION TO BYPASS AND HX 97(GPOLY CAL
ID**	97			ARS #1 HEAT EXCHANGER #2
NSTR	97			0
KARY	97	16	0	REDUNDANT COOLANT LOOPS? 1=YES, 0=NO
ID**	98			SPLITTER - TO WATER SEP 99 AND MIXER 100
NSTR	98	10		SPLIT RATIOS ARE INPUT
VARY	98	66	0.03	SPLIT RATIO CONDENSABLE VAPOR
VARY	98	67	1.00	SPLIT RATIO CONDENSED LIQUID
VARY	98	68	0.03	SPLIT RATIO OXYGEN
VARY	98	69	0.03	SPLIT RATIO NITROGEN
VARY	98	70	0.03	SPLIT RATIO CARBON DIOXIDE
VARY	98	71	0.03	SPLIT RATIO TRACE CONTAMINANTS
VARY	98	72	0.03	SPLIT RATIO SPECIAL FLOW #1 (HYDROGEN)
ID**	99			WATER SEPARATOR
NSTR	99	2		
VARY	99	65	13.1	HEAT ADDED (BTU/HR)
VARY	99	67		CONDENSATE REMOVED, LBM/HR GPOLY1 CALC
VARY	99	68	0.0	CUMULATIVE H2O REMOVED, LBM GPOLY1 CALC
ID**	100			GAS MIXER - FROM WATER SEP AND HEAT EXCHANGER #1
NSTR	100			
ID**	102			GAS MIXER - FROM BYPASS 96 AND MIXER 100
NSTR	102			
ID**	103			FAN FOR COOLING PACKAGE #1 (ARS#1)
NSTR	103	1		INPUT CFM AND Q
VARY	103	76	334.0	FAN FLOW (CFM)
VARY	103	84	1.0	FAN ON/OFF SWITCH,(1.0=ON,0.0=OFF)
VARY	103	91	700.0	FAN HEAT ADDITION (WATTS)
ID**	104			FAN FOR COOLING PACKAGE #2 (ARS #1)
NSTR	104	1		INPUT CFM AND Q
VARY	104	76	334.00	FAN FLOW (CFM)
VARY	104	84	1.0	FAN ON/OFF SWITCH,(1.0=ON,0.0=OFF)
VARY	104	91	700.0	FAN HEAT ADDITION (WATTS)
ID**	105			SPLIT AIR FROM COOLING PKG 2 TO CAT.OX AND CO2 REMVL
NSTR	105			
VARY	105	65	0.00	SR TO CAT.OX/CO2 REMVL AND CABIN-GPOLY CALC
ID**	106			SPLIT AIR FROM COOLING PKG 2 TO CAT.OX AND CO2 REMVL
NSTR	106			
VARY	106	65	0.00	SR TO CAT.OX/CO2 REMVL AND CABIN-GPOLY CALC
ID**	107			GAS MIXER CABIN AIR AND CAT.OX/CO2 REMVL EXIT AIR
NSTR	107			0
ID**	108			GAS MIXER CABIN AIR AND CAT.OX/CO2 REMVL EXIT AIR
NSTR	108			0
ID**	111			CATALYTIC OXIDIZER #1
NSTR	111			
VARY	111	65	28.0	CAT. OX. HEATER POWER (WATTS)
VARY	111	66	1.0	CAT. OX. EFFECTIVENESS
VARY	111	67	2.0	MGT OF HIGH TEMP CATALYST BED(LBM)
VARY	111	68	600.0	OPERATING TEMP OF HIGH TEMP CAT. BED (F)
VARY	111	69	0.1111	FRACTION OF TOTAL FLOW TO HIGH TEMP BED
ID**	112			CATALYTIC OXIDIZER #2
NSTR	112			
VARY	112	65	28.0	CAT. OX. HEATER POWER (WATTS)
VARY	112	66	1.0	CAT. OX. EFFECTIVENESS

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 112	67	2.0	MGT OF HIGH TEMP CATALYST BED(LBM)
VARY 112	68	600.0	OPERATING TEMP OF HIGH TEMP CAT. BED (F)
VARY 112	69	0.1111	FRACTION OF TOTAL FLOW TO HIGH TEMP BED
ID** 151			SPLITTER - CABIN AIR TO COOLING PKG AND SPLIT 155
NSTR 151			
VARY 151	65		FLOW FRACTION TO COOLING AND SLIT 155(GPOLY
ID** 152			SPLITTER - COOLING PKG FLOW TO PACKAGE #1 AND #2
NSTR 152			
VARY 152	65	0.5	FLOW FRACTION TO COOLING PKG #1 AND #2
ID** 153			GAS MIXER - FROM COOLING PKG #1 AND #2
NSTR 153			
ID** 154			SPLITTER - TO CABIN AIR OR ANOTHER MODULE
NSTR 154			
VARY 154	65	0.0	FLOW FRACTION TO CABIN AND MODULE
ID** 155			SPLITTER - CABIN AIR TO CAT OX AND CO2 REMOVAL
NSTR 155			
VARY 155	65		SPLIT RATIO CAT OX AND CO2 REMOVAL(GPOLY CA
ID** 156			SPLITTER - COOLING PKG AIR TO CAT OX AND CO2 REMVL
NSTR 156			
VARY 156	65		SPLIT RATIO TO CAT OX AND CO2 REMOVAL(GPOLY
ID** 157			GAS MIXER - CAT OX PACKAGE #1
NSTR 157			
ID** 158			SPLITTER - TO MIXER 157 AND MIXER 159
NSTR 158			
VARY 158	65	0.5	FLOW FRACTION TO CAT OX #1 AND CAT OX #2
ID** 159			GAS MIXER - CAT OX PACKAGE #2
NSTR 159			
ID** 160			GAS MIXER - CAT OX #1 AND PURGE N2
NSTR 160			
ID** 161			GAS MIXER - CAT OX #2 AND PURGE N2
NSTR 161			
ID** 162			GAS MIXER - CAT OX #2 AND CO2 REMOVAL #2 EXIT AIR
NSTR 162			
ID** 163			SPLITTER - TO CO2 REDUCTION PACKAGE #1 AND #2
NSTR 163			
VARY 163	65	0.5	FLOW FRACTION TO CO2 REDUCTION #1 AND #2
ID** 164			GAS MIXER - EXIT AIR FROM CO2 REDUCTION PKGS #1 AND #2
NSTR 164			
ID** 165			GAS MIXER - MIXER 161 AND MIXER 164
NSTR 165			
ID** 166			GAS MIXER - FROM MIXER 183 AND MIXER 187
NSTR 166			
ID** 167			SPLITTER - TO CO2 REDUCTION PKS #1 AND #2
NSTR 167			
VARY 167	65		FLOW FRACTION TO CO2 RED PKGS #1 AND #2
ID** 168			GAS MIXER - FROM MIXER 184 AND MIXER 167
NSTR 168			
ID** 170			LIQ MIXER - FROM CO2 REDUCTION UNITS
NSTR 170			
ID** 172			SPLITTER - TO MIXER 176 AND MIXER 178
NSTR 172			
VARY 172	65		FLOW FRACTION TO MIXER 176 AND MIXER 178
ID** 173			SPLITTER - TO MIXER 179 AND SPLITTER 177
NSTR 173			
VARY 173	65	1.0	FLOW FRACTION TO MIXER 179 AND SPLIT 177
ID** 174			SPLITTER TO MIXER 176 AND MIXER 180
NSTR 174			
VARY 174	65		FLOW FRACTION TO MIXER 176 AND MIXER 180
ID** 176			GAS MIXER - FROM SPLIT 172 AND MIXER 174
NSTR 176			

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

ID** 177	SPLITTER - TO CONDENSATE AND CH <sub>4</sub> STORAGE		
NSTR 177	1		
VARY 177	66	0.0	SPLIT RATIO FOR CONDENSABLE VAPOR FLOW
VARY 177	67	1.0	SPLIT RATIO FOR CONDENSABLE LIQUID FLOW
VARY 177	68	0.0	SPLIT RATIO FOR OXYGEN FLOW
VARY 177	69	0.0	SPLIT RATIO FOR NITROGEN FLOW
VARY 177	70	0.0	SPLIT RATIO FOR CARBON DIOXIDE FLOW
VARY 177	71	0.0	SPLIT RATIO FOR TRACE CONTAMINANT FLOW
VARY 177	72	0.0	SPLIT RATIO FOR SPECIAL FLOW #1, H <sub>2</sub>
VARY 177	73	0.0	SPLIT RATIO FOR SPECIAL FLOW #2, CH <sub>4</sub>
ID** 178	GAS MIXER - FROM SPLIT 172 AND SPLIT 201		
NSTR 178			
ID** 179	GAS MIXER - FROM SPLIT 173 AND SPLIT 200		
NSTR 179			
ID** 180	GAS MIXER - FROM SPLIT 199 AND SPLIT 174		
NSTR 180			
ID** 181	SPLITTER - N <sub>2</sub> TO SPLIT 182 AND TO SPLIT 194		
NSTR 181			
VARY 181	65		FLOW FRACTION TO SPLIT 182 AND SPLIT 194
ID** 182	SPLITTER - NITROGEN TO MIXER 183 AND MIXER 184		
NSTR 182			
VARY 182	65		FLOW FRACTION TO MIXER 183 AND MIXER 184
ID** 183	GAS MIXER - N <sub>2</sub> FROM MIXER 187 AND SPLIT 182		
NSTR 183			
ID** 184	GAS MIXER - N <sub>2</sub> FROM MIXER 185 AND SPLIT 182		
NSTR 184			
ID** 185	GAS MIXER - CO <sub>2</sub> FROM CO <sub>2</sub> REM. PKG #2 AND H <sub>2</sub> FROM SPLIT 205		
NSTR 185			
ID** 186	GAS MIXER - FROM CO <sub>2</sub> ACCUMULATOR AND H <sub>2</sub> FROM SPLIT 206		
NSTR 186			
ID** 187	GAS MIXER - CO <sub>2</sub> FROM SPLIT 131 AND H <sub>2</sub> FROM SPLIT 207		
NSTR 187			
ID** 188	GAS MIXER - CO <sub>2</sub> FROM CO <sub>2</sub> BUS AND SPLIT 190		
NSTR 188			
ID** 190	SPLITTER - CO <sub>2</sub> TO MIXER 188 AND CO <sub>2</sub> BUS		
NSTR 190			
VARY 190	65		FLOW FRACTION TO MIXER 188 AND CO <sub>2</sub> BUS
ID** 194	SPLITTER - N <sub>2</sub> TO O <sub>2</sub> GEN PKG #1 AND PKG #2		
NSTR 194			
VARY 194	65		FLOW FRACTION TO O <sub>2</sub> GEN PKG #1 AND #2
ID** 195	GAS MIXER - O <sub>2</sub> FROM O <sub>2</sub> GEN PKG #1 AND #2		
NSTR 195			
ID** 197	GAS MIXER - H <sub>2</sub> OR N <sub>2</sub> FROM O <sub>2</sub> GEN PKGS #1 AND #2		
NSTR 197			
ID** 199	SPLITTER - N <sub>2</sub> TO MIXER 180 OR H <sub>2</sub> TO SPLIT 202		
NSTR 199			
VARY 199	65		FLOW FRACTION TO MIXER 180 OR SPLIT 202
ID** 200	SPLITTER - N <sub>2</sub> TO MIXER 179 OR H <sub>2</sub> TO SPLIT 203		
NSTR 200			
VARY 200	65		FLOW FRACTION TO MIXER 179 OR SPLIT 203
ID** 201	SPLITTER - N <sub>2</sub> TO MIXER 178 OR H <sub>2</sub> TO SPLIT 204		
NSTR 201			
VARY 201	65		FLOW FRACTION TO MIXER 178 OR SPLIT 204
ID** 202	SPLITTER - H <sub>2</sub> TO VENT AND SPLIT 207		
NSTR 202			
VARY 202	65	0.0	FLOW FRACTION TO VENT AND SPLIT 207
ID** 203	SPLITTER - H <sub>2</sub> TO VENT AND SPLIT 206		
NSTR 203			
VARY 203	65		FLOW FRACTION TO VENT AND SPLIT 206
ID** 204	SPLITTER - H <sub>2</sub> TO VENT AND SPLIT 205		

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

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NSTR 204
VARY 204 65 0.0 FLOW FRACTION TO VENT AND SPLIT 206
ID** 205 SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 205
VARY 205 65 1.0 SPLIT RATIO CO2 RED AND CO2 REMOVAL(GPOLY C
ID** 206 SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 206
VARY 206 65 FLOW FRACTION TO CO2 RED AND CO2 REMOVAL
ID** 207 SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 207
VARY 207 65 1.0 SPLIT RATIO CO2 RED AND CO2 REMOVAL(GPOLY C
ID** 209 SPLITTER - H2 TO CO2 REMOVAL PKG #1 AND #2
NSTR 209
VARY 209 65 FLOW FRACTION TO CO2 REMOVAL PKG #1 AND #2
ID** 213 GAS MIXER - CO2 FROM CO2 REMOVAL PKGS #1 AND #2
NSTR 213
ID** 216 GAS MIXER - CABIN AIR AND CO2 REMOVAL EXIT
NSTR 216
ID** 217 SPLITTER - H2O TO O2 GENERATION PKG #1 AND #2
NSTR 217
VARY 217 65 0.5 FLOW FRACTION TO O2 GEN PKG #1 AND #2
ID** 218 SPLITTER - H2O TO O2 GENERATION AND CO2 REMOVAL
NSTR 218
VARY 218 65 0.0 FLOW TO O2 GENERATION AND CO2 REMOVAL
ID** 219 SPLITTER - H2O TO CO2 REMOVAL PKG #1 AND #2
NSTR 219
VARY 219 65 0.5 FLOW FRACTION TO CO2 REMOVAL #1 AND #2
ID** 220 TANK - CO2 STORAGE ACCUMULATOR
NSTR 220 01010 COMPUTE OUTLET FLOW IN GPOLY1
VARY 220 68 TANK MAX CAPACITY (LBM)
VARY 220 69 TANK INITIAL FILL (LBM)
VARY 220 70 TANK FLUID TEMPERATURE (F)
VARY 220 71 TANK VOLUME (FT-3)
VARY 220 72 TANK PRESSURE (PSIA)
VARY 220 92 THERMAL CAPACITANCE OF SHELL (BTU/HR)
VARY 220 94 MAX TEMP CHANGE IN ONE TIME STEP
VARY 220 98 FLUID USED FROM TANK - GPOLY2 CALC.
VARY 220 99 FLUID ADDED TO TANK - GPOLY2 CALC.
VARY 220 100 FLUID FLOW - GPOLY1 CALC.
ID** 290
ID** 290 ARS #2 EQUIPMENT
ID** 290
ID** 290 SPLITTER - CABIN AIR BYPASS TO HX 291 AND MIXER 295
NSTR 290
VARY 290 65 0.500 SPLIT RATIO BYPASS AND HX 291-GPOLY CALC
ID** 291 ARS #2 HEAT EXCHANGER #1
NSTR 291
KARY 291 16 0 REDUNDANT COOLANT LOOPS? 1=YES, 0=NO
ID** 292 SPLITTER - TO WATER SEP 293
NSTR 292 10 SPLIT RATIOS ARE INPUT
VARY 292 66 0.030 SPLIT RATIO WATER VAPOR
VARY 292 67 1.000 SPLIT RATIO CONDENSED WATER
VARY 292 68 0.030 SPLIT RATIO OXYGEN
VARY 292 69 0.030 SPLIT RATIO NITROGEN
VARY 292 70 0.030 SPLIT RATIO CARBON DIOXIDE
VARY 292 71 0.030 SPLIT RATIO TRACE CONTAMINANTS
VARY 292 72 0.030 SPLIT RATIO HYDROGEN
ID** 293 WATER SEPARATOR
NSTR 293 2
VARY 293 65 13.10 WATER SEPARATOR HEAT LOAD (BTU/HR)

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TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 293	67		CONDENSATE REMOVED, PPH GPOLY1 CALC
VARY 293	68	0.00	CUMULATIVE H2O REMOVED, LBM GPOLY1 CALC
ID** 294			GAS MIXER - FROM WATER SEP AND HEAT EXCHANGER #1
NSTR 294			
ID** 295			GAS MIXER - BYPASS FLOW AND MIXER 294
NSTR 295			
ID** 296			SPLITTER - CABIN AIR BYPASS TO HX 297 AND MIXER 302
NSTR 296			
VARY 296	65	0.500	SPLIT RATIO BYPASS AND HX 297-GPOLY CALC
ID** 297			ARS #2 HEAT EXCHANGER #2
NSTR 297			
KARY 297	16	0	REDUNDANT COOLANT LOOPS? 1=YES, 0=NO
ID** 298			SPLITTER - TO WATER SEP 299
NSTR 298	10		SPLIT RATIOS ARE INPUT
VARY 298	66	0.030	SPLIT RATIO WATER VAPOR
VARY 298	67	1.000	SPLIT RATIO CONDENSED WATER
VARY 298	68	0.030	SPLIT RATIO OXYGEN
VARY 298	69	0.030	SPLIT RATIO NITROGEN
VARY 298	70	0.030	SPLIT RATIO CARBON DIOXIDE
VARY 298	71	0.030	SPLIT RATIO TRACE CONTAMINANTS
VARY 298	72	0.030	SPLIT RATIO HYDROGEN
ID** 299			WATER SEPARATOR
NSTR 299	2		
VARY 299	65	13.10	WATER SEPARATOR HEAT LOAD (BTU/HR)
VARY 299	67		CONDENSATE REMOVED, PPH GPOLY1 CALC
VARY 299	68	0.0	CUMULATIVE H2O REMOVED, LBM GPOLY1 CALC
ID** 300			GAS MIXER - FROM WATER SEP AND HEAT EXCHANGER #1
NSTR 300			
ID** 302			GAS MIXER - FROM BYPASS 296 AND MIXER 300
NSTR 302			
ID** 303			FAN FOR COOLING PACKAGE #1 (ARS#2)
NSTR 303	1		INPUT CFM AND Q
VARY 303	76	334.0	FAN FLOW (CFM)
VARY 303	84	1.0	FAN ON/OFF SWITCH, (1.0=ON, 0.0=OFF)
VARY 303	91	700.00	FAN HEAT ADDITION (WATTS)
ID** 304			FAN FOR COOLING PACKAGE #2 (ARS #2)
NSTR 304	1		INPUT CFM AND Q
VARY 304	76	334.00	FAN FLOW (CFM)
VARY 304	84	1.0	FAN ON/OFF SWITCH, (1.0=ON, 0.0=OFF)
VARY 304	91	700.00	FAN HEAT ADDITION (WATTS)
ID** 305			SPLIT AIR FROM COOLING PKG 2 TO CAT.OX AND CO2 REMVL
NSTR 305			
VARY 305	65	0.00	SR TO CAT.OX/CO2 REMVL AND CABIN-GPOLY CALC
ID** 306			SPLIT AIR FROM COOLING PKG 2 TO CAT.OX AND CO2 REMVL
NSTR 306			
VARY 306	65	0.00	SR TO CAT.OX/CO2 REMVL AND CABIN-GPOLY CALC
ID** 307			GAS MIXER CABIN AIR AND CAT.OX/CO2 REMVL EXIT AIR
NSTR 307			
ID** 308			GAS MIXER CABIN AIR AND CAT.OX/CO2 REMVL EXIT AIR
NSTR 308			
ID** 311			CATALYTIC OXIDIZER #1
NSTR 311			
VARY 311	65	28.00	CAT. OX. HEATER POWER (WATTS)
VARY 311	66	1.00	CAT. OX. EFFECTIVENESS
VARY 311	67	2.00	MGT OF HIGH TEMP CATALYST BED(LBM)
VARY 311	68	600.0	OPERATING TEMP OF HIGH TEMP CAT. BED (F)
VARY 311	69	0.1111	FRACTION OF TOTAL FLOW TO HIGH TEMP BED
ID** 312			CATALYTIC OXIDIZER #2
NSTR 312			
VARY 312	65	28.00	CAT. OX. HEATER POWER (WATTS)

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 312	66	1.00	CAT. OX. EFFECTIVENESS
VARY 312	67	2.00	MGT OF HIGH TEMP CATALYST BED(LBM)
VARY 312	68	600.0	OPERATING TEMP OF HIGH TEMP CAT. BED (F)
VARY 312	69	0.1111	FRACTION OF TOTAL FLOW TO HIGH TEMP BED
ID** 351			SPLITTER - CABIN AIR TO COOLING PKG AND SPLIT 355
NSTR 351			
VARY 351	65		SPLIT RATIO COOLING AND SPLIT 355-GPOLY CAL
ID** 352			SPLITTER - COOLING PKG FLOW TO PACKAGE #1 AND #2
NSTR 352			
VARY 352	65	0.5	FLOW FRACTION TO COOLING PKG #1 AND #2
ID** 353			GAS MIXER - FROM COOLING PKG #1 AND #2
NSTR 353			
ID** 354			SPLITTER - TO CABIN AIR OR ANOTHER MODULE
NSTR 354			
VARY 354	65	0.0	FLOW FRACTION TO CABIN AND MODULE
ID** 355			SPLITTER - COOLING PKG AIR TO CAT OX AND CO2 REMOVAL (PKG 1
NSTR 355			
VARY 355	65		SPLIT RATIO CAT OX AND CO2 REMOVAL-GPOLY CA
ID** 356			SPLITTER - COOLING PKG AIR TO CAT OX AND CO2 REMOVAL (PKG
NSTR 356			
VARY 356	65		SPLIT RATIO TO CAT OX AND CO2 REM #2-GPOLY
ID** 357			GAS MIXER - CAT OX PACKAGE #1
NSTR 357			
ID** 358			SPLITTER - TO MIXER 357 AND MIXER 359
NSTR 358			
VARY 358	65	0.5	FLOW FRACTION TO CAT OX #1 AND CAT OX #2
ID** 359			GAS MIXER - CAT OX PACKAGE #2
NSTR 359			
ID** 360			GAS MIXER - CAT OX #1 EXIT AIR AND PURGE N2
NSTR 360			
ID** 361			GAS MIXER - CAT OX #2 EXIT AIR AND PURGE N2
NSTR 361			
ID** 362			GAS MIXER- CAT OX #2 EXIT AND CO2 REMOVAL #2 EXIT
NSTR 362			
ID** 363			SPLITTER - TO CO2 REDUCTION PACKAGE #1 AND #2
NSTR 363			
VARY 363	65	0.500	FLOW FRACTION TO CO2 REDUCTION #1 AND #2
ID** 364			GAS MIXER - EXIT AIR FROM CO2 REDUCTION PKGS #1 AND #2
NSTR 364			
ID** 365			GAS MIXER - MIXER 361 AND MIXER 364
NSTR 365			
ID** 366			GAS MIXER - FROM MIXER 383 AND MIXER 387
NSTR 366			
ID** 367			SPLITTER - TO CO2 REDUCTION PKS #1 AND #2
NSTR 367			
VARY 367	65		FLOW FRACTION TO CO2 RED PKGS #1 AND #2
ID** 368			GAS MIXER - FROM MIXER 384 AND MIXER 367
NSTR 368			
ID** 370			GAS MIXER - CO2 REDUCTION PKGS #1 AND #2
NSTR 370			
ID** 372			SPLITTER - TO MIXER 376 AND MIXER 378
NSTR 372			
VARY 372	65		FLOW FRACTION TO MIXER 376 AND MIXER 378
ID** 373			SPLITTER - TO MIXER 379 AND SPLITTER 377
NSTR 373			
VARY 373	65	1.0	FLOW FRACTION TO MIXER 379 AND SPLIT 377
ID** 374			SPLITTER TO MIXER 376 AND MIXER 380
NSTR 374			
VARY 374	65		FLOW FRACTION TO MIXER 376 AND MIXER 380
ID** 376			GAS MIXER - FROM SPLIT 372 AND MIXER 374

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

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NSTR 376
ID** 377      SPLITTER - TO CONDENSATE AND CH4 STORAGE
NSTR 377      1
VARY 377 66    0.0      SPLIT RATIO FOR CONDENSABLE VAPOR FLOW
VARY 377 67    1.0      SPLIT RATIO FOR CONDENSABLE LIQUID FLOW
VARY 377 68    0.0      SPLIT RATIO FOR OXYGEN FLOW
VARY 377 69    0.0      SPLIT RATIO FOR NITROGEN FLOW
VARY 377 70    0.0      SPLIT RATIO FOR CARBON DIOXIDE FLOW
VARY 377 71    0.0      SPLIT RATIO FOR TRACE CONTAMINENT FLOW
VARY 377 72    0.0      SPLIT RATIO FOR SPECIAL FLOW #1, H2
VARY 377 73    0.0      SPLIT RATIO FOR SPECIAL FLOW #2, CH4
ID** 378      GAS MIXER - FROM SPLIT 372 AND SPLIT 401
NSTR 378
ID** 379      GAS MIXER - FROM SPLIT 373 AND SPLIT 400
NSTR 379
ID** 380      GAS MIXER - FROM SPLIT 399 AND SPLIT 374
NSTR 380
ID** 381      SPLITTER - N2 TO SPLIT 382 AND TO SPLIT 394
NSTR 381
VARY 381 65    FLOW FRACTION TO SPLIT 382 AND SPLIT 394
ID** 382      SPLITTER - NITROGEN TO MIXER 383 AND MIXER 384
NSTR 382
VARY 382 65    FLOW FRACTION TO MIXER 383 AND MIXER 384
ID** 383      GAS MIXER - N2 FROM MIXER 387 AND SPLIT 382
NSTR 383
ID** 384      GAS MIXER - N2 FROM MIXER 185 AND SPLIT 182
NSTR 384
ID** 385      GAS MIXER - CO2 FROM SPLIT 391 AND H2 FROM SPLIT 405
NSTR 385
ID** 386      GAS MIXER - FROM CO2 ACCUMULATOR AND H2 FROM SPLIT 406
NSTR 386
ID** 387      GAS MIXER - CO2 FROM CO2 REM PKG #1 AND H2 FROM SPLIT 407
NSTR 387
ID** 388      GAS MIXER - CO2 FROM CO2 BUS AND SPLIT 390
NSTR 388
ID** 390      SPLITTER - CO2 TO MIXER 388 AND CO2 BUS
NSTR 390
VARY 390 65    FLOW FRACTION TO MIXER 388 AND CO2 BUS
ID** 394      SPLITTER - N2 TO O2 GEN PKG #1 AND PKG #2
NSTR 394
VARY 394 65    FLOW FRACTION TO O2 GEN PKG #1 AND #2
ID** 395      GAS MIXER - O2 FROM O2 GEN PKG #1 AND #2
NSTR 395
ID** 397      GAS MIXER - H2 OR N2 FROM O2 GEN PKG #1 AND #2
NSTR 397
ID** 399      SPLITTER - N2 TO MIXER 380 OR H2 TO SPLIT 402
NSTR 399
VARY 399 65    FLOW FRACTION TO MIXER 380 OR SPLIT 402
ID** 400      SPLITTER - N2 TO MIXER 379 OR H2 TO SPLIT 403
NSTR 400
VARY 400 65    FLOW FRACTION TO MIXER 379 OR SPLIT 403
ID** 401      SPLITTER - N2 TO MIXER 378 OR H2 TO SPLIT 404
NSTR 401
VARY 401 65    FLOW FRACTION TO MIXER 378 OR SPLIT 404
ID** 402      SPLITTER - H2 TO VENT AND SPLIT 407
NSTR 402
VARY 402 65    0.0      FLOW FRACTION TO VENT AND SPLIT 407
ID** 403      SPLITTER - H2 TO VENT AND SPLIT 406
NSTR 403
VARY 403 65    FLOW FRACTION TO VENT AND SPLIT 406

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TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

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ID** 404      SPLITTER - H2 TO VENT AND SPLIT 405
NSTR 404
VARY 404 65    0.0          FLOW FRACTION TO VENT AND SPLIT 406
ID** 405      SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 405
VARY 405 65    1.0          SPLIT RATIO CO2 RED AND CO2 REM-GPOLY CALC
ID** 406      SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 406
VARY 406 65    FLOW FRACTION TO CO2 RED AND CO2 REMOVAL
ID** 407      SPLITTER - H2 TO CO2 REDUCTION AND CO2 REMOVAL
NSTR 407
VARY 407 65    1.0          SPLIT RATIO CO2 RED AND CO2 REM-GPOLY CALC
ID** 409      SPLITTER - H2 OR H2O TO CO2 REMOVAL PKG #1 AND #2
NSTR 409
VARY 409 65    FLOW FRACTION TO CO2 REMOVAL PKG #1 AND #2
ID** 413      GAS MIXER - CO2 FROM CO2 REMOVAL PKG #1 AND #2
NSTR 413
ID** 416      GAS MIXER - CABIN AIR AND CO2 REMOVAL EXIT
NSTR 416
ID** 417      SPLITTER - H2O TO O2 GENERATION PKG #1 AND #2
NSTR 417
VARY 417 65    0.5          FLOW FRACTION TO O2 GEN PKG #1 AND #2
ID** 418      SPLITTER - H2O TO O2 GENERATION AND CO2 REMOVAL
NSTR 418
VARY 418 65    0.0          FLOW TO O2 GENERATION AND CO2 REMOVAL
ID** 419      SPLITTER - H2O TO CO2 REMOVAL PKG #1 AND #2
NSTR 419
VARY 419 65    0.0          FLOW FRACTION TO CO2 REMOVAL #1 AND #2
ID** 420      TANK - CO2 STORAGE ACCUMULATOR
NSTR 420      01010          COMPUTE OUTLET FLOW IN GPOLY1
VARY 420 68    TANK MAX CAPACITY (LBM)
VARY 420 69    TANK INITIAL FILL (LBM)
VARY 420 70    TANK FLUID TEMPERATURE (F)
VARY 420 71    TANK VOLUME (FT-3)
VARY 420 72    TANK PRESSURE (PSIA)
VARY 420 92    THERMAL CAPACITANCE OF SHELL (BTU/HR)
VARY 420 94    MAX TEMP CHANGE IN ONE TIME STEP
VARY 420 98    FLUID USED FROM TANK - GPOLY2 CALC.
VARY 420 99    FLUID ADDED TO TANK - GPOLY2 CALC.
VARY 420 100   FLUID FLOW - GPOLY1 CALC.
ID** 500      BOUNDARY: ARS #1 HEAT EXCHANGER #1 COOLANT
NSTR 500
VARY 500 1     497.00        COOLANT FLOW (LBM/HR)
VARY 500 2     40.00         COOLANT TEMP (F)
VARY 500 3     50.00         4 COOLANT PRESSURE (PSIA)
ID** 501      BOUNDARY: ARS #1 HEAT EXCHANGER #2 COOLANT
NSTR 501
VARY 501 1     497.00        COOLANT FLOW (LBM/HR)
VARY 501 2     40.00         COOLANT TEMP (F)
VARY 501 3     50.00         4 COOLANT PRESSURE (PSIA)
ID** 502      BOUNDARY: ARS #1 CO2 REDUCTION #1 COOLANT
NSTR 502
VARY 502 1     60.0          COOLANT FLOW (LBM/HR)
VARY 502 2     38.00         COOLANT TEMP (F)
VARY 502 3     50.00         4 COOLANT PRESSURE (PSIA)
ID** 503      BOUNDARY: ARS #1 CO2 REDUCTION #2 COOLANT
NSTR 503
VARY 503 1     60.0          COOLANT FLOW (LBM/HR)
VARY 503 2     38.00         COOLANT TEMP (F)
VARY 503 3     50.00         4 COOLANT PRESSURE (PSIA)

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TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

ID** 504	BOUNDARY: ARS #1 CO2 REMOVAL #1 COOLANT			
NSTR 504				
VARY 504	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 504	2	45.00	COOLANT TEMP (F)	
VARY 504	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 505	BOUNDARY: ARS #1 CO2 REMOVAL #2 COOLANT			
NSTR 505				
VARY 505	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 505	2	45.00	COOLANT TEMP (F)	
VARY 505	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 506	BOUNDARY: ARS #1 O2 GENERATION #1 COOLANT			
NSTR 506				
VARY 506	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 506	2	45.00	COOLANT TEMP (F)	
VARY 506	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 507	BOUNDARY: ARS #1 O2 GENERATION #2 COOLANT			
NSTR 507				
VARY 507	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 507	2	45.00	COOLANT TEMP (F)	
VARY 507	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 508	BOUNDARY: ARS #2 HEAT EXCHANGER #1 COOLANT			
NSTR 508				
VARY 508	1	497.0	COOLANT FLOW (LBM/HR)	
VARY 508	2	40.00	COOLANT TEMP (F)	
VARY 508	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 509	BOUNDARY: ARS #2 HEAT EXCHANGER #2 COOLANT			
NSTR 509				
VARY 509	1	497.0	COOLANT FLOW (LBM/HR)	
VARY 509	2	40.00	COOLANT TEMP (F)	
VARY 509	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 510	BOUNDARY: ARS #2 CO2 REDUCTION #1 COOLANT			
NSTR 510				
VARY 510	1	60.0	COOLANT FLOW (LBM/HR)	
VARY 510	2	38.00	COOLANT TEMP (F)	
VARY 510	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 511	BOUNDARY: ARS #2 CO2 REDUCTION #2 COOLANT			
NSTR 511				
VARY 511	1	60.0	COOLANT FLOW (LBM/HR)	
VARY 511	2	38.00	COOLANT TEMP (F)	
VARY 511	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 512	BOUNDARY: ARS #2 CO2 REMOVAL #1 COOLANT			
NSTR 512				
VARY 512	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 512	2	45.00	COOLANT TEMP (F)	
VARY 512	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 513	BOUNDARY: ARS #2 CO2 REMOVAL #2 COOLANT			
NSTR 513				
VARY 513	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 513	2	45.00	COOLANT TEMP (F)	
VARY 513	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 514	BOUNDARY: ARS #2 O2 GENERATION #1 COOLANT			
NSTR 514				
VARY 514	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 514	2	45.00	COOLANT TEMP (F)	
VARY 514	3	50.00	4 COOLANT PRESSURE (PSIA)	
ID** 515	BOUNDARY: ARS #2 O2 GENERATION #2 COOLANT			
NSTR 515				
VARY 515	1	5005.0	COOLANT FLOW (LBM/HR)	
VARY 515	2	45.00	COOLANT TEMP (F)	
VARY 515	3	50.00	4 COOLANT PRESSURE (PSIA)	

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

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ID** 516      BOUNDARY: NODE #1 INLET BOUNDARY FLOW
NSTR 516
ID** 517      BOUNDARY: NODE #2 INLET BOUNDARY FLOW
NSTR 517
ID** 518      BOUNDARY: NODE #3 INLET BOUNDARY FLOW
NSTR 518
ID** 519      BOUNDARY: NODE #4 INLET BOUNDARY FLOW
NSTR 519
ID** 540      *****
ID** 540      *
ID** 540      *                LIBRARY OF SUBSYSTEMS                *
ID** 540      *
ID** 540      *****
ID** 540
ID** 540      ----- CO2 REDUCTION SUBSYSTEMS #1 FOR ARS #1 -----
ID** 540
ID** 540      SABATIER
KBAS 540      78  4      187 3      3 4      -163 3      3 4      123      1
NSTR 540
VARY 540 65      HEATER POWER, NORMAL (WATTS)
VARY 540 66      HEATER POWER, STATUP (WATTS)
VARY 540 67      WATER CONDENSED (LBM/HR)
VARY 540 68      METHANE EXIT FLOW (LBM/HR)
ID** 121      BOSCH
KBAS 121      83  1  0      187 0      1      -502 0      1      123      1
NSTR 121      1
VARY 121 65      40.000      MAX. CARBON LOADING FOR CARTRIDGE, LBM
VARY 121 66      0.163      DRY BASIS VOL FRAC OF CO2 IN COMP EXIT GASES
VARY 121 67      0.327      DRY BASIS VOL FRAC OF H2 IN COMP EXIT GASES
VARY 121 68      0.235      DRY BASIS VOL FRAC OF CH4 IN COMP EXIT GASES
VARY 121 69      0.275      DRY BASIS VOL FRAC OF CO IN COMP EXIT GASES
VARY 121 70      0.900      EFFECTIVENESS FACTOR FOR CONDENSER
VARY 121 71      0.850      EFFECTIVENESS FACTOR FOR REGEN HX
VARY 121 73      24.300      REACTOR PRESSURE, PSIA
VARY 121 74      16.900      CONDENSER PRESSURE, PSIA
VARY 121 76      1.000      AERODYNAMIC EFFICIENCY OF COMPRESSOR
VARY 121 77      0.250      MOTOR EFFICIENCY OF COMPRESSOR
VARY 121 78      1230.000      DESIRED REACTOR TEMPERATURE, F
VARY 121 79      6.800      RECYCLE FLOW RATE, PPH
VARY 121 101     6.600      LUMPED THERMAL MASS OF REACTOR, BTU/F
ID** 542      ----- CO2 REDUCTION SUBSYSTEMS #2 FOR ARS #1 -----
ID** 542      SABATIER
KBAS 542      78  4      185 3      3 4      163 3      3 4      164      1
NSTR 542
VARY 542 65      HEATER POWER, NORMAL (WATTS)
VARY 542 66      HEATER POWER, STARTUP (WATTS)
VARY 542 67      WATER CONDENSED (LBM/HR)
VARY 542 68      METHANE EXIT FLOW (LBM/HR)
ID** 123      BOSCH
KBAS 123      83  1  0      185 0      1      -503 0      1      170      1
NSTR 123      1
VARY 123 65      40.000      MAX. CARBON LOADING FOR CARTRIDGE, LBM
VARY 123 66      0.163      DRY BASIS VOL FRAC OF CO2 IN COMP EXIT GASES
VARY 123 67      0.327      DRY BASIS VOL FRAC OF H2 IN COMP EXIT GASES
VARY 123 68      0.235      DRY BASIS VOL FRAC OF CH4 IN COMP EXIT GASES
VARY 123 69      0.275      DRY BASIS VOL FRAC OF CO IN COMP EXIT GASES
VARY 123 70      0.900      EFFECTIVENESS FACTOR FOR CONDENSER
VARY 123 71      0.850      EFFECTIVENESS FACTOR FOR REGEN HX
VARY 123 73      24.300      REACTOR PRESSURE, PSIA

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TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 123	74	16.900	CONDENSER PRESSURE, PSIA
VARY 123	76	1.000	AERODYNAMIC EFFICIENCY OF COMPRESSOR
VARY 123	77	0.250	MOTOR EFFICIENCY OF COMPRESSOR
VARY 123	78	1230.000	DESIRE REACTOR TEMPERATURE, F
VARY 123	79	6.800	RECYCLE FLOW RATE, PPH
VARY 123	101	6.600	LUMPED THERMAL MASS OF REACTOR, BTU/F
ID** 550			----- CO2 REMOVAL SUBSYSTEMS #1 FOR ARS #1 -----
ID** 550			
ID** 550			
ID** 550	EDC		
KBAS 550	76 6	155 2 3	-207 2 3 132 1
NSTR 550			
KARY 550	16	30	NUMBER OF CELLS
VARY 550	65		HEAT TO BE REMOVED BY EDC HEX (BTU/HR)
VARY 550	68		ACTUAL CELL CURRENT DENSITY (AMP/SQ-FT)
VARY 550	69	11.00	DESIGN CELL CURRENT DENSITY (AMP/SQ-FT)
VARY 550	70	3.00	DESIGN PCO2 (MMHG)
VARY 550	71	0.001736	CO2 TRANSFER RATE (LBM-CO2/AMP-HR)
VARY 550	72	0.5	UNIT CELL AREA (SQ-FT/CELL)
VARY 550	73	70.00	CELL OPERATING TEMP (F)
VARY 550	74	14.7	CELL OPERATING PRESSURE (PSIA)
VARY 550	75		MASS FLOW OF WATER PRODUCED (LBM/HR)
VARY 550	76		CURRENT GENERATED (AMP)
VARY 550	77		POWER GENERATED (WATTS)
VARY 550	78		O2 CONSUMED (LBM/HR)
VARY 550	79		CO2 REMOVED (LBM/HR)
VARY 550	80	0.03	H2 CONSUMED (LBM/HR)
ID** 551	SAND		
KBAS 551	73	155 2 3	-219 2 3 133 1
NSTR 551			
ID** 131	MOLECULAR SIEVE		
KBAS 131	84 40	155 2 3	2 3 133 1
NSTR 131		0	
VARY 131	65	60.0	HALF CYCLE TIME, MINUTES
VARY 131	66	1.0	MIN PRESS OF DESORBING MOLE SIEVE BED, PSIA
VARY 131	67	20.0	CO2 ACCUMULATOR PRESSURE, PSIA
VARY 131	68	360.0	MAX TEMP OF DESRB MOL SIEVE BED, F
VARY 131	69	180.0	MAX TEMP OF DESRB SILICA GEL BED, F
VARY 131	70	70.0	CABIN AIR TEMPERATURE, F
VARY 131	71	1.0	FIRST TIME INTO COMPONENT: 1=TRUE, 0=FALSE
VARY 131	72		HALF CYCLE TIME, SECONDS
VARY 131	73		FULL CYCLE TIME, SECONDS
VARY 131	74		COMPUTATION TIME STEP, HOURS
VARY 131	75	1.0	FIRST HALF OF CYCLE: 1=TRUE, 0=FALSE
VARY 131	76	45.0	HX COOLANT INLET TEMPERATURE, F
VARY 131	81		COMPRESSOR POWER, BTU/HR
VARY 131	82		FAN POWER, BTU/HR
VARY 131	83		HEAT GIVEN TO DESRB SILICA GEL BED, BTU/HR
VARY 131	84		HEAT REMOVED BY THE HEAT EXCHANGER, BTU/HR
VARY 131	85		AVG Q FROM DSRBNG SIL GEL TO CABIN, BTU/HR
VARY 131	86		AVG Q FROM DSRBNG MOL SIV TO CABIN, BTU/HR
VARY 131	90	0.0	H2O ADSORBED IN SIL GEL BED #1, LBM
VARY 131	91	0.0	H2O ADSORBED IN SIL GEL BED #2, LBM
VARY 131	92	0.0	CO2 ADSORBED IN MOL SIV BED #1, LBM
VARY 131	93	0.0	CO2 ADSORBED IN MOL SIV BED #2, LBM
VARY 131	94	0.0	H2O ADSORBED IN PRESENT SIL GEL BED, LBM
VARY 131	95	0.0	CO2 ADSORBED IN PRESENT MOL SIV BED, LBM
VARY 131	96	0.0	H2O DESORBED IN PRESENT SIL GEL BED, LBM
VARY 131	97	0.0	H2O DESORBED IN PRESENT MOL SIV BED, LBM
VARY 131	98	0.0	H2O ADSORBED LAST CYCLE, LBM

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 131 99	0.0	CO2 ADSORBED LAST CYCLE, LBM		
VARY 131 100		CYCLE CURRENTLY RUNNING		
VARY 131 101		FAN EXIT TEMPERATURE, F		
VARY 131 102		ADSORBING SIL GEL BED EXIT TEMP, F		
VARY 131 103		ADSORBING MOL SIV BED EXIT TEMP, F		
VARY 131 104		DESORBING SIL GEL BED EXIT TEMP, F		
ID** 132		EDC HEAT EXCHANGER		
KBAS 132	49 1	504 0 1	133	1
NSTR 132	2			
VARY 132 65	944.0	HEAT LOAD FROM EDC OR MOL SIEVE (BTU/HR)		
ID** 553				
ID** 553		----- CO2 REMOVAL SYSTEMS #2 FOR ARS #1 -----		
ID** 553				
ID** 553		EDC		
KBAS 553	76 6	156 2 3	-205 2 3	134 1
NSTR 553				
KARY 553 16	30	NUMBER OF CELLS		
VARY 553 65		HEAT TO BE REMOVED BY EDC HEX (BTU/HR)		
VARY 553 68		ACTUAL CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 553 69	11.00	DESIGN CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 553 70	3.00	DESIGN PCO2 (MMHG)		
VARY 553 71	0.001736	CO2 TRANSFER RATE (LBM-CO2/AMP-HR)		
VARY 553 72	0.5	UNIT CELL AREA (SQ-FT/CELL)		
VARY 553 73	70.00	CELL OPERATING TEMP (F)		
VARY 553 74	14.7	CELL OPERATING PRESSURE (PSIA)		
VARY 553 75		MASS FLOW OF WATER PRODUCED (LBM/HR)		
VARY 553 76		CURRENT GENERATED (AMP)		
VARY 553 77		POWER GENERATED (WATTS)		
VARY 553 78		O2 CONSUMED (LBM/HR)		
VARY 553 79		CO2 REMOVED (LBM/HR)		
VARY 553 80	0.03	H2 CONSUMED (LBM/HR)		
ID** 554		SAMD		
KBAS 554	73	156 2 3	219 2 3	135 1
NSTR 554				
ID** 133		MOLECULAR SIEVE		
KBAS 133	84 40	156 2 3	2 3	135 1
NSTR 133		0		
VARY 133 65	60.0	HALF CYCLE TIME, MINUTES		
VARY 133 66	1.0	MIN PRESS OF DESORBING MOLE SIEVE BED, PSIA		
VARY 133 67	20.0	CO2 ACCUMULATOR PRESSURE, PSIA		
VARY 133 68	360.0	MAX TEMP OF DESRB MOL SIEVE BED, F		
VARY 133 69	180.0	MAX TEMP OF DESRB SILICA GEL BED, F		
VARY 133 70	70.0	CABIN AIR TEMPERATURE, F		
VARY 133 71	1.0	FIRST TIME INTO COMPONENT: 1=TRUE, 0=FALSE		
VARY 133 72		HALF CYCLE TIME, SECONDS		
VARY 133 73		FULL CYCLE TIME, SECONDS		
VARY 133 74		COMPUTATION TIME STEP, HOURS		
VARY 133 75	1.0	FIRST HALF OF CYCLE: 1=TRUE, 0=FALSE		
VARY 133 76	45.0	HX COOLANT INLET TEMPERATURE, F		
VARY 133 81		COMPRESSOR POWER, BTU/HR		
VARY 133 82		FAN POWER, BTU/HR		
VARY 133 83		HEAT GIVEN TO DESRB SILICA GEL BED, BTU/HR		
VARY 133 84		HEAT REMOVED BY THE HEAT EXCHANGER, BTU/HR		
VARY 133 85		AVG Q FROM DSRBNG SIL GEL TO CABIN, BTU/HR		
VARY 133 86		AVG Q FROM DSRBNG MOL SIV TO CABIN, BTU/HR		
VARY 133 90	0.0	H2O ADSORBED IN SIL GEL BED #1, LBM		
VARY 133 91	0.0	H2O ADSORBED IN SIL GEL BED #2, LBM		
VARY 133 92	0.0	CO2 ADSORBED IN MOL SIV BED #1, LBM		
VARY 133 93	0.0	CO2 ADSORBED IN MOL SIV BED #2, LBM		
VARY 133 94	0.0	H2O ADSORBED IN PRESENT SIL GEL BED, LBM		

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY	133	95	0.0	CO2 ADSORBED IN PRESENT MOL SIV BED, LBM		
VARY	133	96	0.0	H2O DESORBED IN PRESENT SIL GEL BED, LBM		
VARY	133	97	0.0	H2O DESORBED IN PRESENT MOL SIV BED, LBM		
VARY	133	98	0.0	H2O ADSORBED LAST CYCLE, LBM		
VARY	133	99	0.0	CO2 ADSORBED LAST CYCLE, LBM		
VARY	133	100		CYCLE CURRENTLY RUNNING		
VARY	133	101		FAN EXIT TEMPERATURE, F		
VARY	133	102		ADSORBING SIL GEL BED EXIT TEMP, F		
VARY	133	103		ADSORBING MOL SIV BED EXIT TEMP, F		
VARY	133	104		DESORBING SIL GEL BED EXIT TEMP, F		
ID**	134			EDC HEAT EXCHANGER		
KBAS	134	49	1	505 0 1	135	1
NSTR	134	2				
VARY	134	65	944.0	HEAT LOAD FROM EDC OR MOL SIEVE (BTU/HR)		
ID**	135			ACCUMULATOR FOR CO2 REMOVAL UNIT #1 IN ARS #1		
KBAS	135	30		-131 2 3	136	1
NSTR	135	00000		FLUID TEMP EQUALS INLET TEMP.		
VARY	135	69	1.10	TOTAL MASS OF FLUID IN TANK, LBM		
VARY	135	70	70.0	FLUID TEMPERATURE IN TANK, F		
VARY	135	71	4.75	TANK VOLUME, CUBIC FEET		
VARY	135	72	30.0	FLUID PRESSURE IN TANK, PSIA		
VARY	135	80	1.10	MASS OF CO2 IN TANK, LBM		
ID**	136			ACCUMULATOR FOR CO2 REMOVAL UNIT #2 IN ARS #1		
KBAS	136	30		-133 2 3	185	1
NSTR	136	00000		FLUID TEMP EQUALS INLET TEMP.		
VARY	136	69	1.10	TOTAL MASS OF FLUID IN TANK, LBM		
VARY	136	70	70.0	FLUID TEMPERATURE IN TANK, F		
VARY	136	71	4.75	TANK VOLUME, CUBIC FEET		
VARY	136	72	30.0	FLUID PRESSURE IN TANK, PSIA		
VARY	136	80	1.10	MASS OF CO2 IN TANK, LBM		
ID**	141			----- O2 GENERATION SUBSYSTEMS #1 FOR ARS #1 -----		
ID**	141					
ID**	141			STATIC FEED SOLID POLYMER ELECTROLYSIS		
KBAS	141	77	2	217 2 3 2 3	142	1
NSTR	141					
KARY	141	16	1	LIGHTSIDE/CONTINUOUS = 1, DARKSIDE = 0		
KARY	141	17	20	NUMBER OF CELLS		
VARY	141	65		TOTAL HEAT TO BE REMOVED BY SPE HX (BTU/HR)		
VARY	141	66		O2 FLOW RATE TO CABIN (LBM/HR)		
VARY	141	67		SPE WATER DEMAND (LBM/HR)		
VARY	141	68		WATER VAPOR FLOW TO CABIN (LBM/HR)		
VARY	141	69		CELL CURRENT (AMPS) - GPOLY CALC.		
VARY	141	70	200.0	CELL OPERATING PRESSURE (PSIA)		
VARY	141	71	155.0	CELL OPERATING TEMP (F)		
VARY	141	72	29.33	NOMINAL CELL CURRENT (AMP/CELL)		
ID**	561			KOH ELECTROLYSIS		
KBAS	561	85		217 0 1	142	1
NSTR	561					
ID**	142			O2 GENERATION HEAT EXCHANGER FOR SYSTEM #1		
KBAS	142	49	1	506 0 1	143	1
NSTR	142	2				
VARY	142	65		HEAT LOAD ELEC CELLS (BTU/HR) GPOLY1 CALC		
ID**	143			----- O2 GENERATION SUBSYSTEMS #2 FOR ARS #1 -----		
ID**	143					
ID**	143			STATIC FEED SOLID POLYMER ELECTROLYSIS		
KBAS	143	77	2	-217 2 3 2 3	144	1
NSTR	143					
KARY	143	16	1	LIGHTSIDE CONTINUOUS=1,DARKSIDE =0		
KARY	143	17	20	NUMBER OF CELLS		

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 143	65			TOTAL HEAT TO BE REMOVED BY SPE HX (BTU/HR)			
VARY 143	66			O2 FLOW RATE TO CABIN (LBM/HR)			
VARY 143	67			SPE WATER DEMAND (LBM/HR)			
VARY 143	68			WATER VAPOR FLOW TO CABIN (LBM/HR)			
VARY 143	69			CELL CURRENT (AMPS) - GPOLY CALC.			
VARY 143	70	200.0		CELL OPERATING PRESSURE (PSIA)			
VARY 143	71	155.0		CELL OPERATING TEMP (F)			
VARY 143	72	29.33		NOMINAL CELL CURRENT (AMP/CELL)			
ID** 563				KOH ELECTROLYSIS			
KBAS 563	85		-217 0 1			144	1
NSTR 563							
ID** 144				O2 GENERATION HEAT EXCHANGER FOR SYSTEM #2			
KBAS 144	49 1		507 0 1			195	1
NSTR 144	2						
VARY 144	65			HEAT LOAD ELEC CELLS (BTU/HR) GPOLY1 CALC			
ID** 570							
ID** 570							
ID** 570							
ID** 570				----- CO2 REDUCTION SUBSYSTEM #1 FOR ARS #2 -----			
ID** 570				SABATIER			
KBAS 570	78 4		387 3 3 4		-363 3 3 4	323	2
NSTR 570							
VARY 570	65			HEATER POWER, NORMAL (WATTS)			
VARY 570	66			HEATER POWER, STARTUP (WATTS)			
VARY 570	67			WATER CONDENSED (LBM/HR)			
VARY 570	68			METHANE EXIT FLOW (LBM/HR)			
ID** 321				BOSCH			
KBAS 321	83 1		387 0 1		-510 0 1	323	2
NSTR 321	1						
VARY 321	65	40.000		MAX. CARBON LOADING FOR CARTRIDGE, LBM			
VARY 321	66	0.163		DRY BASIS VOL FRAC OF CO2 IN COMP EXIT GASES			
VARY 321	67	0.327		DRY BASIS VOL FRAC OF H2 IN COMP EXIT GASES			
VARY 321	68	0.235		DRY BASIS VOL FRAC OF CH4 IN COMP EXIT GASES			
VARY 321	69	0.275		DRY BASIS VOL FRAC OF CO IN COMP EXIT GASES			
VARY 321	70	0.900		EFFECTIVENESS FACTOR FOR CONDENSER			
VARY 321	71	0.850		EFFECTIVENESS FACTOR FOR REGEN HX			
VARY 321	73	24.300		REACTOR PRESSURE, PSIA			
VARY 321	74	16.900		CONDENSER PRESSURE, PSIA			
VARY 321	76	1.000		AERODYNAMIC EFFICIENCY OF COMPRESSOR			
VARY 321	77	0.250		MOTOR EFFICIENCY OF COMPRESSOR			
VARY 321	78	1230.000		DESIRED REACTOR TEMPERATURE, F			
VARY 321	79	6.800		RECYCLE FLOW RATE, PPH			
VARY 321	101	6.600		LUMPED THERMAL MASS OF REACTOR, BTU/F			
ID** 572				CO2 REDUCTION SUBSYSTEM #2 FOR ARS #2			
ID** 572				SABATIER			
KBAS 572	78 4		385 3 3 4		363 3 3 4	364	2
NSTR 572							
VARY 572	65			HEATER POWER, NORMAL (WATTS)			
VARY 572	66			HEATER POWER, STARTUP (WATTS)			
VARY 572	67			WATER CONDENSED (LBM/HR)			
VARY 572	68			METHANE EXIT FLOW (LBM/HR)			
ID** 323				BOSCH			
KBAS 323	83 18		385 0 1		-511 0 1	370	2
NSTR 323	1						
VARY 323	65	40.000		MAX. CARBON LOADING FOR CARTRIDGE, LBM			
VARY 323	66	0.163		DRY BASIS VOL FRAC OF CO2 IN COMP EXIT GASES			
VARY 323	67	0.327		DRY BASIS VOL FRAC OF H2 IN COMP EXIT GASES			
VARY 323	68	0.235		DRY BASIS VOL FRAC OF CH4 IN COMP EXIT GASES			
VARY 323	69	0.275		DRY BASIS VOL FRAC OF CO IN COMP EXIT GASES			
VARY 323	70	0.900		EFFECTIVENESS FACTOR FOR CONDENSER			

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 323	71	0.850	EFFECTIVENESS FACTOR FOR REGEN HX		
VARY 323	73	24.300	REACTOR PRESSURE, PSIA		
VARY 323	74	16.900	CONDENSER PRESSURE, PSIA		
VARY 323	76	1.000	AERODYNAMIC EFFICIENCY OF COMPRESSOR		
VARY 323	77	0.250	MOTOR EFFICIENCY OF COMPRESSOR		
VARY 323	78	1230.000	DESIRED REACTOR TEMPERATURE, F		
VARY 323	79	6.800	RECYCLE FLOW RATE, PPH		
VARY 323	101	6.600	LUMPED THERMAL MASS OF REACTOR, BTU/F		
ID** 580			CO2 REMOVAL SYSTEMS #1 FOR ARS #2*****		
ID** 580					
ID** 580			EDC CO2 REMOVAL SUBSYSTEM		
KBAS 580	76	6	355 2 3	-407 2 3	332 2
NSTR 580					
KARY 580	16	30	NUMBER OF CELLS		
VARY 580	65		HEAT TO BE REMOVED BY EDC HEX (BTU/HR)		
VARY 580	68		ACTUAL CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 580	69	11.00	DESIGN CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 580	70	3.00	DESIGN PCO2 (MMHG)		
VARY 580	71	0.001736	CO2 TRANSFER RATE (LBM-CO2/AMP-HR)		
VARY 580	72	0.50	UNIT CELL AREA (SQ-FT/CELL)		
VARY 580	73	70.0	CELL OPERATING TEMP (F)		
VARY 580	74	14.7	CELL OPERATING PRESSURE (PSIA)		
VARY 580	75		MASS FLOW OF WATER PRODUCED (LBM/HR)		
VARY 580	76		CURRENT GENERATED (AMP)		
VARY 580	77		POWER GENERATED (WATTS)		
VARY 580	78		O2 CONSUMED (LBM/HR)		
VARY 580	79		CO2 REMOVED (LBM/HR)		
VARY 580	80	0.03	H2 CONSUMED (LBM/HR)		
ID** 581			SAMD CO2 REMOVAL SUBSYSTEM		
KBAS 581	73		355 2 3	-419 2 3	333 2
NSTR 581					
ID** 331			MOL SIEVE		
KBAS 331	84	40	355 2 3	2 3	333 2
NSTR 331					
VARY 331	65	60.0	HALF CYCLE TIME, MINUTES		
VARY 331	66	1.0	MIN PRESS OF DESORBING MOLE SIEVE BED, PSIA		
VARY 331	67	20.0	CO2 ACCUMULATOR PRESSURE, PSIA		
VARY 331	68	360.0	MAX TEMP OF DESRB MOL SIEVE BED, F		
VARY 331	69	180.0	MAX TEMP OF DESRB SILICA GEL BED, F		
VARY 331	70	70.0	CABIN AIR TEMPERATURE, F		
VARY 331	71	1.0	FIRST TIME INTO COMPONENT: 1=TRUE, 0=FALSE		
VARY 331	72		HALF CYCLE TIME, SECONDS		
VARY 331	73		FULL CYCLE TIME, SECONDS		
VARY 331	74		COMPUTATION TIME STEP, HOURS		
VARY 331	75	1.0	FIRST HALF OF CYCLE: 1=TRUE, 0=FALSE		
VARY 331	76	45.0	HX COOLANT INLET TEMPERATURE, F		
VARY 331	81		COMPRESSOR POWER, BTU/HR		
VARY 331	82		FAN POWER, BTU/HR		
VARY 331	83		HEAT GIVEN TO DESRB SILICA GEL BED, BTU/HR		
VARY 331	84		HEAT REMOVED BY THE HEAT EXCHANGER, BTU/HR		
VARY 331	85		AVG Q FROM DSRBNG SIL GEL TO CABIN, BTU/HR		
VARY 331	86		AVG Q FROM DSRBNG MOL SIV TO CABIN, BTU/HR		
VARY 331	90	0.0	H2O ADSORBED IN SIL GEL BED #1, LBM		
VARY 331	91	0.0	H2O ADSORBED IN SIL GEL BED #2, LBM		
VARY 331	92	0.0	CO2 ADSORBED IN MOL SIV BED #1, LBM		
VARY 331	93	0.0	CO2 ADSORBED IN MOL SIV BED #2, LBM		
VARY 331	94	0.0	H2O ADSORBED IN PRESENT SIL GEL BED, LBM		
VARY 331	95	0.0	CO2 ADSORBED IN PRESENT MOL SIV BED, LBM		
VARY 331	96	0.0	H2O DESORBED IN PRESENT SIL GEL BED, LBM		

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 331 97	0.0	H2O DESORBED IN PRESENT MOL SIV BED, LBM		
VARY 331 98	0.0	H2O ADSORBED LAST CYCLE, LBM		
VARY 331 99	0.0	CO2 ADSORBED LAST CYCLE, LBM		
VARY 331 100		CYCLE CURRENTLY RUNNING		
VARY 331 101		FAN EXIT TEMPERATURE, F		
VARY 331 102		ADSORBING SIL GEL BED EXIT TEMP, F		
VARY 331 103		ADSORBING MOL SIV BED EXIT TEMP, F		
VARY 331 104		DESORBING SIL GEL BED EXIT TEMP, F		
ID** 332		EDC/MOL SIEVE HEAT EXCHANGER FOR SYSTEM #1		
KBAS 332	49 1 512 0 1		333	2
NSTR 332	2			
VARY 332 65	944.0	HEAT LOAD FROM EDC OR MOL SIEVE (BTU/HR)		
ID** 583				
ID** 583		CO2 REMOVAL SYSTEMS #2 FOR ARS #2*****		
ID** 583				
ID** 583		EDC CO2 REMOVAL SUBSYSTEM		
KBAS 583	76 6 356 2 3 -405 2 3		334	2
NSTR 583				
KARY 583 16	30	NUMBER OF CELLS		
VARY 583 65		HEAT TO BE REMOVED BY EDC HEX (BTU/HR)		
VARY 583 68		ACTUAL CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 583 69	11.00	DESIGN CELL CURRENT DENSITY (AMP/SQ-FT)		
VARY 583 70	3.00	DESIGN PCO2 (MMHG)		
VARY 583 71	0.001736	CO2 TRANSFER RATE (LBM-CO2/AMP-HR)		
VARY 583 72	0.5	UNIT CELL AREA (SQ-FT/CELL)		
VARY 583 73	70.00	CELL OPERATING TEMP (F)		
VARY 583 74	14.7	CELL OPERATING PRESSURE (PSIA)		
VARY 583 75		MASS FLOW OF WATER PRODUCED (LBM/HR)		
VARY 583 76		CURRENT GENERATED (AMP)		
VARY 583 77		POWER GENERATED (WATTS)		
VARY 583 78		O2 CONSUMED (LBM/HR)		
VARY 583 79		CO2 REMOVED (LBM/HR)		
VARY 583 80	0.03	H2 CONSUMED (LBM/HR)		
ID** 584		SAND CO2 REMOVAL SUBSYSTEM		
KBAS 584	73 356 2 3 419 2 3		385	2
NSTR 584				
ID** 333		MOL SIEVE CO2 REMOVAL SUBSYSTEM		
KBAS 333	84 40 356 2 3 2 3		335	2
NSTR 333				
VARY 333 65	60.0	HALF CYCLE TIME, MINUTES		
VARY 333 66	1.0	MIN PRESS OF DESORBING MOLE SIEVE BED, PSIA		
VARY 333 67	20.0	CO2 ACCUMULATOR PRESSURE, PSIA		
VARY 333 68	360.0	MAX TEMP OF DESRB MOL SIEVE BED, F		
VARY 333 69	180.0	MAX TEMP OF DESRB SILICA GEL BED, F		
VARY 333 70	70.0	CABIN AIR TEMPERATURE, F		
VARY 333 71	1.0	FIRST TIME INTO COMPONENT: 1=TRUE, 0=FALSE		
VARY 333 72		HALF CYCLE TIME, SECONDS		
VARY 333 73		FULL CYCLE TIME, SECONDS		
VARY 333 74		COMPUTATION TIME STEP, HOURS		
VARY 333 75	1.0	FIRST HALF OF CYCLE: 1=TRUE, 0=FALSE		
VARY 333 76	45.0	HX COOLANT INLET TEMPERATURE, F		
VARY 333 81		COMPRESSOR POWER, BTU/HR		
VARY 333 82		FAN POWER, BTU/HR		
VARY 333 83		HEAT GIVEN TO DESRB SILICA GEL BED, BTU/HR		
VARY 333 84		HEAT REMOVED BY THE HEAT EXCHANGER, BTU/HR		
VARY 333 85		AVG Q FROM DSRBNG SIL GEL TO CABIN, BTU/HR		
VARY 333 86		AVG Q FROM DSRBNG MOL SIV TO CABIN, BTU/HR		
VARY 333 90	0.0	H2O ADSORBED IN SIL GEL BED #1, LBM		
VARY 333 91	0.0	H2O ADSORBED IN SIL GEL BED #2, LBM		
VARY 333 92	0.0	CO2 ADSORBED IN MOL SIV BED #1, LBM		



TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

VARY 333	93	0.0	CO2 ADSORBED IN MOL SIV BED #2, LBM		
VARY 333	94	0.0	H2O ADSORBED IN PRESENT SIL GEL BED, LBM		
VARY 333	95	0.0	CO2 ADSORBED IN PRESENT MOL SIV BED, LBM		
VARY 333	96	0.0	H2O DESORBED IN PRESENT SIL GEL BED, LBM		
VARY 333	97	0.0	H2O DESORBED IN PRESENT MOL SIV BED, LBM		
VARY 333	98	0.0	H2O ADSORBED LAST CYCLE, LBM		
VARY 333	99	0.0	CO2 ADSORBED LAST CYCLE, LBM		
VARY 333	100		CYCLE CURRENTLY RUNNING		
VARY 333	101		FAN EXIT TEMPERATURE, F		
VARY 333	102		ADSORBING SIL GEL BED EXIT TEMP, F		
VARY 333	103		ADSORBING MOL SIV BED EXIT TEMP, F		
VARY 333	104		DESORBING SIL GEL BED EXIT TEMP, F		
ID** 334			EDC HEAT EXCHANGER FOR SYSSEM #2		
KBAS 334	49	1	513 0 1	385	2
NSTR 334	2				
VARY 334	65	944.0	HEAT LOAD FROM EDC OR MOL SIEVE (BTU/HR)		
ID** 335			ACCUMULATOR FOR CO2 REMOVAL UNIT #1 IN ARS #2		
KBAS 335	30		-331 2 3	336	2
NSTR 335	00000		FLUID TEMP EQUALS INLET TEMP.		
VARY 335	69	1.10	TOTAL MASS OF FLUID IN TANK, LBM		
VARY 335	70	70.0	FLUID TEMPERATURE IN TANK, F		
VARY 335	71	4.75	TANK VOLUME, CUBIC FEET		
VARY 335	72	30.0	FLUID PRESSURE IN TANK, PSIA		
VARY 335	80	1.10	MASS OF CO2 IN TANK, LBM		
ID** 336			ACCUMULATOR FOR CO2 REMOVAL UNIT #2 IN ARS #2		
KBAS 336	30		-333 2 3	385	2
NSTR 336	00000		FLUID TEMP EQUALS INLET TEMP.		
VARY 336	69	1.10	TOTAL MASS OF FLUID IN TANK, LBM		
VARY 336	70	70.0	FLUID TEMPERATURE IN TANK, F		
VARY 336	71	4.75	TANK VOLUME, CUBIC FEET		
VARY 336	72	30.0	FLUID PRESSURE IN TANK, PSIA		
VARY 336	80	1.10	MASS OF CO2 IN TANK, LBM		
ID** 341					
ID** 341			O2 GENERATION SYSTEM #1 FOR ARS #2*****		
ID** 341					
ID** 341			STATIC FEED SOLID POLYMER ELECTROLYSIS		
KBAS 341	77	2	417 2 3 2 3	342	2
NSTR 341					
KARY 341	16	1	LIGHTSIDE CONTINUOUS=1,DARKSIDE =0		
KARY 341	17	20	NUMBER OF CELLS		
VARY 341	65		TOTAL HEAT TO BE REMOVED BY SPE HX (BTU/HR)		
VARY 341	66		O2 FLOW RATE TO CABIN (LBM/HR)		
VARY 341	67		SPE WATER DEMAND (LBM/HR)		
VARY 341	68		WATER VAPOR FLOW TO CABIN (LBM/HR)		
VARY 341	69		CELL CURRENT (AMPS) - GPOLY CALC.		
VARY 341	70	200.0	CELL OPERATING PRESSURE (PSIA)		
VARY 341	71	155.0	CELL OPERATING TEMP (F)		
VARY 341	72	29.33	NOMINAL CELL CURRENT (AMP/CELL)		
ID** 591			KOH ELECTROLYSIS SUBSYSTEM		
KBAS 591	85		417 0 1	342	2
NSTR 591					
ID** 342			O2 GENERATION HEAT EXCHANGER FOR SYSTEM #1		
KBAS 342	49	1	514 0 1	343	2
NSTR 342	2				
VARY 342	65		HEAT LOAD ELECT CELLS (BTU/HR) GPOLY1 CALC		
ID** 343			O2 GENERATION SYSTEM #2 FOR ARS #2*****		
ID** 343					
ID** 343			STATIC FEED SOLID POLYMER ELECTROLYSIS		
KBAS 343	77	2	-417 2 3 2 3	344	2
NSTR 343					

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

KARY	343	16	1	LIGHTSIDE CONTINUOUS=1,DARKSIDE =0				
KARY	343	17	20	NUMBER OF CELLS				
VARY	343	65		TOTAL HEAT TO BE REMOVED BY SPE HX (BTU/HR)				
VARY	343	66		O2 FLOW RATE TO CABIN (LBM/HR)				
VARY	343	67		SPE WATER DEMAND (LBM/HR)				
VARY	343	68		WATER VAPOR FLOW TO CABIN (LBM/HR)				
VARY	343	69		CELL CURRENT (AMPS) - GPOLY CALC.				
VARY	343	70	200.0	CELL OPERATING PRESSURE (PSIA)				
VARY	343	71	155.0	CELL OPERATING TEMP (F)				
VARY	343	72	29.33	NOMINAL CELL CURRENT (AMP/CELL)				
ID**	593			KOH ELECTROLYSIS SUBSYSTEM				
KBAS	593	85	-417 0 1	344	2			
NSTR	593							
ID**	344			O2 GENERATION HEAT EXCHANGER FOR SYSTEM #2				
KBAS	344	49 1	515 0 1	395	2			
NSTR	344	2						
VARY	344	65		HEAT LOAD ELEC CELLS (BTU/HR) GPOLY1 CALC				
TABL	1	1	2	14	0	LIN	LIN	
TITL	1	2		CREHMAN METABOLIC RATE (BTU/HR) VS MISSION TIME (SEC)				
VALU	1	10 2I	0.0	24300.	28800.	42300.	43200.	
VALU	1	11 2D	300.0	300.0	633.4	633.4	450.0	
VALU	1	12 2I	54000.	61200.	64800.	68400.	72000.	
VALU	1	13 2D	633.4	633.4	450.0	450.0	550.0	
VALU	1	14 2I	83700.	86400.				
VALU	1	15 2D	300.0	300.0				
TABL	2	1	2	8		LIN	LIN	
TITL	2	2		PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE				
TITL	2	3		N2 OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)				
TITL	2	4		N2 OPENING FLOWS VS TOTAL PRESSURE (PSIA)				
VALU	2	10 2I	0.0	14.500	14.510	14.563	14.583	
VALU	2	11 2D	67.0	67.0	25.0	7.0	1.0	
VALU	2	12 2I	14.748	100.0				
VALU	2	13 2D	0.0	0.0				
TABL	3	1	2	8		LIN	LIN	
TITL	3	2		PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE				
TITL	3	3		N2 CLOSING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)				
TITL	3	4		N2 CLOSING FLOWS VS TOTAL PRESSURE (PSIA)				
VALU	3	10 2I	0.0	14.590	14.625	14.658	14.680	
VALU	3	11 2D	67.0	67.0	11.0	7.0	0.8	
VALU	3	12 2I	14.813	100.0				
VALU	3	13 2D	0.0	0.0				
TABL	4	1	3	3	14	LIN	LIN	
TITL	4	2		CREHMAN LATENT LOAD (BTU/MAN-HR) VS TIME (SEC) AND TEMP (F)				
VALU	4	10 3I	0.0	24300.	28800.	42300.	43200.	
VALU	4	11 3D	65.0	70.0	70.0	253.375	253.375	
VALU	4	12 3D	70.0	70.0	70.0	305.0	305.0	
VALU	4	13 3D	75.0	70.0	70.0	363.375	363.375	
VALU	4	14 3I	46800.	54000.	61200.	64800.	68400.	
VALU	4	15 3D	65.0	90.0	253.375	253.375	90.0	
VALU	4	16 3D	70.0	135.0	305.0	305.0	135.0	
VALU	4	17 3D	75.0	180.0	363.375	363.375	180.0	
VALU	4	18 3I	72000.	77400.	83700.	86400.		
VALU	4	19 3D	65.0	175.0	175.0	70.0	70.0	
VALU	4	20 3D	70.0	225.0	225.0	70.0	70.0	
VALU	4	21 3D	75.0	280.0	280.0	70.0	70.0	
TABL	5	1	2	4		LIN	STP	
TITL	5	2		NUMBER OF PEOPLE IN HABITAT VS. TIME, SECONDS				
VALU	5	10 2I	0.0	28800.	79200.	86400.		
VALU	5	11 2D	8.0	8.0	8.0	8.0		
TABL	6	1	2	4		LIN	STP	

TABLE C-7 (CONTINUED)

## INPUT DATA FOR SPACE STATION MODEL

TITL	6	2	NUMBER OF PEOPLE IN LABORATORY VS. TIME, SECONDS						
VALU	6	10	2I	0.0	28800.	79200.	86400.		
VALU	6	11	2D	0.0	0.0	0.0	0.0		
TABL	7	1	2		6	LIN	LIN		
TITL	7	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE						
TITL	7	3	O2 OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)						
TITL	7	4	O2 OPENING FLOWS VS TOTAL PRESSURE (PSIA)						
VALU	7	10	2I	0.0	14.510	14.565	14.666	14.700 100.000	
VALU	7	11	2D	10.0	10.0	0.85	0.2	0.0 0.0	
TABL	8	1	2		6	LIN	LIN		
TITL	8	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE						
TITL	8	3	O2 CLOSING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)						
TITL	8	4	O2 CLOSING FLOWS VS TOTAL PRESSURE (PSIA)						
VALU	8	10	2I	0.0	14.605	14.672	14.745	14.819 100.000	
VALU	8	11	2D	10.0	10.0	0.6	0.25	0.0 0.0	
PLOT0									
PLOT2		1	2		HABITAT TEMPERATURE (F)				
PLOT2		1	4		HABITAT PRESSURE (PSIA)				
PLOT2		1	94		HABITAT O2 PRESSURE (PSIA)				
PLOT2		1	98		HABITAT DEW POINT (F)				
PLOT2		1	100		HABITAT CO2 PRESSURE (MMHG)				
PLOT2		2	2		LABORATORY TEMPERATURE (F)				
PLOT2		2	4		LABORATORY PRESSURE (PSIA)				
PLOT2		2	94		LABORATORY O2 PRESSURE (PSIA)				
PLOT2		2	98		LABORATORY DEW POINT (F)				
PLOT2		2	100		LABORATORY CO2 PRESSURE (MMHG)				
PLOT2		28	72		O2 ACCUMULATOR PRESSURE (PSIA)				
PLOT2		131	1		HAB. CO2 SUB #1 ACCUM. INLET FLOW (PPH)				
PLOT2		131	87		CO2 REMOVED BY HAB. SUBSYSTEM #1 (PPH)				
PLOT2		135	1		HAB. SUB. #1 CO2 ACCUM EXIT FLOW (PPH)				
PLOT2		135	72		CO2 ACCUM. PRESSURE (HAB. SUB. #1) (PSIA)				
PLOT2		141	10		O2 PRODUCED BY HAB. O2 GEN #1 (PPH)				
PLOT2		141	14		H2 GEN FROM HAB. O2 GEN #1 (PPH)				
PLOT2		202	33		H2 VENTED FROM HAB. O2 GEN #1 (PPH)				
PLOT2		207	33		H2 TO CO2 RED. FROM HAB O2 GEN #1 (PPH)				
PLOT2		331	1		LAB. CO2 SUB #1 ACCUM. INLET FLOW (PPH)				
PLOT2		331	87		CO2 REMOVED BY LAB. SUBSYSTEM #1 (PPH)				
PLOT2		335	1		LAB. SUB. #1 CO2 ACCUM EXIT FLOW (PPH)				
PLOT2		335	72		CO2 ACCUM. PRESSURE(LAB. SUB. #1) (PSIA)				
PLOT2		341	10		O2 PRODUCED BY LAB. O2 GEN #1 (PPH)				
PLOT2		341	14		H2 GEN FROM LAB. O2 GEN #1 (PPH)				
PLOT2		402	33		H2 VENTED FROM LAB. O2 GEN #1 (PPH)				
PLOT2		407	33		H2 TO CO2 RED. FROM LAB O2 GEN #1 (PPH)				
ENDC									

#### C.4.1.2 Input Data SSDATA Description (Continued)

##### CO<sub>2</sub> Removal

- . EDC
- . Molecular Sieve
- . SAWD

The fifth section contains table data whereby parameters or conditions that vary with time may be input. For example, the number of people in crew #1 for the habitat can be varied with time to permit simulation of the crew moving about the station.

#### C.4.1.3 Input Data Modification

The user has various options to select. These options define the bussing of hydrogen, nitrogen, carbon dioxide, and process air. For carbon dioxide a further choice is provided between intramodular and intermodular bussing. To date, none of the bussing options have been checked; however, the architecture and logic is in place for these options.

The process air bus option provides a path around the station for process air to flow to the various ECLS equipment. Without a bus, air is simply drawn from the room.

#### C.4.1.3 Input Data Modification (Continued)

An intramodule hydrogen bus causes any hydrogen generated from either of two units in the module to be dumped to a common line. The same exists for carbon dioxide but with the addition of a  $\text{CO}_2$  accumulation in each module and no accumulation with each  $\text{CO}_2$  removal unit. For an intermodule  $\text{CO}_2$  bus, the  $\text{CO}_2$  from all  $\text{CO}_2$  removal units dump to a common line with only one  $\text{CO}_2$  accumulator for the station.

At present, the nitrogen bus logic is not in place either in the flow connections or in the subroutines themselves where  $\text{N}_2$  purging needs to be modeled.

The user also can select which type of unit to perform an ECLSS function. The input setup shown in Table C-7 has Bosch for  $\text{CO}_2$  reduction, molecular sieve for  $\text{CO}_2$  removal, and solid polymer electrolysis for oxygen generation. To swap one unit for another to perform a function, simply make the component number the one for that function according to the following table:

<u>Function</u>	<u>Location</u>	Unit	Component
		<u>Number</u>	<u>Number</u>
CO <sub>2</sub> Reduction	Habitat	1	121
CO <sub>2</sub> Reduction	Habitat	2	123
CO <sub>2</sub> Reduction	Laboratory	1	321
CO <sub>2</sub> Reduction	Laboratory	2	323
CO <sub>2</sub> Removal	Habitat	1	131
CO <sub>2</sub> Removal	Habitat	2	133
CO <sub>2</sub> Removal	Laboratory	1	331
CO <sub>2</sub> Removal	Laboratory	2	333
O <sub>2</sub> Generation	Habitat	1	141
O <sub>2</sub> Generation	Habitat	2	142
O <sub>2</sub> Generation	Laboratory	1	341
O <sub>2</sub> Generation	Laboratory	2	343

Units that are not used in the simulation should be numbered 500 or above according to Table C-8.

TABLE C-8  
 COMPONENT NUMBERS FOR UNUSED UNITS

<u>Component Number</u>	<u>Equipment</u>	<u>Location</u>	<u>Unit Number</u>
540	Sabatier	Habitat	1
541	Bosch	"	1
542	Sabatier	"	2
543	Bosch	"	2
550	EDC	"	1
551	SAWD	"	1
552	Molecular Sieve	"	1
553	EDC	"	2
554	SAWD	"	2
555	Molecular Sieve	"	2
560	SPE	"	1
561	KOH	"	1
562	SPE	"	2
563	KOH	"	2
570	Sabatier	Laboratory	1
571	Bosch	"	1
572	Sabatier	"	2
573	Bosch	"	2
580	EDC	"	1
581	SAWD	"	1
582	Molecular Sieve	"	1
583	EDC	"	2
584	SAWD	"	2
585	Molecular Sieve	"	2
590	SPE	"	1
591	KOH	"	1
592	SPE	"	2
593	KOH	"	2

#### C.4.1.4 Program Output

Five output files are generated; three are tabular data and two are for plots. Table C-9 shows the output data for the input file shown in Table C-7. As discussed earlier, plots are generated using the CAETMS software [3]. Plots generated are presented in Figures C-1 through C-20.

#### C.4.2 Operation Using the Langley Prime Computer

For instructions on installing and using a program from Hamilton Standard's IBM to Langley's PRIME, please refer to instructions provided in the ECLSB User's Manual [1], Section 4.2.



[illegible]



HABITAT PARAMETERS										LABORATORY PARAMETERS										REMOVAL				ACCUM INLET/ACCUM EXIT				O2 GENERATED		WATER FLOW			
TIME		IHAB		IDEM		CO2		O2		IPRESS		LAB		DEM		CO2		O2		PRESS		PRESS		PRESS		ACCUM		FLO		O2		WATER FLOW	
		TEMP		PT		PRESS		PRESS		PRESS		TEMP		PT		PRESS		PRESS		PRESS		PRESS		PRESS		FLO		FLO		FLO		FLO	
MIN		F		F		F		F		F		F		F		F		F		F		F		F		F		F		F		F	
491.0	70.2	45.3	2	527	3	164	14	74	170	3	138	7	2	083	3	174	14	71	345	280	0.440	0.439	0.318	0.270	30.3	30.4	350	350	0.80	0.41	0.80	0.41	
496.0	69.2	45.4	2	536	3	156	14	70	169	4	138	7	2	083	3	168	14	68	342	277	0.439	0.439	0.318	0.270	30.5	30.7	350	350	0.80	0.41	0.80	0.41	
501.0	70.1	45.6	2	555	3	160	14	72	170	5	138	7	2	089	3	170	14	69	340	272	0.439	0.439	0.318	0.270	30.8	31.1	350	350	0.80	0.41	0.80	0.41	
506.0	69.4	45.7	2	573	3	165	14	74	170	5	138	8	2	096	3	175	14	71	348	279	0.438	0.437	0.318	0.270	31.1	31.5	350	350	0.80	0.41	0.80	0.41	
511.0	69.8	45.8	2	584	3	160	14	72	169	7	138	9	2	098	3	171	14	69	351	281	0.438	0.437	0.318	0.270	31.3	31.9	350	350	0.80	0.41	0.80	0.41	
516.0	69.6	45.8	2	595	3	158	14	71	169	7	138	9	2	103	3	169	14	68	348	276	0.437	0.436	0.318	0.270	31.6	32.2	350	350	0.80	0.41	0.80	0.41	
521.0	70.3	45.9	2	612	3	162	14	73	170	4	139	0	12	111	3	173	14	70	350	279	0.437	0.436	0.318	0.270	31.9	32.7	350	350	0.80	0.41	0.80	0.41	
526.0	70.2	46.0	2	625	3	162	14	73	170	4	139	1	12	111	3	173	14	70	356	283	0.436	0.436	0.318	0.270	32.2	32.8	350	350	0.80	0.41	0.80	0.41	
531.0	69.7	46.0	2	635	3	159	14	72	169	6	139	1	12	121	3	169	14	69	356	281	0.436	0.436	0.318	0.270	32.4	32.1	350	350	0.80	0.41	0.80	0.41	
536.0	69.9	46.0	2	647	3	159	14	72	170	1	139	2	12	128	3	171	14	70	355	280	0.436	0.436	0.318	0.270	32.4	32.1	350	350	0.80	0.41	0.80	0.41	
541.0	70.3	46.1	2	661	3	161	14	73	170	3	139	3	12	136	3	173	14	71	359	284	0.436	0.436	0.318	0.270	32.4	32.1	350	350	0.80	0.41	0.80	0.41	
546.0	70.1	47.2	2	672	3	160	14	73	169	8	140	7	2	141	3	170	14	70	352	277	0.436	0.436	0.318	0.270	32.4	32.1	350	350	0.80	0.41	0.80	0.41	
551.0	69.4	46.2	2	683	3	164	14	75	170	3	140	4	2	151	3	175	14	72	367	289	0.440	0.439	0.341	0.273	30.3	30.5	350	350	0.80	0.43	0.80	0.	

[illegible]

[illegible]

SPACE STATION OUTPUT PARAMETERS TABLE 1																													
HABITAT PARAMETERS										LABORATORY PARAMETERS										CO2 REMOVAL									
TIME	HAB	IDEM	CO2	O2	PRESS	LAB	IDEM	CO2	O2	PRESS	LAB	IDEM	CO2	O2	PRESS	LAB	IDEM	CO2	O2	ACCUM	INLET	ACCUM	EXIT	ACCUM	O2	GENERATED			
TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	TEMP	PT	REMOVAL	PPH	PPH	PPH	PPH	PPH	PPH	PPH	PPH	PPH
MIN	F	F	F	F	F	F	F	F	F	F	F	F	F	F	F	F	F	F	F	PSIA	PSIA	PSIA	PSIA	PSIA	PSIA	PSIA	PSIA	PSIA	PSIA
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436	0.409	10.345	26.7	32.3	388	388	0.89	10.53							
1226.0	70.7	45.2	3.127	13.169	14.74	70.6	40.5	2.654	13.179	14.71	4221	354	10.446	0.436															



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SPACE STATION OUTPUT PARAMETERS TABLE 2

SPACE STATION OUTPUT PARAMETERS TABLE 2																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																				
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TIME	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG	TEMP	DEM	CO2	O2	PRESS	PT	MMHG

[illegible]



TIME	TEMP	DEM	CO2	O2	TEMP	DEM	CO2	O2	TEMP	DEM	CO2	O2	TEMP	DEM	CO2	O2	TEMP	DEM	CO2	O2
		PT	PRESS			PT	PRESS			PT	PRESS			PT	PRESS			PT	PRESS	
MIN	F		MMHG	PSIA	F		MMHG	PSIA	F		MMHG	PSIA	F		MMHG	PSIA	F		MMHG	PSIA
491.0	76.45	42.99	2.365	3.149	76.45	42.99	2.365	3.149	75.17	40.79	2.219	3.154	75.17	40.79	2.219	3.154	75.17	40.79	2.219	3.154
496.0	75.38	43.09	2.377	3.149	75.38	43.09	2.377	3.149	74.19	40.88	2.226	3.154	74.19	40.88	2.226	3.154	74.19	40.88	2.226	3.154
501.0	76.02	43.21	2.388	3.149	76.02	43.21	2.388	3.149	74.86	40.97	2.234	3.154	74.86	40.97	2.234	3.154	74.86	40.97	2.234	3.154
506.0	76.68	43.33	2.399	3.148	76.68	43.33	2.399	3.148	75.41	41.06	2.242	3.154	75.41	41.06	2.242	3.154	75.41	41.06	2.242	3.154
511.0	75.93	43.40	2.410	3.148	75.93	43.40	2.410	3.148	74.64	41.13	2.250	3.154	74.64	41.13	2.250	3.154	74.64	41.13	2.250	3.154
516.0	75.67	43.45	2.421	3.148	75.67	43.45	2.421	3.148	74.50	41.18	2.258	3.154	74.50	41.18	2.258	3.154	74.50	41.18	2.258	3.154
521.0	76.35	43.52	2.432	3.148	76.35	43.52	2.432	3.148	75.18	41.25	2.266	3.154	75.18	41.25	2.266	3.154	75.18	41.25	2.266	3.154
526.0	76.32	43.58	2.442	3.148	76.32	43.58	2.442	3.148	75.02	41.31	2.274	3.154	75.02	41.31	2.274	3.154	75.02	41.31	2.274	3.154
531.0	75.79	43.61	2.452	3.148	75.79	43.61	2.452	3.148	74.54	41.36	2.282	3.154	74.54	41.36	2.282	3.154	74.54	41.36	2.282	3.154
536.0	76.00	43.65	2.462	3.148	76.00	43.65	2.462	3.148	74.86	41.41	2.290	3.154	74.86	41.41	2.290	3.154	74.86	41.41	2.290	3.154
541.0	76.35	43.70	2.472	3.148	76.35	43.70	2.472	3.148	75.12	41.46	2.298	3.153	75.12	41.46	2.298	3.153	75.12	41.46	2.298	3.153
546.0	76.05	44.76	2.481	3.146	76.05	44.76	2.481	3.146	74.74	42.70	2.306	3.152	74.74	42.70	2.306	3.152	74.74	42.70	2.306	3.152
551.0	76.58	44.52	2.491	3.146	76.58	44.52	2.491	3.146	75.25	42.40	2.314	3.152	75.25	42.40	2.314	3.152	75.25	42.40	2.314	3.152
556.0	75.23	44.57	2.500	3.146	75.23	44.57	2.500	3.146	74.07	42.39	2.323	3.152	74.07	42.39	2.323	3.152	74.07	42.39	2.323	3.152
561.0	75.92	44.46	2.510	3.146	75.92	44.46	2.510	3.146	74.81	42.39	2.331	3.152	74.81	42.39	2.331	3.152	74.81	42.39	2.331	3.152
566.0	76.81	44.49	2.520	3.146	76.81	44.49	2.520	3.146	75.51	42.41	2.339	3.152	75.51	42.41	2.339	3.152	75.51	42.41	2.339	3.152
571.0	75.97	44.46	2.529	3.146	75.97	44.46	2.529	3.146	74.63	42.40	2.347	3.152	74.63	42.40	2.347	3.152	74.63	42.40	2.347	3.152
576.0	75.54	44.41	2.538	3.146	75.54	44.41	2.538	3.146	74.41	42.38	2.356	3.152	74.41	42.38	2.356	3.152	74.41	42.38	2.356	3.152
581.0	76.35	44.41	2.547	3.146	76.35	44.41	2.547	3.146	75.21	42.39	2.364	3.152	75.21	42.39	2.364	3.152	75.21	42.39	2.364	3.152
586.0	76.42	44.41	2.556	3.146	76.42	44.41	2.556	3.146	74.50	42.37	2.380	3.152	74.50	42.37	2.380	3.152	74.50	42.37	2.380	3.152
591.0	75.76	44.37	2.564	3.146	75.76	44.37	2.564	3.146	74.83	42.36	2.388	3.152	74.83	42.36	2.388	3.152	74.83	42.36	2.388	3.152
596.0	75.93	44.35	2.573	3.146	75.93	44.35	2.573	3.146	75.16	42.36	2.396	3.152	75.16	42.36	2.396	3.152	75.16	42.36	2.396	3.152
601.0	76.39	44.35	2.582	3.145	76.39	44.35	2.582	3.145	74.77	43.50	2.403	3.150	74.77	43.50	2.403	3.150	74.77	43.50	2.403	3.150
606.0	76.09	45.35	2.589	3.145	76.09	45.35	2.589	3.145	75.25	43.13	2.412	3.151	75.25	43.13	2.412	3.151	75.25	43.13	2.412	3.151
611.0	76.58	45.07	2.599	3.145	76.58	45.07	2.599	3.145	74.03	43.06	2.420	3.151	74.03	43.06	2.420	3.151	74.03	43.06	2.420	3.151
616.0	75.19	44.97	2.606	3.145	75.19	44.97	2.606	3.145	74.82	43.02	2.428	3.151	74.82	43.02	2.428	3.151	74.82	43.02	2.428	3.151
621.0	75.92	44.92	2.615	3.145	75.92	44.92	2.615	3.145	75.54	43.01	2.436	3.151	75.54	43.01	2.436	3.151	75.54	43.01	2.436	3.151
626.0	76.84	44.93	2.624	3.145	76.84	44.93	2.624	3.145	74.62	42.95	2.443	3.151	74.62	42.95	2.443	3.151	74.62	42.95	2.443	3.151
631.0	75.96	44.86	2.632	3.145	75.96	44.86	2.632	3.145	74.39	42.89	2.451	3.151	74.39	42.89	2.451	3.151	74.39	42.89	2.451	3.151
636.0	75.52	44.77	2.639	3.145	75.52	44.77	2.639	3.145	75.22	42.87	2.459	3.151	75.22	42.87	2.459	3.151	75.22	42.87	2.459	3.151
641.0	76.36	44.75	2.648	3.145	76.36	44.75	2.648	3.145	75.08	42.83	2.467	3.151	75.08	42.83	2.467	3.151	75.08	42.83	2.467	3.151
646.0	76.43	44.73	2.656	3.145	76.43	44.73	2.656	3.145	74.48	42.79	2.474	3.151	74.48	42.79	2.474	3.151	74.48	42.79	2.474	3.151
651.0	75.75	44.67	2.663	3.145	75.75	44.67	2.663	3.145	74.83	42.75	2.482	3.151	74.83	42.75	2.482	3.151	74.83	42.75	2.482	3.151
656.0	75.92	44.62	2.671	3.145	75.92	44.62	2.671	3.145	75.17	42.73	2.490	3.151	75.17	42.73	2.490	3.151	75.17	42.73	2.490	3.151
661.0	76.40	44.61	2.679	3.145	76.40	44.61	2.679	3.145	74.77	43.83	2.496	3.149	74.77	43.83	2.496	3.149	74.77	43.83	2.496	3.149
666.0	76.09	45.59	2.686	3.144	76.09	45.59	2.686	3.144	75.25	43.44	2.504	3.150	75.25	43.44	2.504	3.150	75.25	43.44	2.504	3.150
671.0	76.58	45.29	2.694	3.144	76.58	45.29	2.694	3.144	74.02	43.34	2.512	3.150	74.02	43.34	2.512	3.150	74.02	43.34	2.512	3.150
676.0	75.19	45.17	2.701	3.144	75.19	45.17	2.701	3.144	74.81	43.28	2.519	3.150	74.81	43.28	2.519	3.150	74.81	43.28	2.519	3.150
681.0	75.91	45.10	2.709	3.144	75.91	45.10	2.709	3.144	75.55	43.24	2.526	3.150	75.55	43.24	2.526	3.150	75.55	43.24	2.526	3.150
686.0	76.85	45.10	2.717	3.144	76.85	45.10	2.717	3.144	74.62	43.17	2.534	3.150	74.62	43.17	2.534	3.150	74.62	43.17	2.534	3.150
691.0	75.97	45.01	2.724	3.144	75.97	45.01	2.724	3.144	74.38	43.09	2.541	3.150	74.38	43.09	2.541	3.150	74.38	43.09	2.541	3.150
696.0	75.51	44.91	2.731	3.144	75.51	44.91	2.731	3.144	75.22	43.05	2.548	3.150	75.22	43.05	2.548	3.150	75.22	43.05	2.548	3.150
701.0	76.35	44.88	2.739	3.144	76.35	44.88	2.739	3.144	75.09	43.00	2.555	3.150	75.09	43.00	2.555	3.150	75.09	43.00	2.555	3.150
706.0	76.44	44.85	2.746	3.144	76.44	44.85	2.746	3.144	74.48	42.90	2.561	3.150	74.48	42.90	2.561	3.150	74.48	42.90	2.561	3.150
711.0	75.75	44.71	2.751	3.144	75.75	44.71	2.751	3.144	74.81	42.76	2.566	3.150	74.81	42.76	2.566	3.150	74.81	42.76	2.566	3.150
716.0	75.90	44.48	2.753	3.144	75.90	44.48	2.753	3.144	75.17	42.57	2.569	3.150	75.17	42.57	2.569	3.150	75.17	42.57	2.569	3.150
721.0	76.39	44.19	2.752	3.145	76.39	44.19	2.752	3.145	74.77	43.50	2.569	3.149	74.77	43.50	2.569	3.149	74.77	43.50	2.569	3.149
726.0	76.09	44.88	2.749	3.144	76.09	44.88	2.749	3.144	75.25	42.94	2.571	3.150	75.25	42.94	2.571	3.150	75.25	42.94	2.571	3.150
731.0	76.57	44.33	2.747	3.145	76.57	44.33	2.747	3.145	75.25	42.94	2.571	3.150	75.25	42.94	2.571	3.150	75.25	42.94	2.571	3.150

SPACE STATION OUTPUT PARAMETERS TABLE 2

[illegible]

## SPACE STATION OUTPUT PARAMETERS TABLE 2

NODE 1 PARAMETERS										NODE 2 PARAMETERS										NODE 3 PARAMETERS										NODE 4 PARAMETERS									
TIME	TEMP	DEM	CO2	O2	PT	TEMP	DEM	CO2	O2	PT	TEMP	DEM	CO2	O2	PT	TEMP	DEM	CO2	O2	PT	TEMP	DEM	CO2	O2	PT	TEMP	DEM	CO2	O2	PT									
MIN	F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA										
981.0	75.91	45.05	2.919	3.147		75.91	45.05	2.919	3.147		74.79	43.21	2.733	3.152		74.79	43.21	2.733	3.152		74.79	43.21	2.733	3.152		74.79	43.21	2.733	3.152										
986.0	76.83	45.04	2.925	3.147		76.83	45.04	2.925	3.147		75.54	43.18	2.738	3.152		75.54	43.18	2.738	3.152		75.54	43.18	2.738	3.152		75.54	43.18	2.738	3.152										
991.0	75.97	44.96	2.931	3.147		75.97	44.96	2.931	3.147		74.64	43.11	2.744	3.152		74.64	43.11	2.744	3.152		74.64	43.11	2.744	3.152		74.64	43.11	2.744	3.152										
996.0	75.52	44.87	2.937	3.147		75.52	44.87	2.937	3.147		74.39	43.04	2.749	3.153		74.39	43.04	2.749	3.153		74.39	43.04	2.749	3.153		74.39	43.04	2.749	3.153										
1001.0	76.34	44.85	2.943	3.147		76.34	44.85	2.943	3.147		75.20	43.00	2.755	3.133		75.20	43.00	2.755	3.133		75.20	43.00	2.755	3.133		75.20	43.00	2.755	3.133										
1006.0	76.44	44.81	2.949	3.147		76.44	44.81	2.949	3.147		75.09	42.96	2.761	3.153		75.09	42.96	2.761	3.153		75.09	42.96	2.761	3.153		75.09	42.96	2.761	3.153										
1011.0	75.76	44.75	2.955	3.147		75.76	44.75	2.955	3.147		74.49	42.90	2.766	3.133		74.49	42.90	2.766	3.133		74.49	42.90	2.766	3.133		74.49	42.90	2.766	3.133										
1016.0	75.91	44.70	2.960	3.147		75.91	44.70	2.960	3.147		74.81	42.86	2.772	3.153		74.81	42.86	2.772	3.153		74.81	42.86	2.772	3.153		74.81	42.86	2.772	3.153										
1021.0	76.39	44.68	2.966	3.147		76.39	44.68	2.966	3.147		75.17	42.83	2.777	3.153		75.17	42.83	2.777	3.153		75.17	42.83	2.777	3.153		75.17	42.83	2.777	3.153										
1026.0	76.10	45.63	2.970	3.146		76.10	45.63	2.970	3.146		74.78	43.91	2.781	3.151		74.78	43.91	2.781	3.151		74.78	43.91	2.781	3.151		74.78	43.91	2.781	3.151										
1031.0	76.58	45.28	2.975	3.146		76.58	45.28	2.975	3.146		75.25	43.48	2.786	3.152		75.25	43.48	2.786	3.152		75.25	43.48	2.786	3.152		75.25	43.48	2.786	3.152										
1036.0	75.17	45.09	2.978	3.146		75.17	45.09	2.978	3.146		74.01	43.34	2.791	3.152		74.01	43.34	2.791	3.152		74.01	43.34	2.791	3.152		74.01	43.34	2.791	3.152										
1041.0	75.91	44.94	2.983	3.146		75.91	44.94	2.983	3.146		74.81	43.22	2.795	3.152		74.81	43.22	2.795	3.152		74.81	43.22	2.795	3.152		74.81	43.22	2.795	3.152										
1046.0	76.86	44.82	2.983	3.147		76.86	44.82	2.983	3.147		75.56	43.12	2.798	3.152		75.56	43.12	2.798	3.152		75.56	43.12	2.798	3.152		75.56	43.12	2.798	3.152										
1051.0	75.95	44.62	2.984	3.147		75.95	44.62	2.984	3.147		74.61	42.97	2.801	3.152		74.61	42.97	2.801	3.152		74.61	42.97	2.801	3.152		74.61	42.97	2.801	3.152										
1056.0	75.50	44.39	2.984	3.147		75.50	44.39	2.984	3.147		74.38	42.81	2.803	3.153		74.38	42.81	2.803	3.153		74.38	42.81	2.803	3.153		74.38	42.81	2.803	3.153										
1061.0	76.37	44.21	2.984	3.148		76.37	44.21	2.984	3.148		75.23	42.67	2.805	3.153		75.23	42.67	2.805	3.153		75.23	42.67	2.805	3.153		75.23	42.67	2.805	3.153										
1066.0	76.43	44.01	2.983	3.148		76.43	44.01	2.983	3.148		75.08	42.52	2.806	3.153		75.08	42.52	2.806	3.153		75.08	42.52	2.806	3.153		75.08	42.52	2.806	3.153										
1071.0	75.73	43.78	2.981	3.148		75.73	43.78	2.981	3.148		74.46	42.35	2.807	3.153		74.46	42.35	2.807	3.153		74.46	42.35	2.807	3.153		74.46	42.35	2.807	3.153										
1076.0	75.93	43.55	2.978	3.149		75.93	43.55	2.978	3.149		74.83	42.18	2.807	3.154		74.83	42.18	2.807	3.154		74.83	42.18	2.807	3.154		74.83	42.18	2.807	3.154										
1081.0	76.42	43.34	2.975	3.149		76.42	43.34	2.975	3.149		75.18	42.02	2.806	3.154		75.18	42.02	2.806	3.154		75.18	42.02	2.806	3.154		75.18	42.02	2.806	3.154										
1086.0	76.08	44.16	2.971	3.149		76.08	44.16	2.971	3.149		74.76	43.01	2.805	3.153		74.76	43.01	2.805	3.153		74.76	43.01	2.805	3.153		74.76	43.01	2.805	3.153										
1091.0	76.56	43.72	2.968	3.149		76.56	43.72	2.968	3.149		75.25	42.50	2.804	3.154		75.25	42.50	2.804	3.154		75.25	42.50	2.804	3.154		75.25	42.50	2.804	3.154										
1096.0	75.19	43.48	2.964	3.150		75.19	43.48	2.964	3.150		74.03	42.30	2.803	3.154		74.03	42.30	2.803	3.154		74.03	42.30	2.803	3.154		74.03	42.30	2.803	3.154										
1101.0	75.98	43.28	2.961	3.150		75.98	43.28	2.961	3.150		74.84	42.13	2.802	3.155		74.84	42.13	2.802	3.155		74.84	42.13	2.802	3.155		74.84	42.13	2.802	3.155										
1106.0	76.83	43.13	2.958	3.151		76.83	43.13	2.958	3.151		75.54	41.98	2.801	3.155		75.54	41.98	2.801	3.155		75.54	41.98	2.801	3.155		75.54	41.98	2.801	3.155										
1111.0	75.89	42.96	2.955	3.151		75.89	42.96	2.955	3.151		74.58	41.83	2.800	3.155		74.58	41.83	2.800	3.155		74.58	41.83	2.800	3.155		74.58	41.83	2.800	3.155										
1116.0	75.56	42.79	2.952	3.151		75.56	42.79	2.952	3.151		74.41	41.67	2.799	3.156		74.41	41.67	2.799	3.156		74.41	41.67	2.799	3.156		74.41	41.67	2.799	3.156										
1121.0	76.44	42.66	2.949	3.152		76.44	42.66	2.949	3.152		75.27	41.55	2.797	3.156		75.27	41.55	2.797	3.156		75.27	41.55	2.797	3.156		75.27	41.55	2.797	3.156										
1126.0	76.37	42.54	2.946	3.152		76.37	42.54	2.946	3.152		75.04	41.42	2.796	3.156		75.04	41.42	2.796	3.156		75.04	41.42	2.796	3.156		75.04	41.42	2.796	3.156										
1131.0	75.70	42.42	2.943	3.152		75.70	42.42	2.943	3.152		74.44	41.30	2.794	3.156		74.44	41.30	2.794	3.156		74.44	41.30	2.794	3.156		74.44	41.30	2.794	3.156										
1136.0	76.29	42.30	2.941	3.153		76.29	42.30	2.941	3.153		75.02	41.18	2.793	3.157		75.02	41.18	2.793	3.157		75.02	41.18	2.793	3.157		75.02	41.18	2.793	3.157										
1141.0	76.17	42.20	2.938	3.153		76.17	42.20	2.938	3.153		75.06	41.07	2.792	3.157		75.06	41.07	2.792	3.157		75.06	41.07	2.792	3.157		75.06	41.07	2.792	3.157										
1146.0	75.76	43.18	2.935	3.152		75.76	43.18	2.935	3.152		74.58	42.17	2.789	3.156		74.58	42.17	2.789	3.156		74.58	42.17	2.789	3.156		74.58	42.17	2.789	3.156										
1151.0	76.81	42.81	2.934	3.153		76.81	42.81	2.934	3.153		75.39	41.72	2.788	3.157		75.39	41.72	2.788	3.157		75.39	41.72	2.788	3.157		75.39	41.72	2.788	3.157										
1156.0	75.40	42.72	2.932	3.153		75.40	42.72	2.932	3.153		74.15	41.60	2.787	3.157		74.15	41.60	2.787	3.157		74.15	41.60	2.787	3.157		74.15	41.60	2.787	3.157										
1161.0	76.24	42.64	2.932	3.153		76.24	42.64	2.932	3.153		74.95	41.50	2.786	3.157		74.95	41.50	2.786	3.157		74.95	41.50	2.786	3.157		74.95	41.50	2.786	3.157										
1166.0	76.41	42.61	2.931	3.153		76.41	42.61	2.931	3.153		75.32	41.43	2.786	3.158		75.32	41.43	2.786	3.158		75.32	41.43	2.786	3.158		75.32	41.43	2.786	3.158										
1171.0	75.80	42.57	2.931	3.154		75.80	42.57	2.931	3.154		74.95	41.35	2.785	3.158		74.95	41.35	2.785	3.158		74.95	41.35	2.785	3.158		74.95	41.35	2.785	3.158										
1176.0	75.93	42.55	2.932	3.154		75.93	42.55	2.932	3.154		74.61	41.30	2.785	3.158		74.61	41.30	2.785	3.158		74.61	41.30	2.785	3.158		74.61	41.30	2.785	3.158										
1181.0	76.39	42.56	2.933	3.154		76.39	42.56	2.933	3.154		75.23	41.26	2.786	3.158		75.23	41.26	2.786	3.158		75.23	41.26	2.786	3.158		75.23	41.26	2.786	3.158										
1186.0	76.12	42.57	2.934	3.154		76.12	42.57	2.934	3.154		74.91	41.22	2.786	3.158		74.91	41.22	2.786	3.158		74.91	41.22	2.786	3.158		74.91	41.22	2.786	3.158										
1191.0	75.84	42.58	2.936	3.154		75.84	42.58	2.936	3.154		74.54	41.19	2.787	3.159		74.54	41.19	2.787	3.159		74.54	41.19	2.787	3.159		74.54													

### SPACE STATION OUTPUT PARAMETERS TABLE 2

NODE 1 PARAMETERS										NODE 2 PARAMETERS										NODE 3 PARAMETERS										NODE 4 PARAMETERS									
TIME	TEMP	DEM	CO2	O2	PRESS	TEMP	DEM	CO2	O2	PRESS	TEMP	DEM	CO2	O2	PRESS	TEMP	DEM	CO2	O2	PRESS	TEMP	DEM	CO2	O2	PRESS														
	F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA		F		MMHG	PSIA															
MIN																																							
1226.0	76.79	43.43	2.953	3.154	76.79	43.43	2.953	3.154	75.52	41.87	2.796	3.159	75.52	41.87	2.796	3.159	75.52	41.87	2.796	3.159	75.52	41.87	2.796	3.159															
1231.0	75.99	43.40	2.955	3.154	75.99	43.40	2.955	3.154	74.65	41.83	2.797	3.159	74.65	41.83	2.797	3.159	74.65	41.83	2.797	3.159	74.65	41.83	2.797	3.159															
1236.0	75.56	43.34	2.957	3.154	75.56	43.34	2.957	3.154	74.41	41.77	2.799	3.159	74.41	41.77	2.799	3.159	74.41	41.77	2.799	3.159	74.41	41.77	2.799	3.159															
1241.0	76.35	43.32	2.960	3.154	76.35	43.32	2.960	3.154	75.21	41.73	2.801	3.159	75.21	41.73	2.801	3.159	75.21	41.73	2.801	3.159	75.21	41.73	2.801	3.159															
1246.0	76.41	43.30	2.962	3.154	76.41	43.30	2.962	3.154	75.08	41.70	2.802	3.159	75.08	41.70	2.802	3.159	75.08	41.70	2.802	3.159	75.08	41.70	2.802	3.159															
1251.0	75.76	43.26	2.964	3.154	75.76	43.26	2.964	3.154	74.49	41.66	2.804	3.159	74.49	41.66	2.804	3.159	74.49	41.66	2.804	3.159	74.49	41.66	2.804	3.159															
1256.0	75.95	43.23	2.966	3.155	75.95	43.23	2.966	3.155	74.84	41.62	2.805	3.160	74.84	41.62	2.805	3.160	74.84	41.62	2.805	3.160	74.84	41.62	2.805	3.160															
1261.0	76.40	43.21	2.969	3.153	76.40	43.21	2.969	3.153	75.17	41.59	2.807	3.160	75.17	41.59	2.807	3.160	75.17	41.59	2.807	3.160	75.17	41.59	2.807	3.160															
1266.0	76.07	44.22	2.970	3.153	76.07	44.22	2.970	3.153	74.76	42.74	2.808	3.158	74.76	42.74	2.808	3.158	74.76	42.74	2.808	3.158	74.76	42.74	2.808	3.158															
1271.0	76.56	43.93	2.972	3.154	76.56	43.93	2.972	3.154	75.24	42.35	2.810	3.159	75.24	42.35	2.810	3.159	75.24	42.35	2.810	3.159	75.24	42.35	2.810	3.159															
1276.0	75.22	43.83	2.974	3.154	75.22	43.83	2.974	3.154	74.05	42.27	2.811	3.159	74.05	42.27	2.811	3.159	74.05	42.27	2.811	3.159	74.05	42.27	2.811	3.159															
1281.0	75.97	43.77	2.976	3.154	75.97	43.77	2.976	3.154	74.85	42.20	2.813	3.159	74.85	42.20	2.813	3.159	74.85	42.20	2.813	3.159	74.85	42.20	2.813	3.159															
1286.0	76.82	43.74	2.978	3.154	76.82	43.74	2.978	3.154	75.53	42.15	2.815	3.159	75.53	42.15	2.815	3.159	75.53	42.15	2.815	3.159	75.53	42.15	2.815	3.159															
1291.0	75.91	43.67	2.980	3.155	75.91	43.67	2.980	3.155	74.59	42.09	2.817	3.160	74.59	42.09	2.817	3.160	74.59	42.09	2.817	3.160	74.59	42.09	2.817	3.160															
1296.0	75.56	43.57	2.982	3.155	75.56	43.57	2.982	3.155	74.25	41.95	2.820	3.160	74.25	41.95	2.820	3.160	74.25	41.95	2.820	3.160	74.25	41.95	2.820	3.160															
1301.0	76.40	43.51	2.983	3.155	76.40	43.51	2.983	3.155	75.05	41.88	2.820	3.160	75.05	41.88	2.820	3.160	75.05	41.88	2.820	3.160	75.05	41.88	2.820	3.160															
1306.0	76.38	43.43	2.983	3.155	76.38	43.43	2.983	3.155	74.46	41.79	2.821	3.160	74.46	41.79	2.821	3.160	74.46	41.79	2.821	3.160	74.46	41.79	2.821	3.160															
1311.0	75.72	43.32	2.983	3.155	75.72	43.32	2.983	3.155	74.86	41.70	2.821	3.160	74.86	41.70	2.821	3.160	74.86	41.70	2.821	3.160	74.86	41.70	2.821	3.160															
1316.0	75.98	43.21	2.982	3.156	75.98	43.21	2.982	3.156	75.17	41.62	2.821	3.160	75.17	41.62	2.821	3.160	75.17	41.62	2.821	3.160	75.17	41.62	2.821	3.160															
1321.0	76.41	43.12	2.980	3.156	76.41	43.12	2.980	3.156	74.73	42.70	2.819	3.160	74.73	42.70	2.819	3.160	74.73	42.70	2.819	3.160	74.73	42.70	2.819	3.160															
1326.0	76.04	44.04	2.977	3.156	76.04	44.04	2.977	3.156	75.24	42.25	2.819	3.160	75.24	42.25	2.819	3.160	75.24	42.25	2.819	3.160	75.24	42.25	2.819	3.160															
1331.0	76.55	43.65	2.975	3.156	76.55	43.65	2.975	3.156	74.05	42.11	2.817	3.161	74.05	42.11	2.817	3.161	74.05	42.11	2.817	3.161	74.05	42.11	2.817	3.161															
1336.0	75.22	43.46	2.971	3.156	75.22	43.46	2.971	3.156	74.84	41.97	2.815	3.161	74.84	41.97	2.815	3.161	74.84	41.97	2.815	3.161	74.84	41.97	2.815	3.161															
1341.0	75.97	43.30	2.968	3.157	75.97	43.30	2.968	3.157	75.53	41.85	2.813	3.161	75.53	41.85	2.813	3.161	75.53	41.85	2.813	3.161	75.53	41.85	2.813	3.161															
1346.0	76.82	43.16	2.964	3.157	76.82	43.16	2.964	3.157	74.59	41.71	2.811	3.162	74.59	41.71	2.811	3.162	74.59	41.71	2.811	3.162	74.59	41.71	2.811	3.162															
1351.0	75.89	42.99	2.959	3.157	75.89	42.99	2.959	3.157	74.41	41.56	2.808	3.162	74.41	41.56	2.808	3.162	74.41	41.56	2.808	3.162	74.41	41.56	2.808	3.162															
1356.0	75.56	42.80	2.953	3.158	75.56	42.80	2.953	3.158	75.26	41.42	2.804	3.163	75.26	41.42	2.804	3.163	75.26	41.42	2.804	3.163	75.26	41.42	2.804	3.163															
1361.0	76.44	42.64	2.947	3.159	76.44	42.64	2.947	3.159	74.45	41.14	2.796	3.163	74.45	41.14	2.796	3.163	74.45	41.14	2.796	3.163	74.45	41.14	2.796	3.163															
1366.0	76.37	42.47	2.941	3.159	76.37	42.47	2.941	3.159	74.89	40.99	2.791	3.164	74.89	40.99	2.791	3.164	74.89	40.99	2.791	3.164	74.89	40.99	2.791	3.164															
1371.0	75.69	42.29	2.934	3.159	75.69	42.29	2.934	3.159	75.05	41.28	2.800	3.163	75.05	41.28	2.800	3.163	75.05	41.28	2.800	3.163	75.05	41.28	2.800	3.163															
1376.0	76.05	42.11	2.927	3.160	76.05	42.11	2.927	3.160	75.10	40.84	2.786	3.163	75.10	40.84	2.786	3.163	75.10	40.84	2.786	3.163	75.10	40.84	2.786	3.163															
1381.0	76.27	41.92	2.919	3.160	76.27	41.92	2.919	3.160	74.72	41.89	2.780	3.163	74.72	41.89	2.780	3.163	74.72	41.89	2.780	3.163	74.72	41.89	2.780	3.163															
1386.0	76.01	42.80	2.909	3.160	76.01	42.80	2.909	3.160	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163															
1391.0	76.66	42.34	2.901	3.161	76.66	42.34	2.901	3.161	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163	75.31	41.38	2.774	3.163															
1396.0	75.86	42.10	2.892	3.161	75.86	42.10	2.892	3.161	74.37	41.19	2.768	3.165	74.37	41.19	2.768	3.165	74.37	41.19	2.768	3.165	74.37	41.19	2.768	3.165															
1401.0	76.38	41.68	2.874	3.162	76.38	41.68	2.874	3.162	75.00	40.99	2.762	3.165	75.00	40.99	2.762	3.165	75.00	40.99	2.762	3.165	75.00	40.99	2.762	3.165															
1406.0	76.20	41.68	2.874	3.162	76.20	41.68	2.874	3.162	74.29	40.65	2.749	3.166	74.29	40.65	2.749	3.166	74.29	40.65	2.749	3.166	74.29	40.65	2.749	3.166															
1411.0	75.29	41.50	2.864	3.163	75.29	41.50	2.864	3.163	74.41	40.48	2.742	3.167	74.41	40.48	2.742	3.167	74.41	40.48	2.742	3.167	74.41	40.48	2.742	3.167															
1416.0	75.52	41.31	2.855	3.164	75.52	41.31	2.855	3.164	75.53	40.32	2.735	3.168	75.53	40.32	2.735	3.168	75.53	40.32	2.735	3.168	75.53	40.32	2.735	3.168															
1421.0	76.97	41.14	2.847	3.165	76.97	41.14	2.847	3.165	74.95	40.15	2.728	3.169	74.95	40.15	2.728	3.169	74.95	40.15	2.728	3.169	74.95	40.15	2.728	3.169															
1426.0	76.20	40.97	2.838	3.166	76.20	40.97	2.838	3.166	74.27	39.99	2.721	3.169	74.27	39.99	2.721	3.169	74.27	39.99	2.721	3.169	74.27	39.99	2.721	3.169															
1431.0	75.34	40.80	2.829	3.166	75.34	40.80	2.829	3.166	75.04	39.84	2.715	3.169	75.04	39.84	2.715	3.169	75.04	39.84	2.715	3.169	75.04	39.84	2.715	3.169															
1436.0	76.29	40.64	2.821	3.167	76.29	40.64	2.821	3.167	75.36	39.71	2.709	3.170	75.36	39.71	2.709	3.170	75.36	39.71	2.709	3.170	75.36	39.71	2.709	3.170															
1440.0	76.71	40.52	2.815	3.167	76.71	40.52	2.815	3.167	75.52	39.58	2.702	3.171	75.52	39.58	2.702	3.171	75.52	39.58	2.702	3.171	75.52	39.58	2.702	3.171															

SPACE STATION OUTPUT PARAMETERS TABLE 3

	H2		H2		H2 TO		CO2 REMOVAL		HEAT EXCHANGER		O2 ADDITION		O2 ACCUM
	PRODUCTION		VENTED		CO2 REDUCTION		EXIT CO2 PRESS		EXIT CO2 PRESS		O2 ADDITION		
TIME	HAB1	LAB1	HAB1	LAB1	HAB1	LAB1	HAB1	LAB1	HAB1	LAB1	HAB1	LAB1	O2
MIN	PPH	PPH	PPH	PPH	PPH	PPH	MM HG	MM HG	MM HG	MM HG	PPH	PPH	PSIA
1.0	0.039	0.039	0.039	0.039	0.000	0.000	0.994	0.903	2.807	2.549	0.00	0.00	1052.4
6.0	0.039	0.039	0.039	0.000	0.000	0.000	0.930	0.822	2.625	2.322	0.44	0.38	1051.9
11.0	0.044	0.044	0.044	0.000	0.000	0.000	0.921	0.804	2.600	2.273	0.59	0.56	1049.3
16.0	0.044	0.044	0.044	0.000	0.000	0.000	0.899	0.793	2.540	2.242	0.57	1.43	1048.5
21.0	0.044	0.044	0.044	0.000	0.000	0.000	0.906	0.807	2.561	2.281	0.50	0.51	1049.8
26.0	0.044	0.044	0.044	0.000	0.000	0.000	0.914	0.805	2.581	2.276	0.58	0.53	1048.3
31.0	0.044	0.044	0.044	0.000	0.000	0.000	0.900	0.789	2.544	2.231	1.97	1.97	1045.2
36.0	0.044	0.044	0.044	0.000	0.000	0.000	0.891	0.791	2.519	2.237	0.58	1.14	1043.9
41.0	0.044	0.044	0.044	0.000	0.000	0.000	0.900	0.798	2.544	2.256	0.57	0.55	1043.9
46.0	0.044	0.044	0.044	0.000	0.000	0.000	0.898	0.789	2.537	2.231	1.99	1.01	1041.5
51.0	0.044	0.044	0.044	0.000	0.000	0.000	0.886	0.781	2.504	2.209	1.63	2.25	1037.9
56.0	0.044	0.044	0.044	0.000	0.000	0.000	0.887	0.788	2.507	2.228	0.59	0.60	1037.3
61.0	0.044	0.044	0.044	0.028	0.028	0.024	0.842	0.746	2.517	2.225	1.32	0.59	1036.1
66.0	0.044	0.044	0.044	0.016	0.019	0.028	0.871	0.687	2.474	2.167	2.17	1.85	1032.2
71.0	0.044	0.044	0.044	0.016	0.019	0.028	0.896	0.797	2.533	2.254	0.44	0.46	1032.9
76.0	0.044	0.044	0.044	0.016	0.019	0.028	0.883	0.783	2.497	2.215	2.98	2.84	1028.1
81.0	0.044	0.044	0.044	0.016	0.019	0.028	0.885	0.744	2.503	2.107	3.60	0.58	1024.5
86.0	0.044	0.044	0.044	0.016	0.019	0.028	0.892	0.776	2.521	2.197	0.49	0.52	1021.5
91.0	0.044	0.044	0.044	0.016	0.019	0.028	0.883	0.783	2.498	2.215	0.56	2.01	1019.9
96.0	0.044	0.044	0.044	0.016	0.019	0.028	0.861	0.755	2.436	2.138	3.48	3.07	1014.9
101.0	0.044	0.044	0.044	0.016	0.019	0.028	0.860	0.757	2.434	2.143	0.57	0.58	1013.8
106.0	0.044	0.044	0.044	0.016	0.019	0.028	0.874	0.775	2.470	2.193	0.51	0.52	1013.1
111.0	0.044	0.044	0.044	0.016	0.019	0.028	0.865	0.763	2.448	2.159	1.91	1.37	1010.6
116.0	0.044	0.044	0.044	0.016	0.019	0.028	0.852	0.747	2.411	2.115	1.48	1.52	1007.7
121.0	0.044	0.044	0.044	0.017	0.020	0.027	0.876	0.726	2.435	2.158	0.53	0.54	1008.0
126.0	0.044	0.044	0.044	0.017	0.020	0.027	0.768	0.683	2.421	2.136	0.58	0.57	1006.7
131.0	0.044	0.044	0.044	0.017	0.020	0.027	0.870	0.768	2.459	2.174	0.48	0.46	1006.9
136.0	0.044	0.044	0.044	0.017	0.020	0.027	0.854	0.752	2.415	2.130	1.88	2.26	1003.4
141.0	0.044	0.044	0.044	0.017	0.020	0.027	0.836	0.735	2.365	2.081	1.07	1.17	1001.2
146.0	0.044	0.044	0.044	0.017	0.020	0.027	0.855	0.755	2.419	2.138	0.49	0.47	1001.9
151.0	0.044	0.044	0.044	0.017	0.020	0.027	0.856	0.755	2.421	2.137	0.57	0.55	999.6
156.0	0.044	0.044	0.044	0.017	0.020	0.027	0.837	0.735	2.369	2.098	1.82	1.86	997.2
161.0	0.044	0.044	0.044	0.017	0.020	0.027	0.840	0.741	2.376	2.098	0.54	0.54	997.8
166.0	0.044	0.044	0.044	0.017	0.020	0.027	0.849	0.750	2.403	2.124	0.53	0.51	996.9
171.0	0.044	0.044	0.044	0.017	0.020	0.027	0.840	0.738	2.378	2.092	1.23	0.76	995.1
176.0	0.044	0.044	0.044	0.017	0.020	0.027	0.831	0.731	2.353	2.071	0.59	0.59	994.4
181.0	0.044	0.044	0.044	0.017	0.020	0.026	0.798	0.707	2.375	2.099	0.53	0.52	994.5
186.0	0.044	0.044	0.044	0.017	0.020	0.026	0.756	0.672	2.353	2.066	0.59	0.56	993.3
191.0	0.044	0.044	0.044	0.017	0.020	0.026	0.847	0.746	2.395	2.113	0.46	0.43	993.7
196.0	0.044	0.044	0.044	0.017	0.020	0.026	0.833	0.733	2.356	2.077	1.24	1.32	990.9
201.0	0.044	0.044	0.044	0.017	0.020	0.026	0.815	0.714	2.307	2.022	1.05	0.75	989.5
206.0	0.044	0.044	0.044	0.017	0.020	0.026	0.833	0.733	2.356	2.077	0.48	0.46	990.2
211.0	0.044	0.044	0.044	0.017	0.020	0.026	0.834	0.735	2.360	2.082	0.55	0.53	988.2
216.0	0.044	0.044	0.044	0.017	0.020	0.026	0.834	0.735	2.360	2.082	1.56	1.26	986.6
221.0	0.044	0.044	0.044	0.017	0.020	0.026	0.817	0.716	2.313	2.029	0.54	0.53	987.3
226.0	0.044	0.044	0.044	0.017	0.020	0.026	0.819	0.720	2.317	2.038	0.54	0.53	987.3
226.0	0.044	0.044	0.044	0.017	0.020	0.026	0.828	0.730	2.343	2.067	0.51	0.49	986.5
231.0	0.044	0.044	0.044	0.017	0.020	0.026	0.820	0.720	2.321	2.039	0.81	0.59	985.0
236.0	0.044	0.044	0.044	0.017	0.020	0.026	0.812	0.711	2.297	2.015	0.59	0.58	984.8
241.0	0.044	0.044	0.044	0.018	0.021	0.026	0.779	0.689	2.317	2.042	0.52	0.51	985.0

SPACE STATION OUTPUT PARAMETERS TABLE 3

	H2 PRODUCTION		H2 VENTED		CO2 REDUCTION		H2 TO CO2 REMOVAL		HEAT EXCHANGER		O2 ADDITION		O2 ACCUM	
	HAB1	PPH	HAB1	PPH	HAB1	PPH	HAB1	MM HG	HAB1	MM HG	HAB1	PPH	PSIA	
TIME	HAB1	PPH	HAB1	PPH	HAB1	PPH	HAB1	MM HG <td>HAB1</td> <td>MM HG<td>HAB1</td><td>PPH</td><td>PSIA</td><td></td></td>	HAB1	MM HG <td>HAB1</td> <td>PPH</td> <td>PSIA</td> <td></td>	HAB1	PPH	PSIA	
246.0	0.044	0.044	0.018	0.021	0.026	0.023	0.744	0.660	2.303	2.013	0.57	0.53	983.8	
251.0	0.044	0.044	0.018	0.021	0.026	0.023	0.826	0.726	2.337	2.058	0.45	0.43	984.0	
256.0	0.044	0.044	0.018	0.021	0.026	0.023	0.811	0.714	2.296	2.022	0.93	0.95	981.7	
261.0	0.044	0.044	0.018	0.021	0.026	0.023	0.798	0.696	2.258	1.974	0.60	0.58	981.4	
266.0	0.044	0.044	0.018	0.021	0.026	0.023	0.814	0.715	2.304	2.025	0.48	0.45	981.9	
271.0	0.044	0.044	0.018	0.021	0.026	0.023	0.814	0.715	2.303	2.027	0.54	0.53	979.9	
276.0	0.044	0.044	0.018	0.021	0.026	0.023	0.798	0.698	2.259	1.977	1.20	0.70	979.0	
281.0	0.044	0.044	0.018	0.021	0.026	0.023	0.802	0.702	2.269	1.990	0.53	0.51	979.9	
286.0	0.044	0.044	0.018	0.021	0.026	0.023	0.813	0.711	2.301	2.015	0.51	0.47	979.8	
291.0	0.044	0.044	0.018	0.021	0.026	0.023	0.808	0.701	2.288	1.988	0.60	0.56	977.2	
296.0	0.044	0.044	0.018	0.021	0.026	0.023	0.785	0.694	2.223	1.966	0.58	1.54	976.2	
301.0	0.044	0.044	0.019	0.022	0.025	0.022	0.760	0.672	2.257	1.992	0.52	0.47	977.6	
306.0	0.044	0.044	0.019	0.022	0.025	0.022	0.731	0.648	2.267	1.964	0.56	0.46	976.2	
311.0	0.044	0.044	0.019	0.022	0.025	0.022	0.809	0.709	2.288	2.007	0.45	0.44	975.5	
316.0	0.044	0.044	0.019	0.022	0.025	0.022	0.788	0.696	2.231	1.971	0.70	1.21	973.7	
321.0	0.044	0.044	0.019	0.022	0.025	0.022	0.782	0.680	2.213	1.927	0.59	0.53	974.6	
326.0	0.044	0.044	0.019	0.022	0.025	0.022	0.799	0.698	2.262	1.977	0.47	0.42	974.4	
331.0	0.044	0.044	0.019	0.022	0.025	0.022	0.804	0.698	2.276	1.978	0.54	0.47	973.5	
336.0	0.044	0.044	0.019	0.022	0.025	0.022	0.798	0.681	2.258	1.931	0.88	0.55	972.0	
341.0	0.044	0.044	0.019	0.022	0.025	0.022	0.777	0.686	2.200	1.943	0.52	1.11	971.1	
346.0	0.044	0.044	0.019	0.022	0.025	0.022	0.781	0.694	2.210	1.965	0.51	0.49	972.6	
351.0	0.044	0.044	0.019	0.022	0.025	0.022	0.792	0.685	2.243	1.942	0.58	0.45	971.7	
356.0	0.044	0.044	0.019	0.022	0.025	0.022	0.783	0.679	2.217	1.924	0.57	0.57	970.0	
361.0	0.044	0.044	0.019	0.022	0.025	0.022	0.737	0.656	2.191	1.943	0.52	0.56	970.6	
366.0	0.044	0.044	0.019	0.022	0.025	0.022	0.709	0.635	2.197	1.915	0.56	0.47	970.8	
371.0	0.044	0.044	0.019	0.022	0.025	0.022	0.796	0.693	2.252	1.963	0.43	0.35	970.4	
376.0	0.044	0.044	0.019	0.022	0.025	0.022	0.791	0.680	2.238	1.928	0.60	0.53	968.7	
381.0	0.044	0.044	0.019	0.022	0.025	0.022	0.776	0.663	2.197	1.880	0.59	0.58	967.6	
386.0	0.044	0.044	0.019	0.022	0.025	0.022	0.767	0.681	2.171	1.930	0.46	0.54	968.4	
391.0	0.044	0.044	0.019	0.022	0.025	0.022	0.778	0.683	2.202	1.935	0.52	0.45	968.6	
396.0	0.044	0.044	0.019	0.022	0.025	0.022	0.777	0.667	2.199	1.890	0.66	0.51	967.0	
401.0	0.044	0.044	0.019	0.022	0.025	0.022	0.766	0.670	2.169	1.898	0.52	0.56	966.7	
406.0	0.044	0.044	0.019	0.022	0.025	0.022	0.769	0.678	2.178	1.922	0.50	0.49	967.3	
411.0	0.044	0.044	0.019	0.022	0.025	0.022	0.774	0.670	2.191	1.900	0.57	0.48	966.5	
416.0	0.044	0.044	0.019	0.022	0.025	0.022	0.769	0.664	2.176	1.881	0.56	0.54	965.6	
421.0	0.044	0.044	0.019	0.023	0.024	0.021	0.751	0.642	2.171	1.902	0.51	0.52	965.8	
426.0	0.044	0.044	0.019	0.023	0.024	0.021	0.705	0.623	2.169	1.876	0.55	0.48	965.6	
431.0	0.044	0.044	0.019	0.023	0.024	0.021	0.787	0.678	2.228	1.921	0.43	0.34	965.7	
436.0	0.044	0.044	0.019	0.023	0.024	0.021	0.776	0.666	2.196	1.888	0.58	0.57	963.0	
441.0	0.044	0.044	0.019	0.023	0.024	0.021	0.761	0.651	2.154	1.844	0.58	0.54	964.2	
446.0	0.044	0.044	0.019	0.023	0.024	0.021	0.792	0.671	2.223	1.896	0.45	0.35	965.2	
451.0	0.044	0.044	0.019	0.023	0.024	0.021	0.781	0.655	2.209	1.856	0.59	0.53	962.4	
456.0	0.044	0.044	0.019	0.023	0.024	0.021	0.788	0.660	2.230	1.871	0.50	0.42	963.8	
461.0	0.044	0.044	0.019	0.023	0.024	0.021	0.804	0.671	2.274	1.901	0.48	0.36	963.2	
466.0	0.044	0.044	0.019	0.023	0.024	0.021	0.804	0.663	2.273	1.879	0.56	0.45	961.8	
471.0	0.044	0.044	0.019	0.023	0.024	0.021	0.802	0.657	2.269	1.863	0.54	0.44	962.2	
476.0	0.044	0.044	0.019	0.023	0.024	0.021	0.773	0.639	2.311	1.894	0.48	0.34	962.7	
481.0	0.044	0.044	0.019	0.023	0.024	0.021	0.760	0.625	2.313	1.872	0.52	0.38	961.7	
486.0	0.044	0.044	0.019	0.023	0.024	0.021	0.760	0.625	2.313	1.872	0.52	0.38	961.7	

SPACE STATION OUTPUT PARAMETERS TABLE 3

TIME	H2 PRODUCTION			H2 VENTED			H2 TO CO2 REDUCTION			CO2 REMOVAL			HEAT EXCHANGER			O2 ACCUM		
	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	PPH	MM HG	LAB1	PPH	MM HG	LAB1	PPH	PSIA
491.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.838	0.678	2.369	1.920	0.41	0.41	0.26	962.1	
496.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.832	0.669	2.351	1.894	0.55	0.55	0.44	960.1	
501.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.825	0.657	2.331	1.860	0.54	0.54	0.41	961.5	
506.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.845	0.676	2.389	1.914	0.42	0.42	0.27	962.3	
511.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.853	0.679	2.411	1.923	0.48	0.48	0.33	960.8	
516.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.846	0.666	2.391	1.887	0.55	0.55	0.41	960.3	
521.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.851	0.673	2.405	1.907	0.46	0.46	0.34	961.4	
526.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.864	0.685	2.443	1.939	0.44	0.44	0.29	961.1	
531.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.866	0.679	2.446	1.923	0.52	0.52	0.36	960.1	
536.0	0.044	0.044	0.044	0.019	0.023	0.023	0.024	0.021	0.021	0.863	0.676	2.439	1.914	0.50	0.50	0.37	960.3	
541.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.822	0.656	2.463	1.947	0.44	0.44	0.31	960.8	
546.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.788	0.639	2.464	1.928	0.48	0.48	0.32	960.4	
551.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.894	0.701	2.526	1.985	0.36	0.36	0.20	960.9	
556.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.885	0.691	2.501	1.958	0.52	0.52	0.42	958.4	
561.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.869	0.677	2.457	1.918	0.51	0.51	0.41	959.9	
566.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.893	0.701	2.523	1.984	0.37	0.37	0.23	961.4	
571.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.902	0.706	2.549	1.997	0.44	0.44	0.29	959.7	
576.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.892	0.690	2.520	1.955	0.53	0.53	0.41	958.9	
581.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.893	0.699	2.523	1.979	0.43	0.43	0.33	960.3	
586.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.908	0.713	2.566	2.018	0.40	0.40	0.26	960.4	
591.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.910	0.706	2.570	2.000	0.50	0.50	0.34	959.1	
596.0	0.044	0.044	0.044	0.017	0.023	0.023	0.026	0.021	0.021	0.904	0.702	2.553	1.988	0.48	0.48	0.38	959.2	
601.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.859	0.682	2.575	2.027	0.41	0.41	0.30	960.0	
606.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.891	0.658	2.578	2.011	0.46	0.46	0.30	959.7	
611.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.935	0.731	2.639	2.069	0.33	0.33	0.19	960.1	
616.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.924	0.720	2.609	2.039	0.51	0.51	0.42	957.6	
621.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.906	0.705	2.559	1.997	0.49	0.49	0.40	959.2	
626.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.931	0.731	2.628	2.068	0.35	0.35	0.23	960.7	
631.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.940	0.735	2.654	2.082	0.43	0.43	0.28	958.9	
636.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.927	0.719	2.620	2.036	0.52	0.52	0.41	958.1	
641.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.928	0.728	2.621	2.062	0.42	0.42	0.33	959.6	
646.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.944	0.743	2.666	2.103	0.39	0.39	0.26	959.7	
651.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.944	0.736	2.667	2.083	0.49	0.49	0.34	958.4	
656.0	0.044	0.044	0.044	0.016	0.022	0.022	0.028	0.021	0.021	0.937	0.731	2.648	2.069	0.47	0.47	0.38	958.6	
661.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.890	0.710	2.669	2.111	0.40	0.40	0.30	959.4	
666.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.848	0.680	2.671	2.094	0.45	0.45	0.30	959.1	
671.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.968	0.761	2.733	2.152	0.32	0.32	0.19	959.5	
676.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.956	0.750	2.700	2.122	0.50	0.50	0.42	956.9	
681.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.937	0.733	2.647	2.076	0.49	0.49	0.40	958.6	
686.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.921	0.760	2.718	2.149	0.35	0.35	0.23	960.1	
691.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.971	0.765	2.743	2.164	0.43	0.43	0.28	958.3	
696.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.958	0.747	2.707	2.115	0.52	0.52	0.41	957.5	
701.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.958	0.756	2.707	2.140	0.42	0.42	0.33	959.0	
706.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.974	0.771	2.752	2.183	0.39	0.39	0.26	959.1	
711.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.974	0.764	2.750	2.162	0.49	0.49	0.35	957.8	
716.0	0.044	0.044	0.044	0.015	0.021	0.021	0.029	0.023	0.023	0.963	0.758	2.720	2.147	0.67	0.67	0.39	957.9	
721.0	0.044	0.044	0.044	0.014	0.020	0.020	0.030	0.024	0.024	0.910	0.736	2.727	2.188	0.40	0.40	0.33	958.7	
726.0	0.044	0.044	0.044	0.014	0.020	0.020	0.030	0.024	0.024	0.857	0.702	2.716	2.170	0.45	0.45	0.34	958.4	
731.0	0.044	0.044	0.044	0.014	0.020	0.020	0.030	0.024	0.024	0.979	0.787	2.765	2.228	0.33	0.33	0.22	958.7	

SPACE STATION OUTPUT PARAMETERS TABLE 3

	H2 PRODUCTION			H2 VENTED			H2 TO CO2 REDUCTION			CO2 REMOVAL EXIT CO2 PRESS			HEAT EXCHANGER EXIT CO2 PRESS			O2 ADDITION			O2 ACCUM		
	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	MM HG	LAB1	HAB1	MM HG	LAB1	HAB1	PPH	LAB1	HAB1	PPH	PSIA
TIME	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	PPH	LAB1	HAB1	MM HG	LAB1	HAB1	MM HG	LAB1	HAB1	PPH	LAB1	HAB1	PPH	PSIA
MIN	PPH																				
736.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.024	0.961	0.775	2.715	2.193	0.51	0.47	956.1						
741.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.937	0.757	2.648	2.142	0.50	0.46	957.8							
746.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.961	0.783	2.714	2.216	0.36	0.28	959.2							
751.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.964	0.787	2.724	2.227	0.44	0.36	957.1							
756.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.944	0.767	2.669	2.172	0.53	0.49	956.5							
761.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.944	0.775	2.668	2.195	0.43	0.39	958.0							
766.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.957	0.789	2.704	2.234	0.40	0.34	957.7							
771.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.950	0.779	2.686	2.207	0.51	0.44	956.3							
776.0	0.044	0.044	0.044	0.014	0.020	0.030	0.024	0.939	0.772	2.655	2.187	0.49	0.46	956.6							
781.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.899	0.749	2.688	2.226	0.42	0.35	957.4							
786.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.841	0.712	2.667	2.201	0.47	0.42	956.2							
791.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.959	0.797	2.710	2.257	0.35	0.28	956.9							
796.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.946	0.784	2.673	2.220	0.52	0.48	954.7							
801.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.940	0.766	2.658	2.168	0.51	0.43	956.8							
806.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.953	0.790	2.693	2.236	0.38	0.34	956.2							
811.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.947	0.793	2.676	2.243	0.46	0.44	955.0							
816.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.939	0.773	2.654	2.189	0.54	0.44	955.4							
821.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.948	0.782	2.680	2.213	0.44	0.37	955.8							
826.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.953	0.794	2.692	2.247	0.42	0.39	955.0							
831.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.947	0.784	2.676	2.218	0.52	0.44	954.6							
836.0	0.044	0.044	0.044	0.014	0.019	0.030	0.024	0.948	0.778	2.679	2.204	0.49	0.40	955.0							
841.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.902	0.754	2.699	2.240	0.43	0.37	954.8							
846.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.856	0.719	2.680	2.211	0.49	0.40	954.3							
851.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.972	0.802	2.745	2.270	0.35	0.24	955.2							
856.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.962	0.790	2.718	2.237	0.52	0.46	952.6							
861.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.943	0.770	2.665	2.181	0.52	0.46	953.8							
866.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.966	0.795	2.729	2.251	0.38	0.28	955.2							
871.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.975	0.802	2.755	2.270	0.45	0.34	953.5							
876.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.963	0.788	2.721	2.230	0.53	0.45	952.7							
881.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.964	0.781	2.723	2.211	0.49	0.37	953.9							
886.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.979	0.800	2.767	2.264	0.40	0.30	953.9							
891.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.980	0.798	2.769	2.260	0.48	0.38	952.7							
896.0	0.044	0.044	0.044	0.014	0.019	0.029	0.024	0.974	0.786	2.752	2.224	0.52	0.41	952.8							
901.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.926	0.759	2.774	2.254	0.44	0.34	953.4							
906.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.887	0.732	2.777	2.251	0.45	0.33	953.1							
911.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.007	0.816	2.843	2.308	0.35	0.21	953.5							
916.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.994	0.798	2.809	2.259	0.54	0.44	950.9							
921.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.975	0.782	2.756	2.213	0.50	0.42	952.5							
926.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.002	0.812	2.831	2.298	0.36	0.24	954.0							
931.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.011	0.813	2.856	2.302	0.46	0.30	952.1							
936.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.997	0.792	2.817	2.243	0.54	0.43	951.3							
941.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	0.998	0.805	2.820	2.279	0.42	0.34	952.8							
946.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.015	0.819	2.866	2.319	0.41	0.27	952.8							
951.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.014	0.808	2.865	2.288	0.51	0.36	951.5							
956.0	0.044	0.044	0.044	0.014	0.019	0.030	0.025	1.006	0.804	2.843	2.275	0.48	0.39	951.6							
961.0	0.044	0.044	0.044	0.013	0.019	0.031	0.025	0.956	0.780	2.866	2.320	0.41	0.32	952.4							
966.0	0.044	0.044	0.044	0.013	0.019	0.031	0.025	0.911	0.747	2.866	2.294	0.47	0.32	952.0							
971.0	0.044	0.044	0.044	0.013	0.019	0.031	0.025	1.038	0.833	2.930	2.356	0.34	0.20	952.4							
976.0	0.044	0.044	0.044	0.013	0.019	0.031	0.025	1.025	0.821	2.894	2.323	0.51	0.43	949.9							



SPACE STATION OUTPUT PARAMETERS TABLE 3

TIME	H <sub>2</sub> PRODUCTION			H <sub>2</sub> VENTED			H <sub>2</sub> TO CO <sub>2</sub> REDUCTION			CO <sub>2</sub> REMOVAL EXIT CO <sub>2</sub> PRESS			HEAT EXCHANGER EXIT CO <sub>2</sub> PRESS			O <sub>2</sub> ADDITION			O <sub>2</sub> IACCUM		
	HAB1	LAB1	PPH	HAB1	LAB1	PPH	HAB1	LAB1	PPH	HAB1	LAB1	PPH	HAB1	LAB1	PPH	HAB1	LAB1	PPH	HAB1	LAB1	PPH
MIN																					
981.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.004	0.802	2.837	2.270	0.51	0.42	951.5						
986.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.031	0.829	2.910	2.345	0.37	0.24	953.0						
991.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.040	0.834	2.935	2.360	0.44	0.30	951.2						
996.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.025	0.815	2.896	2.307	0.53	0.42	950.4						
1001.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.025	0.823	2.894	2.329	0.43	0.35	951.8						
1006.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.041	0.839	2.940	2.374	0.40	0.27	951.8						
1011.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.041	0.831	2.940	2.351	0.50	0.36	950.5						
1016.0	0.044	0.044	0.044	0.013	0.013	0.019	0.031	0.025	1.032	0.824	2.915	2.331	0.49	0.39	950.6						
1021.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	0.979	0.798	2.935	2.373	0.41	0.32	951.4						
1026.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	0.931	0.762	2.935	2.353	0.46	0.32	951.1						
1031.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	1.062	0.854	2.998	2.416	0.34	0.20	951.4						
1036.0	0.049	0.049	0.049	0.017	0.017	0.023	0.032	0.026	1.047	0.840	2.956	2.378	0.52	0.44	948.9						
1041.0	0.049	0.049	0.049	0.017	0.017	0.023	0.032	0.026	1.023	0.821	2.890	2.323	0.51	0.43	950.5						
1046.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	1.049	0.850	2.961	2.404	0.36	0.25	952.0						
1051.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	1.055	0.854	2.980	2.416	0.44	0.32	950.2						
1056.0	0.049	0.049	0.049	0.017	0.017	0.023	0.032	0.026	1.037	0.833	2.929	2.358	0.54	0.45	949.4						
1061.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	1.033	0.842	2.919	2.383	0.43	0.38	950.9						
1066.0	0.044	0.044	0.044	0.012	0.012	0.018	0.032	0.026	1.047	0.858	2.958	2.427	0.41	0.31	950.9						
1071.0	0.049	0.049	0.049	0.017	0.017	0.023	0.032	0.026	1.042	0.848	2.944	2.399	0.51	0.41	949.5						
1076.0	0.049	0.049	0.049	0.017	0.017	0.023	0.032	0.026	1.029	0.840	2.906	2.377	0.49	0.44	949.7						
1081.0	0.044	0.044	0.044	0.011	0.011	0.017	0.032	0.026	0.976	0.814	2.919	2.420	0.42	0.37	950.5						
1086.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	0.913	0.774	2.907	2.395	0.48	0.38	950.0						
1091.0	0.044	0.044	0.044	0.011	0.011	0.017	0.032	0.026	1.048	0.868	2.959	2.455	0.35	0.26	950.3						
1096.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.028	0.853	2.905	2.414	0.53	0.51	947.8						
1101.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.004	0.832	2.837	2.355	0.52	0.49	949.5						
1106.0	0.044	0.044	0.044	0.016	0.016	0.022	0.032	0.026	1.029	0.859	2.907	2.432	0.38	0.31	950.7						
1111.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.032	0.863	2.915	2.441	0.46	0.40	948.7						
1116.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.011	0.840	2.857	2.378	0.55	0.51	948.2						
1121.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.012	0.848	2.859	2.401	0.45	0.42	949.6						
1126.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.025	0.863	2.895	2.441	0.43	0.37	949.3						
1131.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.017	0.851	2.874	2.408	0.53	0.47	948.0						
1136.0	0.049	0.049	0.049	0.016	0.016	0.022	0.032	0.026	1.016	0.842	2.872	2.385	0.51	0.44	949.2						
1141.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	0.965	0.817	2.886	2.426	0.44	0.41	948.2						
1146.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	0.899	0.776	2.824	2.394	0.50	0.50	947.7						
1151.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.026	0.867	2.898	2.454	0.37	0.27	949.4						
1156.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.018	0.854	2.877	2.416	0.54	0.47	946.7						
1161.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.010	0.832	2.853	2.354	0.54	0.48	948.7						
1166.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.019	0.857	2.879	2.425	0.40	0.37	948.0						
1171.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.011	0.860	2.857	2.433	0.47	0.47	947.0						
1176.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.004	0.839	2.837	2.375	0.56	0.46	947.5						
1181.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.014	0.846	2.865	2.395	0.46	0.39	947.9						
1186.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.017	0.859	2.874	2.431	0.44	0.41	947.1						
1191.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.011	0.848	2.856	2.400	0.53	0.46	946.8						
1196.0	0.049	0.049	0.049	0.017	0.017	0.022	0.032	0.027	1.012	0.841	2.861	2.382	0.51	0.42	947.2						
1201.0	0.049	0.049	0.049	0.017	0.017	0.022	0.031	0.027	0.963	0.814	2.880	2.418	0.45	0.39	947.0						
1206.0	0.049	0.049	0.049	0.017	0.017	0.022	0.031	0.027	0.915	0.778	2.857	2.386	0.50	0.42	946.6						
1211.0	0.049	0.049	0.049	0.017	0.017	0.022	0.031	0.027	1.036	0.865	2.926	2.449	0.37	0.25	947.5						
1216.0	0.049	0.049	0.049	0.017	0.017	0.022	0.031	0.027	1.025	0.852	2.894	2.411	0.54	0.48	945.0						
1221.0	0.049	0.049	0.049	0.017	0.017	0.022	0.031	0.027	1.003	0.830	2.834	2.349	0.54	0.48	946.2						

SPACE STATION OUTPUT PARAMETERS TABLE 3

TIME	H2 PRODUCTION		H2 VENTED		H2 TO CO2 REDUCTION		CO2 REMOVAL EXIT CO2 PRESS		HEAT EXCHANGER EXIT CO2 PRESS	O2 ADDITION		O2 ACCUM	
	HAB1	PPH	HAB1	PPH	HAB1	PPH	HAB1	MM HG	HAB1	MM HG	HAB1	PPH	O2
1226.0	0.049	0.049	0.017	0.022	0.031	0.027	1.026	0.856	2.899	2.424	0.40	0.31	947.6
1231.0	0.049	0.049	0.017	0.022	0.031	0.027	1.034	0.860	2.922	2.435	0.47	0.36	946.0
1236.0	0.049	0.049	0.017	0.022	0.031	0.027	1.020	0.839	2.881	2.375	0.56	0.48	945.2
1241.0	0.049	0.049	0.017	0.022	0.031	0.027	1.019	0.846	2.879	2.395	0.46	0.40	946.5
1246.0	0.049	0.049	0.017	0.022	0.031	0.027	1.034	0.861	2.920	2.437	0.43	0.34	946.5
1251.0	0.049	0.049	0.017	0.022	0.031	0.027	1.031	0.851	2.913	2.408	0.53	0.42	945.3
1256.0	0.049	0.049	0.017	0.022	0.031	0.027	1.022	0.842	2.889	2.385	0.51	0.44	945.5
1261.0	0.049	0.049	0.017	0.022	0.032	0.027	0.972	0.816	2.909	2.425	0.44	0.37	946.1
1266.0	0.049	0.049	0.017	0.022	0.032	0.027	0.923	0.783	2.903	2.399	0.49	0.38	945.7
1271.0	0.049	0.049	0.017	0.022	0.032	0.027	1.050	0.869	2.964	2.460	0.37	0.25	946.1
1276.0	0.049	0.049	0.017	0.022	0.032	0.027	1.034	0.854	2.921	2.418	0.54	0.49	943.7
1281.0	0.049	0.049	0.017	0.022	0.032	0.027	1.013	0.834	2.863	2.362	0.53	0.46	945.3
1286.0	0.049	0.049	0.017	0.022	0.032	0.027	1.039	0.862	2.935	2.439	0.39	0.29	946.6
1291.0	0.049	0.049	0.017	0.022	0.032	0.027	1.045	0.865	2.952	2.447	0.47	0.36	944.8
1296.0	0.049	0.049	0.017	0.022	0.032	0.027	1.028	0.843	2.904	2.387	0.55	0.48	944.1
1301.0	0.049	0.049	0.017	0.022	0.032	0.027	1.028	0.852	2.904	2.411	0.45	0.39	945.5
1306.0	0.049	0.049	0.017	0.022	0.032	0.027	1.042	0.866	2.943	2.452	0.43	0.33	945.4
1311.0	0.049	0.049	0.017	0.022	0.032	0.027	1.037	0.855	2.929	2.420	0.53	0.43	944.1
1316.0	0.049	0.049	0.017	0.022	0.032	0.027	1.025	0.827	2.897	2.399	0.51	0.45	944.4
1321.0	0.049	0.049	0.016	0.022	0.032	0.027	0.975	0.785	2.916	2.412	0.44	0.38	945.1
1326.0	0.049	0.049	0.016	0.022	0.032	0.027	0.919	0.785	2.903	2.412	0.49	0.39	944.5
1331.0	0.049	0.049	0.016	0.022	0.032	0.027	1.047	0.874	2.956	2.473	0.37	0.26	945.0
1336.0	0.049	0.049	0.016	0.022	0.032	0.027	1.028	0.859	2.904	2.432	0.54	0.50	942.6
1341.0	0.049	0.049	0.016	0.022	0.032	0.027	1.003	0.838	2.835	2.373	0.53	0.48	944.2
1346.0	0.049	0.049	0.016	0.022	0.032	0.027	1.028	0.865	2.903	2.448	0.40	0.31	945.4
1351.0	0.049	0.049	0.016	0.022	0.032	0.027	1.030	0.868	2.909	2.455	0.47	0.40	943.5
1356.0	0.049	0.049	0.016	0.022	0.032	0.027	1.007	0.845	2.845	2.393	0.56	0.51	942.9
1361.0	0.049	0.049	0.016	0.022	0.032	0.027	1.006	0.853	2.843	2.414	0.46	0.42	944.4
1366.0	0.049	0.049	0.016	0.022	0.032	0.027	1.018	0.867	2.876	2.453	0.44	0.37	944.0
1371.0	0.049	0.049	0.016	0.022	0.032	0.027	1.008	0.855	2.848	2.420	0.54	0.47	942.7
1376.0	0.049	0.049	0.016	0.022	0.032	0.027	1.000	0.846	2.827	2.395	0.52	0.46	943.2
1381.0	0.049	0.049	0.017	0.022	0.032	0.027	0.946	0.819	2.824	2.433	0.45	0.44	943.2
1386.0	0.049	0.049	0.017	0.022	0.032	0.027	0.880	0.780	2.792	2.401	0.50	0.45	943.0
1391.0	0.049	0.049	0.017	0.022	0.032	0.027	1.009	0.869	2.850	2.459	0.38	0.29	943.7
1396.0	0.049	0.049	0.017	0.022	0.032	0.027	1.003	0.853	2.835	2.415	0.55	0.48	942.7
1401.0	0.049	0.049	0.017	0.022	0.032	0.027	1.006	0.832	2.843	2.355	0.54	0.41	943.3
1406.0	0.049	0.049	0.017	0.022	0.032	0.027	1.005	0.856	2.841	2.422	0.41	0.43	942.3
1411.0	0.049	0.049	0.017	0.022	0.032	0.027	0.986	0.857	2.788	2.424	0.49	0.53	940.0
1416.0	0.049	0.049	0.017	0.022	0.032	0.027	0.934	0.834	2.642	2.361	0.57	1.48	939.9
1421.0	0.049	0.049	0.017	0.022	0.032	0.027	0.966	0.841	2.732	2.382	0.47	0.36	942.7
1426.0	0.049	0.049	0.017	0.022	0.032	0.027	0.980	0.853	2.770	2.415	0.45	0.39	940.4
1431.0	0.049	0.049	0.017	0.022	0.032	0.027	0.953	0.839	2.694	2.375	0.55	0.59	938.6
1436.0	0.049	0.049	0.017	0.022	0.032	0.027	0.940	0.830	2.659	2.350	0.53	0.51	940.6
1440.0	0.049	0.049	0.017	0.022	0.032	0.027	0.960	0.842	2.716	2.383	0.46	0.38	941.0

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER IC02 REDUCTION										TOTAL	
CONDENSATE					CONDENSATE					COND	
TIME	HAB	LAB	HAB1	LAB1	HAB	LAB	HAB1	LAB1			
MIN	PPH	PPH	PPH	PPH	PPH	PPH	PPH	PPH			
1.0	2.79	2.79	0.000	0.000	0.000	0.000	0.000	0.000	5.57		
6.0	2.28	2.06	0.000	0.000	0.000	0.000	0.000	0.000	4.34		
11.0	1.86	1.37	0.000	0.000	0.000	0.000	0.000	0.000	3.23		
16.0	1.28	1.01	0.000	0.000	0.000	0.000	0.000	0.000	2.29		
21.0	1.29	1.10	0.000	0.000	0.000	0.000	0.000	0.000	2.39		
26.0	1.19	0.90	0.000	0.000	0.000	0.000	0.000	0.000	2.09		
31.0	0.93	0.57	0.000	0.000	0.000	0.000	0.000	0.000	1.50		
36.0	0.74	0.52	0.000	0.000	0.000	0.000	0.000	0.000	1.25		
41.0	0.73	0.48	0.000	0.000	0.000	0.000	0.000	0.000	1.21		
46.0	0.62	0.35	0.000	0.000	0.000	0.000	0.000	0.000	0.96		
51.0	0.48	0.28	0.000	0.000	0.000	0.000	0.000	0.000	0.76		
56.0	0.43	0.27	0.000	0.000	0.000	0.000	0.000	0.000	0.70		
61.0	0.39	0.23	0.252	0.223	0.252	0.223	0.252	0.223	1.10		
66.0	0.67	0.04	0.252	0.223	0.252	0.223	0.252	0.223	13.18		
71.0	0.41	0.26	0.252	0.223	0.252	0.223	0.252	0.223	1.15		
76.0	0.38	0.20	0.252	0.223	0.252	0.223	0.252	0.223	1.06		
81.0	0.35	0.12	0.252	0.223	0.252	0.223	0.252	0.223	0.94		
86.0	0.27	0.14	0.252	0.223	0.252	0.223	0.252	0.223	0.89		
91.0	0.28	0.11	0.252	0.223	0.252	0.223	0.252	0.223	0.86		
96.0	0.24	0.07	0.252	0.223	0.252	0.223	0.252	0.223	0.79		
101.0	0.22	0.06	0.252	0.223	0.252	0.223	0.252	0.223	0.76		
106.0	0.21	0.03	0.252	0.223	0.252	0.223	0.252	0.223	0.72		
111.0	0.19	0.02	0.252	0.223	0.252	0.223	0.252	0.223	0.69		
116.0	0.16	0.03	0.252	0.223	0.252	0.223	0.252	0.223	0.67		
121.0	0.15	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.62		
126.0	5.71	5.23	0.247	0.219	0.247	0.219	0.247	0.219	11.40		
131.0	0.19	0.02	0.247	0.219	0.247	0.219	0.247	0.219	0.68		
136.0	0.20	0.02	0.247	0.219	0.247	0.219	0.247	0.219	0.68		
141.0	0.16	0.03	0.247	0.219	0.247	0.219	0.247	0.219	0.66		
146.0	0.16	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.62		
151.0	0.13	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.60		
156.0	0.12	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.59		
161.0	0.11	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.58		
166.0	0.08	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.55		
171.0	0.08	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.54		
176.0	0.07	0.00	0.247	0.219	0.247	0.219	0.247	0.219	0.54		
181.0	0.05	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.51		
186.0	5.46	4.91	0.241	0.213	0.241	0.213	0.241	0.213	10.83		
191.0	0.09	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.55		
196.0	0.11	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.57		
201.0	0.10	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.55		
206.0	0.08	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.54		
211.0	0.05	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.51		
216.0	0.06	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.52		
221.0	0.05	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.51		
226.0	0.02	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.47		
231.0	0.02	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.48		
236.0	0.02	0.00	0.241	0.213	0.241	0.213	0.241	0.213	0.48		
241.0	0.00	0.00	0.235	0.207	0.235	0.207	0.235	0.207	0.44		

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER CONDENSATE		IC02 REDUCTION CONDENSATE		TOTAL COND	
TIME	HAB	LAB	HAB1	LAB1	
MIN	PPH	PPH	PPH	PPH	PPH
246.0	5.22	4.69	0.235	0.207	10.35
251.0	0.05	0.00	0.235	0.207	0.49
256.0	0.07	0.00	0.235	0.207	0.51
261.0	0.06	0.00	0.235	0.207	0.50
266.0	0.04	0.00	0.235	0.207	0.48
271.0	0.02	0.00	0.235	0.207	0.46
276.0	0.03	0.00	0.235	0.207	0.47
281.0	0.02	0.00	0.235	0.207	0.46
286.0	0.00	0.00	0.235	0.207	0.44
291.0	0.00	0.00	0.235	0.207	0.44
296.0	0.01	0.00	0.235	0.207	0.45
301.0	0.00	0.00	0.230	0.202	0.43
306.0	4.72	4.55	0.230	0.202	9.71
311.0	0.01	0.00	0.230	0.202	0.45
316.0	0.05	0.00	0.230	0.202	0.48
321.0	0.05	0.00	0.230	0.202	0.48
326.0	0.00	0.00	0.230	0.202	0.43
331.0	0.00	0.00	0.230	0.202	0.43
336.0	0.00	0.00	0.230	0.202	0.43
341.0	0.02	0.00	0.230	0.202	0.45
346.0	0.00	0.00	0.230	0.202	0.43
351.0	0.00	0.00	0.230	0.202	0.43
356.0	0.00	0.00	0.230	0.202	0.43
361.0	0.00	0.00	0.226	0.197	0.42
366.0	5.03	4.48	0.226	0.197	9.94
371.0	0.00	0.00	0.226	0.197	0.42
376.0	0.00	0.00	0.226	0.197	0.42
381.0	0.01	0.00	0.226	0.197	0.43
386.0	0.02	0.00	0.226	0.197	0.45
391.0	0.00	0.00	0.226	0.197	0.42
396.0	0.00	0.00	0.226	0.197	0.42
401.0	0.00	0.00	0.226	0.197	0.42
406.0	0.00	0.00	0.226	0.197	0.42
411.0	0.00	0.00	0.226	0.197	0.42
416.0	0.00	0.00	0.226	0.197	0.42
421.0	0.00	0.00	0.221	0.193	9.94
426.0	5.12	4.41	0.221	0.193	0.41
431.0	0.00	0.00	0.221	0.193	0.41
436.0	0.09	0.00	0.221	0.193	0.51
441.0	0.11	0.00	0.221	0.193	0.52
446.0	0.14	0.00	0.221	0.193	0.55
451.0	0.16	0.00	0.221	0.193	0.57
456.0	0.20	0.00	0.221	0.193	0.61
461.0	0.25	0.00	0.221	0.193	0.66
466.0	0.29	0.00	0.221	0.193	0.71
471.0	0.34	0.00	0.221	0.193	0.75
476.0	0.37	0.00	0.221	0.193	0.78
481.0	0.46	0.00	0.224	0.190	0.88
486.0	6.55	4.57	0.224	0.190	11.54

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER										TOTAL									
CONDENSATE					CO2 REDUCTION					COND									
HAB	LAB	HAB1	LAB1		HAB	LAB	HAB1	LAB1		HAB	LAB	HAB1	LAB1		HAB	LAB	HAB1	LAB1	
PPH	PPH	PPH	PPH		PPH	PPH	PPH	PPH		PPH	PPH	PPH	PPH		PPH	PPH	PPH	PPH	
491.0	0.76	0.00	0.224	0.190	1.17														
496.0	0.83	0.00	0.224	0.190	1.24														
501.0	0.76	0.00	0.224	0.190	1.17														
506.0	0.96	0.00	0.224	0.190	1.37														
511.0	1.00	0.00	0.224	0.190	1.42														
516.0	0.94	0.00	0.224	0.190	1.35														
521.0	0.98	0.00	0.224	0.190	1.39														
526.0	1.07	0.00	0.224	0.190	1.48														
531.0	1.06	0.00	0.224	0.190	1.47														
536.0	1.00	0.00	0.224	0.190	1.42														
541.0	1.06	0.00	0.240	0.192	1.49														
546.0	7.32	5.04	0.240	0.192	12.79														
551.0	1.25	0.00	0.240	0.192	1.68														
556.0	1.25	0.02	0.240	0.192	1.71														
561.0	0.99	0.04	0.240	0.192	1.47														
566.0	1.29	0.02	0.240	0.192	1.74														
571.0	1.31	0.01	0.240	0.192	1.75														
576.0	1.18	0.04	0.240	0.192	1.65														
581.0	1.15	0.04	0.240	0.192	1.63														
586.0	1.28	0.02	0.240	0.192	1.73														
591.0	1.25	0.04	0.240	0.192	1.72														
596.0	1.14	0.05	0.240	0.192	1.62														
601.0	1.20	0.03	0.253	0.199	1.68														
606.0	7.43	5.39	0.253	0.199	13.28														
611.0	1.38	0.09	0.253	0.199	1.92														
616.0	1.37	0.08	0.253	0.199	1.91														
621.0	1.07	0.07	0.253	0.199	1.59														
626.0	1.39	0.08	0.253	0.199	1.92														
631.0	1.41	0.07	0.253	0.199	1.93														
636.0	1.25	0.06	0.253	0.199	1.77														
641.0	1.22	0.07	0.253	0.199	1.74														
646.0	1.36	0.06	0.253	0.199	1.87														
651.0	1.32	0.06	0.253	0.199	1.83														
656.0	1.19	0.06	0.253	0.199	1.70														
661.0	1.25	0.06	0.263	0.207	1.78														
666.0	7.48	5.56	0.263	0.207	13.52														
671.0	1.44	0.13	0.263	0.207	2.04														
676.0	1.42	0.12	0.263	0.207	2.00														
681.0	1.10	0.10	0.263	0.207	1.66														
686.0	1.43	0.11	0.263	0.207	2.01														
691.0	1.44	0.10	0.263	0.207	2.02														
696.0	1.28	0.09	0.263	0.207	1.84														
701.0	1.24	0.09	0.263	0.207	1.80														
706.0	1.38	0.09	0.263	0.207	1.94														
711.0	1.31	0.08	0.263	0.207	1.86														
716.0	1.10	0.07	0.263	0.207	1.64														
721.0	1.02	0.07	0.272	0.215	1.58														
726.0	7.11	5.60	0.272	0.215	13.19														
731.0	0.91	0.13	0.272	0.215	1.53														

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER		CO <sub>2</sub> REDUCTION		TOTAL	
CONDENSATE		CONDENSATE		COND	
TIME	HAB	LAB	HAB1	LAB1	
MIN	PPH	PPH	PPH	PPH	PPH
736.0	0.85	0.11	0.272	0.215	1.45
741.0	0.59	0.08	0.272	0.215	1.16
746.0	0.71	0.09	0.272	0.215	1.29
751.0	0.64	0.07	0.272	0.215	1.20
756.0	0.53	0.05	0.272	0.215	1.08
761.0	0.50	0.05	0.272	0.215	1.04
766.0	0.49	0.03	0.272	0.215	1.01
771.0	0.45	0.02	0.272	0.215	0.96
776.0	0.39	0.05	0.272	0.215	0.92
781.0	0.40	0.01	0.271	0.221	0.91
786.0	6.34	5.34	0.271	0.221	12.17
791.0	0.48	0.05	0.271	0.221	1.03
796.0	0.49	0.04	0.271	0.221	1.03
801.0	0.46	0.03	0.271	0.221	0.99
806.0	0.47	0.02	0.271	0.221	0.99
811.0	0.48	0.02	0.271	0.221	1.00
816.0	0.45	0.03	0.271	0.221	0.98
821.0	0.50	0.01	0.271	0.221	1.00
826.0	0.51	0.00	0.271	0.221	1.00
831.0	0.51	0.00	0.271	0.221	1.00
836.0	0.52	0.00	0.271	0.221	1.01
841.0	0.55	0.00	0.269	0.223	1.05
846.0	6.82	5.24	0.269	0.223	12.55
851.0	0.71	0.02	0.269	0.223	1.23
856.0	0.78	0.03	0.269	0.223	1.30
861.0	0.64	0.03	0.269	0.223	1.16
866.0	0.84	0.02	0.269	0.223	1.35
871.0	0.88	0.00	0.269	0.223	1.37
876.0	0.83	0.04	0.269	0.223	1.36
881.0	0.84	0.04	0.269	0.223	1.37
886.0	0.96	0.01	0.269	0.223	1.46
891.0	0.97	0.01	0.269	0.223	1.47
896.0	0.93	0.02	0.269	0.223	1.44
901.0	1.00	0.01	0.274	0.225	1.52
906.0	7.23	5.26	0.274	0.225	12.99
911.0	1.23	0.06	0.274	0.225	1.79
916.0	1.25	0.07	0.274	0.225	1.81
921.0	0.99	0.06	0.274	0.225	1.55
926.0	1.31	0.06	0.274	0.225	1.87
931.0	1.33	0.06	0.274	0.225	1.88
936.0	1.19	0.05	0.274	0.225	1.74
941.0	1.18	0.06	0.274	0.225	1.73
946.0	1.31	0.05	0.274	0.225	1.86
951.0	1.28	0.05	0.274	0.225	1.83
956.0	1.16	0.05	0.274	0.225	1.71
961.0	1.23	0.05	0.283	0.229	1.79
966.0	7.46	5.54	0.283	0.229	13.51
971.0	1.42	0.12	0.283	0.229	2.05
976.0	1.40	0.11	0.283	0.229	2.02

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER		CO <sub>2</sub> REDUCTION		TOTAL	
CONDENSATE		CONDENSATE		COND	
TIME	HAB	LAB	HAB1	LAB1	
MIN	PPH	PPH	PPH	PPH	PPH
981.0	1.09	0.09	0.283	0.229	1.69
986.0	1.41	0.11	0.283	0.229	2.03
991.0	1.43	0.10	0.283	0.229	2.04
996.0	1.27	0.08	0.283	0.229	1.87
1001.0	1.24	0.08	0.283	0.229	1.83
1006.0	1.37	0.08	0.283	0.229	1.97
1011.0	1.34	0.07	0.283	0.229	1.92
1016.0	1.21	0.07	0.283	0.229	1.79
1021.0	1.26	0.07	0.291	0.235	1.86
1026.0	7.50	5.60	0.291	0.235	13.63
1031.0	1.41	0.14	0.291	0.235	2.08
1036.0	1.36	0.13	0.291	0.235	2.01
1041.0	1.02	0.10	0.291	0.235	1.64
1046.0	1.28	0.12	0.291	0.235	1.92
1051.0	1.22	0.10	0.291	0.235	1.85
1056.0	1.03	0.08	0.291	0.235	1.64
1061.0	0.94	0.08	0.291	0.235	1.55
1066.0	0.97	0.08	0.291	0.235	1.57
1071.0	0.87	0.06	0.291	0.235	1.46
1076.0	0.71	0.06	0.291	0.235	1.29
1081.0	0.68	0.05	0.295	0.240	1.26
1086.0	6.70	5.52	0.295	0.240	12.75
1091.0	0.65	0.10	0.295	0.240	1.29
1096.0	0.66	0.09	0.295	0.240	1.28
1101.0	0.47	0.06	0.295	0.240	1.07
1106.0	0.56	0.06	0.295	0.240	1.16
1111.0	0.52	0.04	0.295	0.240	1.09
1116.0	0.44	0.04	0.295	0.240	1.01
1121.0	0.43	0.03	0.295	0.240	0.99
1126.0	0.42	0.01	0.295	0.240	0.96
1131.0	0.40	0.02	0.295	0.240	0.95
1136.0	0.38	0.01	0.295	0.240	0.93
1141.0	0.37	0.00	0.290	0.243	0.90
1146.0	6.71	5.28	0.290	0.243	12.52
1151.0	0.44	0.03	0.290	0.243	1.01
1156.0	0.45	0.03	0.290	0.243	1.01
1161.0	0.43	0.02	0.290	0.243	0.98
1166.0	0.44	0.02	0.290	0.243	0.99
1171.0	0.44	0.00	0.290	0.243	0.98
1176.0	0.43	0.01	0.290	0.243	0.97
1181.0	0.47	0.00	0.290	0.243	1.00
1186.0	0.49	0.00	0.290	0.243	1.02
1191.0	0.49	0.00	0.290	0.243	1.02
1196.0	0.51	0.00	0.290	0.243	1.05
1201.0	0.55	0.00	0.287	0.242	1.08
1206.0	6.82	5.20	0.287	0.242	12.55
1211.0	0.69	0.01	0.287	0.242	1.24
1216.0	0.76	0.02	0.287	0.242	1.31
1221.0	0.60	0.02	0.287	0.242	1.15

SPACE STATION OUTPUT PARAMETERS TABLE 4

HEAT EXCHANGER		CO2 REDUCTION		TOTAL	
CONDENSATE	CONDENSATE	CONDENSATE	CONDENSATE	COND	COND
TIME	HAB	LAB	HAB1	LAB1	
MIN	PPH	PPH	PPH	PPH	PPH
1226.0	0.78	0.03	0.287	0.242	1.33
1231.0	0.78	0.00	0.287	0.242	1.31
1236.0	0.72	0.03	0.287	0.242	1.28
1241.0	0.71	0.02	0.287	0.242	1.26
1246.0	0.77	0.00	0.287	0.242	1.30
1251.0	0.76	0.00	0.287	0.242	1.29
1256.0	0.70	0.00	0.287	0.242	1.23
1261.0	0.73	0.00	0.290	0.242	1.26
1266.0	6.84	5.27	0.290	0.242	12.64
1271.0	0.85	0.04	0.290	0.242	1.42
1276.0	0.88	0.04	0.290	0.242	1.46
1281.0	0.69	0.04	0.290	0.242	1.26
1286.0	0.88	0.03	0.290	0.242	1.45
1291.0	0.87	0.02	0.290	0.242	1.43
1296.0	0.77	0.02	0.290	0.242	1.33
1301.0	0.76	0.02	0.290	0.242	1.31
1306.0	0.80	0.02	0.290	0.242	1.35
1311.0	0.75	0.03	0.290	0.242	1.31
1316.0	0.65	0.03	0.290	0.242	1.21
1321.0	0.67	0.00	0.293	0.243	1.20
1326.0	6.76	5.33	0.293	0.243	12.62
1331.0	0.71	0.05	0.293	0.243	1.30
1336.0	0.70	0.05	0.293	0.243	1.29
1341.0	0.50	0.04	0.293	0.243	1.08
1346.0	0.62	0.03	0.293	0.243	1.19
1351.0	0.57	0.02	0.293	0.243	1.12
1356.0	0.46	0.05	0.293	0.243	1.04
1361.0	0.43	0.03	0.293	0.243	1.00
1366.0	0.42	0.00	0.293	0.243	0.96
1371.0	0.38	0.00	0.293	0.243	0.92
1376.0	0.34	0.00	0.293	0.243	0.88
1381.0	0.32	0.00	0.289	0.244	0.85
1386.0	6.35	5.21	0.289	0.244	12.10
1391.0	0.33	0.01	0.289	0.244	0.88
1396.0	0.30	0.03	0.289	0.244	0.87
1401.0	0.21	0.03	0.289	0.244	0.77
1406.0	0.13	0.00	0.289	0.244	0.66
1411.0	0.22	0.00	0.289	0.244	0.75
1416.0	0.15	0.00	0.289	0.244	0.68
1421.0	0.18	0.00	0.289	0.244	0.72
1426.0	0.11	0.00	0.289	0.244	0.65
1431.0	0.13	0.00	0.289	0.244	0.67
1436.0	0.11	0.00	0.289	0.244	0.65
1440.0	0.10	0.00	0.289	0.244	0.63



## FIGURES C-15 TO C-43

## SAMPLE PROBLEM OUTPUT PLOTS

C-15	Habitat O <sub>2</sub> Partial Pressure.....
C-16	Habitat CO <sub>2</sub> Partial Pressure.....
C-17	Habitat Dew Point Temperature.....
C-18	Habitat Temperature.....
C-19	Lab O <sub>2</sub> Partial Pressure.....
C-20	Lab CO <sub>2</sub> Partial Pressure.....
C-21	Lab Dew Point Temperature.....
C-22	Lab Temperature.....
C-23	CO <sub>2</sub> Accumulator Inlet Flow in Habitat Removal Subsystem #1.....
C-24	CO <sub>2</sub> Removed by Habitat Removal Subsystem #1.....
C-25	CO <sub>2</sub> Accumulator Pressure in Habitat Removal Subsystem #1.....
C-26	Habitat Pressure.....
C-27	CO <sub>2</sub> Accumulator Inlet Flow in Lab Removal Subsystem #1.....
C-28	CO <sub>2</sub> Removed by Lab Removed Subsystem #1.....
C-29	CO <sub>2</sub> Accumulator Pressure in Lab Removal Subsystem #1.....
C-30	Lab Pressure.....
C-31	H <sub>2</sub> Vented from Habitat O <sub>2</sub> Gen Subsystem #1.....
C-32	H <sub>2</sub> Generated from Habitat O <sub>2</sub> Gen Subsystem #1.....
C-33	O <sub>2</sub> Produced by Habitat O <sub>2</sub> Gen Subsystem #1.....
C-34	CO <sub>2</sub> Accumulator Exit Flow in Habitat Removal Subsystem #1.....
C-35	H <sub>2</sub> Vented from Lab O <sub>2</sub> Gen Subsystem #1.....
C-36	H <sub>2</sub> Generated from Lab O <sub>2</sub> Gen Subsystem #1.....
C-37	O <sub>2</sub> Produced by Lab O <sub>2</sub> Gen Subsystem #1.....
C-38	CO <sub>2</sub> Accumulator Exit Flow in Lab Removal Subsystem #1.....
C-39	H <sub>2</sub> to CO <sub>2</sub> Reduction from Lab O <sub>2</sub> Gen Subsystem #1.....
C-40	H <sub>2</sub> to CO <sub>2</sub> Reduction from Habitat O <sub>2</sub> Gen Subsystem #1.....
C-41	Total Water Consumed by O <sub>2</sub> Generation Subsystems.....
C-42	Total Water Produced by CO <sub>2</sub> Reduction Subsystems.....

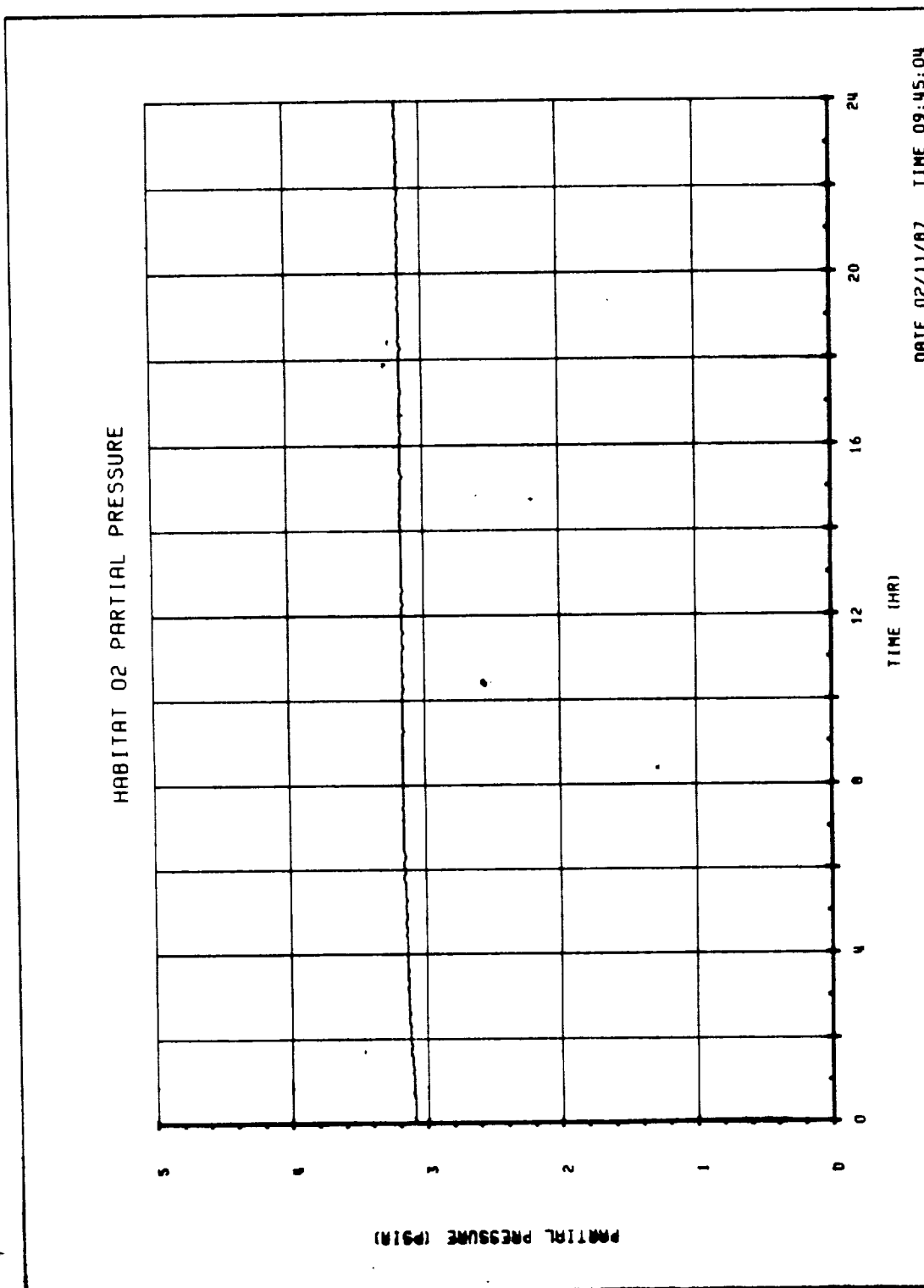


FIGURE C-15  
 HABITAT O2 PARTIAL PRESSURE

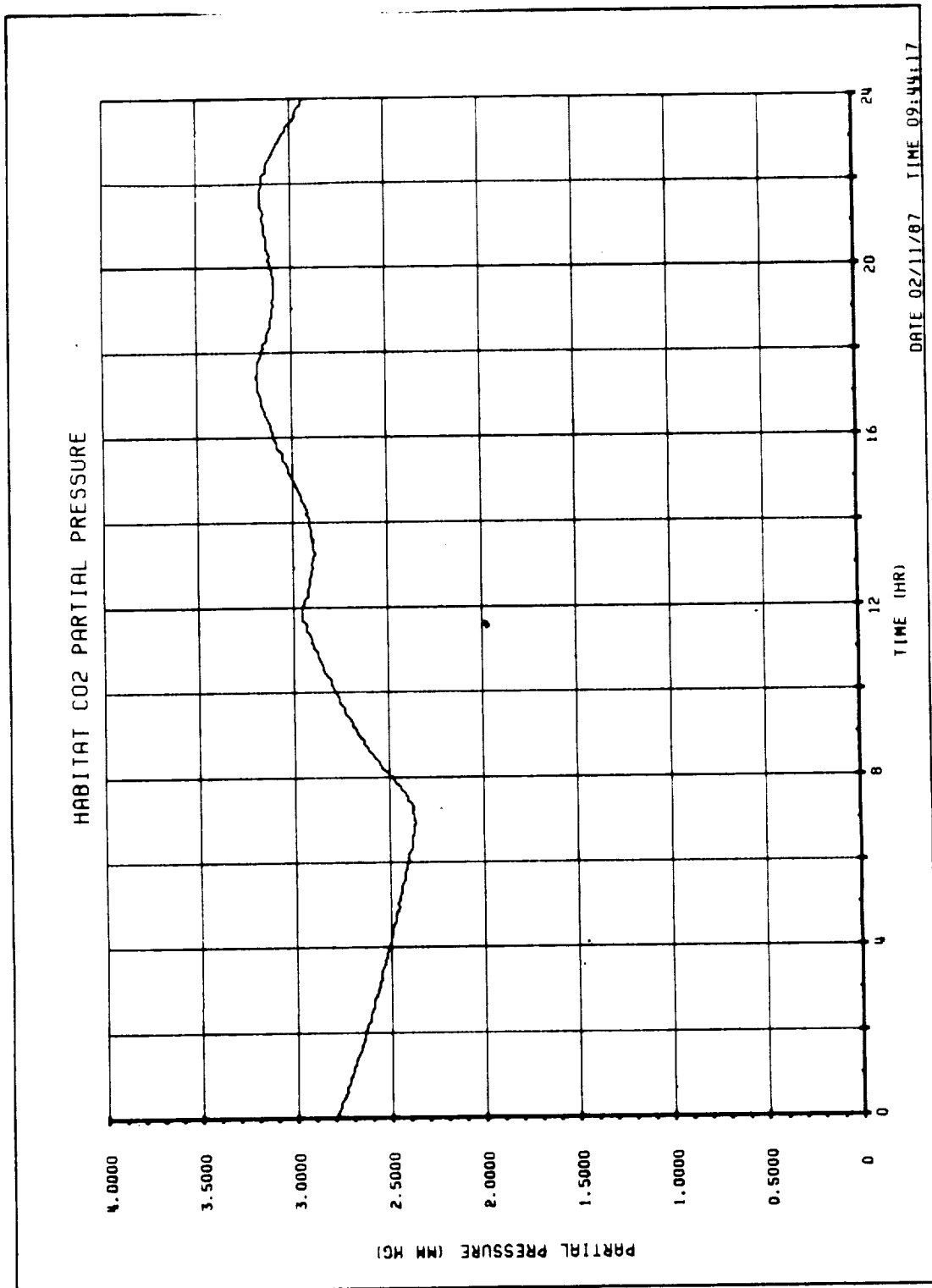


FIGURE C-16  
HABITAT CO2 PARTIAL PRESSURE

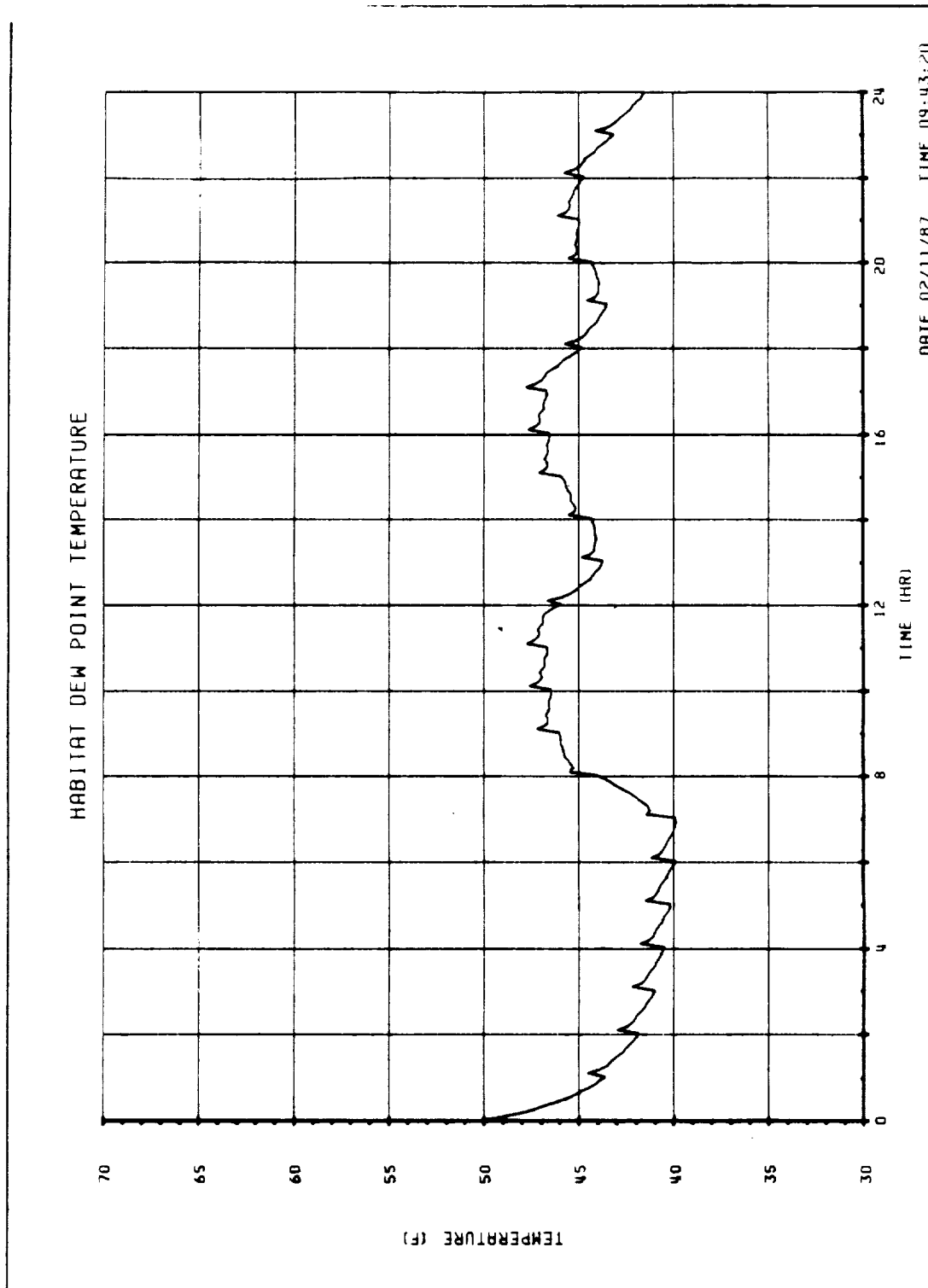


FIGURE C-17  
HABITAT DEW POINT TEMPERATURE

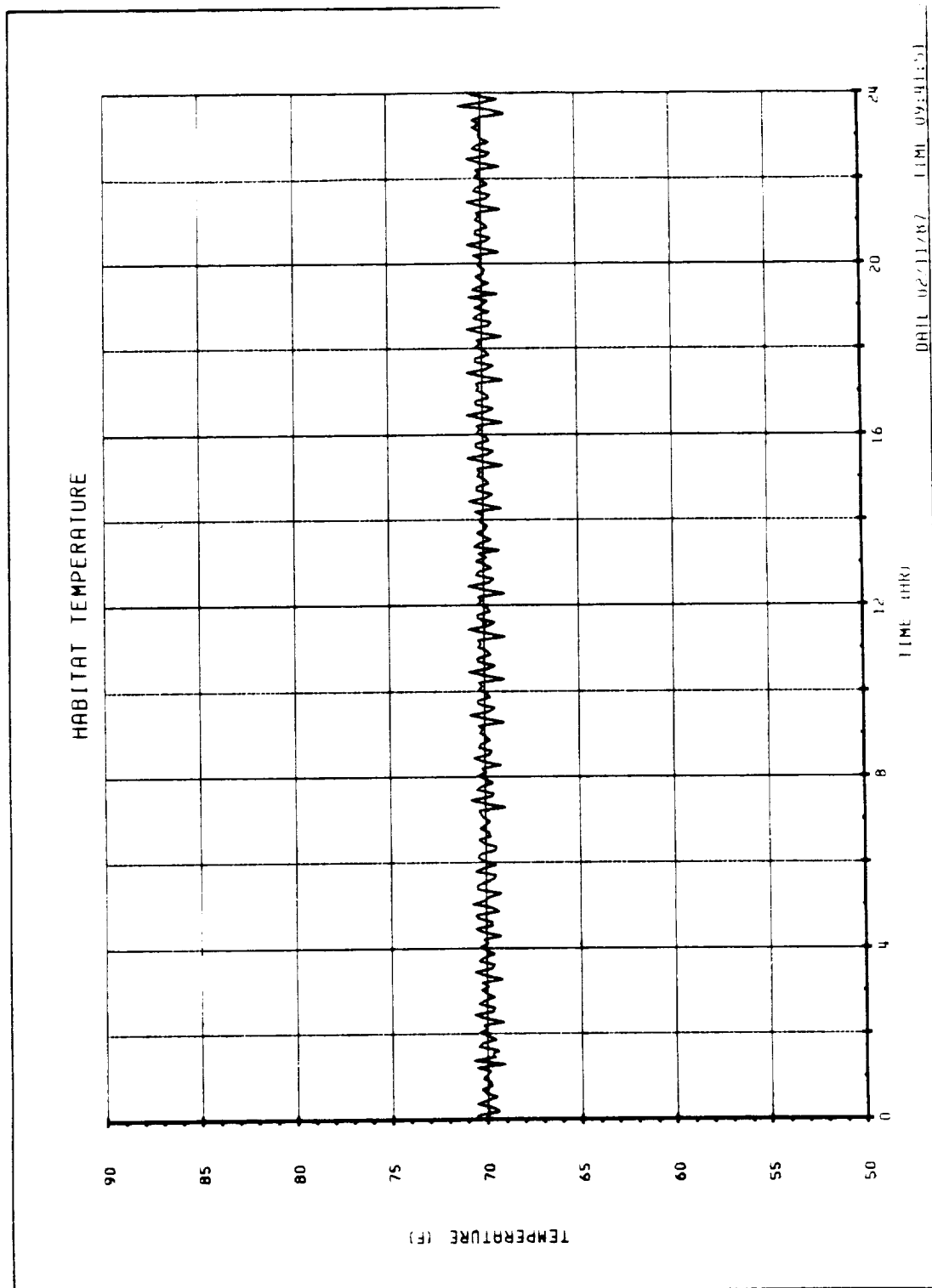


FIGURE C-18  
HABITAT TEMPERATURE

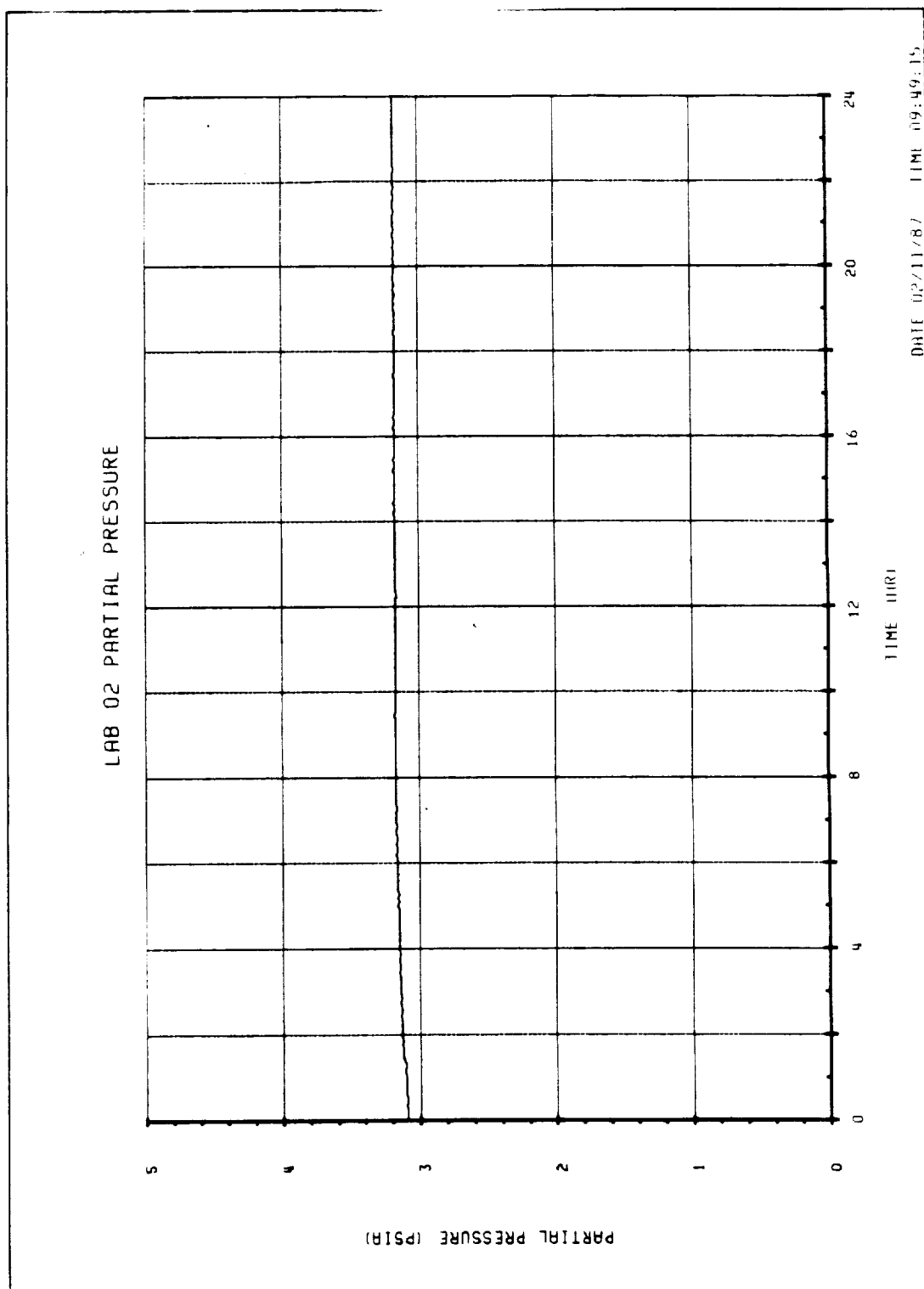


FIGURE C-19  
LAB 02 PARTIAL PRESSURE

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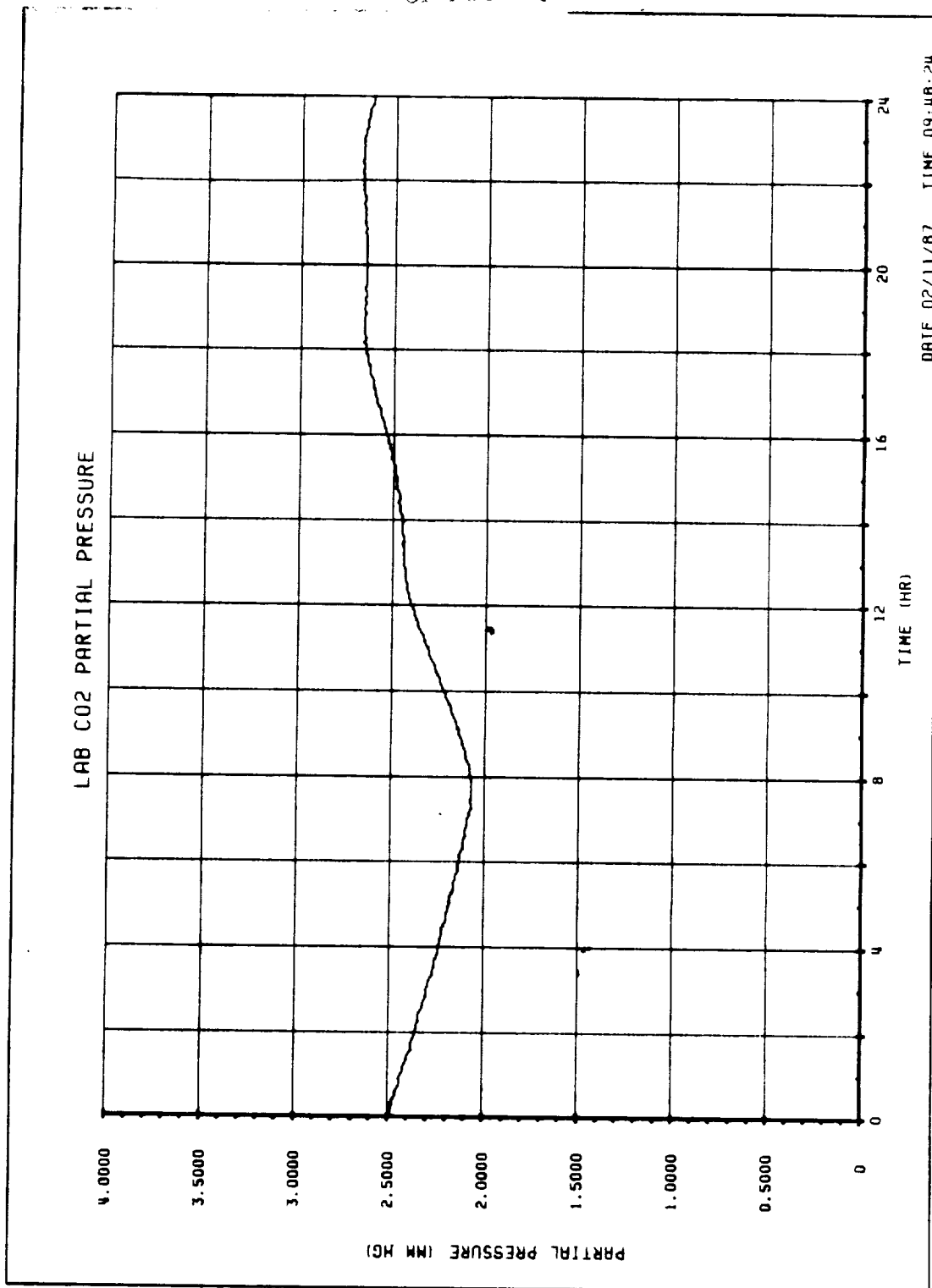


FIGURE C-20  
LAB CO2 PARTIAL PRESSURE

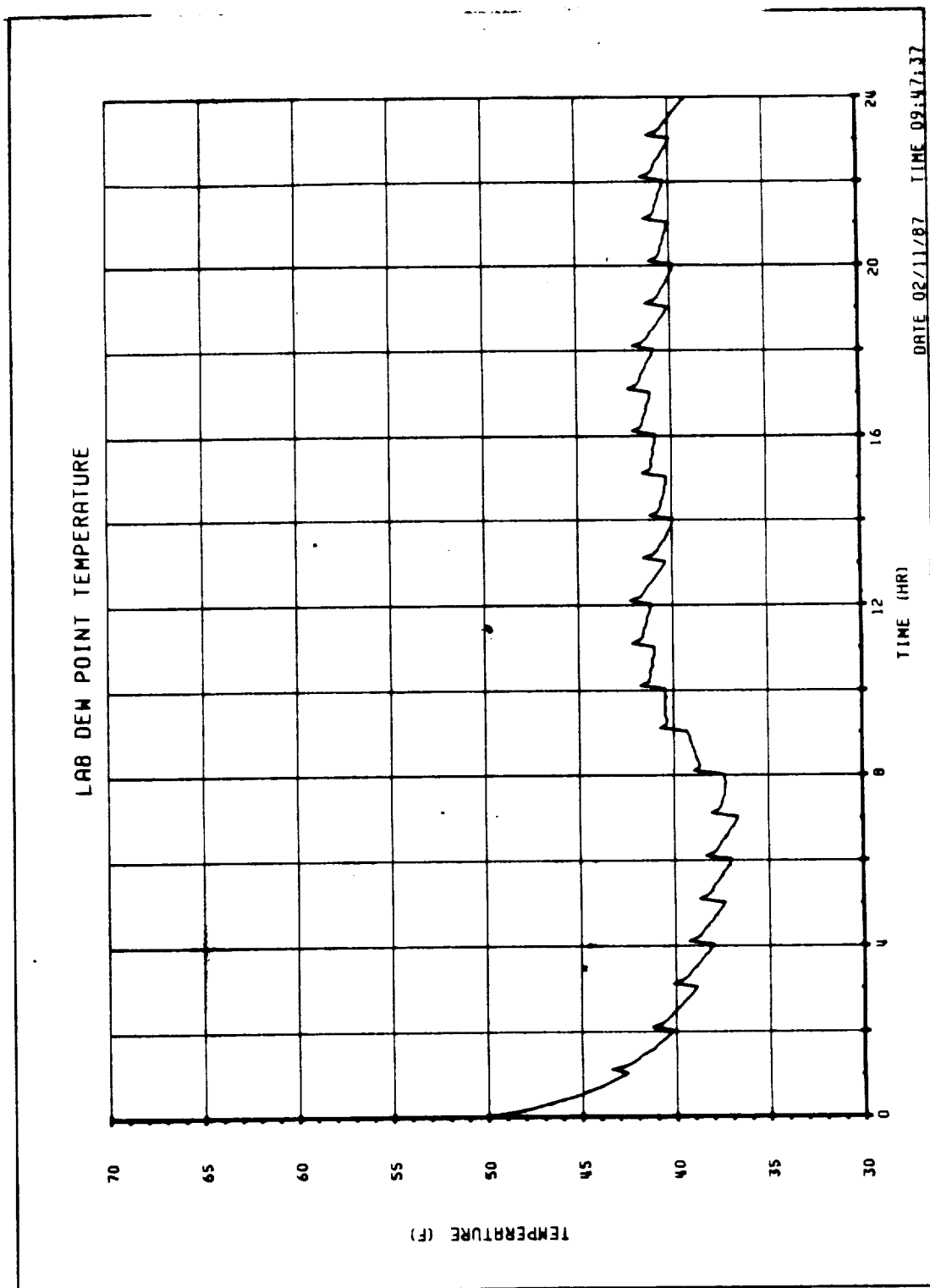


FIGURE C-21  
LAB DEW POINT TEMPERATURE



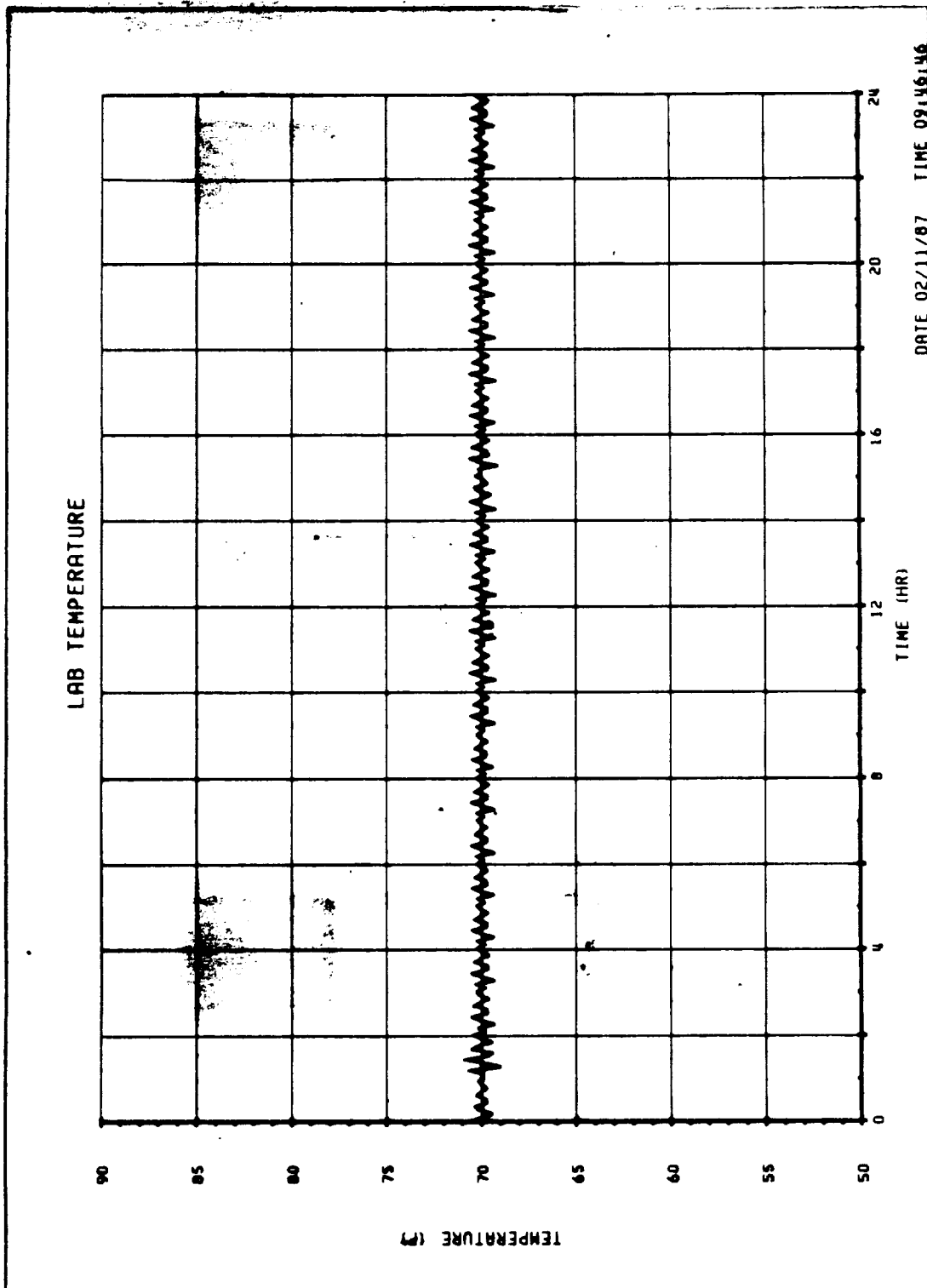


FIGURE C-22  
LAB TEMPERATURE

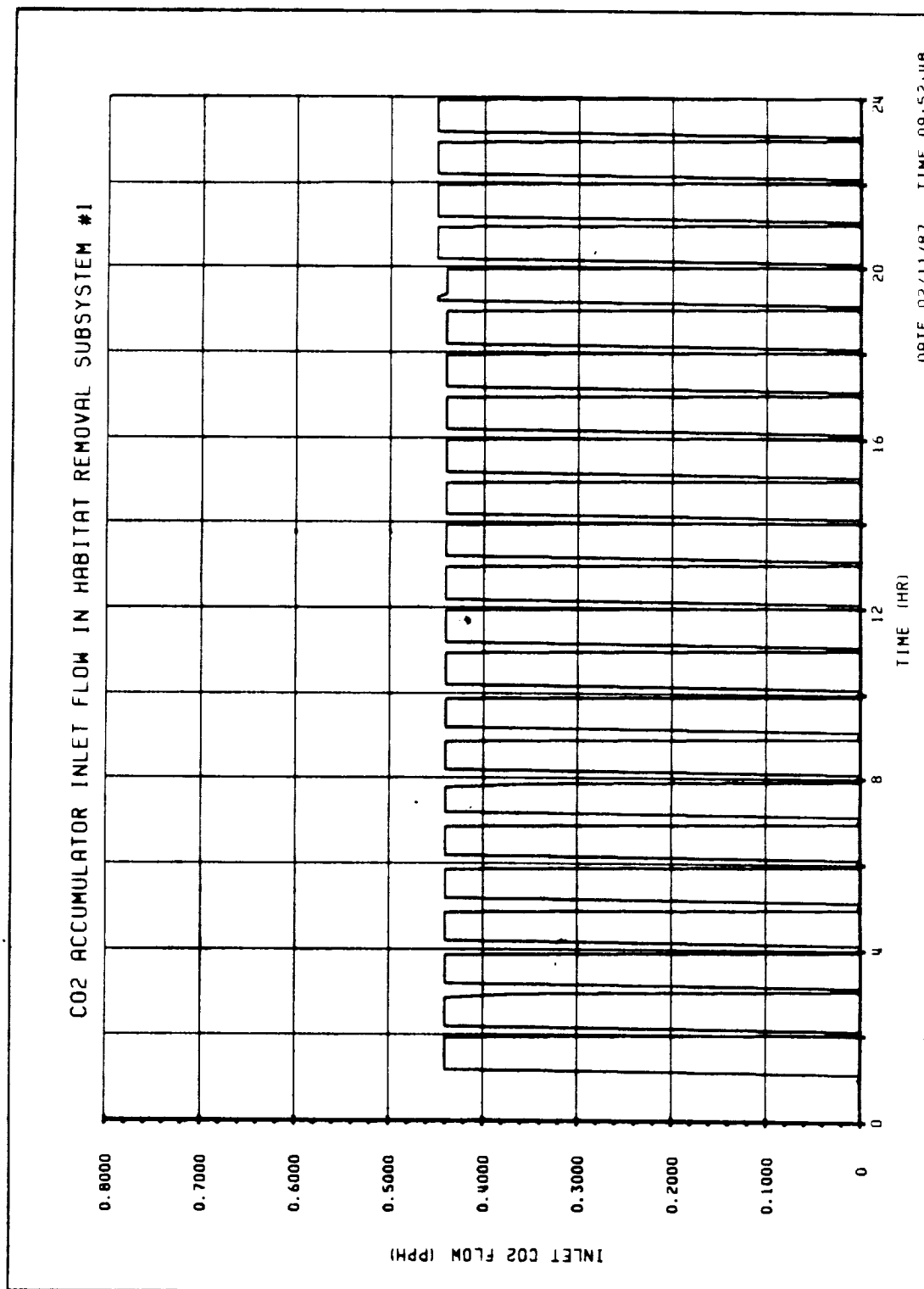


FIGURE C-23  
CO2 ACCUMULATOR INLET FLOW IN HABITAT REMOVAL  
SUBSYSTEM #1

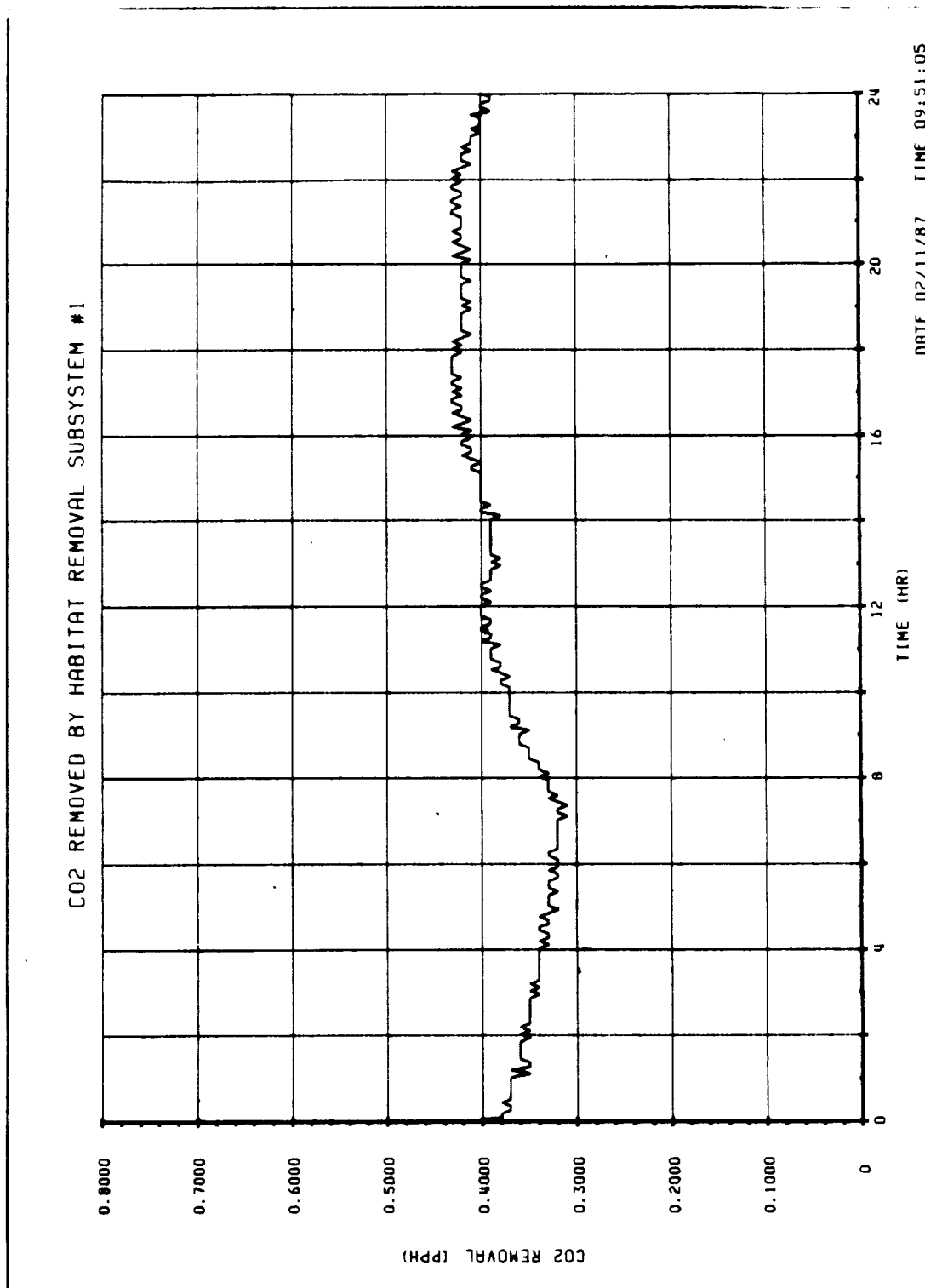


FIGURE C-24  
CO2 REMOVED BY HABITAT REMOVAL SUBSYSTEM #1

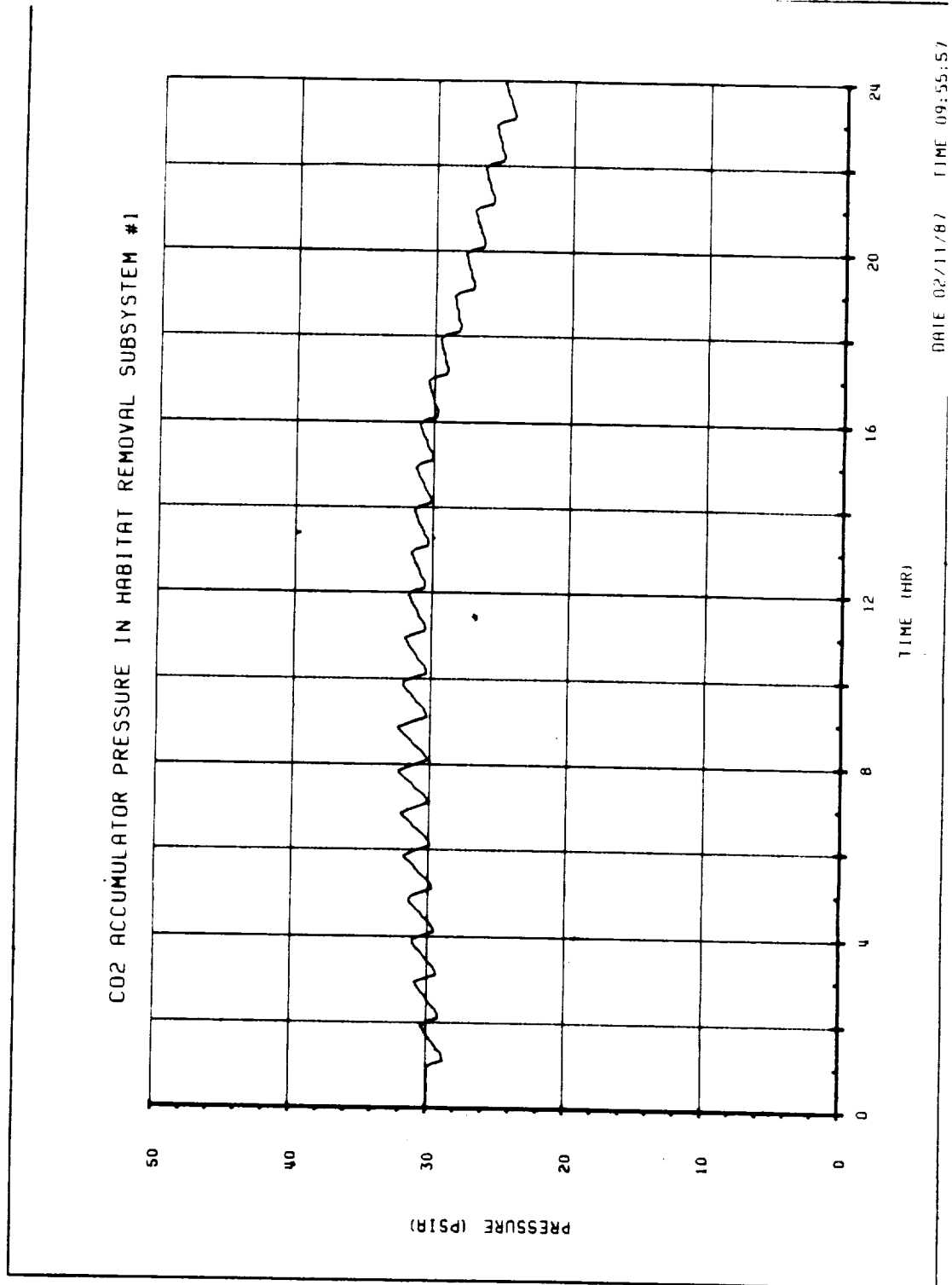


FIGURE C-25  
CO2 ACCUMULATOR PRESSURE IN HABITAT REMOVAL  
SUBSYSTEM #1

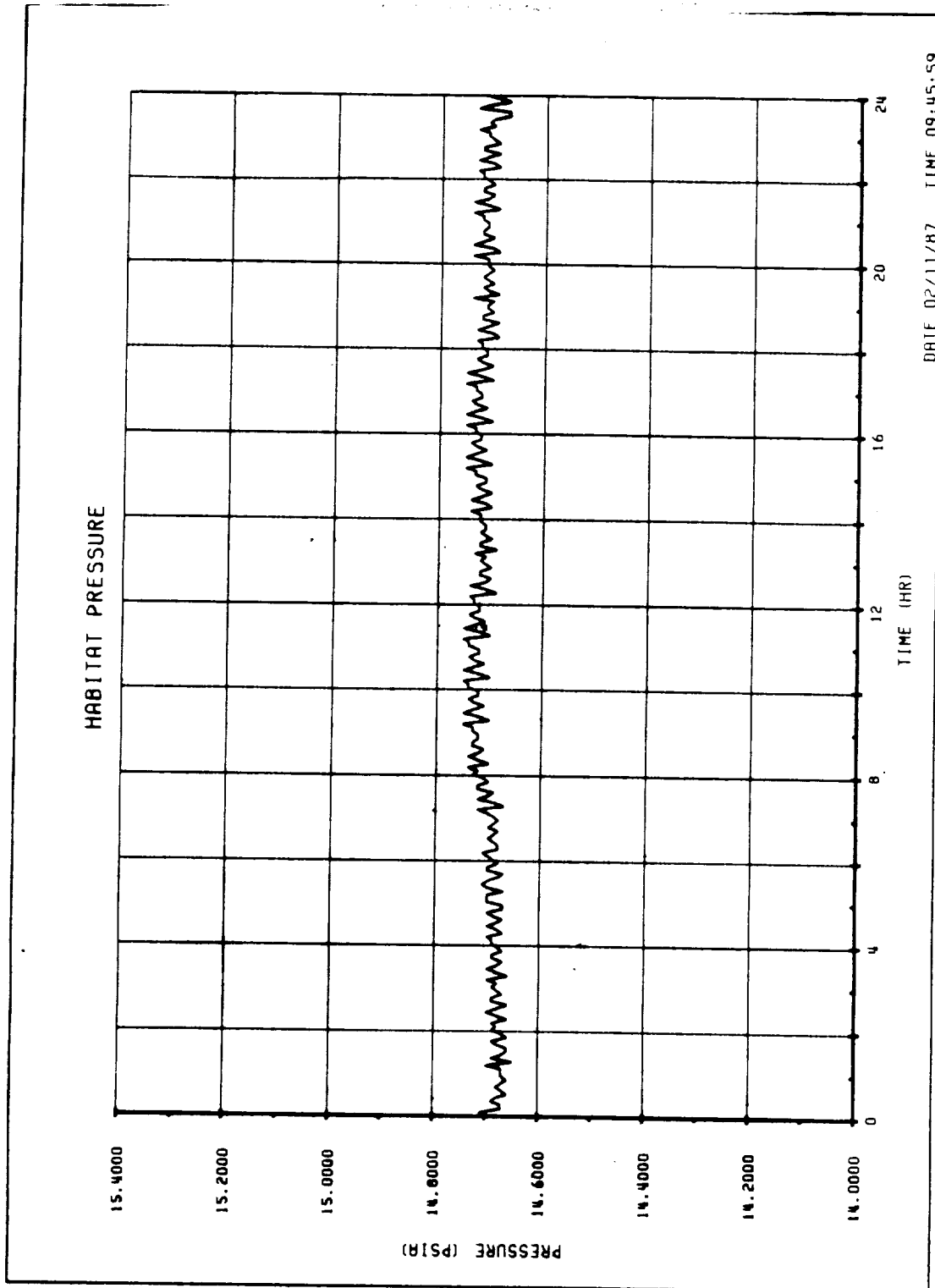


FIGURE C-26  
HABITAT PRESSURE

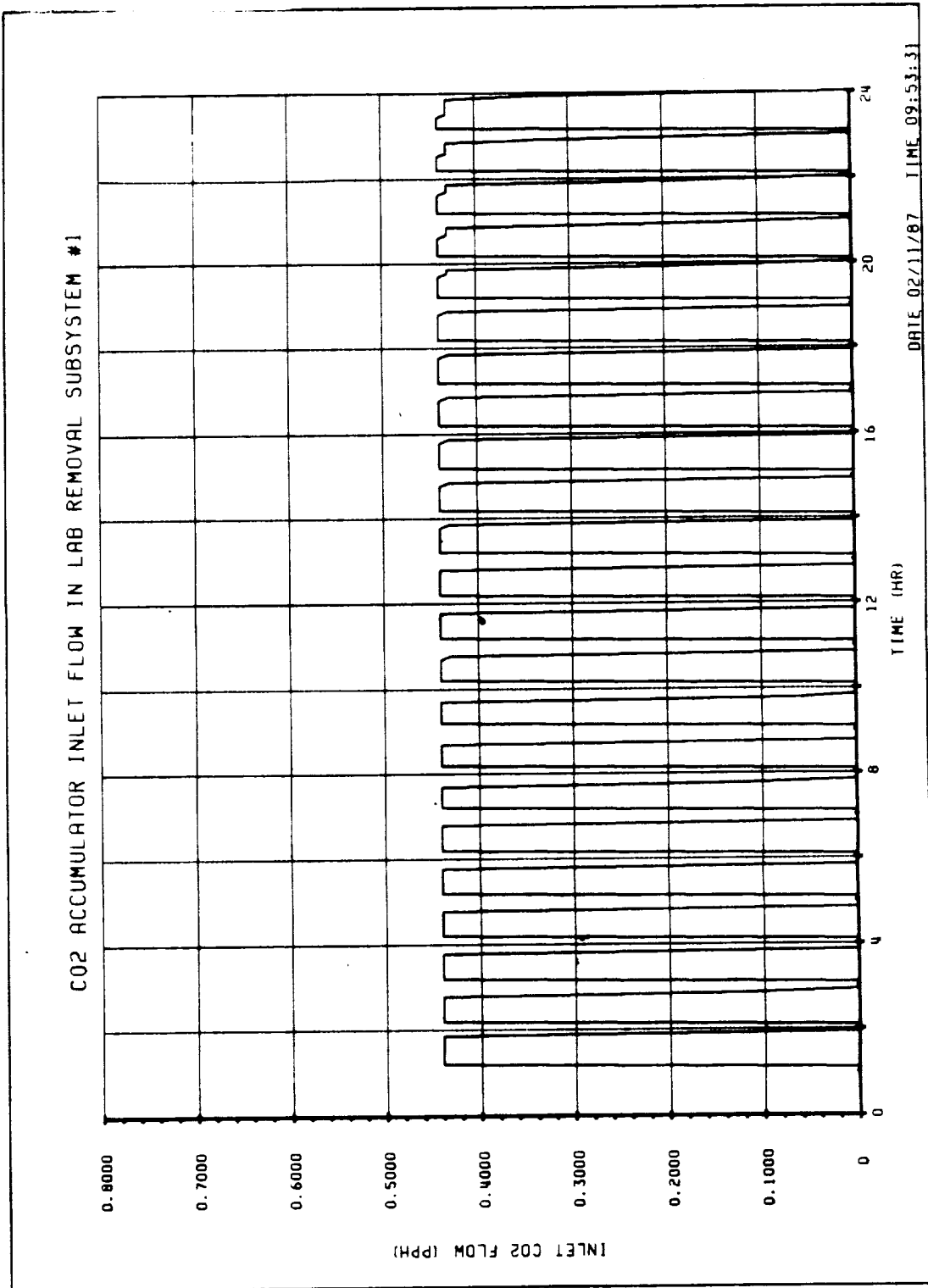


FIGURE C-27  
CO2 ACCUMULATOR INLET FLOW IN LAB REMOVAL SUBSYSTEM #1

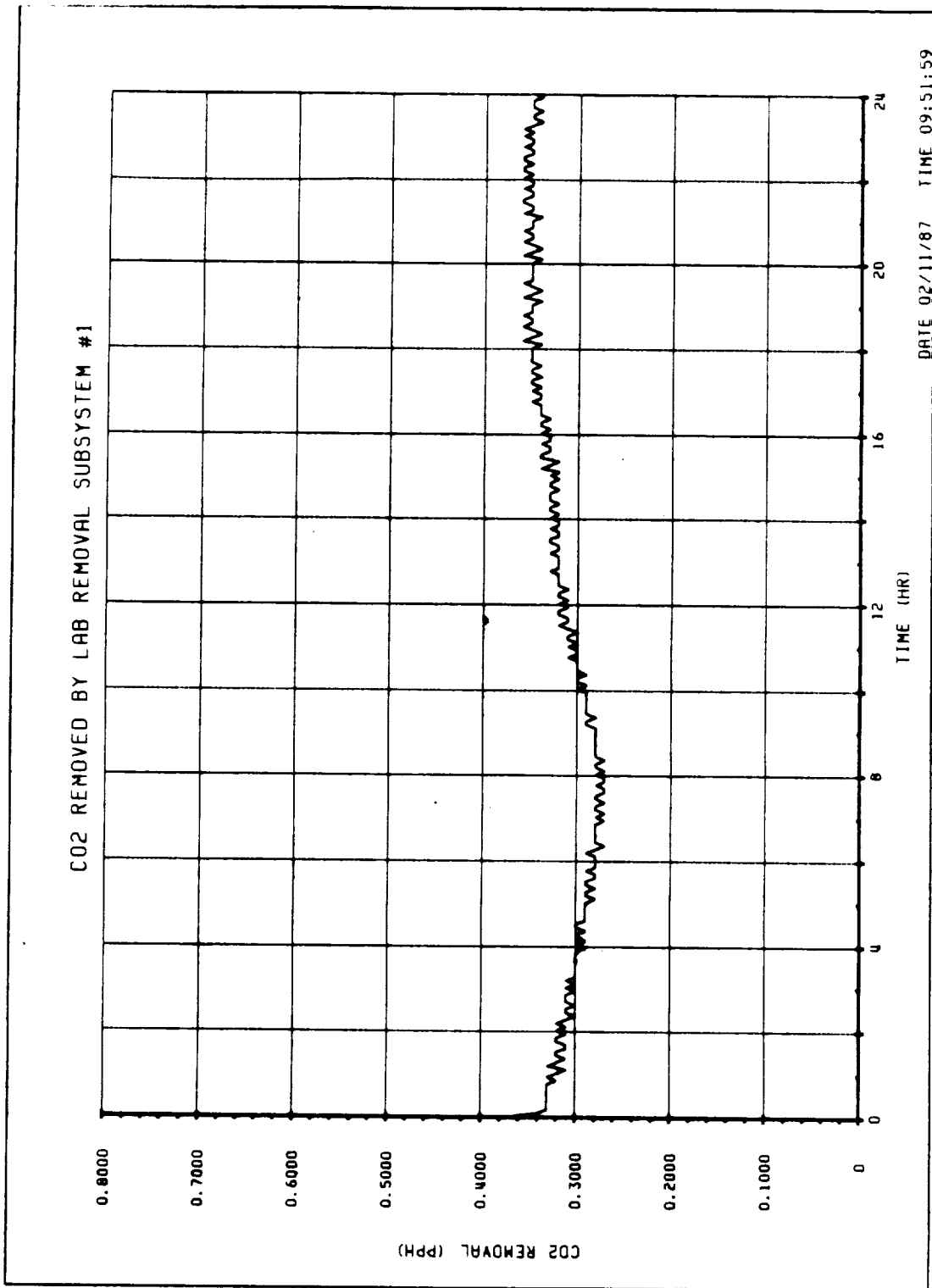


FIGURE C-28  
CO<sub>2</sub> REMOVED BY LAB REMOVAL SUBSYSTEM #1

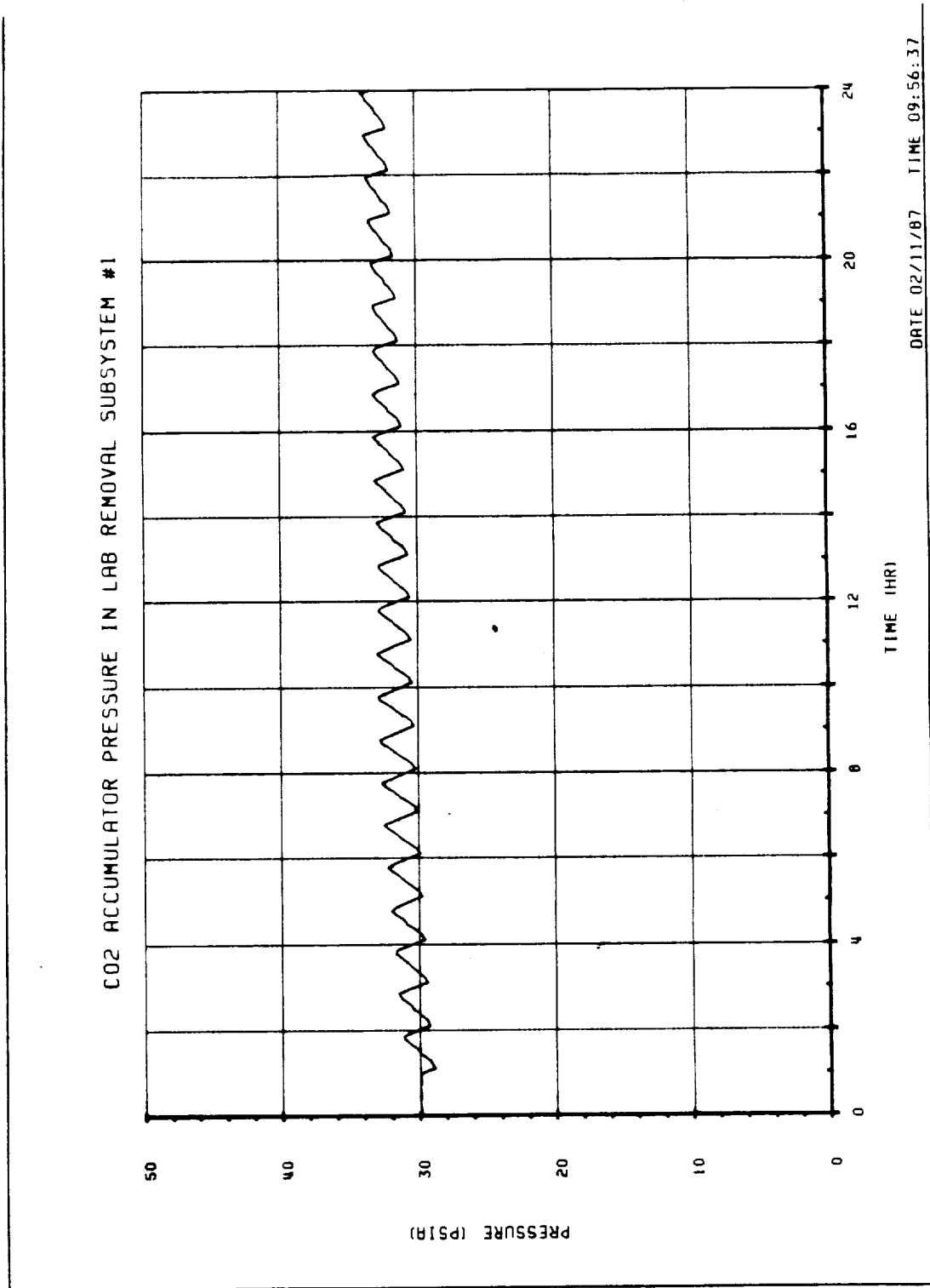


FIGURE C-29  
CO2 ACCUMULATOR PRESSURE IN LAB REMOVAL SUBSYSTEM #1



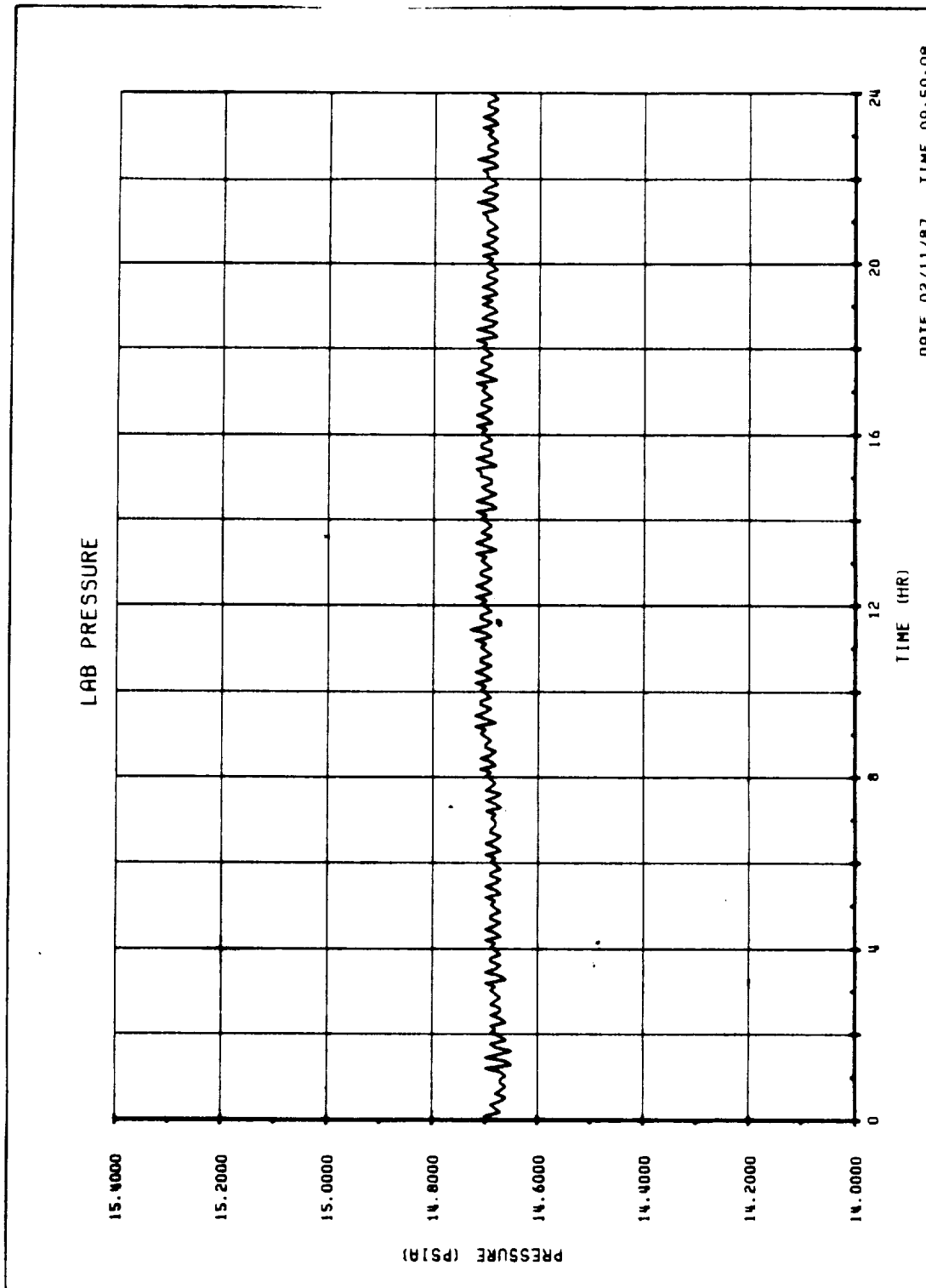


FIGURE C-30  
LAB PRESSURE

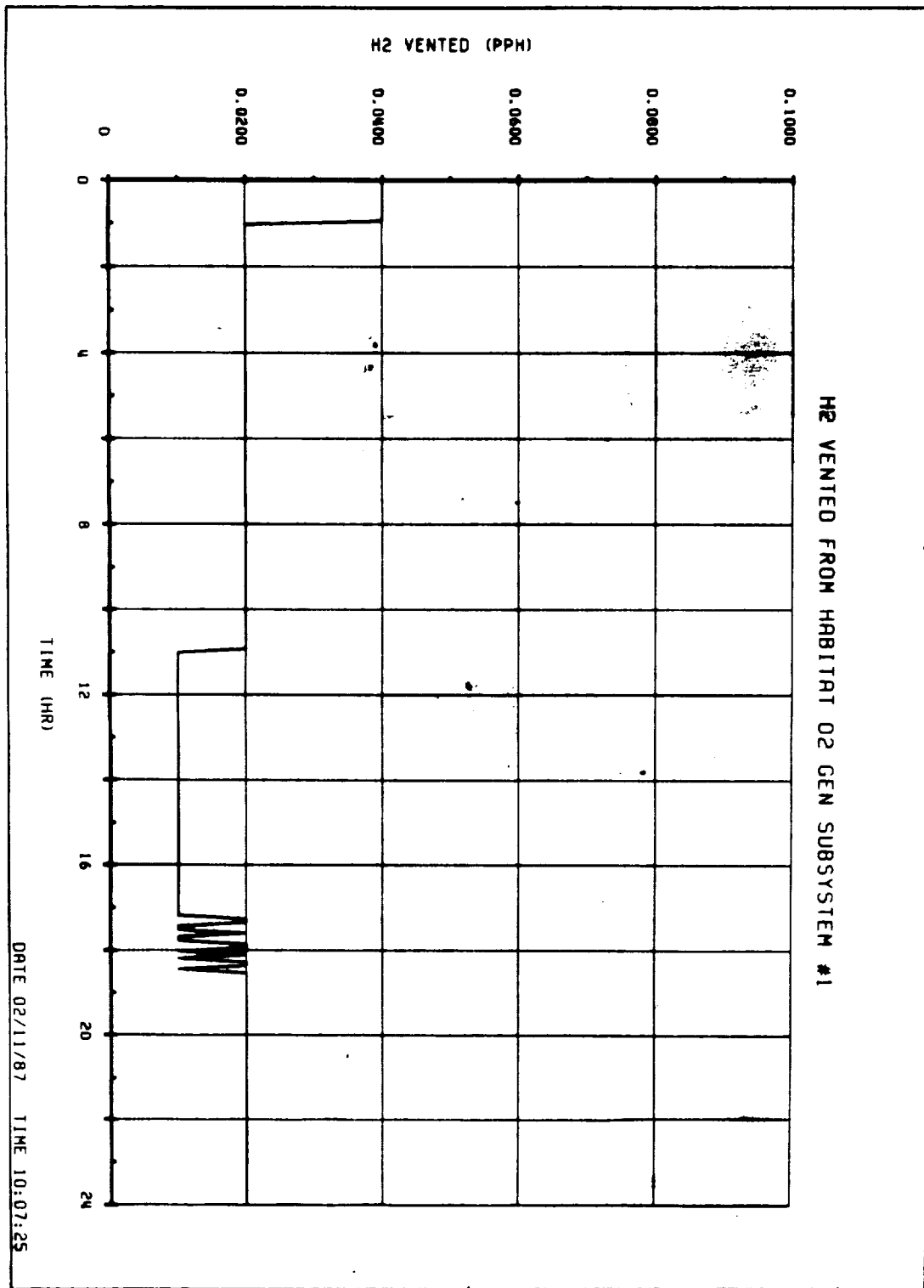


FIGURE C-31  
H2 VENTED FROM HABITAT O2 GEN SUBSYSTEM #1

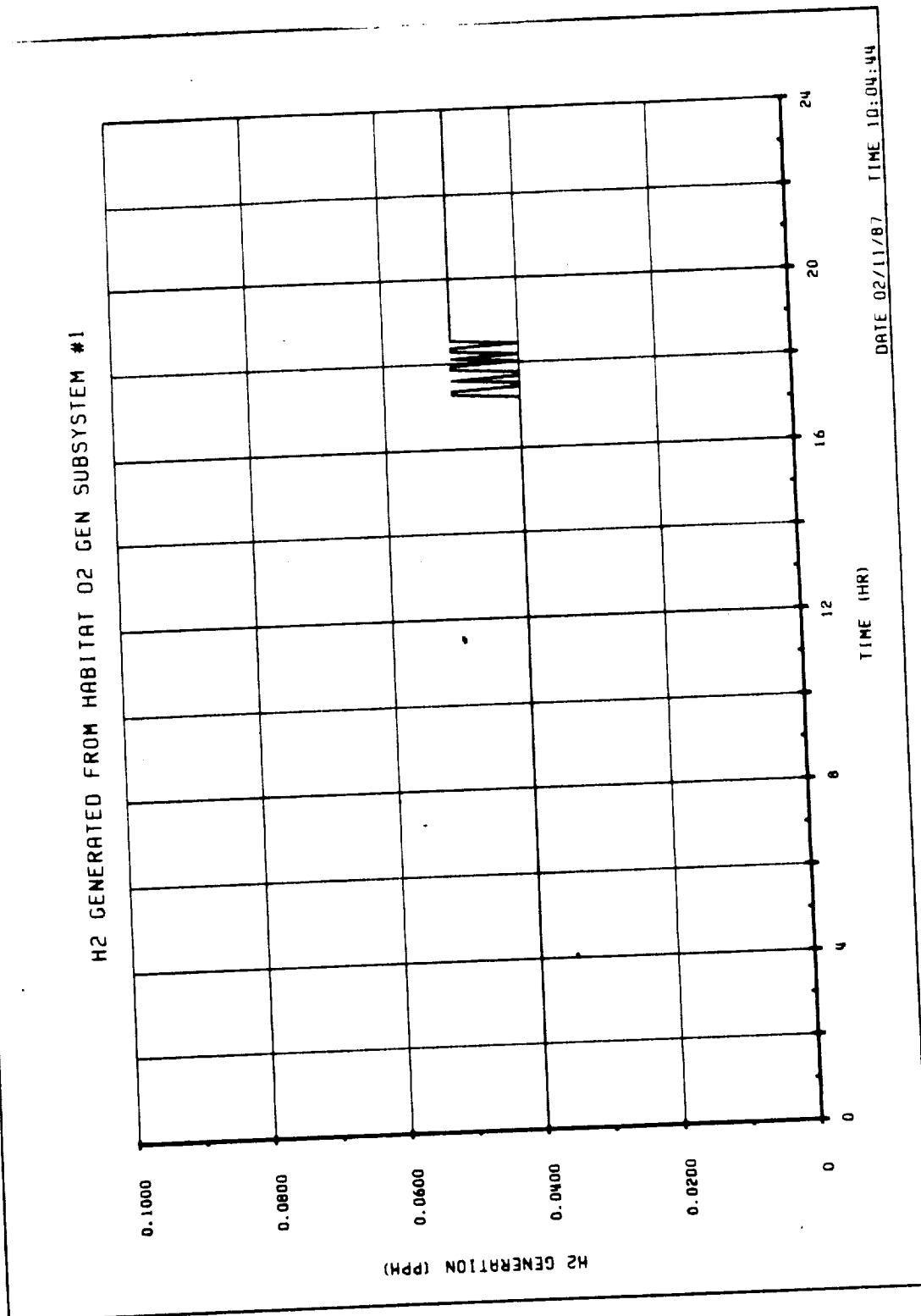


FIGURE C-32  
H2 GENERATED FROM HABITAT O2 GEN SUBSYSTEM #1

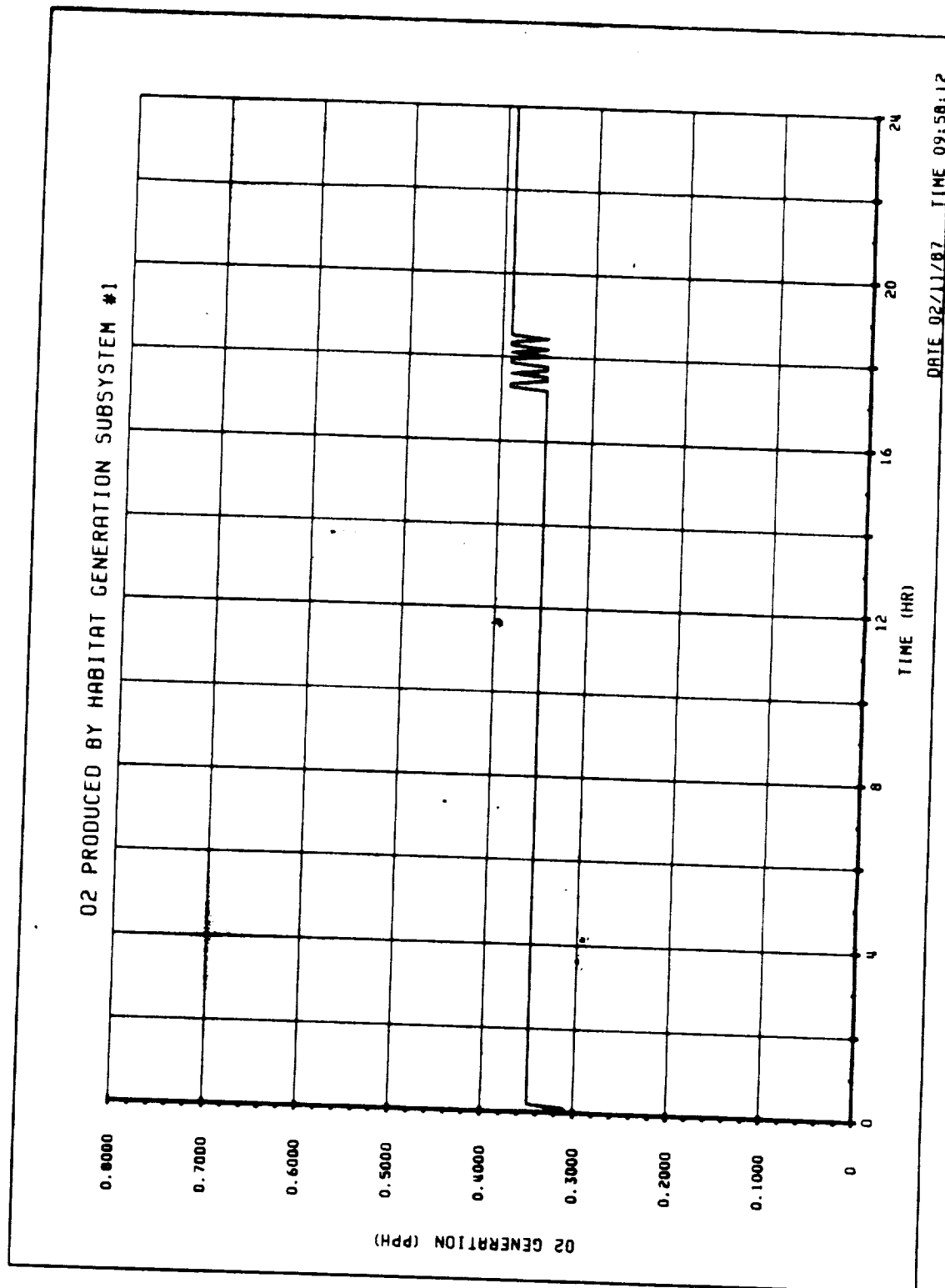


FIGURE C-33  
O2 PRODUCED BY HABITAT O2 GEN SUBSYSTEM #1

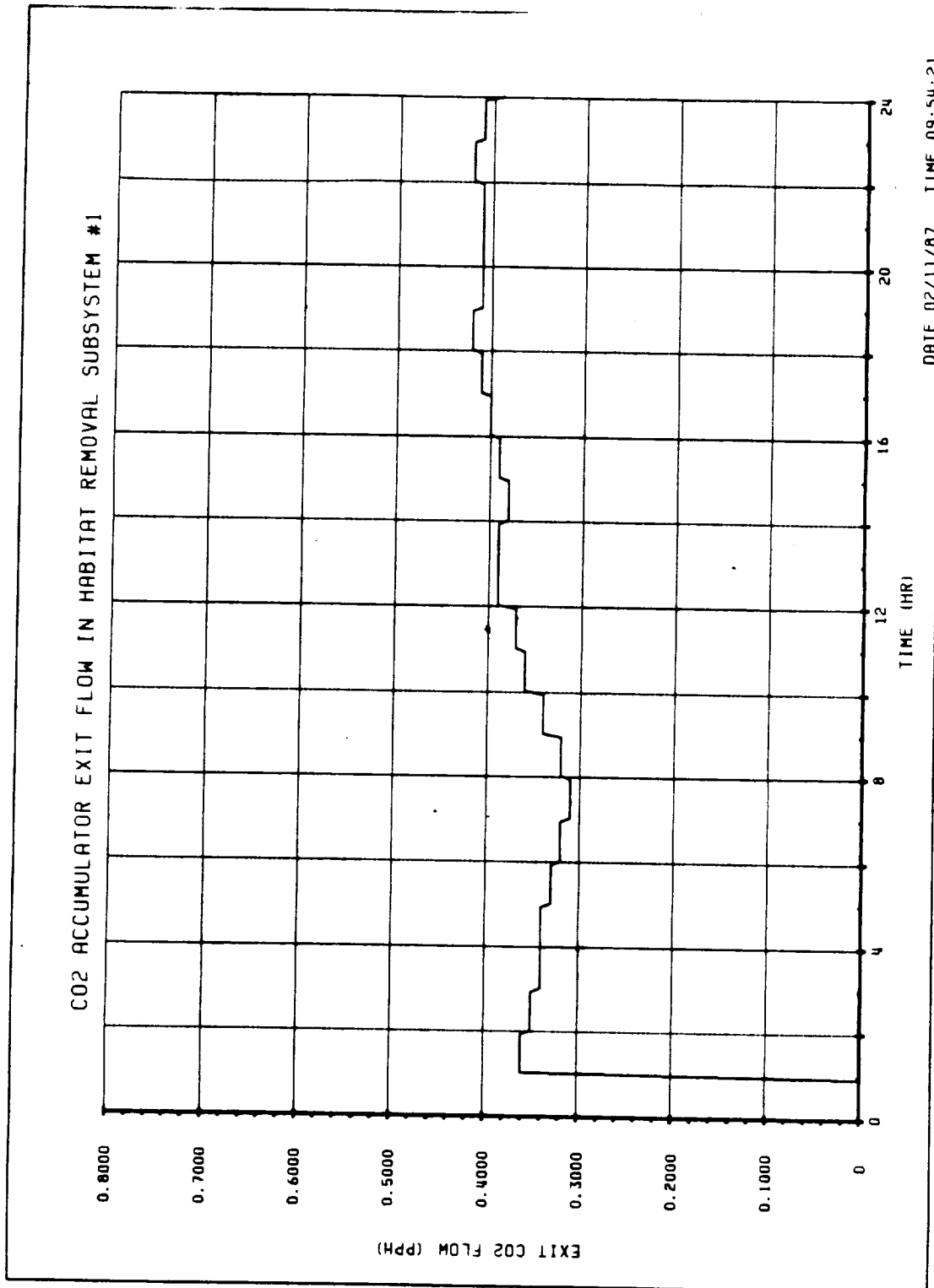


FIGURE C-34  
CO<sub>2</sub> ACCUMULATOR EXIT FLOW IN HABITAT REMOVAL SUBSYSTEM #1

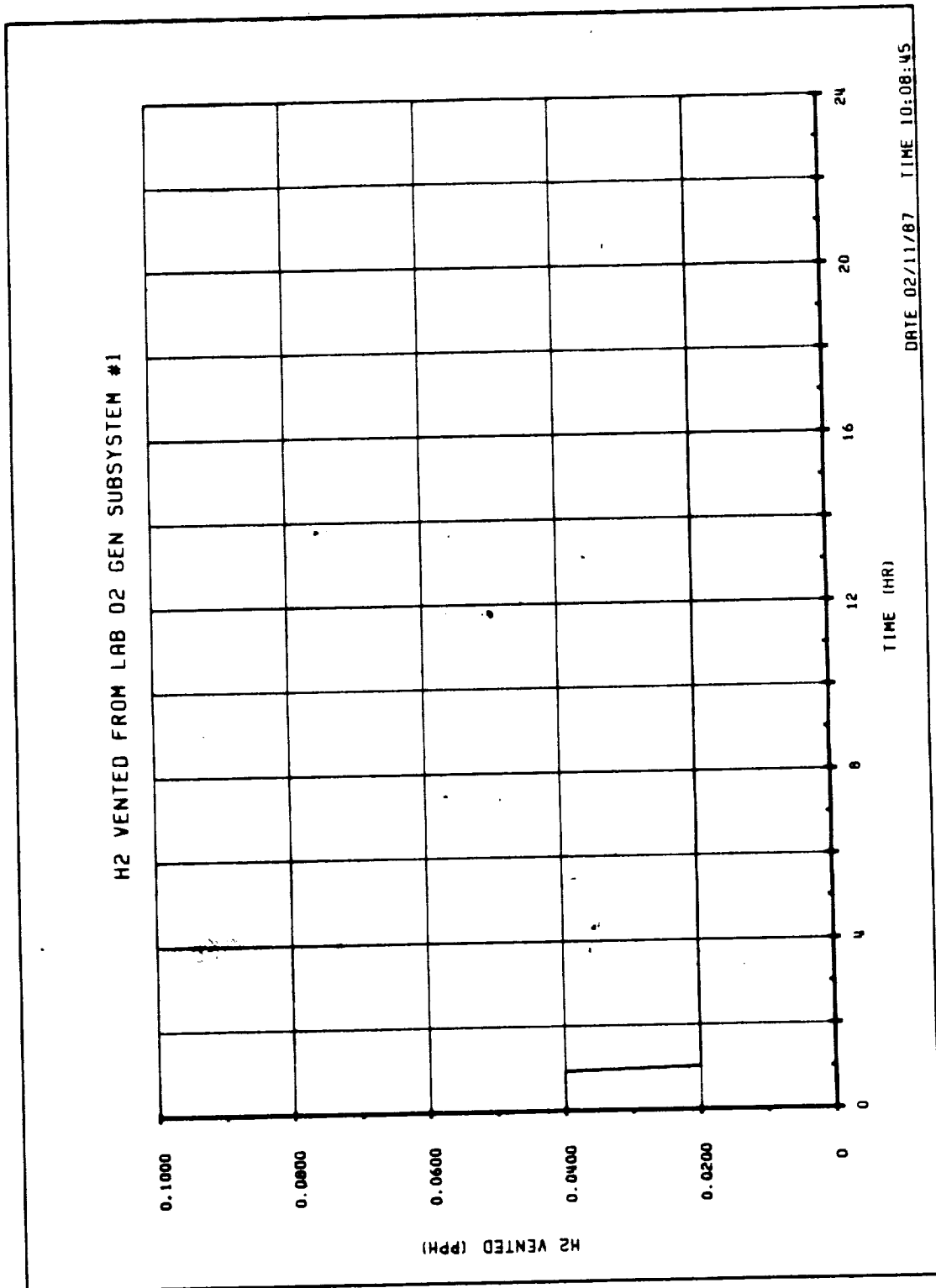


FIGURE C-35  
H2 VENTED FROM LAB O2 GEN SUBSYSTEM #1

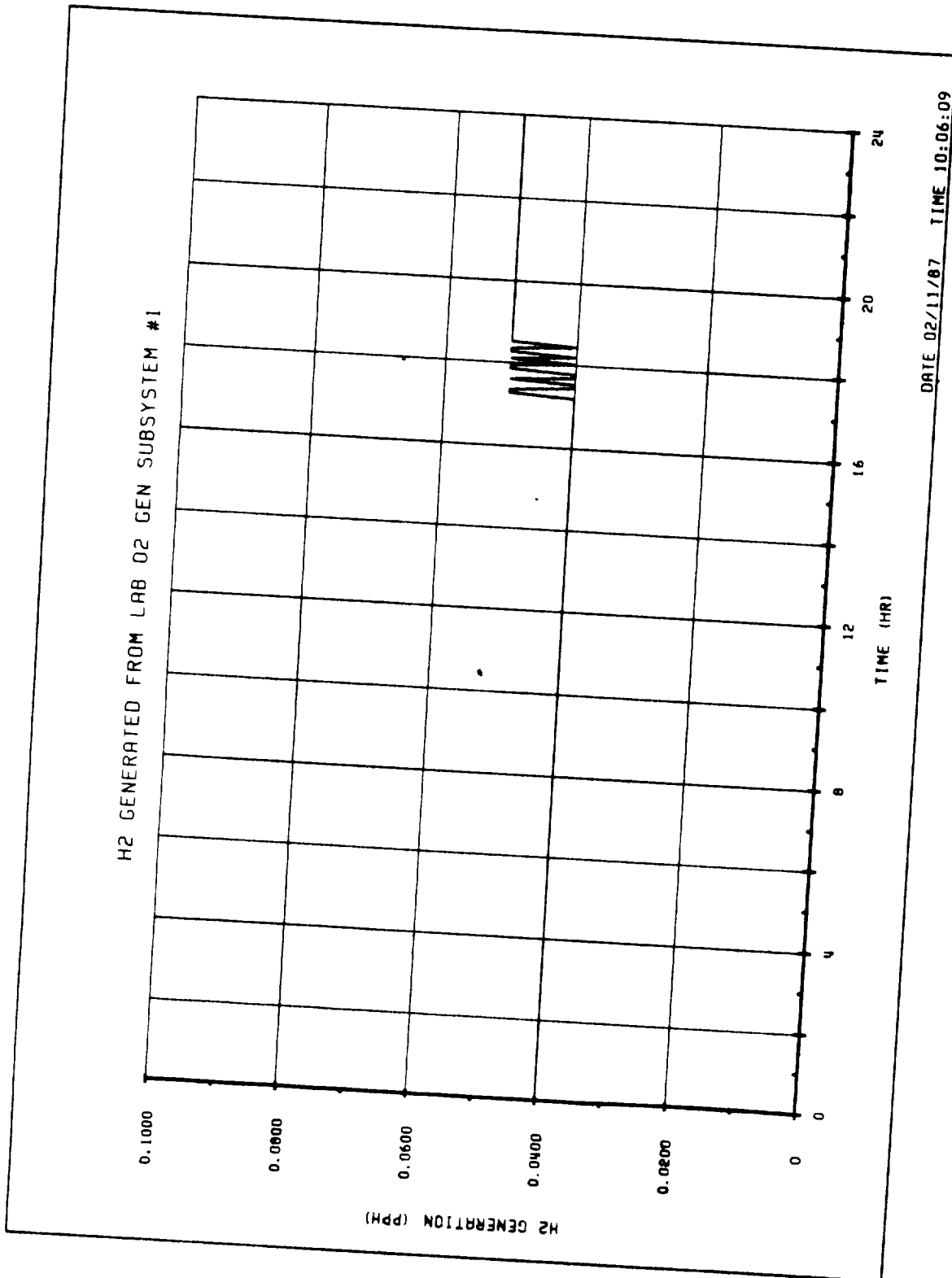


FIGURE C-36  
H2 GENERATED FROM LAB 02 GEN SUBSYSTEM #1

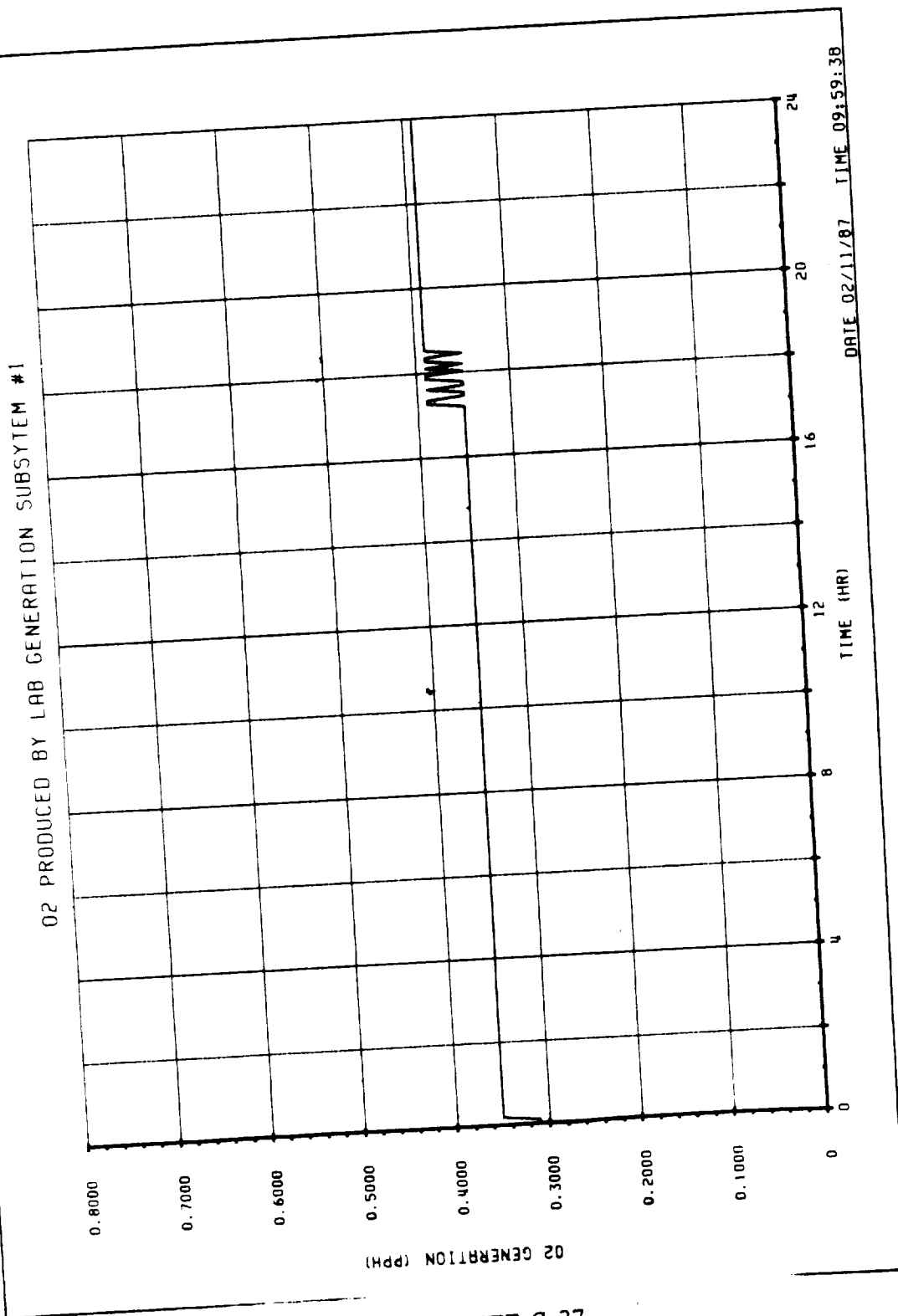


FIGURE C-37  
O2 PRODUCED BY LAB O2 GEN SUBSYSTEM #1



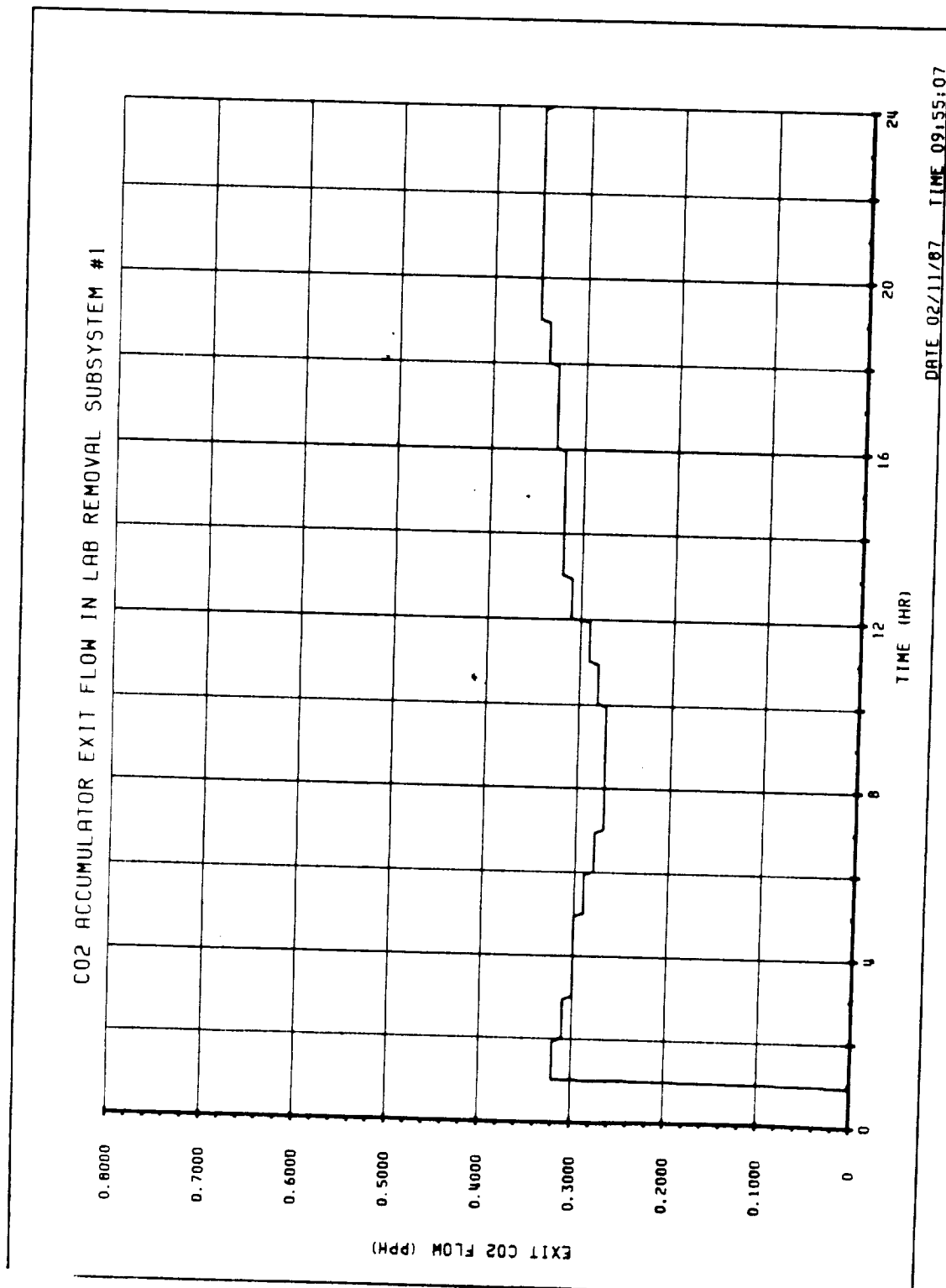


FIGURE C-38  
CO2 ACCUMULATOR EXIT FLOW IN LAB REMOVAL SUBSYSTEM #1

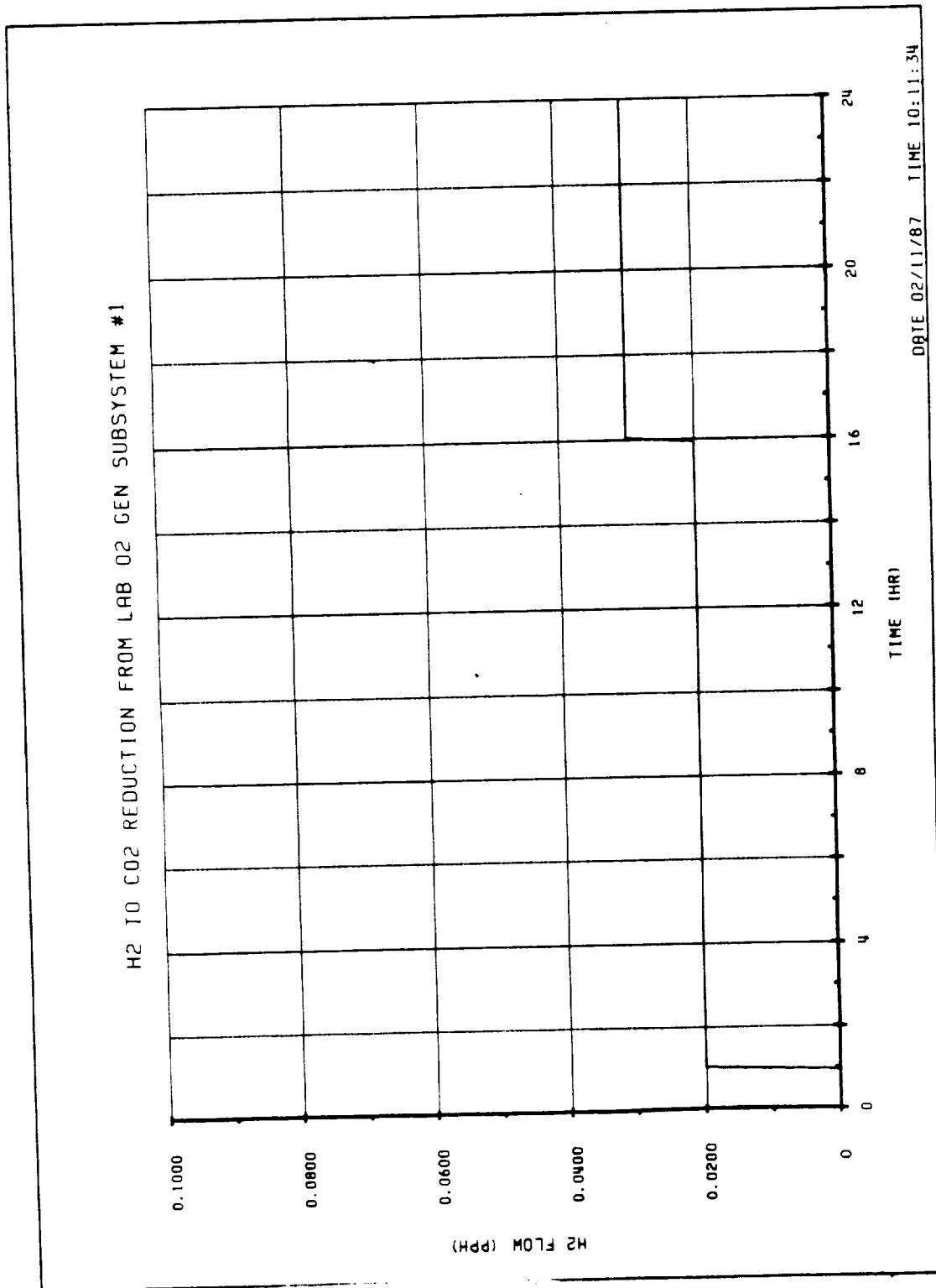


FIGURE C-39  
H2 TO CO2 REDUCTION FROM LAB O2 GEN SUBSYSTEM #1

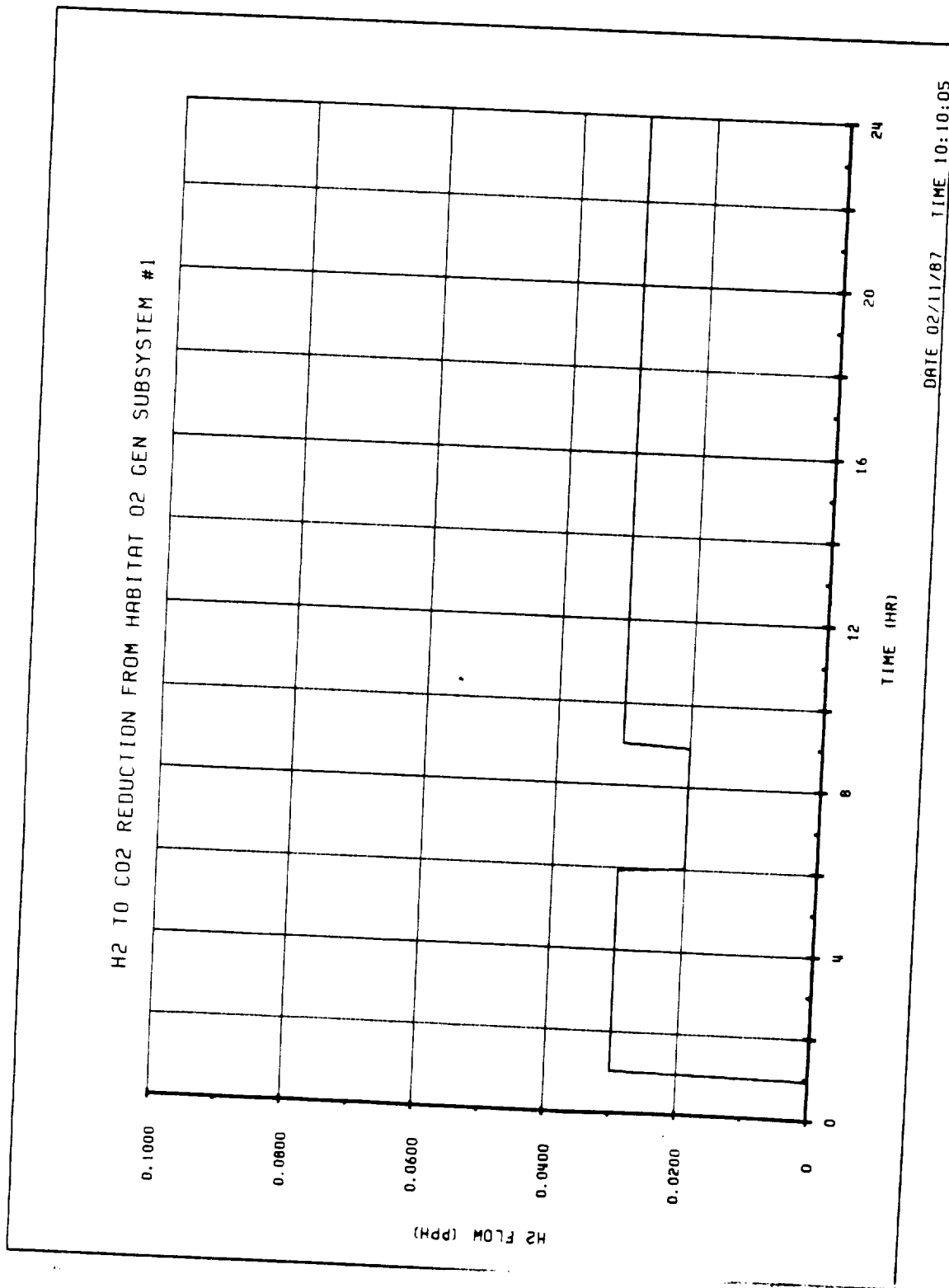


FIGURE C-40  
H2 TO CO2 REDUCTION FROM HABITAT O2 GEN SUBSYSTEM #1

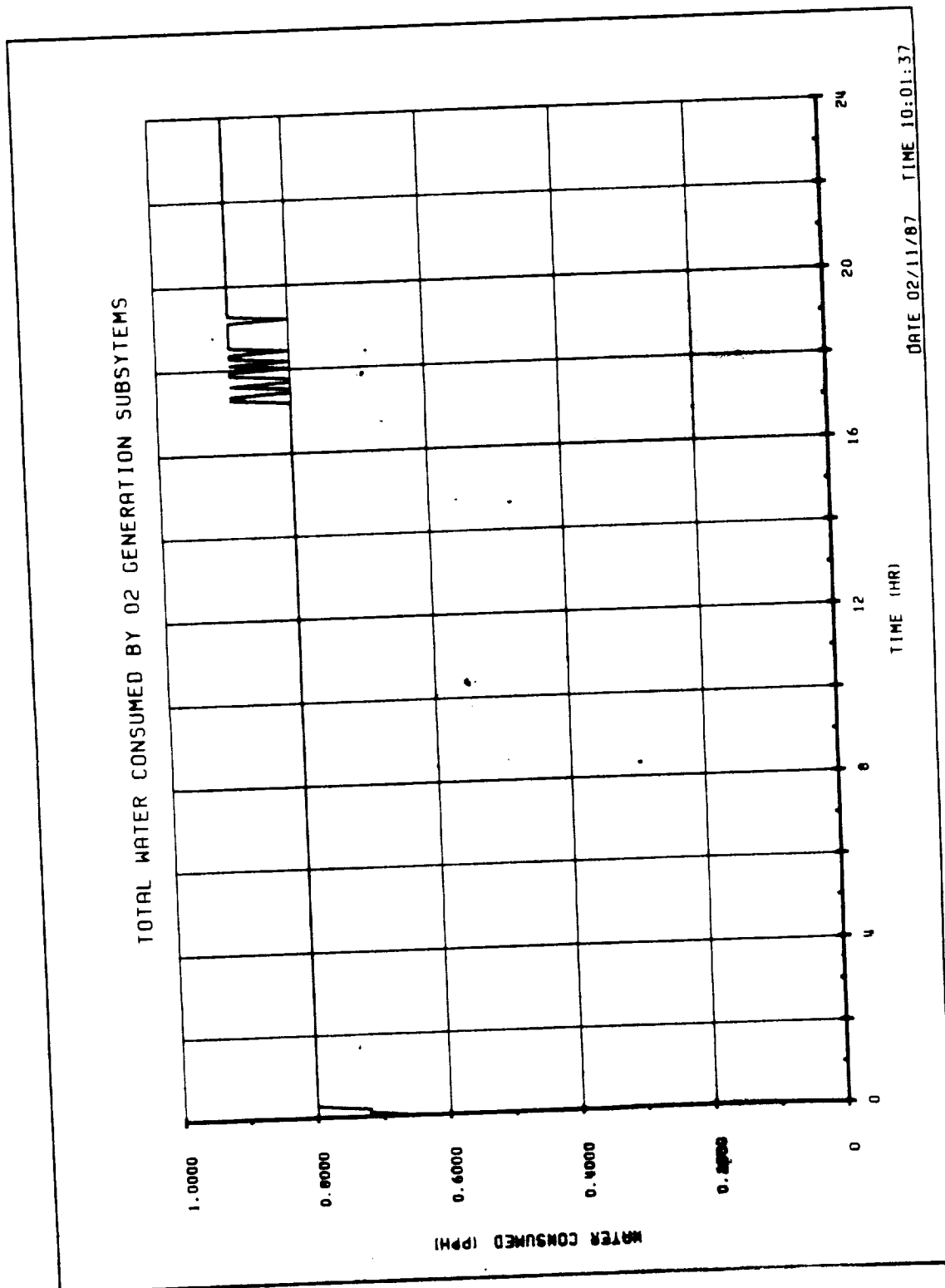


FIGURE C-41  
TOTAL WATER CONSUMED BY O2 GENERATION SUBSYSTEMS

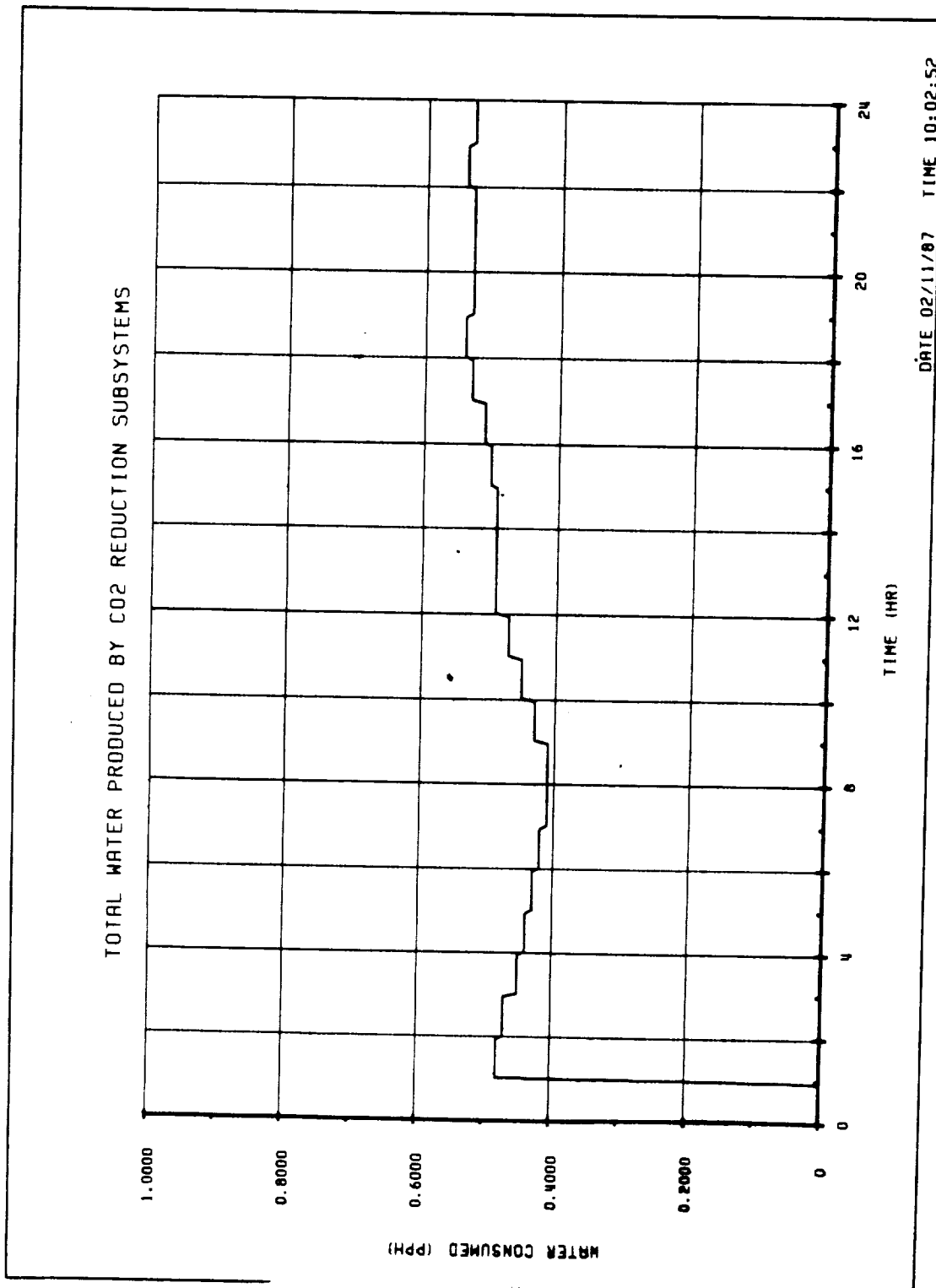


FIGURE C-42  
TOTAL WATER PRODUCED BY CO2 REDUCTION SUBSYSTEMS





## Report Documentation Page

1. Report No.  NASA CR-181736	2. Government Accession No.	3. Recipient's Catalog No.	
4. Title and Subtitle Appendices to the User's Manual for A Computer Program for the Emulation/Simulation of a Space Station Environmental Control and Life Support System		5. Report Date September 1988	
		6. Performing Organization Code	
7. Author(s)  James L. Yanosy		8. Performing Organization Report No.  SVHSER 10639	
		10. Work Unit No.  506--49-31-01	
9. Performing Organization Name and Address Hamilton Standard Division of United Technologies Corporation Windsor Locks, CT 06096		11. Contract or Grant No.  NAS1-17397	
		13. Type of Report and Period Covered  Contractor Report	
12. Sponsoring Agency Name and Address NASA Langley Research Center Hampton, VA 23665-5225		14. Sponsoring Agency Code	
15. Supplementary Notes  Langley Technical Monitors: John B. Hall, Jr., and Lawrence F. Rowell			
16. Abstract A User's Manual for the Emulation Simulation Computer Model was published previously. The model consisted of a detailed model (emulation) of a SAWD CO <sub>2</sub> removal subsystem which operated with much less detailed (simulation) models of a cabin, crew, and condensing and sensible heat exchangers. The purpose was to explore the utility of such an emulation/simulation combination in the design, development, and test of a piece of ARS hardware - SAWD.  Extensions to this original effort are presented in the manual. The first extension is an update of the model to reflect changes in the SAWD control logic which resulted from test. In addition, slight changes were also made to the SAWD model to permit restarting and to improve the iteration technique. The second extension is the development of simulation models for more pieces of air and water processing equipment. Models are presented for: EDC, Molecular Sieve, Bosch, Sabatier, a new condensing heat exchanger, SPE, SFWES, Catalytic Oxidizer, and multi-filtration. The third extension is to create two system simulations using these models. The first system presented consists of one air and one water processing system. The second system consists of a potential Space Station air revitalization system complete with a habitat, laboratory, four modes, and two crews.			
17. Key Words (Suggested by Author(s)) Computer Simulation, Environmental Control, Space Station, Life Support, Computer Modeling		18. Distribution Statement Unclassified - Unlimited Subj. Cat. - 54	
19. Security Classif. (of this report)  Unclassified	20. Security Classif. (of this page)  Unclassified	21. No. of pages  205	22. Price  A10

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